



UNIVERSITI PUTRA MALAYSIA

**PREPARATION OF SOLID HETEROGENEOUS CATALYSTS FOR
BIODIESEL PRODUCTION FROM PALM-BASED FEEDSTOCK**

THEAM KOK LEONG

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BIODIESEL PRODUCTION FROM PALM-BASED FEEDSTOCK**

By

THEAM KOK LEONG

**Thesis Submitted to School of Graduate Studies, Universiti Putra Malaysia, in
Fulfilment of the Requirements for the Degree of Doctor of Philosophy**

April 2015

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Especially Dedicated To

My Dearest Father & Mother

**Theam Lam Seng
Wong Yoke Ngoh**

My Beloved Wife

Lim Ai Sun

My Cute Daughters

**Theam Yu Xuan
Theam Yu Tong**

***Without whose love and continued
support, this thesis would not have
been possible***

Abstract of the thesis presented to the Senate of Universiti Putra Malaysia in fulfilment of the requirement for the degree of Doctor of Philosophy

PREPARATION OF SOLID HETEROGENEOUS CATALYSTS FOR BIODIESEL PRODUCTION FROM PALM-BASED FEEDSTOCK

By

THEAM KOK LEONG

April, 2015

Chairman: Professor Taufiq Yap Yun Hin, PhD
Faculty: Science

Palm fatty acid distillate (PFAD) and palm stearin (PS) are side products from physical refining of crude palm oil, and it can be a good alternative feedstock for biodiesel production. In this study, PS and PFAD were chemically converted into biodiesel using solid base and acid catalysts. The reaction parameters of the catalytic reaction were thoroughly investigated and optimized via Response Surface Methodology. The optimal values of these factors were found to be related to the chemical and physical properties of the feedstock. Four catalysts were synthesized and used to produce biodiesel and these were (i) nanoscale calcium methoxide (CMS), (ii) zirconia supported calcium methoxide (CMSS), (iii) sulfated zirconia (SZ) and, (iv) ball-milled sucrose-derived carbon acid catalyst (S400M). CMS catalyst possesses a novel morphology due to the sonication treatment during preparation of the catalyst. The nanoscale particles gave a high surface area which may provide more active sites for reactants to anchor and react. The results showed that CMS has excellent basicity and high catalytic ability as a heterogeneous solid base catalyst. This catalyst gave 94.7 % of biodiesel yield within 3 hours at temperature of 70°C, methanol molar ratio and catalyst loading of 6 and 1 wt% of PS, respectively. Besides, CMSS catalyst gave the highest biodiesel yield of 98 % at temperature of 70°C, reaction time of 125 min, using 3 % catalyst loading and methanol to PS molar ratio of 11:1. Furthermore, the recycling experiment results showed it had a longer catalyst lifespan, and the zirconia support had proven to be the good stabilizing agent to the calcium methoxide catalyst. This catalyst appeared to be a promising candidate to replace the existing homogeneous catalysts for biodiesel production as it requires short reaction time with high reusability. Moreover, SZ has been extensively studied and optimized as catalyst for the esterification of free fatty acid in PFAD with methanol. The effect of sonication on the phase structure and its catalytic activity was investigated. TPD-NH₃ coupled with mass spectrometer analysis revealed that the first thermal desorption peak of SZ represented the actual acidity of the catalyst. SZ catalyst exhibited a good catalytic performance as a heterogeneous solid acid catalyst which used to esterify PFAD and 97 % of free fatty acid (FFA) conversion was achieved with 2 hours of reaction time, despite its low surface area. A noticeable deactivation of catalyst has been experimentally detected under the optimized reaction conditions. The characterization results showed that the deactivation is due to the leaching of sulfate groups from the catalyst. Furthermore, the other heterogeneous solid acid catalyst i.e. S400M was prepared in the present study which aims to improve the esterification process and reduce the generation of waste from biodiesel production. The experimental results showed that S400M exhibited

good catalytic activity in the esterification of PFAD, providing maximum FFA conversion of 94% at optimum parameters. The good catalytic activity of the aforementioned catalyst in the biodiesel reaction could be attributed to the presence of optimal number of catalytically active acid site density on its surface. The mechanochemical treatment was the good tool to improve the catalytic activity of carbon catalyst by adding extra active sites for esterification of FFA and to intensify the acid strength of the catalyst.



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PENYEDIAAN PEPEJAL PEMANGKIN HEREROGEN UNTUK PENGHASILAN BIODIESEL DARI BAHAN SUAPAN BERASASKAN SAWIT

Oleh

THEAM KOK LEONG

April, 2015

Pengerusi: Profesor Taufiq Yap Yun Hin, PhD
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Asid lemak sawit sulingan (PFAD) dan stearin sawit (PS) adalah produk sampingan daripada penapisan fizikal minyak sawit mentah dan ia boleh menjadi bahan mentah alternatif yang baik untuk penghasilan biodiesel. Dalam kajian ini, PS dan PFAD telah ditukar secara kimia kepada biodiesel dengan menggunakan pemangkin pepejal alkali and asid. Faktor-faktor yang berkait dengan tindak balas pemangkinan telah dikaji dengan teliti dan dioptimumkan melalui Kaedah Respon Permukaan. Nilai yang optimum untuk faktor-faktor ini didapati berkaitan dengan sifat-sifat kimia dan fizikal bahan mentah. Empat pemangkin telah dihasilkan dan digunakan untuk menghasilkan biodiesel dan ini adalah (i) kalsium methoxide dalam saiz nanometer (CMS), (ii) kalsium methoxide disokong oleh zirkonia (CMSS), (iii) zirkonia yang bersulfat (SZ) dan, (iv) pemangkin asid karbon yang dikisar (S400M). Pemangkin CMS memiliki morfologi yang khas disebabkan rawatan sonikasi semasa penyediaan pemangkin tersebut. Zarah nano memberikan kawasan luas permukaan yang tinggi dan ia boleh menyediakan tapak-tapak yang aktif untuk bahan mentah bertindak balas. Hasil kajian ini menunjukkan bahawa CMS sangat beralkali ia boleh digunakan sebagai pemangkin pepejal alkali. Pemangkin ini memberikan 94.7% hasil biodiesel dalam tempoh 3 jam pada suhu 70 °C, nisbah mol methanol kepada PS 6:1 dan 1 % mangkin dari berat PS. Selain itu, pemangkin CMSS memberikan hasil biodiesel yang tertinggi iaitu 98% pada suhu 70C, masa tindak balas 125 min dengan menggunakan 3% pemangkin dan nisbah mol metanol kepada PS 11:1. Seterusnya, keputusan eksperimen kitar semula menunjukkan ia mempunyai jangka hayat yang lebih panjang dan sokongan zirkonia telah membuktikan untuk menjadi agen yang baik untuk menstabilkan pemangkin kalsium methoxide. Pemangkin ini muncul sebagai pengganti yang berpotensi kepada pemangkin homogen yang sedia ada dalam penghasilan biodiesel disebabkan ia memerlukan masa tindak balas yang singkat dan penggunaan semula yang tinggi. Selain itu, SZ telah dikaji dan dioptimumkan sebagai pemangkin dalam penukaran asid lemak bebas dalam PFAD kepada biodiesel. Kesan sonikasi pada struktur fasa pemangkin dan aktivitinya yang telah dikaji. Analisis TPD-NH₃ dengan jisim spektrometer mendedahkan bahawa puncak penyaherapan terma pertama untuk SZ mewakili keasidan sebenar pemangkin tersebut. SZ menunjukkan kemampuan pemangkinan yang baik dalam penukaran PFAD kepada biodiesel sebanyak 97%. Pertukaran tersebut dicapai dengan masa tindak balas selama 2 jam, walaupun luas permukaan BET yang rendah. Penyahaktifan pemangkin telah dikesan di bawah keadaan optimum tindak balas. Keputusan analysis menunjukkan bahawa

penyahaktifan tersebut disebabkan oleh pelarutan kumpulan sulfat dari pemangkin. Tambahan pula, heterogen asid pemangkin pepejal iaitu S400M telah disediakan dalam kajian ini yang bertujuan untuk meningkatkan hasil pengesteran dan mengurangkan penghasilan sisa-sisa daripada pembuatan biodiesel. Keputusan eksperimen menunjukkan bahawa S400M merupakan pemangkin yang mempunyai aktiviti yang tinggi dalam penukaran PFAD kepada biodiesel sebanyak 94 % pada parameter optimum. Aktiviti yang tinggi pada pemangkin ini dalam tindakbalas penghasilan biodiesel boleh dikaitkan dengan kehadiran tapak aktif asid yang berketumpatan tinggi pada permukaannya. Rawatan pengisaran adalah teknik yang baik untuk meningkatkan aktiviti pemangkin karbon pemangkin dengan menambah tapak aktif untuk penukaran FFA dan meningkatkan kekuatan asid pemangkin.



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LIST OF ABBREVIATIONS

AAS	Atomic Absorption Spectroscopy
ANOVA	Analysis of variance
BET	Brunauer Emmer Teller
CCD	Central Composite Design
CMS	Calcium methoxide
CMSS	Calcium methoxide with support
FAME	Fatty acid methyl ester
FESEM	Field Emission Scanning Electron Microscopy
FFA	Free fatty acid
FWHM	Full-Width at Half Maximum
GC	Gas Chromatography
JCPDS	Joint Committee on Powder Diffraction Standards
OVAT	One-Variable-At-A-Time
PFAD	Palm fatty acid distillate
PS	Palm stearin
RSM	Response Surface Methodology
SZ	Sulfated Zirconia
T_{max}	Temperature at peak maximum
TCD	Thermal Conductivity Detector
TPD	Temperature Programmed Desorption
XRD	X-ray Diffraction

CHAPTER 1

INTRODUCTION

1.1 Global Energy Demand

Fossil fuels play an important role on worldwide energy production. As the population growth and industrialization increases, the demand for utilization of energy increases speedily. It causes fossil fuel's resources decreasing and consequent in increasing the price of fossil fuels. Hence, The World Energy Forum predicted that fossil oil will be exhausted in less than 10 decades, if new oil wells are not found (Sharma & Singh, 2009). Besides that, environmental pollution problems have become alarming rate due to the extensive usage of fossil fuels. Therefore, the development of alternative sources to fossil fuels, specifically petroleum-based is required to fulfill the energy demand throughout the world. Renewable energy has gained most focus recently due to its potential to replace fossil fuel, particularly for transportation. Renewable energy from biomass has been successfully developed and used worldwide to reduce the use of fossil fuels. Furthermore, based on the study of International Energy Agency (IEA), only energy produced from renewable sources and waste has the highest potential to replace fossil-fuel energy among other renewable resources as shown in Figure 1.1 (International Energy Agency, 2013)

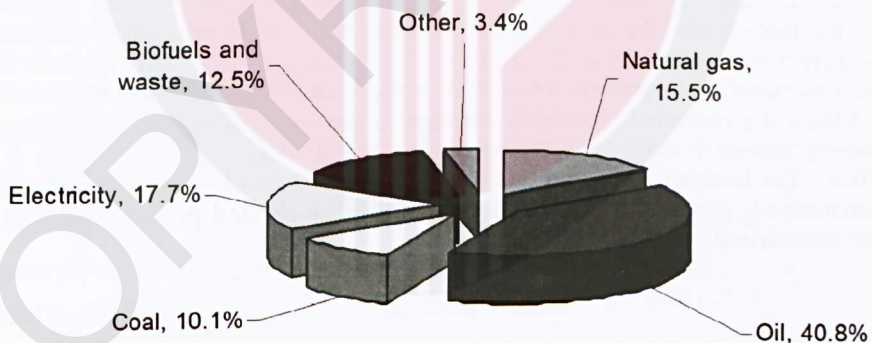


Figure 1.1. World total energy consumption by fuel (Mtoe) in Year 2013. Total: 8,918 million tonnes of oil equivalent (Mtoe). (International Energy Agency, 2013)

The increasing awareness of the depletion of fossil-fuel resources and greenhouse-gas emissions from the fuel combustion has become the main concern to many countries all around the world (Zabeti *et al.*, 2009). Many researchers have started to utilize lipids from biomass to supply power usage because of the gradual increases in the price of petroleum, limited resources of fossil oils and environmental concerns (Laksmono *et al.*, 2013; Sharma *et al.*, 2010; Taufiq-Yap *et al.*, 2011). The environmental benefits of biodiesel have made it more and more attractive in this recent moment. Biodiesel is defined as non-petroleum-based diesel fuel, which is derived from the fats and oils of biomass and used as combusting fuel to generate power in ordinary diesel engines (Agarwal, 2007). The animal fats and vegetable oils belong to lipids, which are the essential products of metabolism of living things, functioning as energy storage. Yet, there are many problems dealt with using the oil and fat from living organism in diesel engines, such as the large molecular size of triglycerides, high viscosity and low combustion efficiency. All of these can be solved if the oils and fats are chemically modified to biodiesel, which has the similar properties with petroleum-based diesel (Murugesan *et al.*, 2009; Wang *et al.*, 2006).

1.2 Biodiesel

The term biodiesel is defined as a fuel comprised of mono-alkyl esters of long chain fatty acids derived from oils or fats of living organism, recognized as B100 in biodiesel standard ASTM D6751, and referring to fatty acid methyl esters (FAME) in European biodiesel standard EN 14214. Furthermore, the prefix “bio” can be related to the biodegradable characteristic of the biodiesel fuel (Gerhard, 2009). Biodiesel is a clear amber yellow liquid with a viscosity similar to that of petroleum diesel. Biodiesel is non-flammable and, in contrast to petroleum diesel, is non-explosive, with a flash point at 150 °C for biodiesel as compared to 187 °C for petroleum diesel (Ma *et al.*, 1998). The fatty acid composition of the triglyceride used in biodiesel production has a significant influence on the physical and chemical properties of biodiesel. Depending on the feedstock of the production, the final product would have slight variation in properties due to the fatty acids’ identities. In the transesterification, triglycerides react with methanol in the presence of catalyst in which ultimately leads to the formation of FAME and glycerol as by-products. Methanol is used as the alcohol for the production, mainly because it is the least-expensive alcohol and widely available (Knothe *et al.*, 2004). The common fatty acid that found in some feedstocks that used in biodiesel production is shown in Table 1.1. In Table 1.2, some physical properties of biodiesel are summarized.

Table 1.1 : The chemical structures of common fatty acids (Lin *et al.*, 2010)

Fatty acid	Chemical structure
Lauric (12 : 0)	$\text{CH}_3(\text{CH}_2)_{10}\text{COOH}$
Myristic (14 : 0)	$\text{CH}_3(\text{CH}_2)_{12}\text{COOH}$
Palmitic (16 : 0)	$\text{CH}_3(\text{CH}_2)_{14}\text{COOH}$
Stearic (18 : 0)	$\text{CH}_3(\text{CH}_2)_{16}\text{COOH}$
Oleic (18 : 1)	$\text{CH}_3(\text{CH}_2)_7\text{CH}=\text{CH}(\text{CH}_2)_7\text{COOH}$
Linoleic (18 : 2)	$\text{CH}_3(\text{CH}_2)_4\text{CH}=\text{CHCH}_2\text{CH}=\text{CH}(\text{CH}_2)_7\text{COOH}$
Linolenic (18 : 3)	$\text{CH}_3\text{CH}_2\text{CH}=\text{CHCH}_2\text{CH}=\text{CHCH}_2\text{CH}=\text{CH}(\text{CH}_2)_7\text{COOH}$
Arachidic (20 : 0)	$\text{CH}_3(\text{CH}_2)_{18}\text{COOH}$
Behenic (22 : 0)	$\text{CH}_3(\text{CH}_2)_{20}\text{COOH}$
Erucic (22 : 1)	$\text{CH}_3(\text{CH}_2)_7\text{CH}=\text{CH}(\text{CH}_2)_{11}\text{COOH}$

Table 1.2 : Physical properties of biodiesel (Demirbas, 2009)

Common name	Biodiesel
Common chemical name	Fatty acid (m)ethyl ester
Chemical formula range	$\text{C}_{14}\text{-C}_{24}$ methyl esters or $\text{C}_{15}\text{-}_{25}\text{H}_{28\text{-}48}\text{O}_2$
Kinematic viscosity range (mm ² /s, at 40°C)	3.3 - 5.2
Density range (kg/m ³ , at 15 °C)	860 - 894
Boiling point range (°C)	> 184
Flash point range (°C)	147 - 177
Distillation range (°C)	197 - 327
Vapour pressure (mm Hg, at 22°C)	< 5
Solubility in water	Insoluble in water
Physical appearance	Light to dark yellow, clear liquid
Odour	Light musty or soapy odour
Biodegradability	More degradable than petroleum diesel
Reactivity	Stable, but avoid strong oxidising agents

1.3 Sources of Biodiesel

Triglyceride which is basically a triester is the major lipid form of energy storage in most living creatures, consisting of a glycerol molecule (triol) esterified with three fatty acid molecules (carboxylic acids with a long hydrocarbon chain). The different types of triglycerides arise from various types of the esterified fatty acids. Fatty acids are generally categorized into two main classes, which are saturated (no C = C) and unsaturated (C = C). Different fatty acids contain distinct numbers of C = C double bonds and number of carbon atoms in their hydrocarbon chain. Therefore, after transesterification in biodiesel production, the biodiesel contains a variety of fatty acid alkyl esters with different hydrocarbon chains, depending on the source of triglycerides used. Other than triglycerides, other compounds contained in natural oils and fats include pigments, waxes, sterols, glycolipids, lipoproteins, hydrocarbons, long chain alcohols, carbohydrates, vitamins (A, D, E and K) in minor concentrations and free fatty acids (Lotero *et al.*, 2005).

Renewable in nature and in environmental friendly ways leads to virgin vegetable oils become most popular as feedstock for the biodiesel synthesis. There are two main categories of vegetable oils, which are edible and non-edible. Edible vegetable oils like canola, soybean, rapeseed, sunflower and corn have been used for biodiesel production and found to be good as a diesel substitute. The non-edible vegetables such as madhuca indica, Jatropha curcas and Pongamia pinnata have also found to be suitable (Tapanes, Gomes, Mesquita & Ceva, 2008).

In order to prevent competition between food and fuel, palm fatty acid distillate is an inedible side product from physical refining of crude palm oil, and it will be a good alternative feedstock for biodiesel production. It exists in solid form at room temperature and it contains high levels of free fatty acid (>82%) compared to its counter parts. However, only 4% of palm fatty acid distillate was estimated for each production of crude palm oil (Top, 2010). The main fatty acid components in palm fatty acid distillate (PFAD) included palmitic acid (C16:0), oleic acid (C18:1), linoleic acid (C18:2), lauric acid (C12:0), and myristic acid (C14:0) (Chongkhong *et al.*, 2007; Mongkolbovornkij *et al.*, 2010). Figure 1.2 shows the fatty composition of PFAD.

Due to the high cost of feedstock, palm stearin (PS) may become a promising alternative of biodiesel production feedstock. Palm stearin is the solid fraction obtained by fractionation of palm oil after crystallization at a controlled temperature. It is not used directly for edible purposes due to its high melting point ranging from 44 to 56 °C (De Martini Soares *et al.*, 2009; Norizzah *et al.*, 2004; Pantzaris, 2000). The liquid fraction is known as palm olein and more expensive as compared to solid fraction due to its wider usage. The physical characteristics of palm stearin differ significantly from those of palm olein. It contains mainly palmitic acid and other fatty acids (Lai *et al.*, 2000). The high degree of saturation of palm stearin poses problems in the manufacture of edible fats such as margarine and shortening as it confers low plasticity to the end product, thus limiting the commercial exploitation of the material (Lai *et al.*, 2000; Laia *et al.*, 2000). Figure 1.3 shows the fatty acid composition of PS.

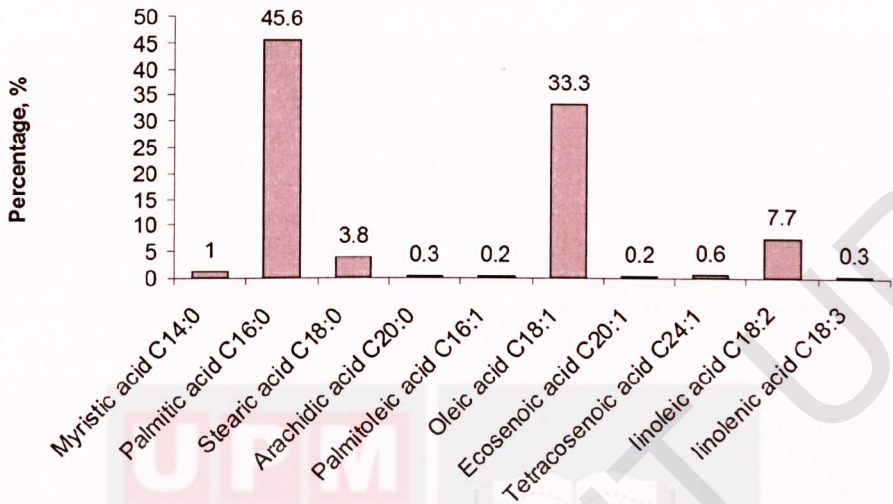


Figure 1.2. Fatty acid composition of palm fatty acid distillate. (Chongkhong et al., 2009)

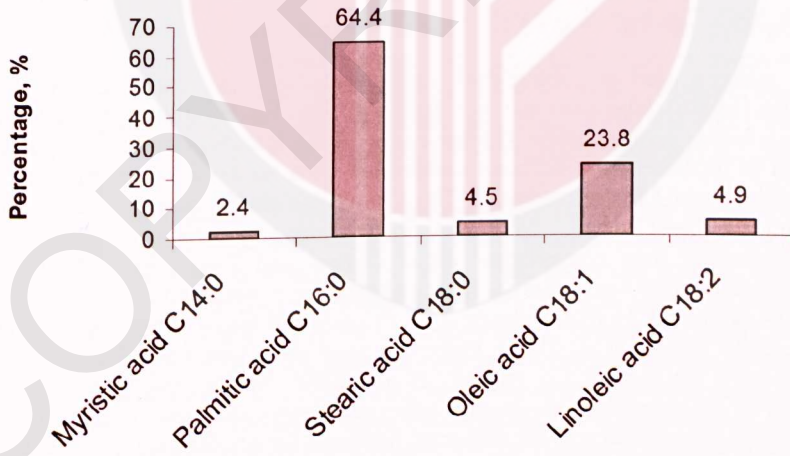


Figure 1.3. Fatty acid composition of palm stearin. (Soares et al., 2009)

1.4 Advantages of Biodiesel Production

The use of biodiesel has attracted huge attention from worldwide countries due to its availability, renewability, non-toxicity, harmless gas emission as well as its biodegradability (Demirbas *et al.*, 2009). The biodiesel synthesized from biomass is biodegradable and has unlimited sources used for synthesis, comparing to the petroleum which is a limited resource. Biodiesel is reported to be highly biodegradable in fresh water and soil medium. About 90-98% of biodiesel is mineralized in 21-28 days under aerobic as well as anaerobic conditions (Leung *et al.*, 2010; Mudge and Pereira, 1999; Sharma *et al.*, 2008). Some authors reported biodiesel-nature fuel blend enhanced the biodegradation rate of diesel fuel and gasoline through cometabolism (Pasqualino *et al.*, 2006; Sharma *et al.*, 2008). This fuel is nontoxic as the raw materials are mainly the vegetable oils and the animal fat.

Moreover, the emission resulted from biodiesel combustion contributes to nearly no harmful effect to the environment since the emission of hazardous gases is significantly reduced (Demirbas *et al.*, 2008). In particular, biodiesel provides significant reductions in particulates and carbon monoxide over petroleum diesel fuel. Furthermore, biodiesel contains virtually trace amount of sulphur, so SO₂ emissions are reduced in direct proportion to the petrol-diesel replacement (Canakci *et al.*, 2009). The oxygen content of biodiesel is 10 – 11% by weight, offering a pathway to recycle carbon dioxide through emission (Lotero *et al.*, 2006). Therefore, air pollution, green house effect and global warming are no longer the problems taken into account power generation by combusting diesel fuel. Instead of using the refined virgin oils, manufacturers also use the waste oils collected from food industries as the lipid feedstock of biodiesel production. Reusing of the waste oils has the benefits of producing environmental-friendly diesel fuel and reducing the amount of waste oil disposal, which leads to water pollution. This is a proper utilization and management of waste oils as combusting fuel (Krawczyk, 1996; Talebian-Kiakalaieh *et al.*, 2013).

The most common used as a diesel-fuel quality factor is cetane number (CN). It is related to the ignition-delay time and combustion quality. Better ignition properties are come from a higher cetane number (Meher *et al.*, 2006). Ramos *et al.* (2009) reported that the CN of biodiesel from different sources has been assumed to ranging from 48 (grape biodiesel) to 61 (palm biodiesel). The CN of biodiesel is generally higher than for conventional diesel due to biodiesel has longer fatty acid carbon chain and more saturated molecules than conventional diesel (Bajpai and Tyagi, 2006; Dermibas, 2005). Some researchers found that the higher percentage of saturated fatty acid methyl ester such as palmitic (C16:0) and stearic (C18:0) acids will lead to a better CN (Bajpai and Tyagi, 2006; Knothe *et al.*, 2003). Therefore, palm methyl ester which rich in these fatty acids gave the highest CN (Ramos *et al.*, 2009). Smoke-opacity percentages during each of the vegetable oils methyl ester were lower than that with petroleum diesel. Besides, it was observed that with pure biodiesel the acceleration time increased by approximately 8 % compared to the normal diesel fuel. (Fontaras *et al.*, 2009). The oxygen content in biodiesel accelerates the combustion process due to the increase of the homogeneity of oxygen with the fuel during combustion and retarded its oxidation potential. Consequently, the combustion efficiency of biodiesel is higher than petroleum diesel (Demirbas, 2007).

1.5 Problem Statement on Biodiesel Production

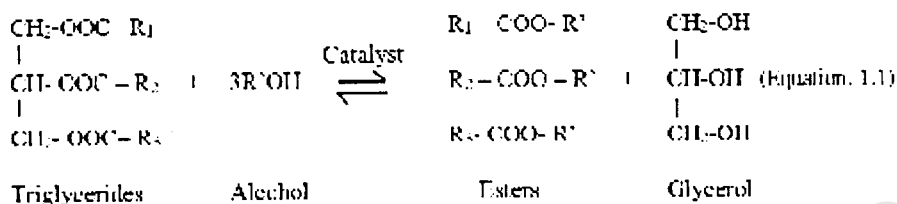
In spite of the advantages of biodiesel stated above, biodiesel has higher cloud point and pour point compared to conventional diesel (Prakash, 1998). Besides that, other disadvantages of biodiesel include its higher viscosity, low energy content, low volatility and injector coking. Furthermore, the biodiesel still has to improve in the future to lower the calorific value, the horsepower output, and its comparatively higher emission of nitrogen oxides (Buyukkaya, 2010). The cost of biodiesel, however, is the main obstacle to commercialization which usually more expensive than petroleum-based diesel fuel from 10 – 50 % (Leung and Guo, 2006). Feedstock costs usually account for 80% of the total cost of the biodiesel production (Demirbas *et al.*, 2008). In order to reduce the cost of raw materials used in biodiesel production, waste oils used for frying food are recycled to be the biodiesel lipid feedstock instead of neat oils. However, the waste oils collected from different restaurants and food industries possess wide ranges of properties, compositions and qualities. Thus, the pre-treatments of waste oils are required to get rid of the impurities and undesired substances which lessen the efficiency of biodiesel production (Yaakob *et al.*, 2013). Furthermore, the line between food and fuel economies is blurred as both fields competing for the same oil resources. In other words, biodiesel is competing with the food industry for limited land availability for the plantation of oil crops (Demirbas, 2008).

Solid heterogeneous catalyst although it can reuse and separate from the reaction mixture, however it has a lower catalytic activity as compared with homogeneous catalyst. Furthermore, solid catalyst also has mass transfer limitation during the catalytic reaction.

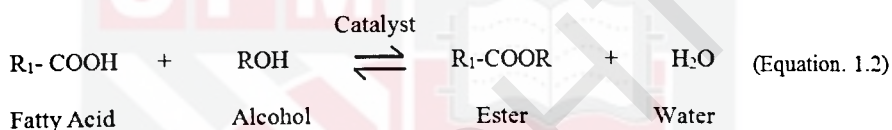
1.6 Synthesis of Biodiesel

Biodiesel can be produced through several pathways, such as pyrolysis, micro emulsion, supercritical methanol method and transesterification of triglycerides and esterification of free fatty acids with alcohols of low molecular weight (Fukuda *et al.*, 2001; Ghoreishi and Moein, 2013; Kusdiana and Saka, 2001; Ma and Hanna, 1999; Schwab *et al.*, 1988; Singh & Singh, 2010; Tan *et al.*, 2010; Warabi *et al.*, 2004).

Transesterification is one of the most commercially compatible methods employed universally to produce biodiesel. Transesterification process is necessary to convert the lipid sources which are oils and fats to much lower molecular species, such as fatty acid methyl esters. A stoichiometry ratio of 3:1 of alcohol to vegetable oils or animal fats is needed for a completion of the transesterification process. Normally, to have an optimum yield of ester from transesterification process, excess alcohol is needed. The present of catalyst usually can enhance the reaction rate and biodiesel yield. Due to the transesterification is a reversible process, excess alcohol is used to shift the equilibrium process to the product side (Ma and Hanna, 1999). Transesterification of triglyceride by using alcohol is shown in the following figure:



Esterification is a chemical reaction involved free fatty acid (FFA) and alcohol as reactants to produce fatty acid alkyl ester and water with the present of acid catalyst (Zhang *et al.*, 2003). The one-step reaction of esterification of FFA is reported to be faster than transesterification of triglycerides as the latter reaction involved multi-steps reaction to form ester (Warabi *et al.*, 2004). The esterification reaction is shown in the following equation:



Among all the alcohol used in synthesizing the biodiesel; methanol and ethanol are the most commonly, especially the methanol. This is because methanol consists of suitable physico-chemical properties, low cost, mild reaction conditions and easy phase separation. Apart from that, higher and secondary alcohols is a good pouring characteristics of their fatty esters at low temperature, however, high price and expensive reaction conditions make these reactants unsuitable for biodiesel production (Leung *et al.*, 2010; Stamenković *et al.*, 2011).

1.7 Objectives

The major objectives of this research study are as followings:

- i. To prepare four solid heterogeneous catalysts and characterize these catalysts using X-ray Diffraction (XRD), Brunauer-Emmett-Teller (BET) surface area measurement, Field Emission Scanning Electron Microscopy (FESEM) and Temperature Programmed Desorption coupled with mass spectrometer.
- ii. To determine the effect of various parameters to the production of biodiesel through transesterification and esterification reaction from palm stearin and palm fatty acid distillate via solid acid and base catalysts..
- iii. To determine the optimum conditions of biodiesel production via Response Surface Methodology (RSM).
- iv. To characterize the optimized biodiesel using acid value test, Atomic Absorption Spectroscopy, CHNS analysis and Gas Chromatography (GC).

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BIODATA OF THE STUDENT

Mr. Theam Kok Leong was born on 4th April 1982 in Kuala Lumpur. He completed his primary and secondary school in SRJK (C) Jinjang Utara and SMK Menjalara, Kepong, Kuala Lumpur. He further completed his form six studies in SMK Maxwell, Kuala Lumpur. He obtained his first degree in Bachelor of Science (Hons.), majoring in Chemistry from Universiti Putra Malaysia, Serdang in the year 2006. He has completed his Master of Science in the field of Catalysis in the same university in 2008. In addition, his PhD course fee was supported by *MyBrain 15* scholarship from Ministry of Education, Malaysia. He is working as a chemistry lecturer since year 2009.



LIST OF PUBLICATIONS

1. **Kok Leong Theam**, Aminul Islam, Yun Hin Taufiq-Yap and Yuen May Choo. Binary metal-doped methoxide catalyst for biodiesel production from palm stearin, *Research on Chemical Intermediates* (2015), DOI 10.1007/s11164-015-2127-x.
2. **Kok Leong Theam**, Aminul Islam, Hwei Voon Lee and Yun Hin Taufiq-Yap. Sucrose-derived catalytic biodiesel synthesis from low cost palm fatty acid distillate, *Process Safety and Environmental Protection* (2015), volume: 95, Page: 126-135.
3. Yun Hin Taufiq-Yap, Hwei Voon Lee, Yin Chang Wong, **Kok Leong Theam** and Wen Jiunn Tang, Effect of different calcination duration on physicochemical properties of vanadium phosphate catalysts, *E-Journal of Chemistry* (2012), volume: 9, Issue: 3, Page: 1440-1448.
4. Y. H. Taufiq-Yap, **K. L. Theam**, G.J. Hutchings, N. Dummer and J. K. Bartley, Effect of Cr, Ni, Fe and Mn dopants on the performance of hydrothermal synthesized vanadium phosphate catalysts for *n*-butane oxidation, *Petroleum Science and Technology* (2010), volume: 28, Issue: 10, Page: 997-1012.
5. Yun Hin Taufiq-Yap and **Kok Leong Theam**, Modification and microstructure study of vanadyl pyrophosphate catalysts synthesized via hydrothermal method, *Proceedings of the Seminar on Science and Technology* (2008), Page: 40-46 (ISBN 978-983-2641-30-8).

List of the seminars/conferences/workshops attended:

1. Seminar on "Small Molecule Single Crystal Diffraction" by Dr. Martin Adam, 17th April 2007, Lecture Hall 207, 2nd Floor, Faculty Science (Participant).
2. Seminar on "Laser Raman Spectroscopy" by Dr. Joel Oswalt, 27th April 2007, Bilik Saintis Gemilang, Faculty Science (Participant).
3. Workshop on "Publishing for Postgraduates", 4-5th June 2007, organised by School of Graduate Studies, Universiti Putra Malaysia, Dewan Persidangan, Center for External Education (Participant).
4. Seminar on "Seminar Sains 2007", 4th August 2007, Dewan Kuliah Akademik Pusat, Universiti Putra Malaysia (Oral presenter).
5. Nobel Laureate Public Lecture-'Investing in the Future' by Nobel Laureate Professor Dr. Ahmed Zewail, 8th August 2007, Exhibition Hall 1, Ground Floor, Kuala Lumpur Convention Centre (KLCC) (Participant).
6. Seminar on "Half-Day Seminar on Oxidation Catalysis", 22th August 2007, Bilik Saintis Gemilang, Faculty of Science (Participant).

7. 12th Asian Chemical Congress (12ACC), 23-25th August 2007, Putra World Trade Centre, Kuala Lumpur, Malaysia (Oral presenter).
8. Seminar on "Short Course in Catalysis", 4-5th December 2007, School of Chemical Sciences, Universiti Sains Malaysia (Participant).
9. Pameran Reka Cipta, Penyelidikan dan Inovasi (PRPI), 27-29th November 2007, Dewan Besar, PKKSSAAS, Universiti Putra Malaysia (Poster presenter).
10. The 6th Asia-Pacific Congress on Catalysis (APCAT-6), 13-17th October 2013, Taipei International Convention Center (TICC), Taiwan (Poster presenter)

