



UNIVERSITI PUTRA MALAYSIA

***EVALUATION OF PERFORMANCE AND FOULING RESISTANCE OF
SANDWICH ULTRAFILTRATION FOR TREATMENT OF FINAL
DISCHARGED PALM OIL MILL EFFLUENT***

NURUL AIN BINTI MAZLAN

FK 2018 166



**EVALUATION OF PERFORMANCE AND FOULING RESISTANCE OF
SANDWICH ULTRAFILTRATION FOR TREATMENT OF FINAL
DISCHARGED PALM OIL MILL EFFLUENT**

By

NURUL AIN BINTI MAZLAN

**Thesis Submitted to the School of Graduate Studies, Universiti Putra
Malaysia, in Fulfilment of the Requirements for the Degree of
Master of Science**

June 2018

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in
fulfilment of the requirement for the degree of Master of Science

**EVALUATION OF PERFORMANCE AND FOULING RESISTANCE OF
SANDWICH ULTRAFILTRATION FOR TREATMENT OF FINAL DISCHARGED
PALM OIL MILL EFFLUENT**

By

NURUL AIN BINTI MAZLAN

June 2018

Chairman : Khairul Faezah Md Yunos, PhD
Faculty : Engineering

Oil palm is the important agriculture industry in Malaysia which consumed hundreds tonnes of water for the proses and 50% of which ends up as effluent. However, water can be sustained and conserved by treating final discharged and recycle back to the plant. Membrane ultrafiltration has been proven a reliable tool in treating wastewater, therefore, it is a promising green technology to treat final discharged from palm oil mill. Thus, this work is carried out to evaluate the effectiveness of ultrafiltration in reclaiming water from final discharged palm oil mill effluent (POME) as well as to investigate the fouling of membrane. Two types of membrane used were polyethersulfone (PES) and regenerated cellulose (RC) of 5kDa and 10 kDa. The first part of this study is to evaluate the effect of parameters that are: pressure (0.5 bar, 1.0 bar, 1.5 bar, 2.0 bar), stirring speed (0 rpm, 400 rpm, 600 rpm, 800 rpm) and pH value (6, 7, 8, 10) on ultrafiltration treatment and fouling resistance. The appropriate filtration condition was recognized and the permeate was further analysed for COD, BOD₅ and suspended solid. Based on the parametric study, selected condition was fixed for the second part to evaluate the effect of sandwich configuration to further improve the final discharged quality and to analyse fouling resistance. Cake layer resistance was found to be dominant for all membranes tested. Two flat membranes were sandwiched together with both effective layer facing up (SS) or the effective layer of the bottom membrane facing down (SB) The results showed of the best permeate quality was achieved with 5 kDa PES membrane at pressure 1.0 bar, 600 rpm and pH 8: the reduction of COD, BOD₅, turbidity, and total dissolved solid were 67.3%, 72.47%, 94.2% and 40% respectively. For sandwich membrane, interestingly, SS-sandwich showed the best permeate

quality with pollutant reduction up to 80-90% (PES 5kDa) compared to 60-70% for single membrane. The quality of permeate from SS-sandwich membrane of 5 kDa was beyond reuse standard and approaching drinking water standard for TSS, TDS and turbidity. Therefore it can be concluded that, with the appropriate arrangement of sandwich membrane and operating condition, water reuse which successfully complies with World Health Organization (WHO) standard can be reclaimed from POME using UF technique



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia
sebagai memenuhi keperluan untuk ijazah Master Sains

**EVALUASI PRESTASI MEMBRANE DAN RINTANGAN KOTORAN
ULTRAFILTRASI SANDWIC SEMASA RAWATAN AIR DARI KILANG
MINYAK KELAPA SAWIT**

Oleh

NURUL AIN BINTI MAZLAN

Jun 2018

**Pengerusi
Fakulti**

**: Khairul Faezah Md Yunos, PhD
: Kejuruteraan**

Minyak kelapa sawit adalah industri terpenting di Malaysia yang menggunakan beratus tan air semasa pemprosesan dan 50% of daripada air yang digunakan menjadi efluen. Membran ultrafiltrasi telah dibuktikan sebagai alat yang dipercayai dalam rawatan air buangan, oleh itu, ia ada teknologi mesra alam yang berpotensi untuk merawat efluen akhir daripada kilang minyak kelapa sawit. Oleh itu, kajian ini dijalankan untuk menilai keberkesanan membran ultrafiltrasi untuk menebus guna air daripada efluen akhir di samping untuk menyiasat rintangan kotoran membran. Dua jenis membran yang digunakan iaitu polyethersulfone (PES) dan regenerated cellulose (RC) bersaiz 5kDa dan 10 kDa. Peringkat pertama kajian ini adalah untuk menilai kesan parameter iaitu: tekanan (0.5 bar, 1.0 bar, 1.5 bar, 2.0 bar), kelajuan aduk (0 rpm, 400 rpm, 600 rpm, 800 rpm) dan pH (6, 7, 8, 10) terhadap rawatan ultrafiltrasi dan rintangan kotoran. Kondisi filtrasi yang wajar di kenal pasti melalui kaedah kajian parameter dan permeat dianalisa lagi untuk COD, BOD₅, dan pepejal terampai. Berdasarkan kajian parametrik, kondisi wajar ditetapkan bagi bahagian kedua untuk mengevaluasi kesan konfigurasi sandwich untuk menambah baik kualiti efluen dan untuk menganalisa rintangan kotoran. Rintangan kotoran kek layer adalah dominan bagi kesemua membran yang diuji. Dua membrane disandwic bersama dengan kedua-dua lapisan efektif mengadap keatas (SS) atau lapisan efektif membran bawah mengadap ke bawah (SB). Hasil kajian menunjukkan kualiti permeat terbaik berjaya diperolehi menggunakan membrane ultrafiltrasi bersaiz 5 kDa pada kondisi 1.0 bar, 600 rpm dan nilai pH 8 dengan pengurangan COD, BOD₅, kekeruhan dan pepejal larut sebanyak 67.3%, 72.47%, 94.2%, dan 40% masing-masing. Bagi membran sandwich, SS-sandwic menunjukkan kualiti permeat terbaik dengan pengurangan bahan pencemar sebanyak 80-90% (PES 5kDa) dibandingkan dengan membran

tunggal iaitu sebanyak 60-70% sahaja. Kualiti permeat yang berjaya mencapai melebihi piawai penggunaan semula air dan menghampiri kualiti piawai air minuman bagi pepejal terampai, pepejal larut dan kekeruhan. Oleh itu, sebagai konklusinya, dengan susunan sandwic dan kondisi operasi yang wajar dan bersesuaian, penggunaan semula air berjaya memenuhi syarat piawai yang ditetapkan oleh organisasi kesihatan dunia (WHO)



ACKNOWLEDGEMENTS

All the praises and thanks be to Allah. This work would not have finished without the help and blessings from Him. Firstly, I would like to express my sincerest gratitude to my supervisor Dr Khairul Faezah bt Md Yunos for the continuous support of my Master study and related research, for her patience, motivation and immense knowledge. Her guidance helped me in the entire research and writing period of this thesis. I would also like to thank my supervisory committee, Dr Azhari Samsu bin Baharuddin and Dr Mohd Nazli Naim, for their insightful comments and encouragement, and also for the challenging questions which motivated me to widen my research from various perspectives.

I also would like to express my thanks to my family especially my parents for providing me with unfailing support and continuous encouragement throughout my years of study and through the process of researching and writing this thesis. Not to forget to all my friends who are always there to support me, especially during the difficult times.

Last but not least, my sincere thanks to all staff and Lab Technicians from Process and Food Engineering Department for their kindness, willingness and cooperation in helping me. This accomplishment would not have been possible without them.

This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfilment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

Khairul Faezah Md Yunos, PhD

Senior Lecturer
Faculty of Engineering
Universiti Putra Malaysia
(Chairman)

Azhari Samsu Baharuddin, PhD

Senior Lecturer
Faculty of Engineering
Universiti Putra Malaysia
(Member)

Mohd Nazli Mohd Naim, PhD

Senior Lecturer
Faculty of Engineering
Universiti Putra Malaysia
(Member)

ROBIAH BINTI YUNUS, PhD

Professor and Dean
School of Graduate Studies
Universiti Putra Malaysia

Date:

Declaration by graduate student

I hereby confirm that:

- this thesis is my original work;
- quotations, illustrations and citations have been duly referenced;
- this thesis has not been submitted previously or concurrently for any other degree at any other institutions;
- intellectual property from the thesis and copyright of thesis are fully-owned by Universiti Putra Malaysia, as according to the Universiti Putra Malaysia (Research) Rules 2012;
- written permission must be obtained from supervisor and the office of Deputy Vice-Chancellor (Research and Innovation) before thesis is published (in the form of written, printed or in electronic form) including books, journals, modules, proceedings, popular writings, seminar papers, manuscripts, posters, reports, lecture notes, learning modules or any other materials as stated in the Universiti Putra Malaysia (Research) Rules 2012;
- there is no plagiarism or data falsification/fabrication in the thesis, and scholarly integrity is upheld as according to the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) and the Universiti Putra Malaysia (Research) Rules 2012. The thesis has undergone plagiarism detection software.

Signature: _____ Date: _____

Name and Matric No.: Nurul Ain Binti Mazlan (GS44721)

Declaration by Members of Supervisory Committee

This is to confirm that:

- the research conducted and the writing of this thesis was under our supervision;
- supervision responsibilities as stated in the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) are adhered to.

Signature: _____
Name of Chairman
of Supervisory
Committee: _____

Signature: _____
Name of Member of
Supervisory
Committee: _____

Signature: _____
Name of Member of
Supervisory
Committee: _____

TABLE OF CONTENTS

	Page
ABSTRACT	i
ABSTRAK	iii
ACKNOWLEDGEMENTS	v
APPROVAL	vi
DECLARATION	viii
LIST OF TABLES	xiii
LIST OF FIGURES	xiv
LIST OF ABBREVIATIONS	xvi
LIST OF NOMENCLATURES	xviii
 CHAPTER	
1 INTRODUCTION	
1.1 Ultrafiltration Membrane	1
1.2 Membrane Fouling	1
1.3 Treatment of POME using membrane	2
1.4 Problem Statement	3
1.5 Objectives of the Research	4
1.6 Scope of Research	4
1.7 Thesis Outline	5
 2 LITERATURE REVIEW	
2.1 Palm oil mill effluent (POME) and its Regulation	7
2.2 POME Treatment	9
2.2.1 Anaerobic and facultative ponds	9
2.2.2 Coagulation and flocculation	11
2.2.3 Membrane Treatment	11
2.3 Membrane Technology in Wastewater Treatment	12
2.3.1 Ultrafiltration Membrane	14
2.3.2 Membrane Materials	15
2.4 Fouling of Ultrafiltration	16
2.4.1 Membrane Fouling Mechanism	17
2.4.2 Effect of Operating Parameters on Membrane Fouling and performance	20
2.4.3 Fouling Resistance-in-series	23
2.5 Modification of Membrane Configuration	24
2.6 Sandwich Membrane	25
2.7 Conclusion	27
 3 MATERIALS AND METHODS / METHODOLOGY	
3.1 Final Discharged from Palm Oil Mill Effluent	28
3.1.1 Characterization of Final Discharged Using FTIR	29
3.2 Characteristics of Ultrafiltration Membrane	29

	3.2.1 Ultrafiltration Membrane Treatment	30
3.3	Experimental Parameters of Ultrafiltration	33
	3.3.1 Sandwich Ultrafiltration Membrane Treatment	35
3.4	Fouling Intensity & Fouling Resistance Model	37
3.5	Analytical method	38
	3.5.1 pH	38
	3.5.2 Suspended Solid	38
	3.5.3 Dissolved solid	39
	3.5.4 Turbidity	39
	3.5.5 Biological oxygen demand (BOD ₅)	40
	3.5.6 Chemical oxygen demand (COD)	41
3.6	Characterization of foul membrane using FESEM	43
4	RESULTS AND DISCUSSION	
	4.1 Characterization of Final Discharged	43
	4.2 Effect of Operating Pressure during Dead-End Ultrafiltration	45
	4.2.1 Effect of Operating Pressure on Permeate Flux	45
	4.2.2 Effect of Operating Pressure on Fouling Resistances and Fouling Intensity	48
	4.2.3 Effect of Operating Pressure on Permeate Quality	51
	4.2.3.1 Total dissolved solid of final discharged after ultrafiltration	51
	4.2.3.2 Turbidity of final discharged after ultrafiltration	52
	4.3 Effect of Stirring Speed during Dead-End Ultrafiltration	53
	4.3.1 Effect of Stirring Speed on Permeate Flux	53
	4.3.2 Effect of Stirring Speed on Fouling Resistance and Fouling Intensity	55
	4.3.3 Effect of Stirring Speed on Permeate Quality	57
	4.3.3.1 Total dissolved solid of final discharged after ultrafiltration	58
	4.3.3.2 Turbidity of final discharged after ultrafiltration	59
	4.4 Effect of pH Value during Dead-End Ultrafiltration	60
	4.4.1 Effect of pH value on permeate flux	60
	4.4.2 Effect of pH value on fouling resistances and fouling intensity	63
	4.4.3 Effect of pH value on permeate quality	64
	4.4.3.1 Total dissolved solid of final discharged after ultrafiltration	64
	4.4.3.2 Turbidity of final discharged after ultrafiltration	66

4.5 Ultrafiltration of POME using sandwich membrane	68
4.5.1 Effect of SS and SB configuration on permeate flux	69
4.5.2 Effect of sandwich configuration on fouling	71
4.5.3 Effect of sandwich configuration on permeate quality	73
5 CONCLUSION AND RECOMMENDATIONS	
5.1 Conclusion	79
5.2 Recommendations for Future Work	80
REFERENCES/BIBLIOGRAPHY	81
APPENDICES	91
BIODATA OF STUDENT	99
LIST OF PUBLICATIONS	100

LIST OF TABLES

Table		Page
2.1	Effluent discharged standards for crude palm oil mills	8
2.2	Size of materials retained, driving force and type of membrane	13
3.1	Characteristics of final discharged	28
3.2	Characteristics of ultrafiltration membrane	31
3.3	Experimental parameters	33
4.1	General assignments of the FTIR spectra of humic acid substance	44
4.2	Comparison of permeate quality of different types of membrane and MWCO	67
4.3	Fouling resistances of different membrane configurations	72
4.4	Comparison of various parameters on quality of treated final discharged after ultrafiltration	76

LIST OF FIGURES

Table		Page
2.1	Flow chart of the palm oil process	8
2.2	POME treatment using ponding treatment system	10
2.3	Operating principle of dead-end mode	13
2.4	Schematic diagrams of the principal types of membranes	15
2.5	Molecular structure of polyethersulfone membrane	15
2.6	Idealised view of fouling, including cake layer, pore blocking and adsorption	17
2.7	Illustration of cake fouling membrane	18
2.8	Illustration of pore blocking fouling membrane	18
2.9	Fouling mechanism during filtration process	19
2.10	Operating principle of cross-flow filtration process	20
2.11	Schematic illustration of UF sandwich configurations	26
3.1	Sample of final discharge	29
3.2	(a)Sample of RC membrane (b) Sample of PES membrane	31
3.3	Ultrafiltration stirred cell set up	32
3.4	Schematic diagram of ultrafiltration stirred batch system	32
3.5	Experimental flowchart	35
3.6	Ultrafiltration membrane configurations: (a) single membrane; (b) SS- sandwich membrane; (c) SB- sandwich membrane	36
3.7	Spectroquant Pharo 100	38
3.8	Senz TDS meter	39
3.9	Turbidimeter HACH 2100AN	39
3.10	The DO procedure	40
3.11	The BOD ₅ procedure	40
3.12	The COD procedure	41
3.13	Field emission scanning electron microscopy	42
4.1	FTIR spectra of samples final discharge of POME	43
4.2	Permeate flux of final discharged at different pressure	45
4.3	Intensity of fouling (%) for the fouled membranes at different pressure	48
4.4	Fouling resistance at different pressure	49
4.5	Different in fouling mechanisms which affect the flux data depending on MWCO	50
4.6	Effect of pressure on dissolved solid after ultrafiltration of final discharged POME	51

4.7	Effect of pressure on turbidity after ultrafiltration of final discharged POME	52
4.8	Permeate flux of final discharged at different stirring speed	53
4.9	Effect of stirring speed on membrane fouling.	56
4.10	Effect of stirred condition on dissolved solid after ultrafiltration of final discharged	58
4.11	Effect of stirred condition on turbidity after ultrafiltration of final discharged	59
4.12	Permeate flux of final discharged at different pH value	61
4.13	Effect of pH value on membrane fouling	63
4.14	Effect of pH value on dissolved solid after ultrafiltration of final discharged POME	65
4.15	Possible particle size at pH 6 and pH 10.13. The left loose structure larger particle size represents for pH 6 and the right dense structure with smaller particle size represents for pH 10.1	65
4.16	Effect of pH value on turbidity after ultrafiltration of final discharged POME	66
4.17	Permeate flux of different sandwich configurations	69
4.18	Fouling resistance of sandwich SS-configuration and SB-configuration of top and bottom membrane of different types of membrane.	71
4.19	Comparison of dissolved solid concentration in permeate after ultrafiltration of final discharged in different configuration.	73
4.20	Comparison of turbidity of permeate after ultrafiltration of final discharged in different configuration.	74
4.21	SEM images of cleaned and fouled membrane	77

LIST OF ABBREVIATIONS

AFM	Atomic Force Microscopy
BOD	Biological Oxygen Demand
CA	Cellulose Acetate
CFV	Cross Flow Velocity
COD	Chemical Oxygen Demand
CP	Concentration Polarization
CSLM	Confocal Scanning Laser Microscopy
DO	Dissolved Oxygen
DOE	Department of Environment
FESEM	Field Emission Scanning Electron Microscopy
MF	Microfiltration
MPOB	Malaysian Palm Oil Board
MPOC	Malaysian Palm Oil Council
MWCO	Molecular weight cut off
NF	Nanofiltration
NOM	Natural Organic Matter
PAC	Palm Kernell Shell-Activated Carbon
PAN	Polyacrylonitrile
PES	Polyethersulfone
POME	Palm oil mill effluent
PS	Polysulfone
PTFE	Polytetrafluoroethylene
RC	Regenerated Cellulose

RO	Reverse Osmosis
RO	Reverse Osmosis
TDS	Total Dissolved Solid
TMP	Transmembrane Pressure
TOC	Total Organic Carbon



LIST OF NOMECLATURES

CH_4	Methane
J	Flux
R_m	Membrane Resistance
R_c	Cake Resistance
R_p	Pore Resistance
NTU	Turbidity



CHAPTER 1

INTRODUCTION

This chapter contains a brief description on ultrafiltration membrane, fouling development of membrane and an overview of application of ultrafiltration membrane in treating final discharged from palm oil mill effluent (POME). Besides, problem statement, objectives and scope of this research were included in this chapter.

1.1 Ultrafiltration Membrane

Membrane is a material which one type of substance can pass more readily than other, this permits the separation of components from water. The implementation of membrane technology in reclamation and reuse of wastewater from industrial plant has grown steadily with rapid growth of human population along with fast industries development caused water scarcity problem become more severe throughout the year (Choi et al., 2005). The main advantage of membrane technology are: compact process and plant, separation based on size exclusion, water quality independent of feed water quality, constant production, easy automation and absence of bacterial regrowth, (Xia et al., 2005). Ultrafiltration (UF) membrane processes appear to be the most suitable membrane for wastewater treatment because they produced high fluxes at relatively low pressure. UF is a low-pressure membrane with pore size diameter between 1 – 100 nm (Koros et al., 1996), where its separation were based on pore sizes. UF can retained bacteria and viruses, which allows its application for water disinfection, producing drinkable water as the permeate of the process (Arnal et al., 2004).

1.2 Membrane Fouling

In spite of all the advantages of UF, the major drawback of membrane application is membrane fouling due to the deposition and accumulation of particulate matter, microorganisms or colloids better known as foulant particle on a membrane surface and/or inside membrane pores (Kraume and Meng, 2012). Membrane fouling causes an increase in membrane cleaning cost, process down time and also shorten membrane lifespan due to frequency and harshness of membrane cleaning condition (Wu *et al.*, 2007).

Previous researchers have carried out great efforts in understanding membrane filtration of bio-products. Tracey and Davis (1994) as well as Bowen, Mohammad and Hilal (1997) reported that membrane pore size and protein concentration

play an important role in membrane fouling in microfiltration of pure bovine serum albumin (BSA). Membrane fouling types changed from internal blocking into cake formation after a period of filtration. Huisman, Prádanos and Hernández (2000) conducted BSA cross-flow ultrafiltration using membranes with different molecular weight cut-off. When a membrane with a small molecular weight cut off (MWCO < 30) is used, membrane fouling at the early stage was determined by the interactions between protein and membrane, whereas in the later period it was dependent on interactions between protein molecules. The membrane plays a trivial effect on the membrane fouling when a large MWCO was used. Blatt *et al.* (1970) claimed that the membrane fouling in protein ultrafiltration depends strongly on the transmembrane pressure. The concentration polarization layer presented an important role under low pressure. At high pressure, the solutes molecules would be deposited onto the membrane surface or adsorbed into the wall surface in a membrane pore.

1.3 Treatment of POME using membrane

Previous studies of UF were mostly focused on filtration to remove natural organic matter (NOM) (Zularisam *et al.*, 2007), such as protein (bovine serum albumin) BSA, humic acid and sodium alginate which parts of NOMs that present in wastewater, river, and seawater (Lee *et al.*, 2005), much less attention has been devoted to elucidate fouling during filtration of final discharged of palm oil mill effluent (POME). Along with the increasing number and scale for the applications of UF, studies of fouling development becomes an important issue as fouling caused increased of maintenance cost if this technology were implemented for pilot operation.

The palm oil industry in Malaysia grows rapidly as our country has become the world's top three producer and exporter of palm oil. Being one of the biggest producers and exporters of palm oil and palm oil products, Malaysia has an important role in fulfilling the growing global need for sustainable oils and fats (Malaysian Palm Oil Board [MPOB], 2014). Unfortunately, along with the increase of this profitable industry, the generation of palm oil mill effluent also increased. According to MPOB (2017), in the year 2014 to 2015 the production of palm oil increase from 19,669,206 tonnes to 19,961,581 tonnes, which means, more than millions of tonnes of palm oil mill effluent has been generated throughout the year. If the effluent is left untreated, it can cause a serious environmental problem. Therefore, it is urgent to find a compromising way to control this problem. The conventional treatment system, anaerobic and aerobic systems are not efficient enough to treat the effluent. The final discharge usually does not comply with the standard discharge limit of the Department of Environment (DOE).

Studies have been done to investigate the effectiveness of membranes for treatment of POME. Wu *et al.* (2007) who studied the effect of pressure on membrane fouling. It was reported that at 0.8 MPa fouling increased up to a

maximum value of 85.8% but simultaneously enabled the recovery of protein and carbohydrate in POME up to 61.4% and 76.4%, respectively. Ahmad *et al.* (2003) used coagulation and flocculation as pre-treatment for POME, before passing through RO and UF membrane. Results showed that the treatment system has a huge potential for producing boiler feed water that can be recycled back to the plant. Hence, UF may work as a reliable tool for treatment of POME. Azmi and Md Yunos (2014) combined adsorption treatment using palm kernel shell-based activated carbon as pre-treatment with ultrafiltration membrane. These authors reported significant reduction of pollutant elements up to 90% at optimum conditions.

However, performance of membrane can be enhanced and fouling can be mitigated by modifying membrane configuration. One of the technique of membrane modification is by stacking two membranes together without any spacer with different configurations, also known as sandwich membrane (Md Yunos and Field, 2008). The purpose of sandwich membrane is to compensate the imperfection of the pore size distribution of available commercial membranes. Feins and Sirkar (2005) successfully improved the selectivity of membranes by stacking 2 to 3 flat UF membranes. Md Yunos and Field (2008) enhanced the efficiency of ultrafiltration membrane during fractionation of protein. Azmi and Md Yunos (2014) successfully improved the quality of permeate from POME using sandwich ultrafiltration technique. They reported that with reverse membrane orientation, the pollutant significantly reduced by almost 99%. However, very little appreciation for the potential of sandwich ultrafiltration either in protein separation or waste treatment has been shown. Therefore, this study focused on the effect of operating parameters on the performance and fouling formation of single membrane and sandwich membrane during treatment of final discharge from (POME).

1.4 Problem Statement

Water scarcity problems have been more severe around the world. The rapid growth of population and industries as well as intense regulations caused the demand for freshwater becomes tripled and continue to rise over the year. Billion tonnes of freshwater are being used by industries during the production process. One of the solutions for addressing this issue by reclamation and reuse of wastewater from municipalities and industrial plants.

The industry that contribute to the most of the effluent is palm oil industry as Malaysian palm oil industry is growing rapidly and become a very important agriculture-based country. However, this important economic activity unfortunately generates an enormous amount of liquid effluent or palm oil mill effluent (POME). It is estimated for 1 tonne of crude palm oil produced, almost 5-7 tonnes of water were used during wet process of palm oil mill and 50% of the water end up as POME (Ahmad *et al.*, 2003). Nevertheless, water can be sustained and conserved by reclaiming water from final discharge of POME using membrane technology as tertiary treatment. However, palm oil industries

always find the membrane technology as the expensive treatment due to high cost of maintenance due to fouling phenomenon. Therefore, it is important to understand the mechanism of fouling in order to control and reduced membrane fouling.

Currently, filtration of POME using UF membrane showed great potential in reclaim better quality of treated POME. However, the industries face the problem in obtaining crystal clear water without using reverse osmosis membrane which is more expensive. This is due to pore size distribution of the membranes often limit the rejection and efficiency of the separation. Although, some commercial membrane today have tighter distribution, it has been found by other researcher that sandwich membrane can improved the rejection characteristics of ultrafiltration membrane.

Sandwich membrane are commonly studied to enhance the separation of different types of proteins such as myoglobin, lysozyme and BSA as different arrangement amplified the separation of different types of protein (Field et al., 2009). Currently, application of sandwich membrane in treatment of pre-treated POME successfully achieved 60% reduction of pollutant. However, in the study, fouling mechanism of membrane occur during treatment was not elucidated. Thus, this project was proposed to study effect of operating parameters on UF membrane performance and fouling resistance and effectiveness of sandwich membrane in reclaiming water from final discharged and how it effect fouling.

1.5 Objectives of the Research

The objectives of this study are as follows:

- i) To study the effect of pressure (0.5 bar, 1.0 bar, 1.5 bar and 2.0 bar), stirred condition (0 rpm, 400 rpm, 600 rpm and 800 rpm) and pH (6,7,8 and 10) on permeate quality and fouling resistance of single membrane and sandwich membrane.
- ii) To evaluate the effectiveness of sandwich membrane in improving the quality of permeate and fouling analysis.

1.6 Scope of Research

The effect of pressure (0.5 bar, 1.0 bar and 2.0 bar), stirred condition (0 rpm, 400 rpm, 600 rpm and 800 rpm) and pH (6, 7, 8 and 10) on permeate quality (total dissolved solid (TDS) and turbidity) and fouling resistance of membrane. Dissolved solid concentration in POME is related to the value of BOD₅ and COD. If dissolved solid in POME reducing, the concentration of BOD₅ and COD also reduced (Azmi and Md Yunos, 2015). Turbidity has the linear relationship with the suspended matter in the solution. These suspended mater create turbidity and impact color to the water (Boyd, 2000). As for fouling study, fouling intensity

and fouling resistance were investigated in this research. Fouling intensity is the study of how intense the fouling of membrane after filtration (Mohammad et al., 2009) while fouling resistance exhibited the fouling occurred during filtration run.

The proper condition was selected for each parameter based on acceptable value of TDS and turbidity and fouling. At this condition, the permeate were further analyse with BOD₅, COD and suspended solid. These values were compared with standard of effluent discharged limit standard (B) stated in Malaysian Department of Environment (DOE),2010, and EPA Guidelines for water reused standard as well as Drinking Water Quality Standard from DOE (2010), which can be seen in Table 4.4.

For second stage of this experiment, the condition was fixed based on first experiment. Sandwich membrane were done by stacking two flat sheet membrane together without any spacer in between. The configuration of sandwich membrane was varied by adjusting the arrangement of the bottom membrane only. The configuration were called SS-Sandwich and SB-Sandwich. S term is referring to skin layer while B referring to the support layer of the membrane. The illustration of sandwich membrane can be seen in Figure 2.7 and Figure 3.6.

1.7 Thesis Outline

Chapter 1 – Introduction

This chapter gives an overview on the background of this research. A brief explanation on ultrafiltration membrane, fouling mechanism during treatment and a brief of palm oil industry in Malaysia. The objectives and research scope also included in this chapter.

Chapter 2 – Literature review

This chapter review previous research of palm oil treatment, application of membrane in palm oil industry and fouling mechanism of ultrafiltration. This overview provides a general discussion of related research.

Chapter 3 – Materials and Method

This chapter present the materials and method includes origin of the sample, types of membrane used and set-up of the experiment. . This includes the experimental details of the proposed technique and procedure used in the thesis.

Chapter 4 - Result and discussion

This chapter present result and discussion on the effect of operating parameters on membrane performance and fouling formation. Also discussion on the effect of sandwich configuration on membrane performance.

Chapter 5- Conclusion

This chapter contains concluding remarks and recommendation for future works.

REFERENCES

- Abadi, S. R. H., Sebzari, M. R., Hemati, M., Rekabdar, F., & Mohammadi, T. (2011). Ceramic membrane performance in microfiltration of oily wastewater. *Desalination*, 265(1), 222–228.
- Abdel-Raouf, N., Al-Homaidan, A. A., & Ibraheem, I. B. M. (2012). Microalgae and wastewater treatment. *Saudi Journal of Biological Sciences*, 19(3), 257–275.
- Abdurahman, N. H., Rosli, Y. M., & Azhari, N. H. (2013). The performance evaluation of anaerobic methods for Palm Oil Mill Effluent (POME) treatment: A review. In *International Perspectives on Water Quality Management and Pollutant Control*. Place of publication: InTech.
- Agamuthu, P., & Tan, E. L. (1985). Digestion of dried palm oil mill effluent by *Cellulomonas* species. *Microbios Letters*, 30(119–120), 109–113.
- Ahmad, A. L., Sumathi, S., & Hameed, B. H. (2005). Residual oil and suspended solid removal using natural adsorbents chitosan, bentonite and activated carbon: A comparative study. *Chemical Engineering Journal*, 108(1), 179–185.
- Ahmad, A., Chong, M., Bhatia, S., & Ismail, S. (2006). Drinking water reclamation from palm oil mill effluent (POME) using membrane technology. *Desalination*, 191(1–3), 35–44.
- Allgeier, S. (2005). *Membrane filtration guidance manual*. Place of publication: USEPA.
- Aziz, H. A., Alias, S., Adlan, M. N., Asaari, A. H., & Zahari, M. S. (2007). Colour removal from landfill leachate by coagulation and flocculation processes. *Bioresource Technology*, 98(1), 218–220.
- Arnal, J., Sancho, Verdú, G., Lora, L., Marín J.F and Cháfer, J. (2004). Selection of the most suitable ultrafiltration membrane for water disinfection in developing countries, *Desalination*, 168, 265– 270.
- Azmi N. S. (2015). *Treatment of palm oil mill effluent using sandwich ultrafiltration technique* [dissertation]. Universiti Putra Malaysia, Malaysia.
- Azmi, N., & Md Yunos, K. (2014). Wastewater treatment of palm oil mill effluent (POME) by ultrafiltration membrane separation technique coupled with adsorption treatment as pre-treatment. *Agriculture and Agricultural Science Procedia*, 2, 257–264.
- Bai, L., Qu, F., Liang, H., Ma, J., Chang, H., Wang, M., & Li, G. (2013). Membrane fouling during ultrafiltration (UF) of surface water: Effects of sludge discharged interval (SDI). *Desalination*, 319, 18–24.

- Baker, R.W. (2004). *Membrane technology and application*. England: McGraw-Hill.
- Bhatia, S., Othman, Z., & Ahmad, A. L. (2007). Coagulation–flocculation process for POME treatment using *Moringa oleifera* seeds extract: Optimization studies. *Chemical Engineering Journal*, 133(1), 205–212.
- Bing-zhi, D., Lin, W., & Nai-yun, G. (2008). The removal of bisphenol A by ultrafiltration. *Desalination*, 221(1–3), 312–317.
- Blatt, W. F., Dravid, A., Michaels, A. S., & Nelsen, L. (1970). Solute polarization and cake formation in membrane ultrafiltration: Causes, consequences and control techniques. *Membrane Science and Technology*, 47.
- Borea, L., Naddeo, V., & Belgiorno, V. (2017). Application of electrochemical processes to membrane bioreactors for improving nutrient removal and fouling control. *Environmental Science and Pollution Research*, 24(1), 321–333.
- Borja, R., Banks, C. J., Khalfaoui, B., & Martin, A. (1996). Performance evaluation of an anaerobic hybrid digester treating palm oil mill effluent. *Journal of Environmental Science and Health Part A*, 31(6), 1379–1393.
- Bowen, W., Mohammad, A., & Hilal, N. (1997). Characterisation of nanofiltration membranes for predictive purposes — Use of salts, uncharged solutes and atomic force microscopy. *Journal of Membrane Science*, 126(1), 91–105.
- Boyd, R. F., & Zydney, A. L. (1997). Sieving characteristics of multilayer ultrafiltration membranes. *Journal of Membrane Science*, 131(1–2), 155–165.
- Burba, P., Shkinev, V., Spivakov B.Ya. (1995). On-line fractionation and characterization of aquatic humic substances by means of sequential-stage ultrafiltration. *Journal of Analytical Chemistry*, 351, 74–82.
- Carbonell-Alcaina, C., Corbatón-Báguena, M. J., Álvarez-Blanco, S., Bes-Piá, M. A., Mendoza-Roca, J. A., & Pastor-Alcañiz, L. (2016). Determination of fouling mechanisms in polymeric ultrafiltration membranes using residual brines from table olive storage wastewaters as feed. *Journal of Food Engineering*, 187, 14–23.
- Chakrabarty, B., Ghoshal, A. K., & Purkait, M. K. (2008). Ultrafiltration of stable oil-in-water emulsion by polysulfone membrane. *Journal of Membrane Science*, 325(1), 427–437.
- Chang, I. S., Le Clech, P., Jefferson, B., & Judd, S. (2002). Membrane fouling in membrane bioreactors for wastewater treatment. *Journal of Environmental Engineering*, 128(11), 1018–1029.
- Cheang, B., and Zydney, A.L. (2004). A two-stage ultrafiltration process for fractionation of whey protein isolate. *Journal of Membrane Science*, 231(1), 159–167.

- Chen, W., Peng, J., Su, Y., Zheng, L., Wang, L., & Jiang, Z. (2009). Separation of oil/water emulsion using Pluronic F127 modified polyethersulfone ultrafiltration membranes. *Separation and Purification Technology*, 66(3), 591–597.
- Cheryan, M., & Rajagopalan, N. (1998). Membrane processing of oily streams. Wastewater treatment and waste reduction. *Journal of Membrane Science*, 151(1), 13–28.
- Choi, H., Zhang, K., Dionysiou, D. D., Oerther, D. B., & Sorial, G. A. (2005). Influence of cross-flow velocity on membrane performance during filtration of biological suspension. *Journal of Membrane Science*, 248(1), 189–199.
- Chollangi, A., & Hossain, M. M. (2007). Separation of proteins and lactose from dairy wastewater. *Chemical Engineering and Processing: Process Intensification*, 46(5), 398–404.
- Corbatón-Báguena, M. J., Álvarez-Blanco, S., & Vincent-Vela, M. C. (2015). Fouling mechanisms of ultrafiltration membranes fouled with whey model solutions. *Desalination*, 360, 87–96.
- Das, R., Bhattacharjee, C., Ghosh, S. (2009). Effects of operating parameters and nature of fouling behaviour in ultrafiltration of sesame protein hydrolysate. *Journal of Desalination*, 237, 258–276.
- Department of Environment: Environmental quality act: Environmental Quality Crude Palm Oil Regulations (1999).p 13.
- Dong, B. Z., Yan, C. H. E. N., Gao, N. Y., & Fan, J. C. (2007). Effect of coagulation pretreatment on the fouling of ultrafiltration membrane. *Journal of Environmental Sciences*, 19(3), 278–283.
- Egal, M., Budtova, T., & Navard, P. (2008). The dissolution of microcrystalline cellulose in sodium hydroxide-urea aqueous solutions. *Cellulose*, 15(3), 361–370.
- El-Abbassi, A., Kiai, H., Raiti, J., & Hafidi, A. (2014). Application of ultrafiltration for olive processing wastewaters treatment. *Journal of Cleaner Production*, 65, 432–438.
- Feins, M., & Sirkar, K. (2005). Novel internally staged ultrafiltration for protein purification. *Journal of Membrane Science*, 248(1–2), 137–148.
- Feins, M., & Sirkar, K. K. (2004). Highly selective membranes in protein ultrafiltration. *Biotechnology and bioengineering*, 86(6), 603–611.
- Ferrando, M., Růžek, A., Zator, M., Lopez, F., & Güell, C. (2005). An approach to membrane fouling characterization by confocal scanning laser microscopy. *Journal of Membrane Science*, 250(1), 283–293.
- Field, R. W., Md Yunos, K. F., & Cui, Z. (2009). Separation of proteins using sandwich membranes. *Desalination*, 245(1–3), 597–605.

- Ghosh, A. M., & Balakrishnan, M. (2003). Pilot demonstration of sugarcane juice ultrafiltration in an Indian sugar factory. *Journal of Food Engineering*, 58(2), 143–150.
- Girard, B., & Fukumoto, L. (2000). Membrane processing of fruit juices and beverages: A review. *Critical Reviews in Food Science and Nutrition*, 40(2), 91–157.
- Guo, W., Ngo, H. H., & Li, J. (2012). A mini-review on membrane fouling. *Bioresource Technology*, 122, 27–34.
- Hammer, B. H., & JR, M. J. H. (2005). *Water and wastewater technology*. Singapore: Prentice Hall.
- He, Y., Li, G., Wang, H., Zhao, J., Su, H., & Huang, Q. (2008). Effect of operating conditions on separation performance of reactive dye solution with membrane process. *Journal of Membrane Science*, 321(2), 183–189.
- He, Y., Xu, P., Li, C., & Zhang, B. (2005). High-concentration food wastewater treatment by an anaerobic membrane bioreactor. *Water Research*, 39(17), 4110–4118.
- Hojjat, M., & Salleh, M. A. M. (2009). Optimization of POME anaerobic pond. *European Journal of Scientific Research*, 32(4), 455–459.
- Howe, K. J., Ishida, K. P., & Clark, M. M. (2002). Use of ATR/FTIR spectrometry to study fouling of microfiltration membranes by natural waters. *Desalination*, 147(1), 251–255.
- Hu, B., & Scott, K. (2007). Influence of membrane material and corrugation and process conditions on emulsion microfiltration. *Journal of Membrane Science*, 294(1), 30–39.
- Huisman, I. H., Prádanos, P., & Hernández, A. (2000). The effect of protein–protein and protein–membrane interactions on membrane fouling in ultrafiltration. *Journal of Membrane Science*, 179(1), 79–90.
- Igwe, J. C., Ogunewe, D. N., & Abia, A. A. (2005). Competitive adsorption of Zn (II), Cd (II) and Pb (II) ions from aqueous and non-aqueous solution by maize cob and husk. *African Journal of Biotechnology*, 4(10), 1113.
- Igwe, J., & Onyegbado, C. (2007). A review of Palm Oil Mill Effluent (POME) water treatment. *Global Journal of Environmental Research*, 1(2), 55–62.
- Isa, M. H. M., Coraglia, D. E., Frazier, R. A., Jauregi, P. (2007). Recovery and purification of surfactin from fermentation broth by a two-step ultrafiltration process. *Journal of Membrane Science*, 296(1), 51–57.
- James, B. J., Jing, Y., & Chen, X. D. (2003). Membrane fouling during filtration of milk—A microstructural study. *Journal of Food Engineering*, 60(4), 431–437.

- Jones, K. L., & O'Melia, C. R. (2000). Protein and humic acid adsorption onto hydrophilic membrane surfaces: Effects of pH and ionic strength. *Journal of Membrane Science*, 165(1), 31–46.
- Jönsson, A., & Trägårdh, G. (1990). Ultrafiltration applications. *Desalination*, 77, 135–179.
- Jucker, C., & Clark, M. M. (1994). Adsorption of aquatic humic substances on hydrophobic ultrafiltration membranes. *Journal of Membrane Science*, 97, 37–52.
- Jun, Z., Yang, F. L., Meng, F. G., Peng, A. N., & Di, W. A. N. G. (2007). Comparison of membrane fouling during short-term filtration of aerobic granular sludge and activated sludge. *Journal of Environmental Sciences*, 19(11), 1281–1286.
- Kabsch-Korbutowicz, M. (2005). Application of ultrafiltration integrated with coagulation for improved NOM removal. *Desalination*, 174(1), 13–22.
- Kang, S. K., & Choo, K. H. (2003). Use of MF and UF membranes for reclamation of glass industry wastewater containing colloidal clay and glass particles. *Journal of Membrane Science*, 223(1), 89–103.
- Kang, S. K., & Choo, K. H. (2003). Use of MF and UF membranes for reclamation of glass industry wastewater containing colloidal clay and glass particles. *Journal of Membrane Science*, 223(1), 89–103.
- Koehler, J. A., Ulbricht, M., & Belfort, G. (2000). Intermolecular forces between a protein and a hydrophilic modified polysulfone film with relevance to filtration. *Langmuir*, 16(26), 10419–10427.
- Koros, W. J., Ma, Y. H., & Shimidzu, T. (1996). Terminology for membranes and membrane processes (IUPAC Recommendations 1996). *Pure and Applied Chemistry*, 68(7), 1479–1489.
- Kumar, R., & Ismail, A. (2015). Fouling control on microfiltration/ultrafiltration membranes: Effects of morphology, hydrophilicity, and charge. *Journal of Applied Polymer Science*, 132(21).
- Latif Ahmad, A., Ismail, S., & Bhatia, S. (2003). Water recycling from palm oil mill effluent (POME) using membrane technology. *Desalination*, 157(1–3), 87–95.
- Le-Clech, P., Chen, V., & Fane, T. A. (2006). Fouling in membrane bioreactors used in wastewater treatment. *Journal of Membrane Science*, 284(1), 17–53.
- Lee, N., Amy, G., Croué, J. P., & Buisson, H. (2005). Morphological analyses of natural organic matter (NOM) fouling of low-pressure membranes (MF/UF). *Journal of Membrane Science*, 261(1), 7–16.
- Lee, S., Lee, K., Wan, W., & Choi, Y. (2005). Comparison of membrane permeability and a fouling mechanism by pre-ozonation followed by membrane filtration and residual ozone in membrane cells. *Desalination*, 178(1–3), 287–294.

- Li, M., Zhao, Y., Zhou, S., Xing, W., & Wong, F. S. (2007). Resistance analysis for ceramic membrane microfiltration of raw soy sauce. *Journal of Membrane Science*, 299(1), 122–129.
- Lim, A. L., & Bai, R. (2003). Membrane fouling and cleaning in microfiltration of activated sludge wastewater. *Journal of Membrane Science*, 216(1), 279–290.
- Lobo, A., Cambiella, Á., Benito, J. M., Pazos, C., & Coca, J. (2006). Ultrafiltration of oil-in-water emulsions with ceramic membranes: Influence of pH and crossflow velocity. *Journal of Membrane Science*, 278(1), 328–334.
- Malaysian Palm Oil Board (MPOB). (2017a). Monthly production of crude palm oil for the month of December 2017. Retrieved from <http://bepi.mpob.gov.my/index.php/en/statistics/production/177-production-017/792-production-of-crude-oil-palm-2017.html>
- Malaysian Palm Oil Board (MPOB). (2017b). Monthly production of palm oil products summary for the month of December 2017. Retrieved from <http://bepi.mpob.gov.my/index.php/my/statistics/production/177-production-2017/791-production-of-oil-palm-products-2017.html>
- Mänttari, M., Pihlajamäki, A., & Nyström, M. (2006). Effect of pH on hydrophilicity and charge and their effect on the filtration efficiency of NF membranes at different pH. *Journal of Membrane Science*, 280(1), 311–320.
- Markandya, A., & Shibli, A. (1995). Regional Overview: Industrial Pollution Control Policies in Asia: How Successful Are the Strategies?. *Asian Journal of Environmental Management*, 3, 87–118.
- Matthiasson, E. (1983). The role of macromolecular adsorption in fouling of ultrafiltration membranes. *Journal of Membrane Science*, 16, 23–36
- Md Yunos, K. M., & Field, R. W. (2008). Rejection amplification in the ultrafiltration of binary protein mixtures using sandwich configurations. *Chemical Engineering and Processing: Process Intensification*, 47(7), 1053–1060.
- Meng, F., Chae, S. R., Drews, A., Kraume, M., Shin, H. S., & Yang, F. (2009). Recent advances in membrane bioreactors (MBRs): membrane fouling and membrane material. *Water Research*, 43(6), 1489–1512.
- Metcalf, E. E., & Eddy, H. P. (2003). *Wastewater engineer treatment disposal, reuse*. New York: McGraw-Hill.
- Mikulášek, P., Doleček, P., & Pospíšil, P. (2004). Crossflow microfiltration of mineral dispersions using ceramic membranes. *Desalination*, 163(1–3), 333–343.
- Mirsaeedghazi, H., Emam-Djomeh, Z., Mousavi, S. M., Aroujalian, A., & Navidbakhsh, M. (2010). Clarification of pomegranate juice by microfiltration with PVDF membranes. *Desalination*, 264(3), 243–248.
- Mohammadi, T., & Esmaeilifar, A. (2004). Wastewater treatment using ultrafiltration at a vegetable oil factory. *Desalination*, 166, 329–337.

- Mohammadi, T., & Esmaeelifar, A. (2005). Wastewater treatment of a vegetable oil factory by a hybrid ultrafiltration-activated carbon process. *Journal of Membrane Science*, 254(1), 129–137.
- Mourad, H., & Martine, M. P. (2002). Analysis of deposit behaviour in crossflow microfiltration by means of thickness measurement. *Chemical Engineering Journal*, 86(3), 251–257.
- Na, J., & Yonggang, Z. (2012). The effect of humic acid on ultrafiltration membrane fouling. *Energy Procedia*, (11), 4821–4829.
- Nakatsuka, S., & Michaels, A. S. (1992). Transport and separation of proteins by ultrafiltration through sorptive and non-sorptive membranes. *Journal of Membrane Science*, 69(3), 189–211.
- Ng, C. Y., Mohammad, A. W., Ng, L. Y., & Jahim, J. M. (2014). Membrane fouling mechanisms during ultrafiltration of skimmed coconut milk. *Journal of Food Engineering*, 142, 190–200.
- Niazmand, R., Razavi, S. M. A., & Farhoosh, R. (2015). Colloid-enhanced ultrafiltration of canola oil: Effect of process conditions and MWCO on flux, fouling and rejections. *Journal of Food Processing and Preservation*, 39(3), 292–300.
- Nourbaksh, H., Alemi, A., Emam-Djomeh, Z., & Mirsaeedghazi, H. (2014). Effect of processing parameters on fouling resistances during microfiltration of red plum and watermelon juices: A comparative study. *Journal of Food Science and Technology*, 51(1), 168–172.
- Nuortila-Jokinen, J., & Nyström, M. (1996). Comparison of membrane separation processes in the internal purification of paper mill water. *Journal of Membrane Science*, 119(1), 99–115.
- Nyström, M., Ruohomäki, K., & Kaipia, L. (1996). Humic acid as a fouling agent in filtration. *Desalination*, 106(1–3), 79–87.
- Oe, T., Koide, H., Hirokawa, H., & Okukawa, K. (1996). Performance of membrane filtration system used for water treatment. *Desalination*, 106(1), 107–113.
- Ognier, S., Wisniewski, C., & Grasmick, A. (2002). Influence of macromolecule adsorption during filtration of a membrane bioreactor mixed liquor suspension. *Journal of Membrane Science*, 209(1), 27–37.
- Onyia, C. O., Uyub, A.M., Akunna, J. C., Norulaini, N. A., & Omar, A. K. M. (2001). Increasing the fertilizer value of palm oil mill sludge: Bioaugmentation in nitrification. *Water Science and Technology*, 44(10), 157–162.
- Pinnekamp J. and Friedrich H. (2003). *Membrane technology for wastewater treatment*. Municipal water and waste management. Place of publication: Name of publisher.

- Poh, P. E., & Chong, M. F. (2009). Development of anaerobic digestion methods for palm oil mill effluent (POME) treatment. *Bioresource Technology*, 100(1), 1–9.
- Pope, J. M., Yao, S., & Fane, A. G. (1996). Quantitative measurements of the concentration polarisation layer thickness in membrane filtration of oil-water emulsions using NMR micro-imaging. *Journal of Membrane Science*, 118(2), 247–257.
- Prazeres, D.M. (1997). A theoretical analogy between multistage ultrafiltration and size exclusion chromatography. *Chemical Engineering Science*, 52(6), 953–960.
- Puro, L., Kallioinen, M., Mänttari, M., Natarajan, G., Cameron, D. C., & Nyström, M. (2010). Performance of RC and PES ultrafiltration membranes infiltration of pulp mill process waters. *Desalination*, 264(3), 249–255.
- Rabiller-Baudry, M., Le Maux, M., Chaufer, B., & Begoin, L. (2002). Characterisation of cleaned and fouled membrane by ATR—FTIR and EDX analysis coupled with SEM: application to UF of skimmed milk with a PES membrane. *Desalination*, 146(1), 123–128.
- Rahimpour, A., Jahanshahi, M., Mortazavian, N., Madaeni, S. S., & Mansourpanah, Y. (2010). Preparation and characterization of asymmetric polyethersulfone and thin-film composite polyamide nanofiltration membranes for water softening. *Applied Surface Science*, 256(6), 1657–1663.
- Ramakrishna, Ma and Matsuura. (2011). *Polymer Membrane*. England: McGraw-Hill.
- Renault, F., Sancey, B., Badot, P. M., & Crini, G. (2009). Chitosan for coagulation/flocculation processes—An eco-friendly approach. *European Polymer Journal*, 45(5), 1337–1348.
- Rickman, M., Pellegrino, J., & Davis, R. (2012). Fouling phenomena during membrane filtration of microalgae. *Journal of Membrane Science*, 423, 33–42.
- Ruohomäki, K., Väisänen, P., Metsämuuronen, S., Kulovaara, M., & Nyström, M. (1998). Characterization and removal of humic substances in ultra-and nanofiltration. *Desalination*, 118(1–3), 273–283.
- Salahi, A., Abbasi, M., & Mohammadi, T. (2010). Permeate flux decline during UF of oily wastewater: Experimental and modeling. *Desalination*, 251(1), 153–160.
- Sivasothy, K. (2000) Palm oil milling technology. In Y. Basiron, B. S. Jalani, and K.W. Chan (eds.) *Advances in Palm Oil Research*, 747(1), 744–782.
- Sójka-Ledakowicz, J., Koprowski, T., Machnowski, W., & Knudsen, H. H. (1998). Membrane filtration of textile dyehouse wastewater for technological water reuse. *Desalination*, 119(1-3), 1-9.
- Susanto, H., & Ulbricht M. (2005). Influence of ultrafiltration membrane characteristics on adsorptive fouling with dextrans. *Journal of Membrane Science*, 266(1–2), 132–142.

- Susanto, H., & Ulbricht, M. (2007). Photografted thin polymer hydrogel layers on PES ultrafiltration membranes: Characterization, stability, and influence on separation performance. *Langmuir*, 23(14), 7818–7830.
- Tansel, B., Dizge, N., & Tansel, I. N. (2017). Analysis of high resolution flux data to characterize fouling profiles of membranes with different MWCO under different filtration modes. *Separation and Purification Technology*, 173, 200–208.
- Tardieu, E., Grasmick, A., Geaugey, V., Manem, J. (1999). Influence of hydrodynamics on fouling velocity in a recirculated MBR for wastewater treatment, *J. Membr. Sci.*, 156,131–140.
- Teixeira, M. R., & Rosa, M. J. (2003). pH adjustment for seasonal control of UF fouling by natural waters. *Desalination*, 151(2), 165–175.
- Tracey, E., & Davis, R. (1994). Protein Fouling of Track-Etched Polycarbonate Microfiltration Membranes. *Journal of Colloid and Interface Science*, 167(1), 104–116.
- Van der Bruggen, B., Vandecasteele, C., Van Gestel, T., Doyen, W., & Leysen, R. (2003). A review of pressure-driven membrane processes in wastewater treatment and drinking water production. *Environmental Progress & Sustainable Energy*, 22(1), 46–56.
- van Reis, R., & Zydney, A. (2001). Membrane separations in biotechnology. *Current Opinion in Biotechnology*, 12(2), 208–211.
- Vrijenhoek, E. M., Hong, S., & Elimelech, M. (2001). Influence of membrane surface properties on initial rate of colloidal fouling of reverse osmosis and nanofiltration membranes. *Journal of Membrane Science*, 188(1), 115–128.
- Wah, W. P., Sulaiman, N. M., Nachiappan, M., & Varadaraj, B. (2002). Pre-treatment and membrane ultrafiltration using treated palm oil mill effluent (POME). *Songklanakarin Journal of Science and Technology*, 24, 891–898.
- Wang, C., Li, Q., Tang, H., Yan, D., Zhou, W., Xing, J., & Wan, Y. (2012). Membrane fouling mechanism in ultrafiltration of succinic acid fermentation broth. *Bioresource Technology*, 116, 366–371
- Wang, K. Y., Chung, T. S., & Gryta, M. (2008). Hydrophobic PVDF hollow fiber membranes with narrow pore size distribution and ultra-thin skin for the fresh water production through membrane distillation. *Chemical Engineering Science*, 63(9), 2587–2594.
- Wu, T. Y., Mohammad, A. W., Jahim, J. M., & Anuar, N. (2009). A holistic approach to managing palm oil mill effluent (POME): Biotechnological advances in the sustainable reuse of POME. *Biotechnology Advances*, 27(1), 40–52.
- Wu, T., Mohammad, A., Md. Jahim, J., & Anuar, N. (2007). Palm oil mill effluent (POME) treatment and bioresources recovery using ultrafiltration membrane:

Effect of pressure on membrane fouling. *Biochemical Engineering Journal*, 35(3), 309–317.

Xia, S., Nan, J., Liu, R. and Li, G. (2004). Study of drinking water treatment by ultrafiltration of surface water and its application to China, *Desalination*, 170, 41–47.

Yorgun, M. S., Balcioglu, I. A., & Saygin, O. (2008). Performance comparison of ultrafiltration, nanofiltration and reverse osmosis on whey treatment. *Desalination*, 229(1–3), 204–216.

Zeng, J., Zheng, L., & Liu, J. (2010). Experiments on clarification of orange juice and fouling resistances by using ceramic microfiltration membrane. *Transactions of the Chinese Society of Agricultural Engineering*, 26(1), 353–358.

Zinatizadeh, A. A. L., Mohamed, A. R., Abdullah, A. Z., Mashitah, M. D., Isa, M. H., & Najafpour, G. D. (2006). Process modeling and analysis of palm oil mill effluent treatment in an up-flow anaerobic sludge fixed film bioreactor using response surface methodology (RSM). *Water Research*, 40(17), 3193–3208.

Zularisam, A. W., Ismail, A. F., & Salim, R. (2006). Behaviours of natural organic matter in membrane filtration for surface water treatment—A review. *Desalination*, 194(1–3), 211–231.

Zularisam, A., Ismail, A., Salim, M., Sakinah, M., & Ozaki, H. (2007). The effects of natural organic matter (NOM) fractions on fouling characteristics and flux recovery of ultrafiltration membranes. *Desalination*, 212(1–3), 191–208.