



**UNIVERSITI PUTRA MALAYSIA**

**SYNTHESIS OF CARBOHYDRATE-DERIVED SOLID ACID CATALYSTS  
FOR BIODIESEL PRODUCTION FROM PALM FATTY ACID DISTILLATE**

**MOHD LOKMAN IBRAHIM**

**FS 2016 15**



**SYNTHESIS OF CARBOHYDRATE-DERIVED SOLID ACID CATALYSTS  
FOR BIODIESEL PRODUCTION FROM PALM FATTY ACID DISTILLATE**

By

**MOHD LOKMAN BIN IBRAHIM**

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in  
Fulfillment of the Requirements for Degree of Doctor of Philosophy**

**March 2016**

1000585001

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



**DEDICATION**

*Special Dedicated to my Mother  
Aminah Bte Semail (1965 - 2013)*



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfillment of the requirement for the Degree of Doctor Philosophy

## **SYNTHESIS OF CARBOHYDRATE-DERIVED SOLID ACID CATALYSTS FOR BIODIESEL PRODUCTION FROM PALM FATTY ACID DISTILLATE**

By

**MOHD LOKMAN BIN IBRAHIM**

**March 2016**

**Chairman : Prof. Taufiq Yap Yun Hin, PhD**  
**Faculty : Science**

High concerns on the energy security and uncontrolled emissions of greenhouse gas had forced all countries to turn towards the utilization of environmentally-friendly and renewable biofuels. In this work, the usage of inexpensive and non-edible oil feedstock such as palm fatty acid distillate (PFAD) for the biodiesel production is recommended.

A highly potential heterogeneous carbon-based solid acid catalyst derived from carbohydrates was successfully developed and applied for biodiesel production. The carbohydrate-derived solid acid catalysts were synthesized by sulfonation of incomplete carbonized carbohydrates using concentrated sulfuric acid. The prepared catalysts underwent a detailed characterization analyses in terms of its active site's functional groups, morphological structure, thermal stability, surface area and density of the acid sites. The catalytic activity of all prepared catalysts had demonstrated the highest conversion of PFAD to biodiesel under the following reaction condition: catalyst loading of 2 wt.%, methanol-to-PFAD molar ratio of 10:1, reaction temperature of 75 °C and the reaction time was 3 h.

In order to improve the esterification reaction process, an efficient microwave batch reactor was fabricated. A study on a microwave-assisted acceleration of esterification rate of PFAD using glucose-derived solid acid catalyst was carried out. It was found that the radio frequency of microwave energy could enhance the reaction rate faster than the conventional heating technique. The results revealed the potential of microwave irradiation; which offers faster esterification rate with advantages of enhancing the FAME yield and reducing the production cost.

Another study was carried out to investigate the effect of high temperature on the esterification reaction of PFAD. The supercritical reactor was used to heat up the reaction system up to sub- and super-critical conditions. The results from the optimization of reaction variables were; reaction temperature of 290 °C, methanol-to-PFAD molar ratio of 6:1, catalyst amount of 1 wt.% and reaction time of 5 min. The esterification of PFAD in supercritical methanol with the presence of glucose- and starch-derived solid acid catalysts at this condition resulted 95.4% and 97.3% of FAME yield, respectively - both catalysts yielded significantly higher conversion compared to

un-catalyzed supercritical methanol reaction with the ability to be recycled up to 10 times.

As a conclusion, it revealed that the sulfonated carbohydrate-derived acid catalysts had high potentials by showing high catalytic activity with better stability and were suitable for the biodiesel production from low-quality feedstock with high FFA content, especially PFAD. The improvement on the reaction rate by applying the invented microwave-assisted and supercritical methanol reactions showed positive outcome – which in turn, proved the fast reaction with high FAME yield.



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk Ijazah Doktor Falsafah

## **SINTESIS MANGKIN ASID PEPEJAL TERBITAN KARBOHIDRAT UNTUK PENGHASILAN BIODIESEL DARIPADA BAHAN ASID LEMAK SAWIT SULINGAN**

Oleh

**MOHD LOKMAN BIN IBRAHIM**

**Mac 2016**

**Pengerusi: Prof. Taufiq Yap Yun Hin, PhD**  
**Fakulti: Sains**

Kebimbangan terhadap sumber bekalan tenaga, harga bahan api yang tidak menentu, dan pembebasan gas rumah hijau yang tidak terkawal menyebabkan kebanyakan negara beralih ke arah penggunaan bahan api-bio yang boleh diperbaharui dan mesra alam. Dalam kajian ini, penggunaan bahan mentah yang murah dan tidak boleh dimakan seperti asid lemak sawit sulingan (PFAD) untuk penghasilan biodiesel telah dikaji dan diguna pakai.

Bahan mangkin heterogen asid pepejal terbitan karbohidrat berasaskan karbon telah berjaya disintesis dan digunakan untuk menghasilkan biodiesel. Bahan mangkin ini telah dihasilkan melalui proses pengulfuran karbohidrat iaitu pemanasan karbohidrat bersama asid sulfuric pekat. Beberapa pencirian bahan mangkin telah dilakukan dengan menggunakan pelbagai teknik seperti analisis kumpulan berfungsi, morfologi permukaan, kestabilan terma, luas permukaan dan kuantiti tapak asid. Aktiviti pemangkinan semua katalis yang disediakan menunjukkan penukaran tertinggi bahan PFAD kepada biodiesel dengan keadaan: 2% bahan mangkin, nisbah molar metanol kepada PFAD (10:1), suhu tindak balas ialah 75 °C dan masa tindak balas ialah 3 jam.

Dalam usaha untuk meningkatkan proses tindak balas pengesteran, satu reactor dengan gelombang mikro telah difabrikasi. Kajian kesan kadar pecutan gelombang mikro terhadap pengesteran bahan PFAD dengan menggunakan mangkin asid pepejal terbitan glukosa telah dijalankan. Keputusan yang diperolehi menunjukkan bahawa tenaga radio berfrekuensi gelombang mikro boleh meningkatkan kadar tindak balas berbanding dengan teknik pemanasan konvensional. Secara keseluruhan kajian yang dilakukan menunjukkan bahawa sinaran gelombang mikro mampu mempercepatkan kadar pengesteran dan meningkatkan produktiviti serta mengurangkan kos pengeluaran.

Kajian seterusnya telah dijalankan untuk mengkaji kesan penggunaan suhu yang tinggi terhadap tindak balas pengesteran PFAD. Reaktor super-genting telah digunakan untuk tindak balas pemanasan sehingga mencapai pada tahap sub- dan super-genting. Suhu tindak balas pada 290 °C, nisbah molar methanol kepada bahan PFAD ialah 6:1, berat

mangkin sebanyak 1% dan dengan masa tindak balas selama 5 min telah dikenalpasti sebagai keadaan tindak balas yang paling optimum. Didapati, pengesteran bahan PFAD kepada biodiesel dalam keadaan super-genting dengan penggunaan mangkin asid pepejal terbitan glukosa dan kanji, masing-masing memberikan peratus hasil pada 95.4% dan 97.3% - Kedua-dua bahan mangkin memberikan peratus penukaran yang lebih tinggi berbanding tindakbalas super-genting yang dijalankan tanpa penggunaan mangkin. Selain itu, bahan mangkin yang digunakan dalam penyelidikan ini didapati mempunyai sifat keboleholangan yang sangat baik dengan 10 kali kitaran.

Akhir sekali, dapat disimpulkan bahawa mangkin asid pepejal terbitan karbohidrat mempunyai aktiviti pemangkinan dan kestabilan yang sangat baik. Bahan mangkin ini sesuai digunakan dalam penukaran bahan mentah berkualiti rendah dengan kandungan FFA yang tinggi seperti PFAD. Kadar tindak balas yang cepat dengan hasil FAME yang tinggi berjaya diperolehi jika menggunakan teknik gelombang micro dan super-genting. Kedua-dua pendekatan ini juga dilihat sebagai suatu alternative baru yang memberi kesan positif - pada masa yang sama meningkatkan kadar tindak balas dan hasil produk biodiesel.



## ACKNOWLEDGEMENT

بِسْمِ اللَّهِ الرَّحْمَنِ الرَّحِيمِ

First and foremost, I thank to Allah s.w.t. for giving me His blessing and strength throughout this research work. Special thanks to Prof Dr. Taufiq Yap and Dr. Umer Rashid for their guidance, encouragement and assistance throughout my Ph.D research work. Special thanks also dedicated to Prof Dr. Zulkarnain Zainal as one of my co-supervisor and Prof Dr. Robiah Yunus as a co-author in two of my research papers.

Special thanks also goes to my father and my mother, thank you for being a loving parent who has always been there for me during your lifetime. Deepest gratitude also to my wife Nur Afidah Abdullah, thank you for being supportive, wonderful memories in our life, your advices, and your Doa' for my success. Also, special gratitude to my daughter Nur Salsabila and my son Muhammad Naufal, and not forget to all my family members.

Nor forgotten, thanks to all my colleagues and friends, especially from Catalysis Science and Technology Research Centre (PutraCAT), staffs and technicians at the Chemistry Department, Faculty of Science and the Advanced Institute of Technology (ITMA), Universiti Putra Malaysia.

Special gratitude also goes to Prof Dr. Motonobu Goto and his research team from the Department of Chemical Engineering, Nagoya University, for their guidance and assistances during my research attachment program on November to December 2014.

Financial support from Universiti Teknologi MARA (UiTM) and Ministry of Higher Education (MOHE) Malaysia through the scholarships of 'Tenaga Pengajar Muda' and 'Basiswa Skim Latihan Akademik Bumiputera and Biasiswa Skim Latihan Akademik IPTA'.

-Alhamdulillah-

## TABLE OF CONTENTS

	Page
<b>ABSTRACT</b>	i
<b>ABSTRAK</b>	iii
<b>ACKNOWLEDGEMENTS</b>	v
<b>APPROVAL</b>	vi
<b>DECLARATION</b>	viii
<b>LIST OF FIGURES</b>	xiv
<b>LIST OF TABLES</b>	xviii
<b>LIST OF ABBREVIATIONS</b>	xx
<b>CHAPTER</b>	
<b>1 INTRODUCTION</b>	
1.1 Green Technology and Alternative Fuels	1
1.2 Biodiesel and its Benefit	2
1.3 Biodiesel Production Process	3
1.4 Catalyst	4
1.5 Problem Statements	5
1.6 Hypothesis of The Research	6
1.7 Objectives of the Research	6
1.8 Scope of the Research	6
1.9 Significant of the Research	7
<b>2 LITERATURE REVIEW</b>	
2.1 Biodiesel: A Potential Source of Renewable Energy	9
2.2 Biodiesel's Feedstock	10
2.3 Preliminary Study of High FFA Feedstock	11
2.4 Catalyst - Homogeneous and Heterogeneous	13
2.4.1 Heterogeneous Carbon-based Solid Acid Catalyst	14
2.4.2 Carbohydrate-derived Solid Acid Catalyst	15
2.5 Biodiesel Production - Esterification and Transesterification Reactions	17
2.6 Reaction Parameters and Operating Conditions	18
2.6.1 Effect of Methanol-to-Oil Molar Ratio	22
2.6.2 Effect of Reaction Temperature	22
2.6.3 Effect of Catalyst Concentration	23
2.6.4 Effect of Reaction Time	23
2.7 Technology in Biodiesel Production Process	24
2.7.1 Conventional Methanol-Reflux Method	24
2.7.2 Autoclave Reactor System	25
2.7.3 Microwave-Irradiation Reactor System	25
2.7.4 Ultrasound-Assisted Reactor System	26
2.7.5 Sub- and Supercritical Methanol Reactor System	27

2.8	Determination of FAME Yield	28
2.9	FAME Properties	29
2.10	Biodiesel Combustion, Emission and Performance	30
<b>3</b>	<b>SYNTHESIS AND CHARACTERIZATION OF CARBOHYDRATE-DERIVED SOLID ACID CATALYST</b>	
3.1	Introduction	33
3.2	Methodology	34
3.2.1	Chemicals and Materials	34
3.2.2	Preparation of Catalysts	34
3.2.3	Characterization of the Catalysts	35
3.2.4	Catalytic Activity Evaluation	37
3.3	Results and Discussion	
3.3.1	Optimization of Carbonization Condition	38
3.3.2	Optimization of Sulfonation Time	39
3.3.3	Characterization of the Catalysts	40
3.3.4	Proposed Carbon Structure of Catalyst	54
3.4	Summary	55
<b>4</b>	<b>ESTERIFICATION OF PALM FATTY ACID DISTILLATE CATALYZED BY CARBOHYDRATE-DERIVED SOLID ACID CATALYST</b>	
4.1	Introduction	56
4.2	Methodology	56
4.2.1	Chemicals and Materials	56
4.2.2	Analysis of Palm Fatty Acid Distillate	57
4.2.3	Esterification of Palm Fatty Acid Distillate	58
4.2.4	Catalyst Reusability and Leaching Test	59
4.3	Results and Discussion	59
4.3.1	Properties of Palm Fatty Acid Distillate	59
4.3.2	Esterification of PFAD	60
4.3.3	Comparison with Commercialized Catalysts	65
4.3.4	Reusability Potential of the Catalysts	66
4.4	Summary	69
<b>5</b>	<b>OPTIMIZATION OF REACTION PARAMETERS BY USING RESPONSE SURFACE METHOD</b>	
5.1	Introduction	70
5.2	Methodology	
5.2.1	Esterification of PFAD	71
5.2.2	Optimization Analysis by Response Surface Methodology	71

5.3	Results and Discussion	72
5.3.1	Regression Analysis	72
5.3.2	Diagnostic Plots	75
5.3.3	Relationship of Variables by 3D-dimensional and Contour Plots	76
5.3.4	Biodiesel Yield at Predicted Optimum Condition	80
5.4	Summary	80
<b>6</b>	<b>MICROWAVE-ASSISTED METHYL ESTER PRODUCTION FROM PALM FATTY ACID DISTILLATE OVER HETEROGENEOUS CARBON BASED SOLID ACID CATALYST</b>	
6.1	Introduction	82
6.2	Methodology	83
6.2.1	Esterification of PFAD by Microwave Reactor	83
6.2.2	Esterification of PFAD by Conventional Heating Technique	83
6.2.3	Biodiesel Analysis	83
6.3	Results and Discussion	
6.3.1	Microwave-assisted Esterification of PFAD	84
6.3.2	The Performance of Esterification Reaction of Microwave-Assisted & Conventional Heating Techniques	86
6.3.3	Reusability of the Catalyst	87
6.4	Summary	88
<b>7</b>	<b>SUB- AND SUPERCRITICAL PROPERTIES OF PALM FATTY ACID DISTILLATE WITH CARBOHYDRATE-DERIVED SOLID ACID CATALYST</b>	
7.1	Introduction	89
7.2	Methodology	90
7.2.1	Esterification of PFAD by Supercritical Methanol	91
7.2.2	Reusability of the Catalysts	92
7.2.3	Determination of FAME Yield	92
7.3	Results and Discussion	
7.3.1	Effect of Different Catalyst Amount	93
7.3.2	Effect of Methanol-to-PFAD Molar Ratio	94
7.3.3	Effect of Reaction Temperature	95
7.3.4	Reaction Rate of Esterification Process	96
7.3.5	The Effect of the Presence of Catalyst	98
7.3.6	Reusability and Deactivation of Catalyst	99
7.3.7	Performance of the Supercritical Technique	100

7.4	Summary	101
<b>8</b>	<b>CHARACTERISTICS AND PROPERTIES OF PFAD METHYL ESTER</b>	
8.1	Introduction	102
8.2	Methodology	
8.2.1	Production of PFAD Biodiesel	102
8.2.2	Characterization of PFAD Biodiesel	102
8.2.3	Standard Methods	103
8.3	Results and Discussion	
8.3.1	Infrared Spectroscopy	104
8.3.2	Gas Chromatography-Flame Ionization Detector	104
8.3.3	Gas Chromatography-Mass Spectrometry	105
8.3.4	Proton-Nuclear Magnetic Resonance	107
8.3.5	Quality Assessment and PFAD Biodiesel Properties	110
8.4	Summary	111
<b>9</b>	<b>SUMMARY, GENERAL CONCLUSION AND RECOMMENDATION FOR FUTURE RESEARCH</b>	
9.1	Conclusions	112
9.2	Recommendation	103
	<b>REFERENCES</b>	115
	<b>APPENDICES</b>	128
	<b>BIODATA OF STUDENT</b>	142
	<b>LIST OF PUBLICATIONS</b>	143

## LIST OF FIGURES

Figure		Page
1.1	Estimation of fossil oil production in comparison with world population	1
1.2	Ethanol, biodiesel, and HVO global production, 2000-2013	2
1.3	The effect of catalyst on the activation energy of the reaction	4
1.4	Overview of research workflow	8
2.1	Overview: the common type of catalysts	13
2.2	Schematic structure of solid acid catalyst derived from D-glucose after sulfonation process	16
2.3	Illustration of molecular rearrangement during the preparation of solid acid catalyst derived from D-glucose; (A) Pyrolysis, (B) carbonization and (C) sulfonation	16
2.4	Esterification reaction of free fatty acid with methanol in the presence of an acid catalyst	17
2.5	Transesterification reaction of triglycerides with methanol to FAMES	17
2.6	Illustration of a reversible transesterification reaction of triglycerides and methanol in the presence of a basic catalyst by three-step process	18
2.7	TLC results of yield composition at different reaction times	24
2.8	Schematic diagram of an autoclave reactor	25
2.9	Schematic design of a microwave reactor	26
2.10	Scheme of a flow-type ultrasound reactor	27
2.11	Schematic diagram of supercritical reactor	28
3.1	Infrared spectra of carbohydrate-derived solid acid catalysts: (a) incomplete carbonized carbon, (b) glucose-SO <sub>3</sub> H, (c) sucrose-SO <sub>3</sub> H, (d) maltose-SO <sub>3</sub> H, (e) cellulose-SO <sub>3</sub> H and (f) starch-SO <sub>3</sub> H	41
3.2	SEM images (500 × magnification) of carbohydrate-derived solid acid catalysts (a) glucose-SO <sub>3</sub> H (b) starch-SO <sub>3</sub> H, (c) sucrose-SO <sub>3</sub> H, (d) cellulose-SO <sub>3</sub> H and (e) maltose-SO <sub>3</sub> H	43
3.3	EDX spectra of carbohydrate-derived solid acid catalysts (a) Incomplete carbonized carbon, (b) Glucose-SO <sub>3</sub> H, (c) Starch-SO <sub>3</sub> H, (d) Maltose-SO <sub>3</sub> H, (e) Cellulose-SO <sub>3</sub> H and (f) Sucrose-SO <sub>3</sub> H	44
3.4	XRD patterns of carbohydrate-derived solid acid catalysts; (a) glucose-SO <sub>3</sub> H, (b) starch-SO <sub>3</sub> H, (c) maltose-SO <sub>3</sub> H, (d)	45

	sucrose-SO <sub>3</sub> H and (e) cellulose-SO <sub>3</sub> H	
3.5	TGA thermograms of carbon-based solid acid catalyst before and after sulfonation (a) incomplete carbonized glucose, (b) glucose-SO <sub>3</sub> H, (c) cellulose-SO <sub>3</sub> H, (d) maltose-SO <sub>3</sub> H, (e) starch-SO <sub>3</sub> H and (f) sucrose-SO <sub>3</sub> H.	48
3.6	NH <sub>3</sub> -TPD patterns of carbohydrate-derived solid acid catalysts(i) before and (ii) after sulfonation	50
3.7	N <sub>2</sub> adsorption-desorption isotherms and pore size distribution of (a) IC-starch and (b) Starch-SO <sub>3</sub> H catalyst	51
3.8	XPS analysis (wide scan) of Starch-SO <sub>3</sub> H catalyst	53
3.9	XPS analysis (narrow scan) in (a) C 1s region, (b) O 1s region and (c) S 2p region of Starch-SO <sub>3</sub> H.	54
3.10	Proposed (a) 2-D and (b) 3-D schematic structures of carbohydrate-derived solid acid catalyst	55
4.1	GC-MS chromatogram of PFAD consist of (a) myristic acid, (b) palmitic acid, (c) stearic acid, (d) oleic acid and (e) linoleic acid	60
4.2	Mechanism acid-catalyzed esterification of the PFAD by Glucose-SO <sub>3</sub> H catalyst	61
4.3	Effect of different methanol-to-PFAD molar ratio on esterification of PFAD (Operating parameters: reaction temperature of 65 °C, catalyst amount of 2 wt.% and reaction time of 3 h)	62
4.4	Effect of different catalyst amount on esterification of PFAD. (Operating parameters: reaction temperature of 65 °C, methanol-to-PFAD molar ratio of 10:1 and reaction time of 3 h)	63
4.5	Effect of reaction temperature on the conversion of PFAD (Operating parameters: methanol-to-PFAD molar ratio of 10:1, catalyst amount of 2 wt.% and reaction time of 3 h)	64
4.6	The reaction time of the esterification of PFAD (Operating parameters: 2 wt.% of catalyst, 10:1 of methanol-to-PFAD molar ratio and 75 °C of reaction temperature)	65
4.7	The catalytic activity of the carbohydrate-derived solid acid catalyst at optimized reaction condition. Reaction conditions: catalyst amount, 2 wt.%; methanol-to-PFAD molar ratio, 10:1; reaction temperature, 75 °C; reaction time, 3 h)	66
4.8	Reusability and leaching analysis of (a) starch-SO <sub>3</sub> H and (b) glucose-SO <sub>3</sub> H catalysts. (Reaction condition: catalyst amount 2 wt.%, methanol-to- PFAD molar ratio 10:1, reaction temperature 75 °C and reaction time 3 h)	68
5.1	Diagnostic plots (a) plots of predicted data versus the actual	76

	data (b) plots of residuals versus the predicted response (c) Normal probability plots of the residuals	
5.2	3D-response surface and contour plots (a) catalyst amount vs. reaction time, (b) methanol vs. catalyst loading and (c) methanol vs. reaction time.	79
6.1	Effect of catalyst amount on esterification of PFAD under microwave irradiation	84
6.2	Effect of methanol-to-PFAD molar ratio on the esterification of PFAD under microwave irradiation	85
6.3	Effect of reaction temperature on esterification of PFAD under microwave irradiation	86
6.4	Comparison of the performance of microwave irradiation and conventional heating techniques on the conversion of PFAD	87
6.5	Catalyst reusability and recycling analysis. (Reaction condition: catalyst amount, 3 wt %; methanol-to-PFAD molar ratio, 12:1; reaction temperature, 75 °C; reaction time, 15 min)	88
7.1	Phase diagram (a) methanol/corn oil mixture and (b) methanol/rapeseed oil mixture	90
7.2	Schematic diagram of supercritical reactor	91
7.3	Effect of catalyst amount on FAME yield and system pressure in supercritical methanol. (Operating parameters: methanol/PFAD molar ratio of 6/1, reaction temperature of 290 °C, reaction time of 30 min)	94
7.4	Effect of methanol/PFAD molar ratio on FAME yield in supercritical methanol. (Operating parameters: reaction temperature of 290 °C, catalyst amount of 1 wt.%, reaction time of 30 min, and $P = 20 - 30$ MPa)	95
7.5	Effect of reaction temperature on FAME yield in supercritical methanol. (Operating parameters: methanol/PFAD molar ratio of 6/1, catalyst amount of 1 wt.%, reaction time of 10 min and $P = 20 - 30$ MPa).	96
7.6	Esterification reaction rate in sub- and supercritical methanol at 190 and 290 °C with sulfonated carbon-based solid acid catalyst (a) Glucose-SO <sub>3</sub> H and (b) Starch-SO <sub>3</sub> H. (Operating parameters: methanol/PFAD molar ratio of 6/1, catalyst amount of 1 wt.% and $P = 20 - 30$ MPa).	97
7.7	Comparison between catalyzed reaction and non-catalyzed reaction in supercritical methanol. (Optimum operating parameters: methanol/PFAD molar ratio of 6/1, catalyst amount of 1 wt.%, reaction temperature of 290 °C and $P = 20 - 30$ MPa).	98



7.8	Reusability potential and deactivation analysis of the catalysts. (Operating parameters: methanol/PFAD molar ratio of 6/1, catalyst amount of 3 wt.%, reaction temperature of 290 °C, reaction time of 10 min and $P = 20 - 30$ MPa).	99
7.9	Comparison of the performance of the methanol-reflux (reaction temperature: 75 °C), microwave-irradiation (reaction temperature: 75 °C) and supercritical-methanol (reaction temperature: 290 °C) esterification of PFAD catalyzed by glucose-SO <sub>3</sub> H catalyst in each optimized condition	100
8.1	IR spectrum of PFAD biodiesel	155
8.2	GC-MS chromatogram of PFAD biodiesel	106
8.3	The mass spectra of fatty acid methyl esters: (a) methyl tetradecanoate, (b) methyl hexadecanoate, (c) methyl linoleate, (d) methyl oleate and (e) methyl stearate	107
8.4	<sup>1</sup> H-NMR spectrum of PFAD methyl ester	109

## LIST OF TABLES

Table		Page
2.1	Values for American Society for Testing and Materials (ASTM) standards of maximum allowed quantities in diesels and biodiesels	9
2.2	Example of fatty acid profiles of PFAD provided by Chumporn Palm Oil Industry Public Company Limited, Thailand	11
2.3	List of analysis methods for vegetable oil	12
2.4	Advantage and disadvantage of homogeneous and heterogeneous catalyst	14
2.5	Comparison of different types of catalysts, reaction temperatures, reaction times and methanol-to-oil molar ratios and percentages of biodiesel produced from high FFA feedstock	20
2.6	Fuel properties of biodiesel according to requirement of biodiesel standards and test methods	30
2.7	Comparison of estimation combustion characteristics of different biodiesels in engines	31
3.1	Effect of calcination temperature and calcination time on the texture properties and catalytic activity of the glucose carbon catalyst	38
3.2	Effect of different sulfonation time on acid sites density, S content, surface area and FFA conversion	39
3.3	Code name for carbohydrate-derived solid acid catalysts	40
3.4	Elemental analysis of carbohydrate-derived solid acid catalysts	44
3.5	Carbohydrate-derived solid acid catalyst coded, physico-chemical properties and catalytic evaluation	52
4.1	Physicochemical properties, fatty acid compositions and characteristics of PFAD	60
5.1	Levels of the esterification condition variables	71
5.2	Experimental design generated by RSM, and responses from each reaction	72
5.3	Sequential model sum of squares	73
5.4	ANOVA analysis of response surface quadratic model	74
7.1	The critical properties of the methanol/PFAD mixtures at various composition calculated by Lydersens's method of group contributions with the application of Lorentz-	95

	Berthelot-type mixing rules	
8.1	Fatty acid composition of PFAD biodiesel oil	105
8.2	Fuel properties of PFAD methyl esters in comparison with biodiesel standards	110



## LIST OF ABBREVIATIONS

$P_c$	Critical pressure
$T_c$	Critical temperature
MW	Molecular weight
T	Reaction temperature
t	Reaction time
$S_{BET}$	BET surface area
$P_o$	Vapour pressure
$P/P_o$	Relative pressure
P	Reaction pressure
R	Alkyl group
c	BET Constant
M	Molarity
m	mol
°C	Degree celcius
h	Hour
min	Minutes
$\mu$ L	Microliter
mg	Miligram
PFAD	Palm Fatty Acid Distillate
CPO	Crude Palm Oil
ANOVA	Analysis of VAriance
ASTM	American Society for Testing and Materials
EN	European Standard
CCD	Central Composite Design
FFA	Free fatty acid
TGs	Triglycerides
MGs	Monoglycerides
DGs	Diglycerides
DOE	Design of Experiment
FAME	Fatty acid methyl ester
GC-FID	Gas Chromatography-Flame Ionization Detector\
GC-MS	Gas Chromatography- Mass Spectrometer
AV	Acid value
SV	Saponification value
NaOH	Sodium hydroxide
KOH	Potassium hydroxide
$CH_3OH$	Methanol
$C_2H_5OH$	Ethanol
$H_2SO_4$	Sulphuric acid
KBr	Potassium bromide
XRD	X-ray Diffraction analysis
TG-DTG	Thermal Gravimetry-Differential Thermal Gravimetric
FESEM	Field Emission Scanning Electron Microscopy
BET	Brunauer-Emmett-Teller
FTIR	Fourier Transform Infrared Spectroscopy
$NH_3$ -TPD	Ammonia-Temperature Programmed Desorption
$NaHCO_3$	Sodium Hydrogen Carbonate

HCl	Hydrochloric Acid
GHG	Life-cycle Greenhouse Gas
NO <sub>x</sub>	Nitrogen dioxide
XPS	X-ray Photoelectron Spectroscopy
PP	Pour Point
CP	Cloud Point
RSM	Response Surface Methodology
CHNOS	Carbon Hydrogen Nitrogen Oxygen Sulfur element analysis
EDX	Energy Dispersive X-ray
-PWM	-Pulse Width Modulation



# CHAPTER 1

## INTRODUCTION

### 1.1 Green Technology and Alternative Fuels

Currently, the negative environmental impact from the burning of fossil fuels, coals, and compressed natural gas has become one of the major problems occurring worldwide (Amigun *et al.*, 2008; Demirbas, 2008). Climate changes occur when the greenhouse effect increases from the burning of fossil fuels as evidenced by flash floods, windstorms, heat waves, and sudden droughts in a number of countries (Lam & Lee, 2011). Furthermore, the global energy demand is increasing while energy sources from fossil fuels are rapidly diminishing.

Fossil fuels are one of the non-renewable energy resources, which will be exhausted in several decades if large-scale of energy source is used continuously (Aguilera *et al.*, 2009). As shown in Figure 1.1, the world production of fossil oil is at the peak of the production, and it was expected to diminish as reaching the year 2050. As a result of those scenarios, replacing petroleum consumption, minimizing future costs, and eliminating the negative impact on health and the environment are crucial. Thus, the replacement of non-renewable energy source with renewable resources is imperative to fulfill the needs of the energy demand without causing harm to the environment and mankind.

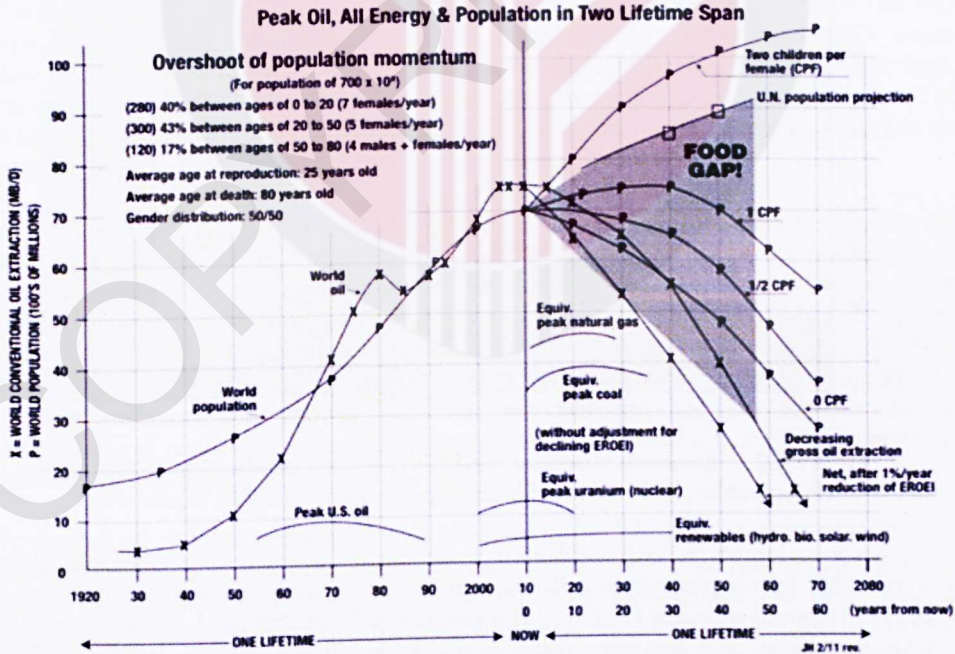
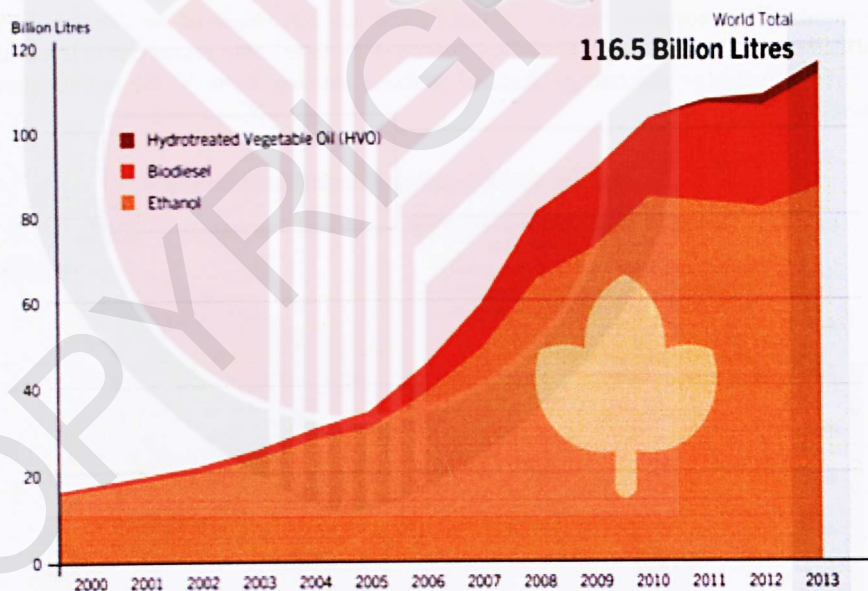


Figure 1.1 Estimation of fossil oil production in comparison with world population (ASPO-USA Supplement, November 2011)

Because of that crisis, different types of energy are being utilized to cover up the high demand of petroleum-based fuel such as the wind turbines, river dams, solar panels, geothermal power and biofuels. Since past decades the production of bio-fuel, ethanol and hydro treated vegetable oil are increased significantly and became the most common alternative fuels, as shown in Figure 1.2. In this work, only the potential of bio-fuel derived natural renewable resource or known as biodiesel has been focused and investigated as the alternative fossil-fuel replacement.

## 1.2 Biodiesel and its Benefit

Basically, biomass can be converted to biofuels such as biogas, biodiesel, and bioethanol (Peng-Lim *et al.*, 2012). The feedstocks of biofuel are differentiating each other and the availability of feedstock is highly dependent on agro-climatic conditions of the region. As reported by Lam & Lee (2011), biodiesel has similar properties as fossil fuels in terms of the chemical structure and energy content. Thus, biodiesels became the most suitable bio-fuels to replace non-renewable diesel fuel as the energy source for transportation and industries. Furthermore, the modification of the engine system is not required due to the compatibility of biodiesel in normal diesel engine and it has been used widely in Europe and the United States (Xue *et al.*, 2011).



**Figure 1.2 Ethanol, biodiesel, and HVO global production, 2000-2013**  
(Renewables, 2014 Global Status Report - Paris: REN21, Secretariat)

Biodiesel or known as fatty acid alkyl ester can be derived from vegetable oils or animal fats by simple transesterification and esterification processes (Rashid *et al.*, 2013). Biodiesel is meant for standard diesel engines whether used directly or blended with petroleum. For instance, some available biodiesels include B100 (100% of biodiesel), B20 (blended with 20% of biodiesel) and B5 (blended with 5% of biodiesel) (Dubé *et al.*, 2007; Szybist *et al.*, 2007). Biodiesel was introduced as early as 1853 by Patrick Duffy (Duffy, 1853), which was about 40 years before Rudolf Diesel had

developed the first model of a diesel engine on the 10<sup>th</sup> August 1893 (Henriques, 1898).

Al Zuhair (2007) and Agarwal *et al.* (2007) reported that the biodiesel has an excellent combustion emission profile by producing lower emission of carbon monoxide, unburned hydrocarbon and particulate matters. The combustion of biodiesel produces low concentration of CO<sub>2</sub> to the atmosphere, thus eliminating the green house effect. The properties of biodiesels such as biodegradable in nature, low toxicity, lower sulfur content, high volatility, high flammability, high cetane number (shorter ignition delays) and better lubricity have made it acceptable as an emerging renewable energy resource for replacement of petroleum-based fuel (Boehman, 2005; Knothe *et al.*, 2006; Sharma & Singh, 2010).

### 1.3 Biodiesel Production Process

The most important factors for choosing the technology to be employed for biodiesel production is quality of the oil; consisting with different amount of free fatty acid (FFA), moisture and saturation level of vegetable oils and animal fats. The common virgin oil such as palm oil, soybean oil and canola oil are the most expensive feedstock and not compatible for low-cost biodiesel production. As reported some years ago, 70% from the total cost of biodiesel production is originated from the price of the feedstock and followed by the costs of the solvent, energy power and maintenance (Ma & Hanna, 1999). For that reason, an ideal way to reduce the cost of biodiesel production is by using the cheaper feedstock such as animal fats, greases and waste oils.

Canakci & Gerpen (2001) studied the production of biodiesel from high FFA fats and oils. They reported that 2.5 billion pounds of restaurant's and fast-food stall's waste fats were collected yearly. The authors also mentioned the price of the animal feed, tallow, grease, blood and hydrolyzed feather meal were less than \$0.02 per pound. In addition to these findings, it was also stated that the usage of waste materials is possible for lowering the cost of biodiesel production by 50 to 70%.

In this work, a high FFA content of non-edible by-product from refinery of palm oil known as palm fatty acid distillate (PFAD) was chosen as the test oil for production of fatty acid methyl ester (FAME) or known as biodiesel. In 2014, Malaysia is exporting 25.02 million metric tons of crude palm oil with the total income of RM63.36 billion, and known as the second largest country of crude palm oil producer after Indonesia; besides producing 1.11 million metric tons of PFAD as the side-product of palm oil refinery process (Zain, 2015). The crude oil refining process is the process for purification of crude palm oil and it is required to remove the FFA or PFAD to produce refined vegetable oil.

A number of research groups had studied the usage of PFAD as starting materials for biodiesel production including Yujaroen *et al.*, (2009), Cho *et al.*, (2012), Chongkhong *et al.*, (2007) and Chongkhong *et al.*, (2009). Nowadays, PFAD has been used in animal feed industry, cosmetic industry and soap industry (Mielke, 2010). In our investigation, we found out that the utilization of PFAD as the biodiesel's feedstock could maximize the biodiesel productivity by enhancing the production yield, lowering the production cost and also had potential in improving the management of abundance waste materials, which can lead to the environmental pollution.

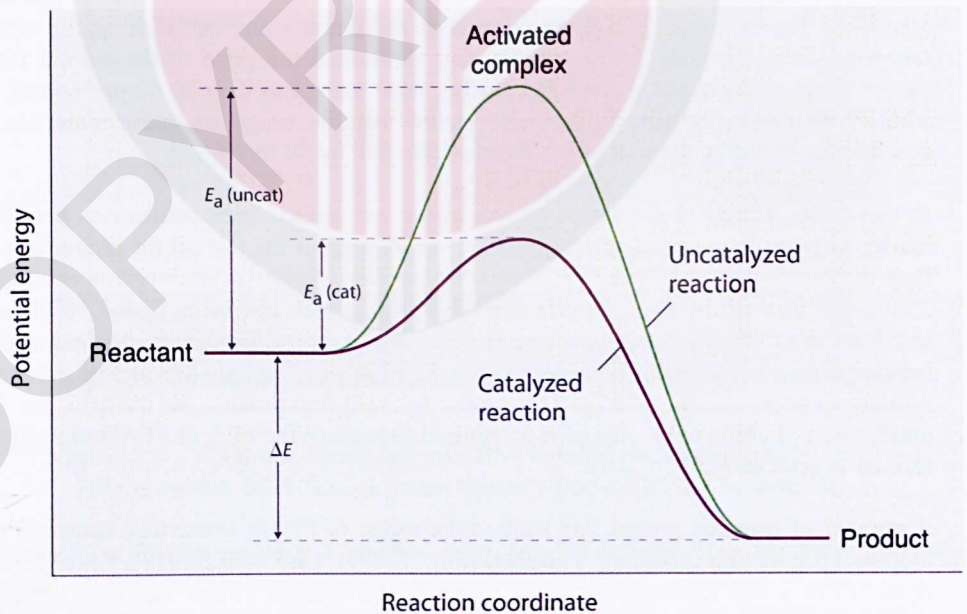


## 1.4 Catalyst

The utilization of catalyst in biodiesel production is important in order to increase the FAME yield and improve the production process. Basically, catalyst is defined as any substance with a potential to increase or to speed up the reaction rate of certain chemical reaction by providing the alternative way with lower activation energy as shown in Figure 1.3. There are two main types of catalysts which were normally used in the biodiesel production process; homogeneous and heterogeneous catalyst. Homogeneous catalyst is the catalyst that has the same phase with the reactant or the sample feedstock. Meanwhile, the heterogeneous catalyst is the catalyst which has a different phase from the reactants (Astruc *et al.*, 2005; Phan *et al.*, 2006).

The homogeneous base and acid catalysts are the common catalyst for biodiesel production. However, it could cause many obstacles such as the equipment corrosion, difficulties in separation and abundance of toxic wastewater after biodiesel purification process. To overcome the stated problems, the heterogeneous solid catalyst is used and it allows more environmentally friendly process for biodiesel production (Islam *et al.*, 2012), it also had the potential to eliminate the separation, purification, corrosion and environmental problems.

A number of heterogeneous solid acid catalysts have been introduced in past decades, for instance carbon-based catalyst (Deshmane *et al.*, 2013; Wang *et al.*, 2013), metal-based catalyst (Islam *et al.*, 2012; Jacobson *et al.*, 2008) and polymer-based catalyst (Yamaguchi *et al.*, 2009). However, each catalyst has individual drawbacks and limitation in certain reaction conditions; they include expensive materials, complicated preparation step, less activity and stability.



**Figure 1.3** The effect of catalyst on the activation energy of the reaction (Clark, 2012)

Recently, the heterogeneous poly-aromatic carbon-based solid acid catalyst becomes an attractive catalyst due to its cheaper cost preparation, good stability of carbon structure, high surface area, modification ability, and high catalytic activity. Thus, it would be a good catalyst for low-cost biodiesel production. Carbon-based solid acid catalyst can be easily synthesized from cheap biomass materials such as wheat (Wang *et al.*, 2013), carbohydrates (Deshmane *et al.*, 2013), oil-cake wastes (Konwar, Das, *et al.*, 2014) and empty fruit bunch (Yaakob *et al.*, 2012). Different carbon precursors give different catalytic profiles with different reaction performance. A fundamental study needs to be done to understand the activity related to the network of carbon structure and its criteria and properties.

In this work, a number of carbon-based solid acid catalysts were prepared from the carbohydrate species. The performance of each catalyst was investigated by carry out the reaction of PFAD with methanol at different operating condition and different type of reactors.

### 1.5 Problem Statements

The growing of the motorization and industrialization worldwide has led to the high demand of the petroleum-based fuel. Today, the sources of petroleum fuel are drained and exhausted. High-energy demand and the depletion of petroleum source had caused the great increase in price of fossil fuel, which only makes the replacing of fossil fuel with bio-fuel more crucial than ever. However, biodiesel too, carries a high price tag in the industry because of the expensive feedstock, expensive reactor and high maintenance. The use of non-edible waste material helps in reducing the cost of biodiesel production. In this work, PFAD oil has been used as the biodiesel's starting material, which was believed to have a significant potential as the next biodiesel feedstock. Indirectly, the waste management from palm oil factory also could be improved.

In the production of biodiesel, a catalyst is very important to improve the efficiency of the process. Heterogeneous catalyst was used instead of homogeneous catalyst due to the difficulties in separation and corrosion problem. However, the catalytic activity and the stability of the heterogeneous catalyst are the key factors in synthesizing a novel catalyst. To overcome this matter, the poly-aromatic carbon-based solid acid catalysts were introduced in this research, which had proved to have high catalytic activity and good stability.

The extended reaction time by classical methanol reflux method reduces the efficiency of the process. In this work, several approaches were carried out to increase the reaction rate; there are by the bombardment of microwave irradiation directly to the molecular level of the reaction mixture, and by heating the reaction mixture up to the supercritical level, where the boundaries between methanol and oil are removed. The basic understandings on these approaches will be discussed and reported in this thesis.

## 1.6 Hypothesis of the Research

The catalytic activity of the heterogeneous catalyst is strongly related to their surface characteristic and density of the active site. In this work, the carbohydrate-derived solid acid catalysts were activated with the sulfuric acid to generate the sulfonic functional group on the poly-aromatic carbon structure. Theoretically, high density of acid active site will escalate the activity of the catalysts, thus, more acid sites introduced on the structure of carbohydrate-derived solid acid catalyst resulted more catalytic activity.

Normally, the biodiesel is produced in an open system by simple methanol-reflux process at 65 °C for several hours. In this research, the potential of the microwave and the supercritical methanol reactors were introduced with the objective to enhance the reaction rate of both esterification and transesterification processes. The particular reactors had been used previously for the non-catalytic reaction of biodiesel production; however, the reaction rate had not improved significantly. The main idea is to introduce the heterogeneous solid catalyst into the reactor system. It was suggested that, the existence of the carbohydrate-derived solid acid catalyst in the reaction system helps to increase the reaction rate significantly and enhanced the yield of the biodiesel, hence reduces the time consumption needed to complete the reaction.

## 1.7 Objectives of the Research

The purpose of this research is to study the biodiesel production from PFAD, which is catalyzed by highly efficient heterogeneous solid acid catalyst derived from carbohydrates. There are 6 main objectives have been highlighted and concentrated:

1. To synthesis and characterize the heterogeneous carbohydrate-derived solid acid catalyst.
2. To evaluate the potential of PFAD as low-quality biodiesel feedstock.
3. To optimize the parameter condition for esterification of PFAD.
4. To investigate the effect of microwave-irradiation on esterification of PFAD.
5. To study the effect of supercritical temperature on esterification of PFAD.
6. To evaluate and investigate the properties of PFAD biodiesel.

## 1.8 Scope of the Research

This research covers the development of the low-cost biodiesel production process by using the low quality biodiesel feedstock such as PFAD as the main oil test. The PFAD is the by-product from the refinery process of crude palm oil containing large numbers of FFA in the range of 80-90 wt.%. Theoretically, direct esterification of PFAD with the methanol produces fatty acid methyl ester (FAME), water and small amount of glycerol as side product. Heterogeneous carbon-based solid acid catalysts derived from carbohydrate species were used to catalyze the reaction system instead of homogeneous catalyst. Detail characterization analysis of the catalyst and optimization process of the catalytic reaction were carried out and discussed in this thesis with the main purpose to understand the behavior of the catalyst toward the production of biodiesel. The microwave and supercritical methanol reactors were used to study the possibility and the potential to increase the reaction rate of the process and to shorten the reaction time. The biodiesel produced from this research have been analyzed through the quality

assessment analysis according to the American Society for Testing and Materials (ASTM) and European (EN) standard methods.

## 1.9 Significant of the Research

In this work, a series of carbohydrate-derived solid acid catalysts were prepared and characterized, which was believed, had high potential to be used for the biodiesel production from high FFA feedstock, due to high catalytic activity, stability and recycle ability without any negative impact to the instrument and environment. The influence of different type of reactors was investigated in order to determine the most potential method to improve the reaction process, such as the microwave reactor equipped with temperature and power controller and the application of supercritical methanol reactor was used to study the behavior of the reaction mixture at supercritical state. The explanation on the heterogeneous carbohydrate-derived solid acid catalyst and both reactors in the production of the biodiesel from low-quality feedstock are the main cores in this work. Figure 1.4 shows the overall overview of the research flow in this work, which covers: (1) preparation and characterization of 5 types of carbohydrate-derived solid acid catalysts, (2) the collection and analysis of biodiesel feedstock, (3) catalytic evaluation of the catalyst, (4) optimization of the reaction conditions, (5) biodiesel production using the alternative methods (e.g., microwave-irradiation and supercritical-solvent techniques) and (6) Quality assessment of the product.

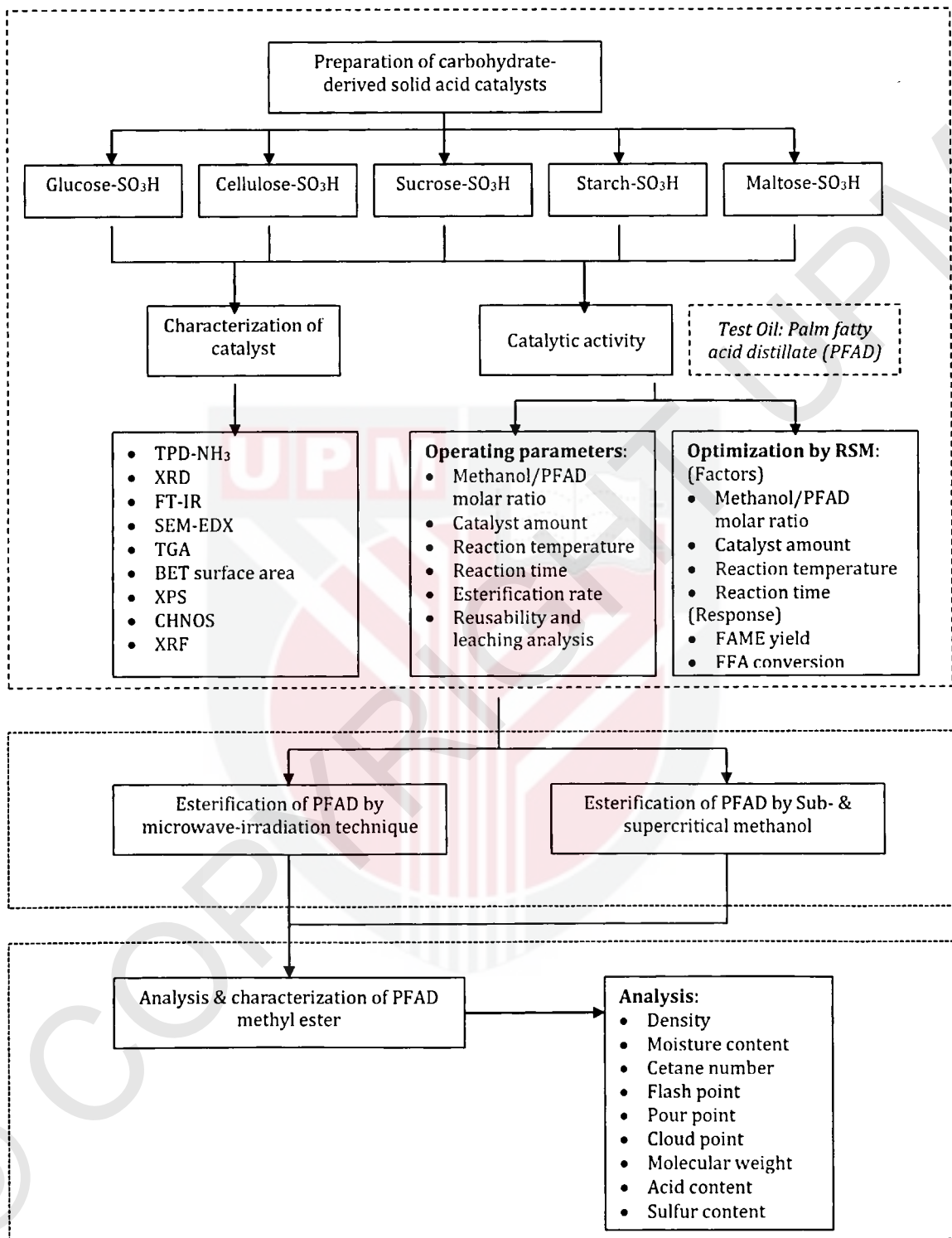


Figure 1.4 Overview of research workflow

## REFERENCES

- (AOCS) American Oil Chemists' Society. (n.d.). Retrieved from aocs.org
- (ISO) International Organization for Standardization. (n.d.).
- Abdulagatov, I. M., Polikhronidi, N. G., Abdurashidova, a., Kiselev, S. B., & Ely, J. F. (2005). Thermodynamic properties of methanol in the critical and supercritical regions. *International Journal of Thermophysics* 26(5): 1327–1368.
- Agarwal, D., & Agarwal, A. K. (2007). Performance and emissions characteristics of Jatropa oil (preheated and blends) in a direct injection compression ignition engine. *Applied Thermal Engineering* 27(13): 2314–2323.
- Aguilera, R. F., Eggert, R. G., Lagos, G., & Tilton, J. E. (2009). Depletion and the future availability of petroleum resources. *Energy Journal* 30(1): 141–174.
- Mushtaq Ahmad, Mir Ajab Khan, Muhammad Zafar and Shazia Sultana (2011). Biodiesel from Non Edible Oil Seeds: a Renewable Source of Bioenergy, Economic Effects of Biofuel Production, Dr. Marco Aurelio Dos Santos Bernardes (Ed.). InTech.
- Al Zuhair, S. (2007). Production of biodiesel: possibilities and challenges. *Bofuels Bioprod* 1(1): 57–66.
- Alhassan, F. H., Yunus, R., Rashid, U., Sirat, K., Islam, A., Lee, H. V., & Taufiq-Yap, Y. H. (2013). Production of biodiesel from mixed waste vegetable oils using Ferric hydrogen sulphate as an effective reusable heterogeneous solid acid catalyst. *Applied Catalysis A: General* 456: 182–187.
- Alves, C. T., Oliveira, A., Carneiro, S. A. V., Silva, A. G., Andrade, H. M. C., Vieira De Melo, S. B., & Torres, E. (2013). Transesterification of waste frying oil using a zinc aluminate catalyst. *Fuel Processing Technology* 106: 102–107.
- American Standards for Testing of Materials (ASTM), West Conshohocken, PA. Standards D93, D 97, D 130, D 445, D 613, D 664, D 874, D 2500, D 4294, D 5949, D 6079, D 6371, D 6584, D6751. (n.d.). Retrieved from www.astm.org
- Amigun, B., Sigamoney, R., & von Blottnitz, H. (2008). Commercialisation of biofuel industry in Africa: A review. *Renewable and Sustainable Energy Reviews* 12: 690–711.
- Anikeev, V. I., Stepanov, D. A., & Yermakova, A. (2013). The Journal of Supercritical Fluids Phase diagrams for vegetable oil / methanol mixtures. *The Journal of Supercritical Fluids* 81: 99–102.
- Asri, N. P., Machmudah, S., Wahyudiono, Suprpto, Budikarjono, K., Roesyadi, A., & Goto, M. (2013). Palm oil transesterification in sub- and supercritical methanol with heterogeneous base catalyst. *Chemical Engineering and Processing: Process Intensification* 72: 63–67.
- Astruc, D., Lu, F., & Aranzaes, J. R. (2005). Nanoparticles as recyclable catalysts: The frontier between homogeneous and heterogeneous catalysis. *Angewandte Chemie - International Edition* 44: 7852–7872.
- Atadashi, I. M., Aroua, M. K., Abdul Aziz, a. R., & Sulaiman, N. M. N. (2012).

- Production of biodiesel using high free fatty acid feedstocks. *Renewable and Sustainable Energy Reviews* 16(5): 3275–3285.
- Azcan, N., & Yilmaz, O. (2013). Microwave assisted transesterification of waste frying oil and concentrate methyl ester content of biodiesel by molecular distillation. *Fuel* 104: 614–619.
- Badday, A. S., Abdullah, A. Z., & Lee, K. T. (2013). Optimization of biodiesel production process from *Jatropha* oil using supported heteropolyacid catalyst and assisted by ultrasonic energy. *Renewable Energy* 50: 427–432.
- Barakos, N., Pasiadis, S., & Papayannakos, N. (2008). Transesterification of triglycerides in high and low quality oil feeds over an HT2 hydrotalcite catalyst. *Bioresource Technology* 99: 5037–5042.
- Basha, S. A., Gopal, K. R., & Jebaraj, S. (2009). A review on biodiesel production, combustion, emissions and performance. *Renewable and Sustainable Energy Reviews* 13: 1628–1634.
- Bezerra, M. A., Santelli, R. E., Oliveira, E. P., Villar, L. S., & Escalera, L. A. (2008). Response surface methodology (RSM) as a tool for optimization in analytical chemistry. *Talanta* 76: 965–977.
- Binner, J. G. P., Hassine, N. A., & Cross, T. E. (1995). The possible role of the pre-exponential factor in explaining the increased reaction rates observed during the microwave synthesis of titanium carbide. *Journal of Materials Science* 30(21): 5389–5393.
- Boehman, A. L. (2005). Biodiesel production and processing. *Fuel Processing Technology* 86: 1057–1058.
- Boey, P. L., Ganesan, S., Maniam, G. P., Khairuddean, M., & Efendi, J. (2013). A new heterogeneous acid catalyst for esterification: Optimization using response surface methodology. *Energy Conversion and Management* 65: 392–396.
- Bunyakiat, K., Makmee, S., Sawangkeaw, R., & Ngamprasertsith, S. (2005). Continuous production of biodiesel via transesterification from vegetable oils in supercritical methanol. *Energy and Fuels* 20(8): 812–817.
- Buyukkaya, E. (2010). Effects of biodiesel on a di diesel engine performance, emission and combustion characteristics. *Fuel* 89(10): 3099–3105.
- Canakci, M., & Gerpen, J. Van. (2001). Biodiesel production from oils and fats with high free fatty acids 44(6): 1429–1436.
- Canakci, M., & Van Gerpen, J. (2001). A Pilot Plant to Produce Biodiesel from High Free Fatty Acid Feedstocks. *American Society of Agricultural Engineers* 46(4): 945–954.
- Çaylı, G., & Küsefoğlu, S. (2008). Increased yields in biodiesel production from used cooking oils by a two step process: Comparison with one step process by using TGA. *Fuel Processing Technology* 89: 118–122.
- CEN (European Committee for Standardization), Brussels, Belgium. Standard EN 14214, automotive fuels e fatty acid methyl esters (FAME) for diesel engines e requirements and test methods; 2008. (n.d.).

- Chen, G., & Fang, B. (2011). Preparation of solid acid catalyst from glucose-starch mixture for biodiesel production. *Bioresource Technology* 102(3): 2635–2640.
- Chhetri, A. B., Tango, M. S., Budge, S. M., Watts, K. C., & Islam, M. R. (2008). Non-edible plant oils as new sources for biodiesel production. *International Journal of Molecular Sciences* 9: 169–180.
- Chin, L. H., Abdullah, a. Z., & Hameed, B. H. (2012). Sugar cane bagasse as solid catalyst for synthesis of methyl esters from palm fatty acid distillate. *Chemical Engineering Journal* 183: 104–107.
- Cho, H. J., Kim, J. K., Ahmed, F., & Yeo, Y. K. (2013). Life-cycle greenhouse gas emissions and energy balances of a biodiesel production from palm fatty acid distillate (PFAD). *Applied Energy* 111: 479–488.
- Cho, H. J., Kim, J. K., Hong, S. W., & Yeo, Y. K. (2012a). Development of a novel process for biodiesel production from palm fatty acid distillate (PFAD). *Fuel Processing Technology* 104: 271–280.
- Cho, H. J., Kim, S. H., Hong, S. W., & Yeo, Y. K. (2012b). A single step non-catalytic esterification of palm fatty acid distillate (PFAD) for biodiesel production. *Fuel* 93: 373–380.
- Chongkhong, S., Tongurai, C., & Chetpattananondh, P. (2009). Continuous esterification for biodiesel production from palm fatty acid distillate using economical process. *Renewable Energy* 34: 1059–1063.
- Chongkhong, S., Tongurai, C., Chetpattananondh, P., & Bunyakan, C. (2007). Biodiesel production by esterification of palm fatty acid distillate. *Biomass and Bioenergy* 31: 563–568.
- Chopey, N. P. (1994). *Handbook of Chemical Engineering Calculation*. New York: McGraw-Hill.
- Cintas, P., Mantegna, S., Gaudino, E. C., & Cravotto, G. (2010). A new pilot flow reactor for high-intensity ultrasound irradiation. Application to the synthesis of biodiesel. *Ultrasonics Sonochemistry* 17(6): 985–989.
- Clark, C. (2012). Principles of General Chemistry. Chapter 14: Chemical Kinetics. pp. 1766: *Creative Commons*.
- Dawodu, F. a., Ayodele, O., Xin, J., Zhang, S., & Yan, D. (2014). Effective conversion of non-edible oil with high free fatty acid into biodiesel by sulphonated carbon catalyst. *Applied Energy* 114: 819–826.
- Dehkhoda, A. M., West, A. H., & Ellis, N. (2010). Biochar based solid acid catalyst for biodiesel production. *Applied Catalysis A: General* 382: 197–204.
- Demirbas, A. (2008). Biofuels sources, biofuel policy, biofuel economy and global biofuel projections. *Energy Conversion and Management* 49: 2106–2116.
- Deshmane, C. a., Wright, M. W., Lachgar, A., Rohlfig, M., Liu, Z., Le, J., & Hanson, B. E. (2013). A comparative study of solid carbon acid catalysts for the esterification of free fatty acids for biodiesel production. Evidence for the leaching of colloidal carbon. *Bioresource Technology* 147: 597–604.



- Dhar, A., Kevin, R., & Agarwal, A. K. (2012). Production of biodiesel from high-FFA neem oil and its performance, emission and combustion characterization in a single cylinder DIC engine. *Fuel Processing Technology* 97: 118–129.
- Do Nascimento, L. A. S., Angélica, R. S., Da Costa, C. E. F., Zamian, J. R., & Da Rocha Filho, G. N. (2011). Conversion of waste produced by the deodorization of palm oil as feedstock for the production of biodiesel using a catalyst prepared from waste material. *Bioresource Technology* 102: 8314–8317.
- Du, Z., Tang, Z., Wang, H., Zeng, J., Chen, Y., & Min, E. (2013). Research and development of a sub-critical methanol alcoholysis process for producing biodiesel using waste oils and fats. *Chinese Journal of Catalysis* 34(1): 101–115.
- Dubé, M. a., Tremblay, a. Y., & Liu, J. (2007). Biodiesel production using a membrane reactor. *Bioresource Technology* 98(3): 639–647.
- Duffy, P. (1853). *On the Constitution of Stearine*: London.
- Dupont, P., Védrine, J. C., Paumard, E., Hecquet, G., & Lefebvre, F. (1995). Heteropolyacids supported on activated carbon as catalysts for the esterification of acrylic acid by butanol. *Applied Catalysis A, General* 129(95): 217–227.
- El Sherbiny, S. a., Refaat, A. a., & El Sheltawy, S. T. (2010). Production of biodiesel using the microwave technique. *Journal of Advanced Research* 1(4): 309–314.
- Encinar, J. M., González, J. F., Martínez, G., Sánchez, N., & Pardal, a. (2012). Soybean oil transesterification by the use of a microwave flow system. *Fuel* 95: 386–393.
- Freedman, B., Pryde, E. H., & Mounts, T. L. (1984). Variables affecting the yields of fatty esters from transesterified vegetable oils. *Journal of the American Oil Chemists Society* 61(10): 1638–1643.
- Fukuda, I., Kondo, A., & Noda, H. (2001). Biodiesel Fuel Production by Tranesterification of Oils. *Jorurnal of Bioscience and Bioengineering* 92(5): 405–416.
- Fukuhara, K., Nakajima, K., Kitano, M., Kato, H., Hayashi, S., & Hara, M. (2011). Structure and catalysis of cellulose-derived amorphous carbon bearing SO<sub>3</sub>H groups. *ChemSusChem* 4(6): 778–784.
- Furuta, S., Matsuhashi, H., & Arata, K. (2004). Biodiesel fuel production with solid superacid catalysis in fixed bed reactor under atmospheric pressure. *Catalysis Communications* 5(12): 721–723.
- Ganapathy, T., Gakkhar, R. P., & Murugesan, K. (2011). Influence of injection timing on performance, combustion and emission characteristics of Jatropha biodiesel engine. *Applied Energy* 88(12): 4376–4386.
- Ghadge, S. V., & Raheman, H. (2006). Process optimization for biodiesel production from mahua (*Madhuca indica*) oil using response surface methodology. *Bioresource Technology* 97(3): 379–384.
- Ghoreishi, S. M., & Moein, P. (2013). Biodiesel synthesis from waste vegetable oil via transesterification reaction in supercritical methanol. *Journal of Supercritical Fluids* 76: 24–31.

- Gole, V. L., & Gogate, P. R. (2013). Intensification of synthesis of biodiesel from non-edible oil using sequential combination of microwave and ultrasound. *Fuel Processing Technology* 106: 62–69.
- Graboski, M. S., & McCormick, R. L. (1998). Combustion of fat and vegetable oil derived fuels in diesel engines. *Progress in Energy and Combustion Science* 24: 125-164.
- Gui, M. M., Lee, K. T., & Bhatia, S. (2009). Supercritical ethanol technology for the production of biodiesel: Process optimization studies. *Journal of Supercritical Fluids* 49: 286–292.
- Guo, F., & Fang, Z. (2011). Biodiesel Production with Solid Catalysts. *Biodiesel Feedstocks and Processing Technologies*, pp.1–21: InTech.
- Guo, F., Fang, Z., & Zhou, T. J. (2012). Conversion of fructose and glucose into 5-hydroxymethylfurfural with lignin-derived carbonaceous catalyst under microwave irradiation in dimethyl sulfoxide-ionic liquid mixtures. *Bioresource Technology* 112: 313–318.
- Guo, F., Xiu, Z. L., & Liang, Z. X. (2012). Synthesis of biodiesel from acidified soybean soapstock using a lignin-derived carbonaceous catalyst. *Applied Energy* 98: 47–52.
- Hara, M., Yoshida, T., Takagaki, A., Takata, T., Kondo, J. N., Hayashi, S., & Domen, K. (2004). A carbon material as a strong protonic acid. *Angewandte Chemie - International Edition* 43: 2955–2958.
- Hayyan, a, Alam, M. Z., & Mirghani, M E S., Kabbashi, N A., Hakimi, N I N M., Siran, Y M., Tahiruddin, S. (2010). Production of Biodiesel from Sludge Palm Oil by Esterification Process. *Energy and Power Engineering* 4(1): 11–17.
- Hayyan, A., Alam, M. Z., Mirghani, M. E. S., Kabbashi, N. A., Hakimi, N. I. N. M., Siran, Y. M., & Tahiruddin, S. (2011). Reduction of high content of free fatty acid in sludge palm oil via acid catalyst for biodiesel production. *Fuel Processing Technology* 92(5): 920–924.
- Henriques, R. (1898). Uber partielle Verseifung von Olen und Fetten. *Zeitschrift Fur Angewandte Chemie* 15: 338–345.
- Hernando, J., Leton, P., Matia, M. P., Novella, J. L., & Alvarez-Builla, J. (2007). Biodiesel and FAME synthesis assisted by microwaves: Homogeneous batch and flow processes. *Fuel* 86: 1641–1644.
- Hindryawati, N., & Maniam, G. P. (2015). Novel utilization of waste marine sponge (*Demospongiae*) as a catalyst in ultrasound-assisted transesterification of waste cooking oil. *Ultrasonics Sonochemistry* 22: 454–462.
- Huang, J., Wang, Y., Li, S., Roskilly, A. P., Yu, H., & Li, H. (2009). Experimental investigation on the performance and emissions of a diesel engine fuelled with ethanol-diesel blends. *Applied Thermal Engineering* 29(11-12): 2484–2490.
- Islam, A., Taufiq-Yap, Y. H., Chu, C.-M., Chan, E.-S., & Ravindra, P. (2012). Studies on design of heterogeneous catalysts for biodiesel production. *Process Safety and Environmental Protection* 91: 131-144.

- Jacobson, K., Gopinath, R., Meher, L. C., & Dalai, A. K. (2008). Solid acid catalyzed biodiesel production from waste cooking oil. *Applied Catalysis B: Environmental* 85: 86–91.
- Juan, J. C., Kartika, D. A., Wu, T. Y., & Hin, T. Y. Y. (2011). Biodiesel production from jatropha oil by catalytic and non-catalytic approaches: An overview. *Bioresource Technology* 102(2): 452–460.
- Kannahi, M., & Arulmozhi, R. (2013). Production of biodiesel from edible and non-edible oils using *Rhizopus oryzae* and *Aspergillus niger*. *Asian Journal of Plant* 3(5): 60–64.
- Kaplan, C., Arslan, R., & Sürmen, A. (2006). Performance Characteristics of Sunflower Methyl Esters as Biodiesel. *Energy Sources, Part A: Recovery, Utilization, and Environmental Effects* 28: 751-755.
- Kastner, J. R., Miller, J., Geller, D. P., Locklin, J., Keith, L. H., & Johnson, T. (2012). Catalytic esterification of fatty acids using solid acid catalysts generated from biochar and activated carbon. *Catalysis Today* 190(1): 122–132.
- Khemthong, P., Luadthong, C., Nualpaeng, W., Changsuwan, P., Tongprem, P., Viriya-Empikul, N., & Faungnawakij, K. (2012). Industrial eggshell wastes as the heterogeneous catalysts for microwave-assisted biodiesel production. *Catalysis Today* 190(1):112–116.
- Kim, D., Choi, J., Kim, G.-J., Seol, S. K., & Jung, S. (2011). Accelerated esterification of free fatty acid using pulsed microwaves. *Bioresource Technology* 102: 7229–7231.
- Kim, J. H., Fang, B., Kim, M. S., Yoon, S. B., Bae, T. S., Ranade, D. R., & Yu, J. S. (2010). Facile synthesis of bimodal porous silica and multimodal porous carbon as an anode catalyst support in proton exchange membrane fuel cell. *Electrochimica Acta* 55(26): 7628–7633.
- Kılıç, M., Uzun, B. B., Pütün, E., & Pütün, A. E. (2013). Optimization of biodiesel production from castor oil using factorial design. *Fuel Processing Technology* 111: 105–110.
- Knothe, G. (2006). Analyzing Biodiesel: Standarts and other Methods. *JAACS* 83(10): 823-833.
- Knothe, G. (2008). “Designer” biodiesel: Optimizing fatty ester composition to improve fuel properties. *Energy and Fuels* 22(2): 1358–1364.
- Knothe, G., & Kenar, J. A. (2004). Determination of the fatty acid profile by H-1-NMR spectroscopy. *European Journal of Lipid Science and Technology* 106(2): 88–96.
- Knothe, G., Sharp, C. a., & Ryan, T. W. (2006). Exhaust emissions of biodiesel, petrodiesel, neat methyl esters, and alkanes in a new technology engine. *Energy and Fuels* 20: 403–408.
- Konwar, L. J., Boro, J., & Deka, D. (2014). Review on latest developments in biodiesel production using carbon-based catalysts. *Renewable and Sustainable Energy Reviews* 29: 546–564.
- Konwar, L. J., Das, R., Thakur, A. J., Salminen, E., Mäki-Arvela, P., Kumar, N., Deka,

- D. (2014). Biodiesel production from acid oils using sulfonated carbon catalyst derived from oil-cake waste. *Journal of Molecular Catalysis A: Chemical* 388-389: 167–176.
- Koopmans, C., Iannelli, M., Kerep, P., Klink, M., Schmitz, S., Sinnwell, S., & Ritter, H. (2006). Microwave-assisted polymer chemistry: Heck-reaction, transesterification, Baeyer-Villiger oxidation, oxazoline polymerization, acrylamides, and porous materials. *Tetrahedron* 62(19): 4709–4714.
- Kusdiana, D., & Saka, S. (2001). Kinetics of transesterification in rapeseed oil to biodiesel fuel as treated in supercritical methanol. *Fuel* 80: 693–698.
- Ladommatos, N., Parsi, M., & Knowles, A. (1996). The effect of fuel cetane improver on diesel pollutant emissions. *Fuel* 75(1): 8–14.
- Lam, M. K., & Lee, K. T. 2011. Production of biodiesel using palm oil. *Biofuels* (1st ed.). pp. 353-374: Elsevier Inc.
- Lee, H. V., Juan, J. C., & Taufiq-Yap, Y. H. (2015). Preparation and application of binary acid–base CaO–La<sub>2</sub>O<sub>3</sub> catalyst for biodiesel production. *Renewable Energy* 74: 124–132.
- Lee, H. V., Yunus, R., Juan, J. C., & Taufiq-Yap, Y. H. (2011). Process optimization design for jatropha-based biodiesel production using response surface methodology. *Fuel Processing Technology* 92: 2420–2428.
- Lertsathapornasuk, V., Pairintra, R., Aryasuk, K., & Krisnangkura, K. (2008). Microwave assisted in continuous biodiesel production from waste frying palm oil and its performance in a 100kW diesel generator. *Fuel Processing Technology* 89(12): 1330–1336.
- Leung, D. Y. C., & Guo, Y. (2006). Transesterification of neat and used frying oil: Optimization for biodiesel production. *Fuel Processing Technology* 87: 883–890.
- Lin, Y. C., Hsu, K. H., & Lin, J. F. (2014). Rapid Jatropha-biodiesel production assisted by a microwave system and sodium methoxide catalyst. *Fuel* 135: 435–442.
- Liu, T., Li, Z., Li, W., Shi, C., & Wang, Y. (2013). Preparation and characterization of biomass carbon-based solid acid catalyst for the esterification of oleic acid with methanol. *Bioresource Technology* 133: 618–621.
- Liu, Y., Wang, L., & Yan, Y. (2009). Biodiesel synthesis combining pre-esterification with alkali catalyzed process from rapeseed oil deodorizer distillate. *Fuel Processing Technology* 90(7-8): 857–862.
- Lotero, E., Liu, Y., Lopez, D. E., Suwannakarn, K., Bruce, D. a., & Goodwin, J. G. (2005). Synthesis of biodiesel via acid catalysis. *Industrial and Engineering Chemistry Research* 44: 5353–5363.
- Lou, W. Y., Zong, M. H., & Duan, Z. Q. (2008). Efficient production of biodiesel from high free fatty acid-containing waste oils using various carbohydrate-derived solid acid catalysts. *Bioresource Technology* 99: 8752–8758.
- Lu, X. B., He, R., & Bai, C. X. (2002). Synthesis of ethylene carbonate from supercritical carbon dioxide/ethylene oxide mixture in the presence of

- bifunctional catalyst. *Journal of Molecular Catalysis A: Chemical* 186: 1–11.
- Lundstedt, T., Seifert, E., Abramo, L., Thelin, B., Nystrom, A., Pettersen, J., & Bergman, R. (1998). Experimental design and optimization. *Chemometrics and Intelligent Laboratory Systems* 42(1-2): 3–40.
- Ma, F., & Hanna, M. A. (1999). Biodiesel production: A review. *Bioresource Technology* 70: 1-15.
- Mar, W. W., & Somsook, E. (2012). Sulfonic-functionalized carbon catalyst for esterification of high free fatty acid. *Procedia Engineering* 32: 212–218.
- Marchetti, J. M., Miguel, V. U., & Errazu, a. F. (2008). Techno-economic study of different alternatives for biodiesel production. *Fuel Processing Technology* 89(8): 740–748.
- Mathiyazhagan, M., Ganapathi, a., Jaganath, B., Renganayaki, N., & Sasireka, N. (2011). Production of Biodiesel from Non-edible Plant Oils having High FFA Content. *International Journal of Chemical and Environmental Engineering* 2(2): 119–122.
- Melero, J. A., Bautista, L. F., Morales, G., & Iglesias, J. (2015). Acid-catalyzed production of biodiesel over arenesulfonic SBA-15: Insights into the role of water in the reaction network 75: 425–432.
- Mielke, T. (2010). The price outlook of palm and lauric oils and impacts from the global vegetable oil markets – A fundamental approach.
- Mo, X., Lotero, E., Lu, C., Liu, Y., & Goodwin, J. G. (2008). A novel sulfonated carbon composite solid acid catalyst for biodiesel synthesis. *Catalysis Letters* 123: 1–6.
- Montgomery, D. C. (2001). *Design and analysis experiments* (5th ed.). New York: John Wiley & Sons.
- Motasemi, F., & Ani, F. N. (2012). A review on microwave-assisted production of biodiesel. *Renewable and Sustainable Energy Reviews* 16(7): 4719–4733.
- Musharraf, S. G., Ahmed, M. A., Zehra, N., Kabir, N., Choudhary, M. I., & Rahman, A.-U. (2012). Biodiesel production from microalgal isolates of southern Pakistan and quantification of FAMES by GC-MS/MS analysis. *Chemistry Central Journal* 6(1): 149.
- Nakajima, K., & Hara, M. (2012). Amorphous Carbon with SO<sub>3</sub>H Groups as a Solid Brønsted Acid Catalyst. *ACS Catalysis* 2: 1296–1304.
- Nakajima, K., Hara, M., & Hayashi, S. (2007). Environmentally benign production of chemicals and energy using a carbon-based strong solid acid. *Journal of the American Ceramic Society* 90: 3725–3734.
- Nakpong, P., & Wootthikanokkhan, S. (2010). High free fatty acid coconut oil as a potential feedstock for biodiesel production in Thailand. *Renewable Energy* 35(8): 1682–1687.
- Nehdi, I. A., Sbihi, H. M., Mokbli, S., Rashid, U., & Al-Resayes, S. I. (2015). Yucca aloifolia oil methyl esters. *Industrial Crops and Products* 69: 257–262.

- Okamura, M., Takagaki, A., Toda, M., Kondo, J. N., Domen, K., Tatsumi, T., Hayashi, S. (2006). Acid-catalyzed reactions on flexible polycyclic aromatic carbon in amorphous carbon. *Chemistry of Materials* 18(5): 3039–3045.
- Olivares-Carrillo, P., Quesada-Medina, J., Pérez de los Ríos, A., & Hernández-Fernández, F. J. (2014). Estimation of critical properties of reaction mixtures obtained in different reaction conditions during the synthesis of biodiesel with supercritical methanol from soybean oil. *Chemical Engineering Journal* 241: 418–432.
- Ormsby, R., Kastner, J. R., & Miller, J. (2012). Hemicellulose hydrolysis using solid acid catalysts generated from biochar. *Catalysis Today* 190(1): 89–97.
- Peng, B.-X., Shu, Q., Wang, J.-F., Wang, G.-R., Wang, D.-Z., & Han, M.-H. (2008). Biodiesel production from waste oil feedstocks by solid acid catalysis. *Process Safety and Environmental Protection* 86: 441–447.
- Peng-Lim, B., Ganesan, S., Maniam, G. P., & Khairuddean, M. (2012). Sequential conversion of high free fatty acid oils into biodiesel using a new catalyst system. *Energy* 46(1): 132–139.
- Petchmala, A., Laosiripojana, N., Jongsomjit, B., Goto, M., Panpranot, J., Mekasuwandumrong, O., & Shotipruk, A. (2010). Transesterification of palm oil and esterification of palm fatty acid in near- and super-critical methanol with SO<sub>4</sub>-ZrO<sub>2</sub> catalysts. *Fuel* 89(9): 2387–2392.
- Phan, A. N., & Phan, T. M. (2008). Biodiesel production from waste cooking oils. *Fuel* 87: 3490–3496.
- Phan, N. T. S., Van Der Sluys, M., & Jones, C. W. (2006). On the nature of the active species in palladium catalyzed Mizoroki-Heck and Suzuki-Miyaura couplings - Homogeneous or heterogeneous catalysis, a critical review. *Advanced Synthesis and Catalysis* 348: 609–679.
- Ping, B. T. Y., & Yusof, M. (2009). Characteristics and Properties of Fatty Acid Distillates from Palm Oil. *Oil Palm Bulletin* 59: 5–11.
- Puhan, S., Vedaraman, N., Sankaranarayanan, G., & Ram, B. V. B. (2005). Performance and emission study of Mahua oil (madhuca indica oil) ethyl ester in a 4-stroke natural aspirated direct injection diesel engine. *Renewable Energy* 30(8): 1269–1278.
- Rakopoulos, C. D., Antonopoulos, K. a., Rakopoulos, D. C., Hountalas, D. T., & Giakoumis, E. G. (2006). Comparative performance and emissions study of a direct injection Diesel engine using blends of Diesel fuel with vegetable oils or bio-droksupels of various origins. *Energy Conversion and Management* 47: 3272–3287.
- Rashid, U., & Anwar, F. (2008). Production of biodiesel through optimized alkaline-catalyzed transesterification of rapeseed oil. *Fuel* 87(3): 265–273.
- Rashid, U., Anwar, F., Ashraf, M., Saleem, M., & Yusup, S. (2011). Application of response surface methodology for optimizing transesterification of Moringa oleifera oil: Biodiesel production. *Energy Conversion and Management* 52(8-9): 3034–3042.

- Rashid, U., Anwar, F., & Knothe, G. (2011). Biodiesel from Milo (*Thespesia populnea* L.) seed oil. *Biomass and Bioenergy* 35(9): 4034–4039.
- Rashid, U., Anwar, F., Moser, B. R., & Ashraf, S. (2008). Production of sunflower oil methyl esters by optimized alkali-catalyzed methanolysis. *Biomass and Bioenergy* 32: 1202–1205.
- Rashid, U., Ibrahim, M., Yasin, S., Yunus, R., Taufiq-Yap, Y. H., & Knothe, G. (2013). Biodiesel from *Citrus reticulata* (mandarin orange) seed oil, a potential non-food feedstock. *Industrial Crops and Products* 45: 355–359.
- Rashid, U., Knothe, G., Yunus, R., & Evangelista, R. L. (2014). Kapok oil methyl esters. *Biomass and Bioenergy* 66: 419–425.
- Saka, S., & Kusdiana, D. (2001). Biodiesel fuel from rapeseed oil as prepared in supercritical methanol. *Fuel* 80: 225–231.
- Saka, S., Kusdiana, D., & Minami, E. (2006). Non-catalytic biodiesel fuel production with supercritical methanol technologies. *Journal of Scientific and Industrial Research* 65: 420–425.
- Samniang, A., Tipachan, C., & Kajorncheappun-ngam, S. (2014). Comparison of biodiesel production from crude *Jatropha* oil and Krating oil by supercritical methanol transesterification. *Renewable Energy* 68: 351–355.
- Sharma, Y. C., & Singh, B. (2009). Development of biodiesel: Current scenario. *Renewable and Sustainable Energy Reviews* 13: 1646–1651.
- Sharma, Y. C., & Singh, B. (2010). An ideal feedstock, kusum (*Schleichera triguga*) for preparation of biodiesel: Optimization of parameters. *Fuel* 89(7): 1470–1474.
- Shikha, K., & Rita, C. Y. (2012). Biodiesel production from non edible-oils: A review. *Journal of Chemical and Pharmaceutical Research* 4(9): 4219–4230.
- Shin, H. Y., Lee, S. H., Ryu, J. H., & Bae, S. Y. (2012). Biodiesel production from waste lard using supercritical methanol. *Journal of Supercritical Fluids* 61: 134–138.
- Shirini, F., Mamaghani, M., & Seddighi, M. (2013). Sulfonated rice husk ash (RHA-SO<sub>3</sub>H): A highly powerful and efficient solid acid catalyst for the chemoselective preparation and deprotection of 1,1-diacetates. *Catalysis Communications* 36: 31–37.
- Shu, Q., Gao, J., Liao, Y., & Wang, J. (2011). Reaction kinetics of biodiesel synthesis from waste oil using a carbon-based solid acid catalyst. *Chinese Journal of Chemical Engineering* 19(1): 163–168.
- Shu, Q., Gao, J., Nawaz, Z., Liao, Y., Wang, D., & Wang, J. (2010). Synthesis of biodiesel from waste vegetable oil with large amounts of free fatty acids using a carbon-based solid acid catalyst. *Applied Energy* 87(8): 2589–2596.
- Shu, Q., Nawaz, Z., Gao, J., Liao, Y., Zhang, Q., Wang, D., & Wang, J. (2010). Synthesis of biodiesel from a model waste oil feedstock using a carbon-based solid acid catalyst: Reaction and separation. *Bioresource Technology* 101(14): 5374–5384.

- Shu, Q., Zhang, Q., Xu, G., Nawaz, Z., Wang, D., & Wang, J. (2009). Synthesis of biodiesel from cottonseed oil and methanol using a carbon-based solid acid catalyst. *Fuel Processing Technology* 90(7-8): 1002–1008.
- Silva, G. F., Camargo, F. L., & Ferreira, A. L. O. (2011). Application of response surface methodology for optimization of biodiesel production by transesterification of soybean oil with ethanol. *Fuel Processing Technology* 92(3): 407–413.
- Srilatha, K., Prabhavathi Devi, B. L. A., Lingaiah, N., Prasad, R. B. N., & Sai Prasad, P. S. (2012). Biodiesel production from used cooking oil by two-step heterogeneous catalyzed process. *Bioresource Technology* 119: 306–311.
- Szybist, J. P., Song, J., Alam, M., & Boehman, A. L. (2007). Biodiesel combustion, emissions and emission control. *Fuel Processing Technology* 88(7): 679–691.
- Takagaki, A., Toda, M., Okamura, M., Kondo, J. N., Hayashi, S., Domen, K., & Hara, M. (2006). Esterification of higher fatty acids by a novel strong solid acid. *Catalysis Today* 116: 157–161.
- Tan, K. T., Gui, M. M., Lee, K. T., & Mohamed, A. R. (2010). An optimized study of methanol and ethanol in supercritical alcohol technology for biodiesel production. *Journal of Supercritical Fluids* 53(1-3): 82–87.
- Tariq, M., Ali, S., Ahmad, F., Ahmad, M., Zafar, M., Khalid, N., & Khan, M. A. (2011). Identification, FT-IR, NMR (1H and 13C) and GC/MS studies of fatty acid methyl esters in biodiesel from rocket seed oil. *Fuel Processing Technology* 92(3): 336–341.
- Tashtoush, G., Al-Widyan, M. I., & Al-Shyoukh, A. O. (2003). Combustion performance and emissions of ethyl ester of a waste vegetable oil in a water-cooled furnace. *Applied Thermal Engineering* 23(3): 285–293.
- Taufiq-Yap, Y. H., Lee, H. V., Hussein, M. Z., & Yunus, R. (2011). Calcium-based mixed oxide catalysts for methanolysis of *Jatropha curcas* oil to biodiesel. *Biomass and Bioenergy* 35(2): 827–834.
- Taufiq-Yap, Y. H., Lee, H. V., Yunus, R., & Juan, J. C. (2011). Transesterification of non-edible *Jatropha curcas* oil to biodiesel using binary Ca-Mg mixed oxide catalyst: Effect of stoichiometric composition. *Chemical Engineering Journal* 178: 342–347.
- Thanh, L. T., Okitsu, K., Sadanaga, Y., Takenaka, N., Maeda, Y., & Bandow, H. (2010). A two-step continuous ultrasound assisted production of biodiesel fuel from waste cooking oils: A practical and economical approach to produce high quality biodiesel fuel. *Bioresource Technology* 101(14): 5394–5401.
- Tomasevic, A. V., & Siler-Marinkovic, S. S. (2003). Methanolysis of used frying oil. *Fuel Processing Technology* 81(1): 1–6.
- Trakarnpruk, W. (2012). Biodiesel Production from Palm Fatty Acids Distillate Using Tungstophosphoric Acid- and Cs-salt Immobilized-Silica. *Walailak J Sci & Tech* 9(1): 37–47.
- Uzun, B. B., Kiliç, M., Özbay, N., Pütün, A. E., & Pütün, E. (2012). Biodiesel production from waste frying oils: Optimization of reaction parameters and



- determination of fuel properties. *Energy* 44: 347–351.
- Van Manh, D., Chen, Y. H., Chang, C. C., Chang, M. C., & Chang, C. Y. (2011). Biodiesel production from Tung oil and blended oil via ultrasonic transesterification process. *Journal of the Taiwan Institute of Chemical Engineers* 42(4): 640–644.
- Varma, R. S. (2001). Solvent-free accelerated organic syntheses using microwaves. *Pure and Applied Chemistry* 73: 193–198.
- Veljković, V. B., Avramović, J. M., & Stamenković, O. S. (2012). Biodiesel production by ultrasound-assisted transesterification: State of the art and the perspectives. *Renewable and Sustainable Energy Reviews* 16: 1193–1209.
- Walas, S. M. (1985). *Phase Equilibria in Chemical Engineering*. Butterworth: Boston.
- Wan Omar, W. N. N., & Amin, N. A. S. (2011). Biodiesel production from waste cooking oil over alkaline modified zirconia catalyst. *Fuel Processing Technology* 92(12): 2397–2405.
- Wang, B., Li, S., Tian, S., Feng, R., & Meng, Y. (2013). A new solid base catalyst for the transesterification of rapeseed oil to biodiesel with methanol. *Fuel* 104: 698–703.
- Wang, C., Hu, Y., Chen, Q., Lv, C., & Jia, S. (2013). Bio-oil upgrading by reactive distillation using p-toluene sulfonic acid catalyst loaded on biomass activated carbon. *Biomass and Bioenergy*, 56, 405–411.
- Xue, J., Grift, T. E., & Hansen, A. C. (2011). Effect of biodiesel on engine performances and emissions. *Renewable and Sustainable Energy Reviews* 15(2): 1098–1116.
- Yaakob, Z., Sukarman, I. S. Bin, Narayanan, B., Abdullah, S. R. S., & Ismail, M. (2012). Utilization of palm empty fruit bunch for the production of biodiesel from *Jatropha curcas* oil. *Bioresource Technology* 104: 695–700.
- Yamaguchi, D., Kitano, M., Suganuma, S., Nakajima, K., Kato, H., & Hara, M. (2009). Hydrolysis of cellulose by a solid acid catalyst under optimal reaction conditions. *Journal of Physical Chemistry C* 113: 3181–3188.
- Ye, B., Qiu, F., Sun, C., Li, Y., & Yang, D. (2014). Transesterification of Soybean Oil to Biodiesel in a Microwave-Assisted Heterogeneous Catalytic System. *Chemical Engineering and Technology* 37(2): 283–292.
- Yee, K. F., Wu, J. C. S., & Lee, K. T. (2011). A green catalyst for biodiesel production from *jatropha* oil: Optimization study. *Biomass and Bioenergy* 35(5): 1739–1746.
- Yu, C. W., Bari, S., & Ameen, A. (2002). A comparison of combustion characteristics of waste cooking oil with diesel as fuel in a direct injection diesel engine. *Proceedings of the Institution of Mechanical Engineers, Part D: Journal of Automobile Engineering* 216 (3): 237–243.
- Yujaroen, D., Goto, M., Sasaki, M., & Shotipruk, A. (2009). Esterification of palm fatty acid distillate (PFAD) in supercritical methanol: Effect of hydrolysis on reaction reactivity. *Fuel* 88(10): 2011–2016.

- Zain, F. N. A. S. M. 2015. Industri sawit pemangkin ekonomi negara. pp. 11: Berita Harian.
- Zhang, J., Wang, K., Guo, S., Wang, S., Liang, Z., Chen, Z., Xu, Q. (2014). One-step carbonization synthesis of hollow carbon nanococoons with multimodal pores and their enhanced electrochemical performance for supercapacitors. *ACS Applied Materials and Interfaces* 6(3): 2192–2198.
- Zhang, X., Su, F., Song, D., An, S., Lu, B., & Guo, Y. (2015). Applied Catalysis B : Environmental Preparation of efficient and recoverable organosulfonic acid functionalized alkyl-bridged organosilica nanotubes for esterification and transesterification 163: 50–62.
- Zhao, B., & Collinson, M. M. (2010). Well-Defined Hierarchical Templates for Multimodal Porous Material Fabrication (5): 4312–4319.
- Zhao, J., Yang, L., Li, F., Yu, R., & Jin, C. (2009). Structural evolution in the graphitization process of activated carbon by high-pressure sintering. *Carbon* 47(3): 744–751.
- Zheng, M., Mulenga, M. C., Reader, G. T., Wang, M., Ting, D. S. K., & Tjong, J. (2008). Biodiesel engine performance and emissions in low temperature combustion. *Fuel* 87(6): 714–722.
- Zong, M.-H., Duan, Z.-Q., Lou, W.-Y., Smith, T. J., & Wu, H. (2007). Preparation of a sugar catalyst and its use for highly efficient production of biodiesel. *Green Chemistry* 9: 434-437.

## BIODATA OF STUDENT

The name is Mohd Lokman Ibrahim, was born on 25<sup>th</sup> June 1986 in Machang, Kelantan. He had completed primary education at SK Manek Urai Baru, Kuala Krai, Kelantan from 1993 to 1998. Completed high school at SMK Seri Intan, Machang, Kelantan on 2003. He graduated from matriculation education at Kolej MARA Kulim, Kedah in 2005 and furthers his 3 years first degree in Bachelor of Science majoring in Chemistry at Universiti Teknologi Malaysia (UTM) and graduated on 2008. He continued his Degree of Masters in Chemistry at Department of Chemistry Faculty of Science, UTM under supervision of the late Prof. Dr. Alias Mohd Yusof and graduated in 2011. He got 2 years experience working as the research officer in Institute of Pharmaceutical & Nutraceutical Malaysia (IPHARM), Pulau Pinang. Then, he pursued his Doctor of Philosophy in Catalysis at Catalysis Science & Technology Research Centre (PutraCAT), Department of Chemistry, Faculty of Science under supervision of Prof Dr. Taufiq Yap Yun Hin. His Ph.D study has been supported by Universiti Teknologi MARA and Malaysia's Ministry of Higher Education. He experienced with two-month attachment studies at Prof Motonobu Goto's Laboratory, Department of Chemical Engineering, University of Nagoya, Japan. His contribution in research has received recognition when his research papers were accepted and published in high impact factor journal.

## LIST OF PUBLICATIONS

### A. Publication:

- Ibrahim M. Lokman, Umer Rashid, Robiah Yunus, and Yun Hin Taufiq-Yap.** (2014). Carbohydrate-derived Solid Acid Catalysts for Biodiesel Production from Low-Cost Feedstocks: A Review. *Catalysis Reviews: Science and Engineering*, **56**: 187–219. (Impact factor: 8.471, Q1). <http://dx.doi.org/10.1080/01614940.2014.891842>
- Ibrahim M. Lokman, Umer Rashid, Yun Hin Taufiq-Yap.** (2015). Meso- and macroporous sulfonated starch solid acid catalyst for esterification of palm fatty acid distillate. *Arabian Journal of Chemistry*. xx:xxx-xxx. (Impact factor: 3.725, Q1). <http://dx.doi.org/10.1016/j.arabjc.2015.06.034>
- Ibrahim M. Lokman, Umer rashid, Yun Hin Taufiq-Yap.** (2015). Production of Biodiesel from Palm Fatty Acid Distillate using Sulphonated-Glucose Solid Acid Catalyst: Characterization and Optimization. *Chinese Journal of Chemical Engineering*. **23**: 1857-1864. (Impact factor: 1.2, Q3). <http://dx.doi.org/10.1016/j.cjche.2015.07.028>
- Ibrahim M. Lokman, Umer Rashid, Yun Hin Taufiq-Yap, Robiah Yunus.** (2015). Methyl ester production from palm fatty acid distillate using sulfonated-glucose derived solid acid catalyst. *Renewable Energy*. **81**: 347-354. (Impact factor: 3.374, Q1). <http://dx.doi.org/10.1016/j.renene.2015.03.045>
- Ibrahim M. Lokman, Umer Rashid, Zulkarnain Zainal, Yun Hin Taufiq-Yap.** (2014). Microwave-assisted biodiesel production by esterification of palm fatty acid distillate. *Journal of Oleo Science*. **63**(9): 849-855. (Impact factor: 1.242, Q3). <http://dx.doi.org/10.5650/jos.ess14068>
- Ibrahim M. Lokman, Umer Rashid, Yun Hin Taufiq-Yap.** (2015). Microwave-assisted Methyl Ester Production from Palm Fatty Acid Distillate over Heterogeneous Carbon-based Solid Acid Catalyst. *Chemical Engineering Technology*. **38**: 1837-1844 (Impact factor: 2.442, Q1). <http://dx.doi.org/10.1002/ceat.201500265>
- Ibrahim M. Lokman, Motonobu Goto, Umer Rashid, Yun Hin Taufiq-Yap.** (2016). Sub- and supercritical esterification of palm fatty acid distillate with carbohydrate-derived solid acid catalyst. *Chemical Engineering Journal*. **284**: 872-878. (Impact factor: 4.321, Q1). <http://dx.doi.org/10.1016/j.cej.2015.08.102>

## **B. Paper Presented at Conference:**

**Ibrahim M. Lokman, Saman A.F., Umer Rashid, Taufiq-Yap, Y.H.** Quality evaluation of methyl ester derived from palm fatty acid distillate. The 6<sup>th</sup> Basic Science International Conference. Malang, Indonesia. 2-3 March 2016.

**Ibrahim M. Lokman, Umer Rashid, Taufiq-Yap, Y.H.** Methanolysis of palm fatty acid distillate (PFAD) using starch-derived solid acid catalyst: Optimization process of reaction parameters Malaysia International Conference on Oils and Fats 2014. Hotel Bangi-Putrajaya. August 20-21, 2014.

**Ibrahim M. Lokman, Umer Rashid, Taufiq-Yap, Y.H.** Synthesis of Glucose-Derived Solid Acid Catalyst for Production of Biodiesel from Palm Fatty Acid Distillate. The Seventh Jordan International Chemical Engineering (JiChE 07) Conference. 4th to 6th November 2014. Amman, Jordan.

**Ibrahim M. Lokman, Umer Rashid, Taufiq-Yap, Y.H.** Low-cost biodiesel production from palm fatty acid distillate (PFAD) using glucose-derived solid acid catalyst: Optimization process of reaction parameters. International Symposium on EcoTopia Science. Nagoya Universiti, Nagoya, Japan. December 13-15, 2013.

## **C. Award:**

**Silver Medal, PRPI 14, Pameran Rekacipta, Penyelidikan dan Inovasi 2014, Universiti Putra Malaysia. (Ibrahim M. Lokman, Umer Rashid, Taufiq-Yap, Y.H.)** Research entitled: Solvothermal Technology for Biodiesel Production.

## **D. List of Seminar and Workshop Attended:**

Workshop on Advanced Materials and Nanotechnology 2015 (WAMN 2015), 4 – 5<sup>th</sup> November 2015, Institute of Advanced Technology, UPM.

Surface Science and Catalysts Characterization Workshop, 23-24 September 2014, Bangunan Pentadbiran, UPM.

Advanced Materials Characterization by Multitechnique XPS. Universiti Kebangsaan, Malaysia (2013).

Carnival Science & Innovation Activities (North Zone). Year of National Science and Innovation (2012). Universiti Teknologi MARA, Kedah, Malaysia.

Agilent LC1260 Fluorescence Detector Basic Hardware and Software Operation, Intitute Pharmaceutical and Nutraceutical Malaysia (2011).

Ph.D Research Methodology. Institute Leadership & Quality Management Universiti Teknologi MARA (2011).

Occupational of Economic Commercialization Development ± Good Laboratory Practice (OECD-GLP). Institute Pharmaceutical & Nutraceutical Malaysia (2011).

