



UNIVERSITI PUTRA MALAYSIA

**CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND
CYLINDERS IN VISCOUS FLUIDS**

SYAKILA BINTI AHMAD

IPM 2009 4



**CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND
CYLINDERS IN VISCOUS FLUIDS**

By

SYAKILA BINTI AHMAD

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,
in Fulfilment of the Requirements for the Degree of Doctor of Philosophy**

May 2009



To My Beloved Family and Friends.



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfilment of the requirement for the degree of Doctor of Philosophy

**CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND
CYLINDERS IN VISCOUS FLUIDS**

By

SYAKILA BINTI AHMAD

May 2009

Chairman : Norihan Md. Arifin, PhD

Institute : Institute for Mathematical Research

Convection is the heat transfer process which is frequently encountered in environmental and engineering applications. In this study, the problems of steady laminar convection boundary layer flows over needles and cylinders immersed in an incompressible and viscous fluid are theoretically considered. The dimensional partial differential equations governing the boundary layer flows are first transformed into non-dimensional equations. These equations are then transformed using non-similar transformation. Then, these transformed nonlinear systems of equations are solved using an implicit finite difference scheme known as the Keller-box method, which has been found to be very suitable in dealing with nonlinear and parabolic equations. The complete numerical method used in this study is programmed in Fortran. Numerical computations are carried out for various values of the dimensionless parameters of the problems, which include the Prandtl number Pr , the ratio of the major and minor axes of the cylinder b_c/a_c , the mixed convection parameter λ , the modified mixed convection parameter $\hat{\lambda}$, the transverse curvature parameter Λ , the parameter a representing the needle size and the viscosity/temperature parameter θ_r . Numerical results



presented in this study are the skin friction coefficient, the heat transfer coefficient, the local Nusselt number, the cylinder temperature as well as the velocity and temperature profiles. The obtained results show that the flow and the thermal characteristics are significantly influenced by these parameters.



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia
sebagai memenuhi keperluan untuk ijazah Doktor Falsafah

**ALIRAN LAPISAN SEMPADAN OLAKAN PADA JARUM DAN SILINDER
DALAM BENDALIR LIKAT**

Oleh

SYAKILA BINTI AHMAD

Mei 2009

Pengerusi : Norihan Md. Arifin, PhD

Institut : Institut Penyelidikan Matematik

Olakan adalah suatu proses pemindahan haba yang sering berlaku dalam persekitaran dan juga dalam kebanyakan aplikasi kejuruteraan. Dalam kajian ini, masalah aliran lapisan sempadan olakan mantap dan berlamina terhadap jarum dan silinder dalam bendalir likat dan tak termampatkan telah dipertimbangkan secara teori. Persamaan pembezaan separa berdimensi yang menakluk aliran lapisan sempadan terlebih dahulu dijelmakan kepada persamaan tak berdimensi. Seterusnya, persamaan tersebut akan dijelma menggunakan penjelmaan tak serupa. Sistem persamaan terjelma tak linear yang diperoleh diselesaikan secara berangka menggunakan skim beza sehingga tersirat iaitu kaedah kotak Keller yang merupakan satu kaedah yang sangat sesuai untuk menyelesaikan persamaan tak linear dan parabolik. Kaedah berangka yang digunakan dalam kajian ini telah dibangunkan dalam bentuk pengaturcaraan komputer dengan menggunakan Fortran. Pengiraan berangka dilakukan untuk pelbagai nilai parameter tak berdimensi seperti nombor Prandtl Pr , nisbah paksi major dan minor silinder b_c/a_c , parameter olakan campuran λ , parameter olakan campuran ubahan $\hat{\lambda}$, parameter kelengkungan melintang Λ , parameter a yang mewakili saiz jarum dan parameter



kelikatan/suhu θ_r . Keputusan berangka yang dipersembahkan dalam kajian ini adalah pekali geseran kulit, pekali pemindahan haba, nombor Nusselt setempat, suhu silinder beserta profil halaju dan suhu. Keputusan yang diperoleh menunjukkan bahawa ciri-ciri aliran dan terma adalah sangat dipengaruhi oleh parameter-parameter yang dipertimbangkan di atas.

ACKNOWLEDGEMENTS

Bismillahirrahmanirrahim. Alhamdulillah. In the Name of Allah, the most Beneficent and the most Merciful, I would like to express my great appreciation for the guidance and assistance received throughout the journey of this thesis writing.

My deepest thanks to my respected supervisor and co-supervisors; Assoc. Prof. Dr. Norihan Md. Arifin, Assoc. Prof. Dr. Roslinda Mohd Nazar and Dr. Abdul Aziz Jaafar for their valuable guidance, knowledge, times and support, and also for making this thesis possible. I would also like to extend my appreciation to Prof. Ioan Pop from University of Cluj, Romania, for his motivation and support.

Many thanks to the Institute for Mathematical Research, Universiti Putra Malaysia (UPM) for giving me the opportunity to do my research here and also for providing me with a very good research environment and equipments. My special thanks to the staffs from the institute who have been very supportive and very helpful during my course of study here. Also thanks to all the staffs in UPM who have involved directly or indirectly during my studies and also during the preparation of this thesis. I would also like to express my sincere thanks to Universiti Sains Malaysia (USM) and Ministry of Higher Education Malaysia for the financial support throughout the course of my study.

I would like to thank all my friends and research colleagues who kindly provided valuable and helpful comments in the preparation of this thesis. Finally, thank you very much to the most important person in my life, my parent and members of the family for their unconditional love and support especially during the hard times. May Allah bless you all.



I certify that a Thesis Examination Committee has met on 27 May 2009 to conduct the final examination of Syakila binti Ahmad on her thesis entitled "Convection Boundary Layer Flows Over Needles and Cylinders in Viscous Fluids" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U.(A) 106] 15 March 1998. The Committee recommends that the student be awarded the Doctor of Philosophy.

Members of the Thesis Examination Committee were as follows:

Noor Akma Ibrahim, PhD
Associate Professor
Institute for Mathematical Research
Universiti Putra Malaysia
(Chairman)

Malik Abu Hassan, PhD
Professor
Institute for Mathematical Research
Universiti Putra Malaysia
(Internal Examiner)

Mohd Noor Saad, PhD
Lecturer
Institute for Mathematical Research
Universiti Putra Malaysia
(Internal Examiner)

Bachok Taib, PhD
Professor
Center for Graduate Studies
Universiti Sains Islam Malaysia
Malaysia
(External Examiner)



BUJANG KIM HUAT, PhD
Professor and Deputy Dean
School of Graduate Studies
Universiti Putra Malaysia

Date: 13 July 2009



This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfilment of the requirement for the degree of Doctor of Philosophy. The members of the Supervisory Committee were as follows:

Norihan Md. Arifin, PhD

Associate Professor
Institute for Mathematical Research
Universiti Putra Malaysia
(Chairman)

Abdul Aziz Jaafar, PhD

Lecturer
Institute for Mathematical Research
Universiti Putra Malaysia
(Member)

Roslinda Mohd Nazar, PhD

Associate Professor
Institute for Mathematical Research
Universiti Putra Malaysia
(Member)

HASANAH MOHD. GHAZALI, PhD

Professor and Dean
School of Graduate Studies
Universiti Putra Malaysia

Date: 17 July 2009



DECLARATION

I hereby declare that the thesis is based on my original work except for quotations and citations, which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at UPM or other institutions.



SYAKILA BINTI AHMAD

Date: 10 July 2009

TABLE OF CONTENTS

	Page
DEDICATION	ii
ABSTRACT	iii
ABSTRAK	v
ACKNOWLEDGEMENTS	vii
APPROVAL	viii
DECLARATION	x
LIST OF TABLES	xiv
LIST OF FIGURES	xv
LIST OF ABBREVIATIONS	xxii
CHAPTER	
1 INTRODUCTION	1
1.1 Forced, Free and Mixed Convection	1
1.2 Viscous Fluid	2
1.3 Boundary Layer Theory	3
1.4 The Effects of Prandtl Number on Boundary Layer	5
1.5 Objectives and Scope	7
1.6 Literature Review	8
1.6.1 Free Convection over Cylinders of Elliptic Cross Section	9
1.6.2 Forced and Mixed Convection over Thin Needles	10
1.6.3 Mixed Convection over Slender Cylinder	11
1.6.4 Mixed Convection over Horizontal Circular Cylinder	12
1.6.5 The Keller-box Method	13
1.7 Governing Equations	14
1.7.1 The Dimensional Equations, Boundary Layer and Boussinesq Approximations	15
1.7.2 The Non-dimensional Equations	23
1.7.3 Non-similar Transformation	24
1.8 Thesis Outline	25
2 THE KELLER-BOX METHOD	27
2.1 Introduction	27
2.2 The Finite Difference Method	28



2.3	Newton Method	33
2.4	Block Elimination Method	37
2.5	Initial Conditions	46
3	FREE CONVECTION BOUNDARY LAYER FLOW OVER CYLINDERS OF ELLIPTIC CROSS SECTION	51
3.1	Introduction	51
3.2	Constant Surface Heat Flux	52
	3.2 Mathematical Formulation	52
	3.3 Solution Procedure	53
	3.4 Results and Discussion	55
3.2	Temperature-dependent Viscosity	67
	3.2 Mathematical Formulation	67
	3.3 Solution Procedure	70
	3.4 Results and Discussion	71
3.5	Conclusions	83
4	FORCED CONVECTION BOUNDARY LAYER FLOW OVER A MOVING THIN NEEDLE	85
4.1	Introduction	85
4.2	Mathematical Formulation	87
4.3	Solution Procedure	89
4.4	Results and Discussion	91
4.5	Conclusions	98
5	MIXED CONVECTION BOUNDARY LAYER FLOW ALONG VERTICAL THIN NEEDLES	100
5.1	Introduction	100
5.2	Mathematical Formulation	101
5.3	Solution Procedure	103
5.4	Results and Discussion	105
5.5	Conclusions	111
6	MIXED CONVECTION BOUNDARY LAYER FLOW ALONG VERTICAL MOVING THIN NEEDLES	112
6.1	Introduction	112
6.2	Variable Wall Temperature	114
	6.2.1 Mathematical Formulation	114
	6.2.2 Solution Procedure	116
	6.2.3 Results and Discussion	117



6.3	Variable Surface Heat Flux	124
	6.3.1 Mathematical Formulation	124
	6.3.2 Solution Procedure	126
	6.3.3 Results and Discussion	127
6.4	Conclusions	134
7	MIXED CONVECTION BOUNDARY LAYER FLOW ALONG A VERTICAL MOVING SLENDER CYLINDER	136
	7.1 Introduction	136
	7.2 Mathematical Formulation	137
	7.3 Solution Procedure	140
	7.4 Results and Discussion	143
	7.5 Conclusions	149
8	MIXED CONVECTION BOUNDARY LAYER FLOW PAST AN ISOTHERMAL HORIZONTAL CIRCULAR CYLINDER WITH TEMPERATURE-DEPENDENT VISCOSITY	151
	8.1 Introduction	151
	8.2 Mathematical Formulation	153
	8.3 Solution Procedure	157
	8.4 Results and Discussion	159
	8.5 Conclusions	166
9	CONCLUSIONS	168
	9.1 Summary of Research	168
	9.2 Further Research	171
	REFERENCES	173
	APPENDICES	187
	BIODATA OF STUDENT	208



LIST OF TABLES

Table		Page
3.1	Values of the cylinder temperature θ_w for $Pr = 1$ with blunt orientation ($b_c/a_c = 0.1$ and 0.25) compared to Merkin (1977a)	57
3.2	Values of the cylinder temperature θ_w for $Pr = 1$ with blunt orientation ($b_c/a_c = 0.5$ and 0.75) compared to Merkin (1977a)	58
3.3	Values of the cylinder temperature θ_w for $Pr = 1$ with slender orientation ($b_c/a_c = 1$ and 0.75) compared to Merkin (1977a)	59
3.4	Values of the cylinder temperature θ_w for $Pr = 1$ with slender orientation ($b_c/a_c = 0.5$ and 0.25) compared to Merkin (1977a)	60
3.5	Values of the heat transfer q_w for $Pr = 1$ with blunt orientation ($b_c/a_c = 0.1$ and 0.25) when $\theta_r \rightarrow -\infty$	73
3.6	Values of the heat transfer q_w for $Pr = 1$ with blunt orientation ($b_c/a_c = 0.5$ and 0.75) when $\theta_r \rightarrow -\infty$	74
3.7	Values of the heat transfer q_w for $Pr = 1$ with slender orientation ($b_c/a_c = 1$ and 0.75) when $\theta_r \rightarrow -\infty$	75
3.8	Values of the heat transfer q_w for $Pr = 1$ with slender orientation ($b_c/a_c = 0.5$ and 0.25) when $\theta_r \rightarrow -\infty$	76
4.1	Skin friction coefficient $C_f Re^{1/2}$ over thin needles for $m = 0$	93
4.2	Values of $\theta'(a)$ over thin needles for $m = 0$ and $a = 0.1$	93



LIST OF FIGURES

Figure		Page
1.1	The velocity and thermal boundary layers	4
1.2	The effect of Prandtl number Pr on velocity and thermal boundary layers thicknesses	6
1.3	The types of fluid for various values of Prandtl number Pr	7
1.4	Physical model and coordinate system for free convection over a cylinder of elliptic cross section	18
2.1	Net rectangle for difference approximations	29
2.2	Flow diagram for the Keller-box method	50
3.1	Physical model and coordinate system for free convection over a cylinder of elliptic cross section with constant surface heat flux	53
3.2	The local skin friction coefficient C_f for various Pr with blunt orientation ($b_c/a_c = 0.1$)	61
3.3	The cylinder temperature θ_w for various Pr with blunt orientation ($b_c/a_c = 0.1$)	61
3.4	The local skin friction C_f coefficient for various Pr with slender orientation ($b_c/a_c = 0.75$)	62
3.5	The cylinder temperature θ_w for various Pr with slender orientation ($b_c/a_c = 0.75$)	62
3.6	The local skin friction coefficient C_f for $Pr = 0.7$ and 6.8 with blunt orientation (various b_c/a_c)	64



3.7	The cylinder temperature θ_w for $Pr = 0.7$ and 6.8 with blunt orientation (various b_c/a_c)	64
3.8	The local skin friction coefficient C_f for $Pr = 0.7$ and 6.8 with slender orientation (various b_c/a_c)	65
3.9	The cylinder temperature θ_w for $Pr = 0.7$ and 6.8 with slender orientation (various b_c/a_c)	65
3.10	Velocity profiles f' at lower stagnation point of the cylinder, $x = 0$ for various Pr with $b_c/a_c = 0.1$ (blunt orientation)	66
3.11	Temperature profiles θ at lower stagnation point of the cylinder, $x = 0$ for various Pr with $b_c/a_c = 0.1$ (blunt orientation)	67
3.12	Physical model and coordinate system for free convection over a cylinder of elliptic cross section with temperature-dependent viscosity	68
3.13	Heat transfer q_w for $Pr = 1$ (blunt: $b_c/a_c = 0.1$)	77
3.14	Heat transfer q_w for $Pr = 1$ (blunt: $b_c/a_c = 0.25$)	78
3.15	Heat transfer q_w for $Pr = 1$ (blunt: $b_c/a_c = 0.5$)	78
3.16	Heat transfer q_w for $Pr = 1$ (blunt: $b_c/a_c = 0.75$)	79
3.17	Heat transfer q_w for $Pr = 6.8$ (slender: $b_c/a_c = 1.0$)	79
3.18	Heat transfer q_w for $Pr = 6.8$ (slender: $b_c/a_c = 0.75$)	80
3.19	Heat transfer q_w for $Pr = 6.8$ (slender: $b_c/a_c = 0.5$)	80
3.20	Heat transfer q_w for $Pr = 6.8$ (slender: $b_c/a_c = 0.25$)	81
3.21	Temperature profiles θ at $\zeta \approx 0$ for blunt orientation with $b_c/a_c = 0.1$ for $Pr = 1$ and 6.8	82

3.22	Temperature profiles θ at $\zeta \approx 0$ for slender orientation with $b_c/a_c = 0.25$ for $Pr = 1$ and 6.8	82
4.1	Physical model and coordinate system for forced convection over a moving thin needle	88
4.2	Variation of the skin friction coefficient $C_f Re^{1/2}$ with a when $m = 0$	94
4.3	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with a for various values of Pr when $m = 0$	95
4.4	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with Pr for various values of a when $m = 0$	96
4.5	Velocity profiles f' for various values of a when $m = 0$	97
4.6	Temperature profiles θ for various values of a when $Pr = 0.7$ (air) and $m = 0$	97
4.7	Temperature profiles θ for various values of Pr when $m = 0$ and $a = 0.01$	98
5.1	Physical model and coordinate system for mixed convection along a vertical thin needle	102
5.2	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 0$ (paraboloid)	106
5.3	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 0$ (paraboloid)	107
5.4	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 1$ (cylinder)	108
5.5	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 1$ (cylinder)	108

5.6	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = -1$ (cone)	109
5.7	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = -1$ (cone)	109
5.8	Velocity profiles f' for various values of a with $Pr = 0.7$, $m = 1$ and $\lambda = -3$	110
5.9	Temperature profiles θ for various values of a with $Pr = 0.7$, $m = 1$ and $\lambda = -3$	110
6.1	Physical model and coordinate system for mixed convection along a vertical moving thin needle with variable wall temperature	115
6.2	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 0$	118
6.3	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 0$	119
6.4	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = 2.5$ (assisting flow)	120
6.5	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = 2.5$ (assisting flow)	120
6.6	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = -2.5$ (opposing flow)	121
6.7	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = -2.5$ (opposing flow)	122
6.8	Velocity profiles f' for various values of a with $Pr = 0.7$, $m = 0$ and $\lambda = 5$ (assisting flow)	123
6.9	Temperature profiles θ for various values of a with $Pr = 0.7$, $m = 0$ and $\lambda = 5$ (assisting flow)	123



6.10	Physical model and coordinate system for mixed convection along a vertical moving thin needle with variable surface heat flux	125
6.11	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with λ for various values of a when $Pr = 0.7$ and $m = 0$	128
6.12	Variation of the reduced surface temperature $\theta(a)$ with λ for various values of a when $Pr = 0.7$ and $m = 0$	129
6.13	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = 3$ (assisting flow)	130
6.14	Variation of the reduced surface temperature $\theta(a)$ with Pr for various values of a when $m = 0$ and $\lambda = 3$ (assisting flow)	130
6.15	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Pr for various values of a when $m = 0$ and $\lambda = -3$ (opposing flow)	132
6.16	Variation of the reduced surface temperature $\theta(a)$ with Pr for various values of a when $m = 0$ and $\lambda = -3$ (opposing flow)	132
6.17	Velocity profiles f' for various values of a with $Pr = 0.7$, $m = 0$ and $\lambda = 5$ (assisting flow)	133
6.18	Temperature profiles θ for various values of a with $Pr = 0.7$, $m = 0$ and $\lambda = 5$ (assisting flow)	134
7.1	Physical model and coordinate system for mixed convection along a moving vertical slender cylinder	138
7.2	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Λ for the case of assisting flow with various values of Pr and $\hat{\lambda}$	144
7.3	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with Λ for the case of assisting flow with various values of Pr and $\hat{\lambda}$	144
7.4	Variation of the skin friction coefficient $C_f Re_x^{1/2}$ with Λ for the case of opposing flow with various values of Pr and $\hat{\lambda}$	145



7.5	Variation of the local Nusselt number $Nu_x Re_x^{-1/2}$ with Λ for the case of opposing flow with various values of Pr and $\hat{\lambda}$	146
7.6	The effect of transverse curvature Λ on velocity profiles f' for the case of assisting flow with $\hat{\lambda} = 1$ and Pr = 0.7	147
7.7	The effect of transverse curvature Λ on temperature profiles θ for the case of assisting flow with $\hat{\lambda} = 1$ and Pr = 0.7	147
7.8	The effect of modified mixed convection parameter $\hat{\lambda}$ on velocity profiles f' for the case of assisting flow with $\Lambda = 3.21$ and Pr = 0.7, 6.8, 10	148
7.9	The effect of modified mixed convection parameter $\hat{\lambda}$ on temperature profiles θ for the case of assisting flow with $\Lambda = 3.21$ and Pr = 0.7, 6.8, 10	149
8.1	Physical model and coordinate system for mixed convection past a horizontal circular cylinder	155
8.2	The skin friction coefficient C_f for various values of λ when Pr = 1 (case of constant viscosity)	160
8.3	The Nusselt number Nu for various values of λ when Pr = 1 (case of constant viscosity)	161
8.4	The skin friction coefficient C_f for various values of θ_r when Pr = 0.7 and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	162
8.5	The Nusselt number Nu for various values of θ_r when Pr = 0.7 and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	163
8.6	The skin friction coefficient C_f for various values of θ_r when Pr = 7 and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	163
8.7	The Nusselt number Nu for various values of θ_r when Pr = 7 and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	164



8.8	Variation of the separation point x_s with λ for $\text{Pr} = 0.7$ when $ \theta_r = 2, 4$ and $ \theta_r \rightarrow \infty$ (constant viscosity)	165
8.9	Variation of the separation point x_s with λ for $\text{Pr} = 7$ when $ \theta_r = 2, 4$ and $ \theta_r \rightarrow \infty$ (constant viscosity)	165
8.10	Variation of the separation point x_s with λ for $\text{Pr} = 1$ when $ \theta_r \rightarrow \infty$ (constant viscosity)	166



LIST OF ABBREVIATIONS

a	dimensionless needle size
a_c	length of semi-major axis for a cylinder of elliptic cross section
a_{cc}	radius of the circular cylinder
b_c	length of semi-minor axis for a cylinder of elliptic cross section
C_f	skin friction coefficient
f	non-dimensional stream function
g	acceleration due to gravity
Gr	Grashof number
k	thermal conductivity of the fluid
m	power index
Nu	Nusselt number
Nu_x	local Nusselt number
Pr	Prandtl number
q_w	heat flux from the cylinder
$R(x)$	non-dimensional needle radius
Re	Reynolds number
Re_x	local Reynolds number
T	non-dimensional fluid temperature
T_r	reference temperature
T_w	needle or cylinder temperature
T_∞	ambient temperature
u, v	non-dimensional velocity components along the x - and y - directions, respectively, for a cylinder of elliptic cross section and a circular cylinder



u, v	non-dimensional velocity components along the x – and r – directions, respectively, for a thin needle and a slender cylinder
$u_e(x)$	non-dimensional velocity outside boundary layer
U_∞	free stream velocity
x, y	non-dimensional Cartesian coordinates along the surface of the cylinder and normal to it, respectively, for a cylinder of elliptic cross section and a circular cylinder
x, r	non-dimensional axial and radial coordinates, respectively, for a thin needle and a slender cylinder
x_s	boundary layer separation point

Greek symbols

α	thermal diffusivity
β	thermal expansion coefficient
δ_h	velocity boundary layer thickness
δ_T	thermal boundary layer thickness
ΔT	characteristic temperature
η	similarity variable
γ	thermal property of the fluid
θ	non-dimensional temperature
θ_r	viscosity/temperature parameter
λ	mixed convection parameter
$\hat{\lambda}$	modified mixed convection parameter
Λ	transverse curvature parameter
ν	kinematic viscosity
ν_∞	constant kinematic viscosity of the ambient fluid

μ	dynamic viscosity
μ_∞	constant dynamic viscosity of the ambient fluid
ξ	non-dimensional coordinate
ρ	fluid density
τ_w	wall shear stress
ψ	stream function
ζ	eccentric angle of a cylinder of elliptic cross section

Subscripts

c	refers to a cylinder of elliptic cross section
cc	refers to a circular cylinder
w	condition at the surface of the cylinder
∞	ambient/free stream condition

Superscripts

'	differentiation with respect to y
-	dimensional variables