



***MAGNETOHYDRODYNAMICS BOUNDARY LAYER FLOW OF
NON-NEWTONIAN FLUID OVER A PERMEABLE SHRINKING
SURFACE***

RUSYA IRYANTI BINTI YAHAYA

IPM 2019 11



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By

RUSYA IRYANTI BINTI YAHAYA

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,
in Fulfilment of the Requirements for the Degree of Master of Science**

March 2019

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DEDICATIONS

**To my beloved
parents and family.
Thank you for everything.**



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfilment
of the requirement for the degree of Master of Science

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March 2019

Chairman : Norihan Md Arifin, PhD
Institute : Institute For Mathematical Research

Non-Newtonian fluids are fluids whose viscosities cannot be described by Newton's law of viscosity and are dependent on the shear rate. The magnetohydrodynamics (MHD) boundary layer flow of three types of non-Newtonian fluids, namely, the Carreau fluid, Casson fluid and micropolar fluid are studied in this thesis. These fluids flow over a permeable shrinking surface, with different boundary conditions considered for each fluid. The MHD flow of Carreau fluid over a non-linearly shrinking sheet with thermal radiation and convective boundary condition is studied as the first problem. Then, the MHD flow of Casson fluid near a stagnation point on a linearly shrinking sheet is considered as the second problem. The effects of slip and homogeneous-heterogeneous reactions are studied in this problem. Meanwhile, the third problem discussed the effects of thermal radiation on the MHD flow of micropolar fluid over an exponentially shrinking sheet. The governing partial differential equations of these problems are transformed into ordinary differential equations using the similarity transformations. Then, these equations are solved along the boundary conditions using a numerical method called the shooting method, with the computations done in the Maple software. The effects of various parameters on the flow, concentration and thermal fields of the fluids are discussed and presented in tables and graphs. At some values of the parameters, dual solutions are obtained. Therefore, stability analysis is performed to determine the significance of these solutions to the problems. The smallest eigenvalues for the first and second solutions are computed using the bvp4c solver in MATLAB. The first solution is found to have positive smallest eigenvalues, while the second solution has negative smallest eigenvalues. Thus, the first solution is stable and significant, whereas the second solution is unstable and less significant to the problems. The presence of a magnetic field and suction are observed to boost the velocity of the fluids but causes the temperature of

the fluids to drop. Besides that, the increase in these parameters enhances the **concentration of reactants in the second problem and the microrotation of micropolar fluid in the third problem.**



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk ijazah Master Sains

**ALIRAN LAPISAN SEMPADAN MAGNETOHIDRODINAMIK BAGI
BENDALIR BUKAN NEWTONAN TERHADAP PERMUKAAN
TELAP MENGECEUT**

Oleh

RUSYA IRYANTI BINTI YAHAYA

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Bendalir bukan Newtonan ialah bendalir yang mana kelikatannya tidak dapat diperihalkan dengan hukum kelikatan Newton dan bergantung kepada kadar ricih. Aliran lapisan sempadan magnetohidrodinamik (MHD) bagi tiga jenis bendalir bukan Newtonan iaitu bendalir Carreau, bendalir Casson dan bendalir mikropolar telah dikaji di dalam tesis ini. Bendalir-bendalir ini mengalir terhadap permukaan telap mengecut dengan syarat-syarat sempadan yang berbeza bagi setiap bendalir. Aliran MHD bendalir Carreau terhadap helaian mengecut secara tak linear dengan radiasi terma dan syarat sempadan olakan telah dikaji sebagai masalah yang pertama. Kemudian, aliran MHD bendalir Casson berhampiran titik genangan di helaian mengecut secara linear telah dipertimbangkan sebagai masalah yang kedua. Dalam masalah ini, kesan gelincir dan tindak balas homogen-heterogen telah dikaji. Sementara itu, kesan radiasi terma pada aliran MHD bendalir mikropolar terhadap helaian mengecut secara eksponen telah dibincangkan sebagai masalah yang ketiga. Persamaan menakluk bagi masalah-masalah ini yang berbentuk persamaan pembezaan separa telah dijelmakan kepada persamaan pembezaan biasa dengan menggunakan penjelmaan keserupaan. Kemudian, persamaan ini diselesaikan bersama-sama syarat sempadan dengan menggunakan sebuah kaedah berangka yang dipanggil kaedah tembakan dengan pengiraannya dilakukan dalam perisian Maple. Kesan pelbagai parameter terhadap medan aliran, kepekatan dan terma bendalir telah dibincangkan dan ditunjukkan dalam bentuk jadual dan graf. Pada sesetengah nilai parameter, penyelesaian dual diperolehi. Oleh itu, analisis kestabilan telah dilakukan bagi menentukan kepentingan penyelesaian tersebut kepada masalah-masalah ini. Nilai-nilai eigen terkecil bagi penyelesaian pertama dan kedua telah dikira menggunakan solver `bvp4c` di MATLAB. Penyelesaian pertama didapati mempunyai nilai-nilai eigen terkecil positif, sementara penyelesaian kedua mempunyai nilai-nilai eigen terkecil negatif.

Oleh itu, penyelesaian pertama adalah stabil dan penting, manakala penyelesaian kedua adalah tidak stabil dan kurang penting kepada masalah-masalah ini. Kehadiran medan magnet dan sedutan didapati membantu meningkatkan halaju bendalir tetapi menyebabkan suhu bendalir menurun. Selain itu, peningkatan kedua-dua parameter ini telah meningkatkan kepekaan bahan tindak balas dalam masalah kedua dan putaran mikro bendalir mikropolar dalam masalah ketiga.



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This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfilment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

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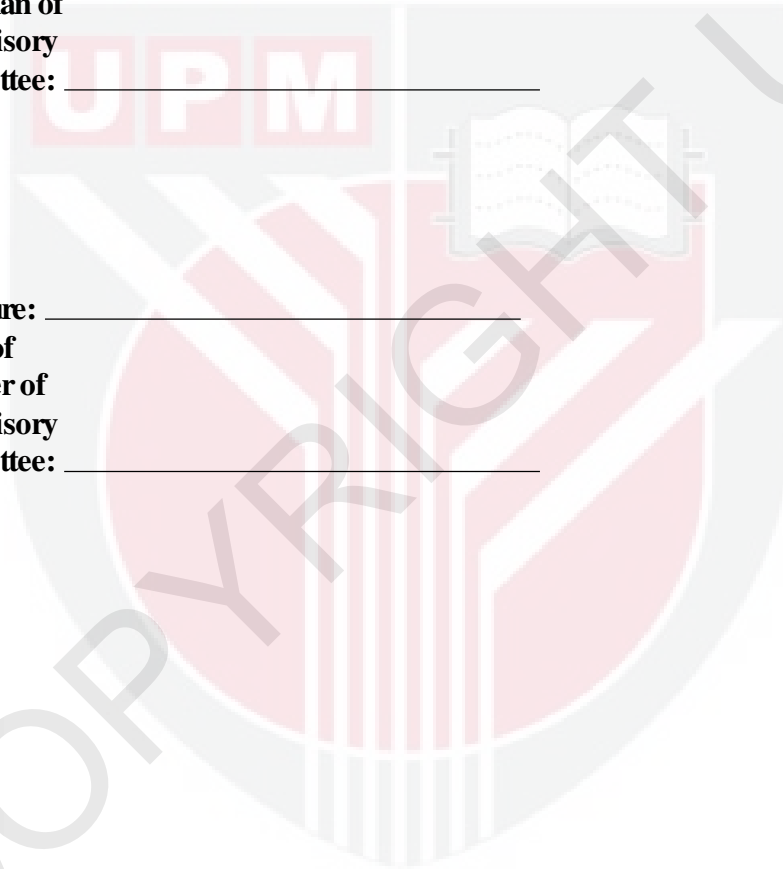


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LIST OF ABBREVIATIONS

MHD	Magnetohydrodynamics
bvp4c	Boundary value problem with fourth-order accuracy
a	Acceleration
a₁ a₂ a^{**} B₀ c v₀	Constants
b r	Constants related to shrinking speed
B	Strength of magnetic field
c_p	Specific heat
C_{r1} C_{r2}	Concentration of chemical species R₁ and R₂, respectively
C_{r0}	Uniform concentration of chemical species R₁
C_f	Local skin friction coefficient
D_{R1} D_{R2}	Diffusion coefficients for chemical species R₁ and R₂, respectively
F[*]	Force
G[*]	Slope
h_f	Convective heat transfer coefficient
j	Microinertia per unit mass
k_c k_s	Rate constants
k[*]	Mean absorption coefficient
K	Strength of homogeneous reaction
K_s	Strength of heterogeneous reaction
K[*]	Material parameter
L	Characteristic length
L[*]	Velocity slip length parameter
m	Mass
m_x	Wall couple stress
M	Magnetic parameter
M_x	Local couple stress
M[*]	Momentum
n	Power law index
n[*]	Constant for concentration of microelements
N	Microrotation or angular velocity
N_R	Radiation parameter
Nu_x	Local Nusselt number
O	Initial point
O[*]	Target point
p	Pressure
p_y	Yield stress
Pr	Prandtl number
q_r	Radiative heat flux
q_w	Wall heat transfer
R	Gas constant
R₁ R₂	Chemical species

R_m	Magnetic Reynolds number
Re	Reynolds number
s	Strength of stagnation flow
S	Suction or mass transfer parameter
Sc	Schmidt number
t	Time
T	Fluid temperature
T_f	Convective fluid temperature
T_w	Temperature of the sheet
T_0	Rate of temperature increment along the sheet
T	Free stream temperature
u, v	Velocity components in x- and y-directions, respectively
u_e	Velocity of external flow
u_w	Variable wall velocity or velocity of the sheet
u_0	Initial velocity
U	Characteristic velocity
v_w	Mass transfer velocity
v^*	Velocity
We	Weissenberg number

Greek symbols

b	Casson parameter
d	Ratio of diffusion coefficients
d_l	Boundary layer thickness
d_t	Thermal boundary layer thickness
h	Similarity variable
G	Material constant called relaxation time
g	Unknown eigenvalue
k	Vortex viscosity
k^*	Thermal conductivity
l	Shrinking parameter
m	Dynamic viscosity
m_B	Plastic dynamic viscosity
m_0	Permeability of free space
n	Kinematic viscosity
pc	Critical value for the product of the component of the deformation rate with itself
y	Stream function
r	Density
s	Electrical conductivity
s^*	Stefan-Boltzmann constant
t	Shear stress
t_w	Wall shear stress

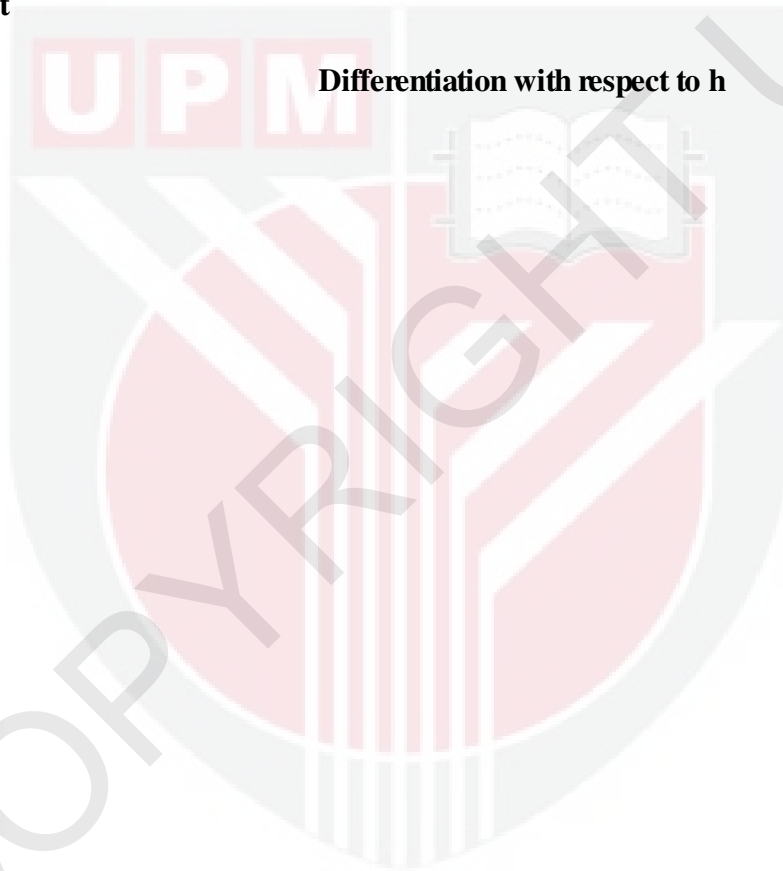
t^*	Dimensionless time variable
q	Dimensionless temperature
q_w	Temperature ratio parameter
u	Velocity slip parameter
j	Biot number
x	Magnetic diffusivity
z	Spin gradient viscosity

Subscript

w	Condition at the wall or surface of the sheet Free stream condition
-----	--

Superscript

0	Differentiation with respect to h
-----	-------------------------------------



CHAPTER 1

INTRODUCTION

This chapter contains the introduction to some of the terms used in this thesis. A brief history and definitions of these terms are given to enhance the understanding of the studied problems.

1.1 Fluid

Fluid is any substance that deforms continuously under applied shear stress. Shear stress is tangential stress that acts along the surface of a body and is defined as the ratio of applied force to the cross-sectional area of the body. The inability of fluid to resist stress no matter how small the amount is, causes the fluid to deform continuously and flow. According to Çengel and Turner (2004), when a fluid is at rest, the only stress that acts towards the surface of the body is the normal stress called pressure. The supporting walls of the fluid, for example, a liquid container helps to eliminate the shear stress. When the walls are removed, shear develops and the fluid flows. The examples of fluids are liquids, gases and plasmas.

There are two types of fluid flow namely the laminar flow and the turbulent flow, as illustrated in Figure 1.1 and Figure 1.2 respectively. Laminar flow commonly occurs when a fluid with high viscosity flows slowly in a relatively small channel. In laminar flow, the fluid particles move in an orderly manner and parallel to the wall of the flow channel. The layers of the fluid slide parallel to each other without any disturbance or interference. However, the laminar flow can be transformed into a turbulent flow and vice versa by changing certain conditions, for example, the flow area.

The transition from laminar to turbulent flow was studied by Osborne Reynolds in **1880s. A dimensionless parameter called the Reynolds number was introduced to identify the fluid flow as laminar or turbulent (Barnes, 2000).** The Reynolds number can be defined as the ratio of inertial forces to viscous forces, and it depends on the characteristic length and the properties of the fluid such as the velocity, density, and viscosity. At low Reynolds number, the fluid flow is laminar. However, as the Reynolds number exceeds a certain value, the flow becomes turbulent.

Turbulent flow occurs when a fluid with high velocity flows rapidly through a large diameter channel. The flow is irregular and chaotic as the fluid layers slide past each other randomly and get mixed together. A fluid that is in turbulent flow contains high kinetic energy. Once the energy is dissipated, the flow becomes laminar again.

If the fluid properties of the flow, for example, the velocity, temperature, density and

pressure does not depend on time, the flow is said to be steady. Otherwise, the flow is unsteady. The study on the flow of fluid is called fluid dynamics.

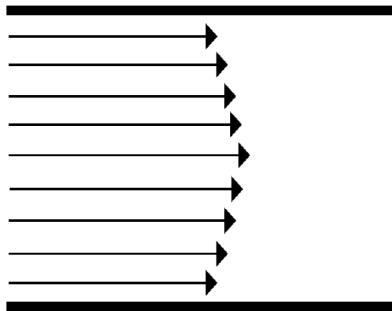


Figure 1.1. Laminar flow

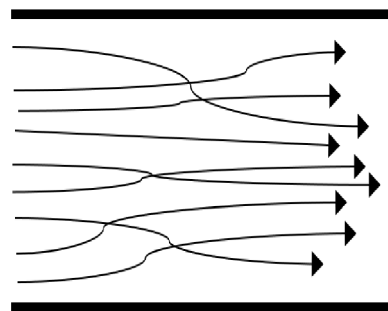


Figure 1.2. Turbulent flow

1.2 Non-Newtonian Fluid

Non-Newtonian fluid is fluid that does not obey Newton's law of viscosity. **Newton's law of viscosity states that the shear stress, τ between adjacent fluid layers is directly proportional to the velocity gradients, dV/dn between the two layers. This relationship can be written as follows:**

$$\tau = \mu \frac{dV}{dn}$$

where the velocity gradient dV/dn represents the shear rate. The ratio of shear stress to shear rate is constant at a given temperature and pressure. The proportionality constant is defined as the coefficient of viscosity, μ and becomes

$$\tau = \mu \left(\frac{dV}{dn} \right)$$

A fluid that obeys this law is known as the Newtonian fluid. The viscosity of the Newtonian fluid is independent of the shear rate and constant under all flow conditions with constant temperature and pressure. The examples of Newtonian fluid are **water and organic solvents.**

On the other hand, the viscosity of non-Newtonian fluid depends on the shear rate **and in some instances, is time-dependent.** According to Levenspiel (2014), there are three classes of non-Newtonian fluids. The first class of non-Newtonian fluids is time-independent fluids or also known as the generalized Newtonian fluids (Chhabra, 2010). For this class of fluids, the shear rate only depends on the shear stress, if and only if the temperature of the fluids remains constant (Collyer, 1973). The main types of fluids that belong to this class are Bingham plastic fluids, pseudoplastic fluids and dilatant fluids. Bingham plastic fluid, for example, toothpaste exhibits yield stress **where an enough shear stress is needed to overcome the yield stress and makes the fluid flow.** Once the fluid flow, it behaves as a Newtonian fluid with the shear rate proportional to the shear stress. Next, the pseudoplastic fluid is also known as shear-

thinning fluid where the apparent viscosity of this fluid decreases with increasing shear rate, for example in a paint. Conversely, the dilatant fluid is known as shear-thickening fluid where the apparent viscosity of this fluid increases with increasing shear rate, for example in a quicksand.

The next class of non-Newtonian fluid is time-dependent fluids where the behaviour depends on the history of treatment of the fluids. This class of fluids is divided into two subgroups, namely the thixotropic fluids and the rheopectic fluids. At a constant shear rate, the viscosity of a thixotropic fluid decreases with time while for rheopectic fluid, the viscosity increases with time. The examples for the thixotropic fluid are drilling fluids and printing inks while for the rheopectic fluid is bentonite clay.

Finally, the third class of non-Newtonian fluid is viscoelastic fluids. According to Irgens (2014), viscoelastic materials can be classified either as solids or fluids. The reason is that the materials exhibit both the elastic properties of solids and the flow behaviour of fluids. These fluids will deform and flow when subjected to stress. Examples of viscoelastic fluids are gels and bitumen.

In this thesis, the modelled fluids in the problems are Carreau fluid, Casson fluid and micropolar fluid. Carreau fluid and Casson fluid are time-independent non-Newtonian fluids. Carreau fluid has the behaviour of Newtonian fluid at a low shear rate and as power-law fluid at a high shear rate. Power-law fluid is characterized by the power-law index, n . At $n = 1$, the fluid has the behaviour of a Newtonian fluid, when $n < 1$, the fluid behaves as shear-thinning fluid and when $n > 1$, the fluid behaves as shear-thickening fluid. Meanwhile, Casson fluid is a shear-thinning fluid that exhibits yield stress. The fluid has an infinite viscosity at zero rate of shear, no flow occurs below the yield stress and zero viscosity at an infinite rate of shear. As for micropolar fluid, it is a class of non-Newtonian fluids described by the micropolar theories. Lukaszewicz (1999) stated that micropolar fluid is fluid with microstructures. The microstructures have their own internal angular momentum that is independent of the fluid motion.

1.3 Boundary Layer

A boundary layer is a thin layer of viscous fluid, formed near the surface of an object that is in contact with the moving stream of a fluid. Boundary layer theory was first introduced by Ludwig Prandtl, in a paper titled "On the Motion of a Fluid with Very Small Viscosity". This paper was first presented at the Third International Congress of Mathematicians in 1904 at Heidelberg and then published in the year after (Tani, 1977). Generally, this paper is concerned with the flow and behaviour of a fluid with small viscosity near the wall of a solid boundary. It was found that the smaller the viscosity, the thinner the boundary layer.

The formation of the boundary layer is as illustrated in Figure 1.3. In this figure, a fluid is assumed to flow with an initial velocity, u_0 towards a stationary solid boundary located along the x-axis. As the fluid flows, the fluid molecules adjacent to the solid boundary adheres to the solid surface and becomes stationary, provided that a no-slip condition is assumed. This occurs due to the frictional force between the solid surface and the fluid. The viscosity or the resistance of fluid towards flow causes the fluid molecules near the solid surface to slow down as it collides with the stationary fluid molecules attached on the surface of the solid boundary. The velocity of the fluid decreases and this effect persisted throughout the region near the solid boundary. At some distance, the flow of the fluid is not affected by the collisions anymore. This region is known as the free stream region where the effect of viscosity is negligible, and the fluid velocity is the same as the initial velocity, u_0 . Meanwhile, the region at which the velocity gradient ranges from zero to 99% of the free stream velocity is known as the boundary layer. The thickness of the boundary layer is given by δ_l .

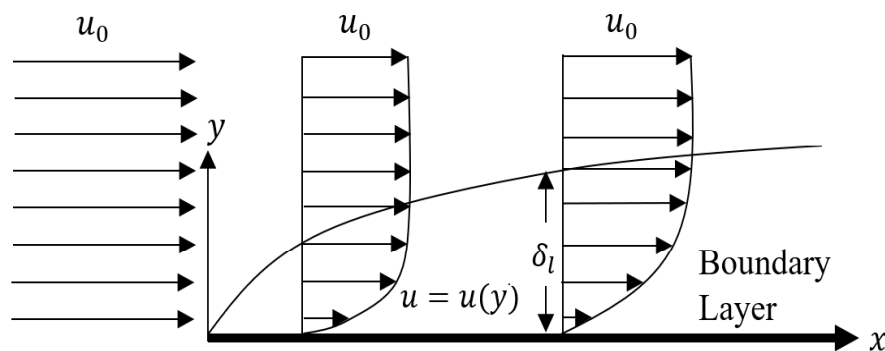


Figure 1.3. The formation of boundary layer

In Figure 1.4, the formation of the thermal boundary layer is shown. Now, the fluid is assumed to flow with a temperature of T , while the solid boundary has a temperature of T_w . Since the temperature $T_w < T$, heat is transferred from the solid surface to the fluid and causes the fluid temperature to increase. This effect persists throughout the fluid layers due to heat transfer. However, the farther the fluid layer from the solid surface, the smaller the amount of heat transferred to the layer. Thus, at some distance from the solid boundary, the temperature of the fluid does not change and is equal to the free stream temperature, T . Therefore, the thermal boundary layer can be defined as the region from the solid surface to the point at which the temperature is 99% of the free stream temperature. The thickness of the thermal boundary layer is given by δ_t .

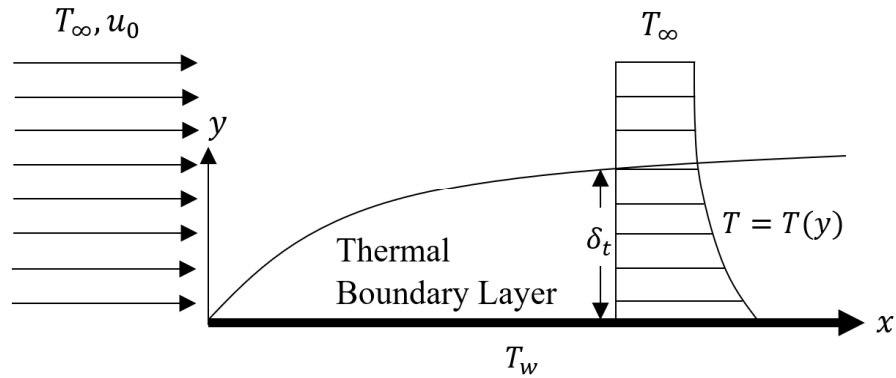


Figure 1.4. The formation of thermal boundary layer

1.4 Stagnation Point

Stagnation point exists on the surface of a solid boundary. At the stagnation point, the fluid flow is brought to rest by the solid boundary which causes the fluid velocity to become zero. Besides that, the pressure, heat transfer and mass deposition rates are said to be the highest at this point (Wang, 2008). According to Drazin and Riley (2006), the stagnation point is the point where the fluid stream attaches to or separates from the solid boundary. As a steady viscous fluid with a velocity of \mathbf{u}_e flows towards a stationary solid boundary, the fluid stream then hits a point on the surface of the boundary and is brought to rest by it. This point is known as the stagnation point. The fluid then divides about the stagnation streamline, as shown in Figure 1.5. Above the stagnation streamline, the fluid flows to the higher region of the solid boundary while below the stagnation streamline, the fluid flows to the lower region of the solid boundary. The flow of fluid near the stagnation point is called the stagnation point flow (Batchelor, 2000).

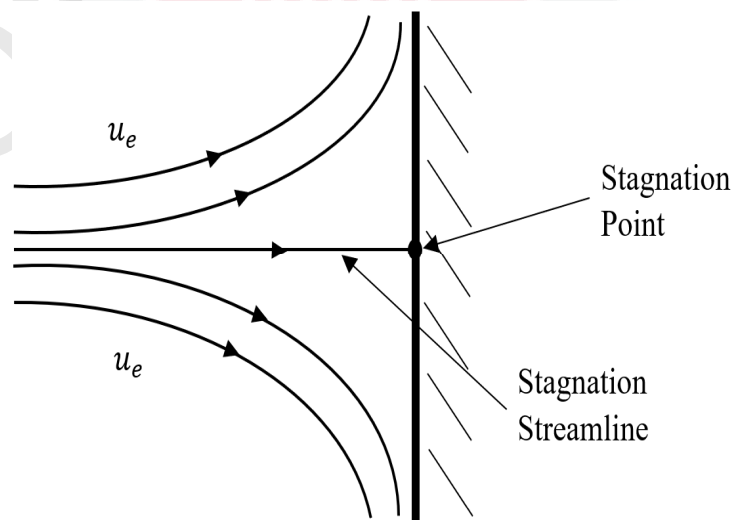


Figure 1.5. Stagnation point

1.5 Types of Effects

In the study of boundary layer flow, various types of effects such as magnetohydrodynamics, thermal radiation, chemical reactions and slip are considered. The influence of these effects on the flow, thermal and concentration fields of the fluids can be analysed by introducing these effects into the governing equations or boundary conditions of the flow problem. Some of the effects considered in this thesis are magnetohydrodynamics, thermal radiation, homogeneous-heterogeneous reactions and slip. A brief explanation about these effects is given in the following subsections.

1.5.1 Magnetohydrodynamics

Magnetohydrodynamics (MHD) studies the flow of an electrically conducting fluid in the presence of a magnetic field. According to Roberts (1967), MHD is also known as hydromagnetics or magneto-fluid dynamics. The study on MHD flow was established during the late 1930s or early 1940s. In 1942, an important finding called the Alfvén wave was made, which led to the growth of MHD. According to Cramer (2001), this finding proved that electromagnetic waves can propagate in conducting fluids. Some of the examples on the applications of MHD are in thermonuclear fusion, electromagnetic pump and electromagnetic stirring.

In MHD, the flow of conducting fluid across the magnetic field creates a potential difference that causes electric currents to flow. According to Davidson (2001), the induced electric currents will give rise to a second magnetic field called the induced magnetic field. Then, this leads to the change such that the fluid appears to ‘drag’ the magnetic field lines along with it. Besides that, the interaction will also give rise to Lorentz forces that inhibit the relative movement of the magnetic field and the fluid.

One of the important dimensionless parameter in MHD is the magnetic Reynolds number, R_m which can be defined as

$$R_m = \frac{UL}{\nu_m} = UL\eta_0 s$$

where U is the characteristic velocity, L is the characteristic length and $\nu_m = \frac{1}{\eta_0 s}$ is the magnetic diffusivity with η_0 as the permeability of free space and s as the electrical conductivity. The magnetic Reynolds number gives an estimation of the relative effects of magnetic induction to magnetic diffusion. If R_m is very large, then the diffusion of the magnetic field can be neglected. The magnetic field lines become ‘frozen’ into the conducting fluid and move along with the fluid. Meanwhile, when R_m is very small, the magnetic induction can be neglected as the magnetic diffusion dominates over the induction of the magnetic field.

1.5.2 Heat Transfer

Heat is a form of energy that can be transferred from one medium to another, provided that there is a temperature difference between the mediums. The heat energy is transferred from a medium with a higher temperature to the ones with a lower temperature. This process continues until an equilibrium is achieved within these mediums. As an example, consider a situation where a warm drink is placed in a refrigerator, the warm drink then cools down. The reason is that heat from the warm drink is transferred to the cold surroundings of the refrigerator. The transfer of heat continues until both mediums reach the same temperature.

The study on the exchange of heat energy between mediums that occurs due to a temperature difference is known as the heat transfer. The rate of heat transfer is defined as the amount of heat being transferred per unit time, and it depends on the magnitude of the temperature gradient. The temperature gradient or the rate of change of temperature is the difference in temperature per unit length. The increase in temperature gradient will increase the rate of heat transfer.

Heat can be transferred from one medium to another by conduction, convection and radiation. Conduction takes place in solids and fluids. In conduction, the transfer of energy occurs within a substance or across substances which are in physical contact. The energy is transferred from the more energetic particles to the less energetic particles through the particles interaction. In fluids, conduction may occur through collisions and diffusions of the molecules during the random motion. Whereas in solids, conduction occurs through the vibrations of the molecules and the energy transported by the free electrons. The rate of heat conduction depends on the temperature difference between the mediums. Besides that, it also depends on the geometry of the medium, for example, the thickness and the material of the medium.

The next mode of heat transfer is convection, which involves both solids and fluids. In convection, the transfer of energy occurs between a solid surface and an adjacent moving fluid through the bulk motion of the fluid. As an example, consider a cold air blown towards a hot block. First, the heat is transferred from the surface of the block to the adjacent air layer through conduction. Then, convection occurs within the air where the heated air near the surface moves up while the cold air sinks down. Thus, both the effects of conduction and fluid motion are involved in convection. The faster the fluid motion, the higher the rate of convection heat transfer. If the fluid is not in motion or static, then the only form of heat transfer between the fluid and the solid surface is conduction. Besides that, the heat transfer within a fluid that causes phase change is also considered as convection, for example, boiling that involves the transition from a liquid phase to the gas phase. There are two types of convection which are free convection and forced convection. Free convection or natural convection is solely due to the density difference caused by the temperature difference in the fluid. The hot and less dense fluid moves up while the cold and

denser fluid moves down, and this brings about the bulk fluid movement. If the fluid movement is due to external force, for example, from fan, pump, wind or compressor, then the convection is called forced convection. The combination of free convection and forced convection which significantly and simultaneously contribute to the heat transfer is called mixed convection (Dawood et al., 2015).

Radiation is the energy that is emitted by a matter in the form of electromagnetic waves or photons. The emission occurs due to the molecular and atomic agitation associated with the internal energy of the matter (Siegel and Howell, 1992). Radiation that is related to heat transfer and temperature is known as thermal radiation. Thermal radiation can occur through solids and fluids. Any matter with a temperature above absolute zero emits thermal radiation. The absence of medium does not hinder thermal radiation because the photons which transport the emitted energy can travel through a vacuum. The importance of thermal radiation is for solar energy technologies and combustion chamber.

Finally, all modes of heat transfer can occur in a fluid, but not all can happen simultaneously. A static fluid may have heat transfer through conduction and radiation while a moving fluid may have convection and radiation. Thus, convection and conduction may occur in fluid but not simultaneously.

1.5.3 Homogeneous-Heterogeneous Reactions

Any chemical reactions with reactants and products that are in the same phase (solid, liquid or gaseous) are known as homogeneous reaction, for example, the reaction between liquids. In fluid flow, this reaction usually occurs in the bulk of the fluid. Meanwhile, a heterogeneous reaction is any chemical reactions with different phases of reactants, such as the reaction between solid and liquid, and also the reaction on catalytic surfaces. In fluid flow over a solid boundary, the heterogeneous reaction usually occurs at the surface of the solid boundary.

1.5.4 Slip Boundary Condition

No-slip and slip boundary conditions are commonly considered in the flow velocity of a fluid. In the case of no-slip boundary condition or also known as the no-velocity-offset boundary condition, the fluid layer that is in contact with the solid boundary is assumed to have equal velocity as the boundary (Rapp, 2017). Thus, the relative movement between the boundary and the fluid layer is zero. However, there is relative movement between the boundary and the fluid layer in the slip boundary condition, or also known as the velocity-offset boundary condition. Therefore, the velocity of the fluid layer is unequal to the boundary. The slip boundary condition

can be written as:

$$u_w = L^* \left. \frac{u}{y} \right|_w$$

where L^* is the slip length which describes the hypothetical distance inside the boundary at which the flow velocity would reach the velocity of the boundary, as shown in Figure 1.6.

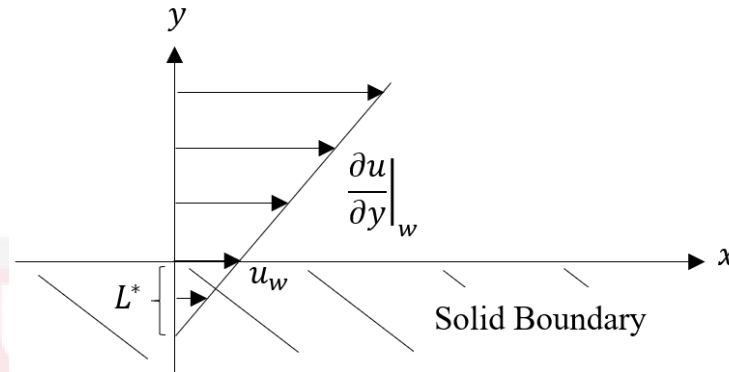


Figure 1.6. Slip boundary condition

1.6 Shrinking Surface

In 1961, Sakiadis (1961a) did a study on the boundary layer flow due to a moving continuous solid surface. This flow usually occurred in the manufacturing of polymer sheet where the sheet is being issued continuously from a slit. In this process, the sheet is sometimes stretched to obtain the desired thickness, and this process needs to be controlled. In the study by Sakiadis (1961b), the continuous surface was considered to move with a constant velocity of $u_w = u_0$. In addition, the surface can also be considered moving with a variable velocity, $u_w = u_w(x)$. The variable wall velocity can also be called the stretching or shrinking wall velocity, depending on the sign of $u_w(x)$. The sign of $u_w(x)$ is positive for stretching surface while negative for shrinking surface.

The first study on fluid flow towards a contracting or shrinking surface was by Wang (1990). Then, Miklavčič and Wang (2006) considered the flow over a shrinking sheet where the sheet velocity is towards a fixed point. In this study, the vorticity of the shrinking sheet is found to be unconfined within the boundary layer. Therefore, the flow on a shrinking sheet is unlikely to exist, unless an adequate amount of suction is imposed on the surface of the sheet. The imposition of suction causes the fluid near the sheet to be sucked out through the sheet surface. Thus, the sheet surface must be porous or permeable to enable suction.

1.7 Stability Analysis

Stability analysis is a method used in determining the stability of solutions. In a problem with more than one solution, stability analysis is carried out to identify which solutions are stable and unstable. The stable solution is physically meaningful and realisable in practice, while the unstable solution is insignificant to the problem.

Stability analysis was first performed by Merkin (1986). In the study, two solutions were obtained and divided into the upper branch solution and the lower branch solution. Before conducting the stability analysis, the problem was first considered as an unsteady problem or also known as the time-dependent problem. Then, a linear eigenvalue problem was introduced, with g as the unknown eigenvalue. The smallest value of g was computed using numerical computation. The results revealed that the upper branch solutions had positive values of g , while the lower branch solutions had negative values of g . A conclusion was made that the upper branch solution was stable while the lower branch solution was unstable.

Therefore, stability analysis is important especially for problems with more than one solution. This analysis helps to identify the stable solution which is significant to the problem.

1.8 Problem Statement

The non-Newtonian fluids have various applications in industrial and engineering processes. Hence, attracts researchers to performed multiple studies on the boundary layer flow of this type of fluids, especially the Carreau fluid, Casson fluid and micropolar fluid. In these studies, a variety of conditions are considered in the fluid flow, for example, the slip effect, suction, thermal radiation, mixed convection and convective boundary condition. However, the following issues are found:

1. Only certain combinations of the conditions are discussed in one s study, for example, the combination of suction and thermal radiation. Other conditions may be overlooked or left out by the researchers for others to study.
2. In consequences, a literature gap is created.

In response to this problem, we will discuss the effects of some of the overlooked conditions to the flow of Carreau fluid, Casson fluid and micropolar fluid, with the hope of filling the existing literature gap. These conditions will be introduced as additional parameters in the governing equations and boundary conditions of the fluids. Then, a numerical method called the shooting method will be used to solve these equations subject to the boundary conditions. In this thesis, stability analysis will be

carried out to determine the stability and significance of the solutions to the problems. Thus, eases the process of choosing a physically meaningful solution, where the effects of the additional parameters on the fluids can be analysed by observing the behaviour of this solution.

1.9 Objectives and Scope of Study

The objective of this thesis is to analyse the mathematical model of non-Newtonian fluid for the following problems:

1. MHD flow of Carreau fluid over a non-linearly shrinking sheet with suction, thermal radiation and convective boundary condition.
2. MHD flow of Casson fluid over a linearly shrinking sheet with slip, suction and homogeneous-heterogeneous reactions.
3. MHD flow of micropolar fluid over an exponentially shrinking sheet with suction and thermal radiation.

The first problem extends the study by Khan et al. (2016b) to the case of a non-linearly shrinking sheet with suction, while the second problem extends the study by Sheikh and Abbas (2017) to the case of MHD flow over a linearly shrinking sheet. In the third problem, the study by Aurangzaib et al. (2016b) is extended to the case of MHD flow over an exponentially shrinking sheet with thermal radiation. In addition, stability analysis will be done in these problems.

The scope of the study is limited to the steady, incompressible and two-dimensional MHD fluid flow over a permeable shrinking sheet. Besides that, the magnetic Reynolds number in each of the problems is assumed to be very small. This assumption is made to neglect the effect of the induced magnetic field.

1.10 Outline of the Thesis

There are seven chapters in this thesis. The first chapter, Chapter 1 is the introduction. In this chapter, some brief definition and history are given for the reader to have a better understanding of the terms used in this thesis. Besides that, the objectives and the thesis outline are also described in the first chapter to provide the reader with some ideas about the thesis.

Chapter 2 comprises the literature reviews related to the studied problems. The previous studies done by other researchers on Carreau fluid, Casson fluid and micropolar

fluid are summarised and discussed in this chapter. Then, the general mathematical formulation of the studied problems and the numerical methods used in these problems are explained in Chapter 3.

Next, Chapter 4 to Chapter 6 present a detailed discussion on the three problems listed in the previous section. Chapter 4 discussed the MHD boundary layer flow of Carreau fluid over a non-linearly shrinking sheet in the presence of thermal radiation, suction and convective boundary condition. Meanwhile, Chapter 5 explained the MHD flow of Casson fluid over a linearly shrinking sheet with slip, suction and homogeneous-heterogeneous reactions. The MHD boundary layer flow of micropolar fluid over an exponentially shrinking sheet with suction and thermal radiation is discussed in Chapter 6. In general, these chapters contain an introduction section, followed by the mathematical analysis and stability analysis sections, the results and discussion section and finally, the conclusions section. The summary of this thesis is made in the last chapter, Chapter 7 and some ideas on the possible future work are included in this chapter.

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