



UNIVERSITI PUTRA MALAYSIA

***BIO-OIL PRODUCTION VIA SOLVOLYSIS OF OIL PALM EMPTY FRUIT
BUNCH USING ZN-SUPPORTED ZEOLITE CATALYST***

RACHEL TANG DUO YAO

FS 2017 70



**BIO-OIL PRODUCTION VIA SOLVOLYSIS OF OIL PALM EMPTY FRUIT
BUNCH USING ZN-SUPPORTED ZEOLITE CATALYST**

By

RACHEL TANG DUO YAO

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,
in Fulfillment of the Requirements for the Degree of
Master of Science**

May 2017

COPYRIGHT

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



DEDICATION

This thesis is dedicated to my family, especially to my beloved aunt, Madam Lim Chiew Neo for her love and support, my siblings and last but not least, my beloved grandmother. Thank you very much.



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfillment of the requirement for the Degree of Master of Science

BIO-OIL PRODUCTION VIA SOLVOLYSIS OF OIL PALM EMPTY FRUIT BUNCH USING ZN-SUPPORTED ZEOLITE CATALYST

By

RACHEL TANG DUO YAO

May 2017

Chairman : Professor Taufiq-Yap Yun Hin, PhD
Faculty : Science

Biomass is one of the renewable energy that has been revealing its potential as a substituent for natural fossil fuels recently. Nowadays, converting biomass via liquefaction technology appears to be another alternative to obtain valuable high energy products such as biofuel, gas and char. In this study, oil palm empty fruit bunch (EFB) has been chosen as the source of biomass for biomass-to-biofuel conversion. The main focus of the study was on the presence of different composition of Zn supported on zeolite ZSM-5 as solid acid catalyst to enhance the production of bio-oil from the biomass. The prepared catalysts were characterized using X-ray diffraction (XRD), *Brunauer–Emmett–Teller* (BET), field-emission scanning electron microscope with energy-dispersive X-Ray spectroscopy (FE-SEM/EDX) and temperature-programmed desorption (TPD)–NH₃. Gas chromatography mass spectroscopy (GC-MS) was employed for bio-oil analysis. Conversion of EFB to liquid products was carried out by using an autoclave. The production of bio-oil from EFB was subjected to a series of optimization tests: reaction temperature, reaction time, catalyst loading and catalyst composition. The optimum condition for the conversion of EFB to liquid products was achieved at 180°C for 90 min with 0.5wt% of 15% Zn supported on ZSM-5. Without the presence of the catalyst, there are many compounds found in the bio-oil such as aromatics compounds, phenols and others. In contrast, high selectivity towards the production of furfural (approximate 83% of total compounds in the bio-oil) was reported under optimum condition with the presence of catalyst. Phenols were also found to be the second highest compound obtained after furfural (~8.2%). This value-added product obtained in this study is a very useful chemical feedstock especially in adhesive industry.

Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk Ijazah Master Sains

**PENGHASILAN BIO-MINYAK MELALUI SOLVOLISIS KELAPA SAWIT
TANDAN BUAH KOSONG DENGAN MENGGUNAKAN PEMANGKIN Zn
BERPENYOKONG ZEOLIT**

Oleh

RACHEL TANG DUO YAO

Mei 2017

Pengerusi : Profesor Taufiq-Yap Yun Hin, PhD
Fakulti : Sains

Biojisim adalah salah satu tenaga boleh diperbaharui yang telah mendedahkan potensinya sebagai gantikan bahan api fosil semula jadi baru-baru ini. Pada masa kini, penukaran biojisim melalui teknologi pencairan telah menjadi salah satu alternatif untuk mendapatkan produk tenaga tinggi yang berharga seperti bahan api bio, gas dan arang. Dalam kajian ini, kelapa sawit tandan buah kosong (EFB) telah dipilih sebagai sumber biojisim untuk penukaran biojisim ke bahan api bio. Fokus utama kajian ini adalah untuk mengenai kesan komposisi zink yang berbeza disokong pada pemangkin zeolite ZSM-5 bagi meningkatkan pengeluaran minyak bio daripada biojisim. Ciri-ciri pemangkin yang telah disediakan telah dianalisis oleh pembelauan sinar-X (XRD), analisis luas permukaan Brunauer-Emmett-Teller (S_{BET}), mikroskop imbasan elektron pancaran medan yang dilengkapi dengan tenaga serakan spektroskopi sinar-X (FE-SEM/EDX) dan penyahjerapan suhu terancang- NH_3 (TPD- NH_3). Gas kromatografi yang dilengkapi dengan spektroskopi jisim (GC-MS) telah digunakan untuk analisis bio-minyak. Penukaran EFB kepada produk cecair telah dilakukan dengan menggunakan autoklaf. Penghasilan bio-minyak daripada EFB telah dikaji melalui siri ujian optimasi: suhu reaksi, masa reaksi, muatan pemangkin dan komposisi pemangkin. Keadaan optimum bagi penukaran EFB ke produk cecair telah dicapai pada suhu $180^{\circ}C$ selama 90 min dengan 0.5 peratusan jisim daripada 15% Zn disokong pada ZSM-5. Tanpa pemangkin, sebatian-sebatian yang dapat dikesan dalam bio-minyak yang dihasilkan adalah seperti kompaun aromatik, fenol dan lain-lain. Sebaliknya, pemilihan yang tinggi terhadap penghasilan fufural (anggaran 83% daripada jumlah sebatian bio-minyak) dicapai di bawah keadaan optimum dengan kehadiran pemangkin. Fenol juga dikenali sebagai sebatian kedua tinggi yang diperolehi selepas fufural ($\sim 8.2\%$). Produk nilai tambah yang diperolehi dalam kajian ini adalah bahan mentah kimia yang sangat berguna terutamanya dalam industri pelekat.

ACKNOWLEDGEMENTS

First and foremost, I would like to take this opportunity to thank God for His guidance, leading and faithfulness throughout the years of my master degree.

Sincere and deepest appreciation to my supervisor, Prof. Dr. Taufiq Yap Yun Hin for his generous guidance, dedicated supervision, precious advices, encouragements, tolerance and unfailing help throughout the course of this work.

Special thanks to all my lab mates in PutraCAT for their priceless help, advices, suggestions, encouragements, supports and companion. Not forgetting all the staffs in the Department of Chemistry, Faculty of Science for giving their hands in helping me for my data analysis.

Financial support from Universiti Putra Malaysia and sponsorship from the Ministry of Education is also gratefully acknowledged.

Last but not least, I am very grateful for my beloved family and friends for their endurance, unconditional love and trust in my capability that makes this work come to past.

Thank you.

This thesis was submitted to the Senate of the Universiti Putra Malaysia and has been accepted as fulfillment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

Taufiq-Yap Yun Hin, PhD

Professor
Faculty of Science
Universiti Putra Malaysia
(Chairman)

Zulkarnain Zainal, PhD

Professor
Faculty of Science
Universiti Putra Malaysia
(Member)

ROBIAH BINTI YUNUS, PhD

Professor and Dean
School of Graduate Studies
Universiti Putra Malaysia

Date:

Declaration by graduate student

I hereby confirm that:

- this thesis is my original work;
- quotations, illustrations and citations have been duly referenced;
- this thesis has not been submitted previously or concurrently for any other degree at any institutions;
- intellectual property from the thesis and copyright of thesis are fully-owned by Universiti Putra Malaysia, as according to the Universiti Putra Malaysia (Research) Rules 2012;
- written permission must be obtained from supervisor and the office of Deputy Vice-Chancellor (Research and innovation) before thesis is published (in the form of written, printed or in electronic form) including books, journals, modules, proceedings, popular writings, seminar papers, manuscripts, posters, reports, lecture notes, learning modules or any other materials as stated in the Universiti Putra Malaysia (Research) Rules 2012;
- there is no plagiarism or data falsification/fabrication in the thesis, and scholarly integrity is upheld as according to the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) and the Universiti Putra Malaysia (Research) Rules 2012. The thesis has undergone plagiarism detection software

Signature: _____ Date: _____

Name and Matric No.: Rachel Tang Duo Yao , GS 30887

TABLE OF CONTENTS

	Page
ABSTRACT	i
ABSTRAK	ii
ACKNOWLEDGEMENTS	iii
APPROVAL	iv
DECLARATION	vi
LIST OF TABLES	x
LIST OF FIGURES	xi
LIST OF ABBREVIATIONS	xiii
 CHAPTER	
1 INTRODUCTION	1
1.1 Background and Definitions	1
1.1.1 Worldwide Energy Consumption and Consequences	1
1.1.2 Biomass: The Promising Renewable Energy Source and Its Advantages	2
1.1.3 Catalyst	4
1.2 Problem Statement	5
1.3 Objectives	6
1.4 Scope of study	7
 2 LITERATURE REVIEW	8
2.1 Biomass: The Biofuel Feedstock	8
2.1.1 Oil Palm Biomass as Renewable Energy Source	8
2.1.2 Oil Palm Empty Fruit Bunch (EFB)	10
2.2 Thermochemical Conversion of Biomass	11
2.2.1 Pyrolysis	12
2.2.2 Gasification	13
2.2.3 Liquefaction	14
2.3 Direct Liquefaction of Biomass	15
2.4 Catalyzed Liquefaction of Biomass	16
2.4.1 Liquefaction by Homogeneous Catalysts	16
2.4.2 Liquefaction by Heterogeneous Catalysts	17
2.5 Previous Studies on Bio-oil Production from Oil Palm Empty Fruit Bunch (EFB)	18
2.6 Catalytic Biomass Conversion using Zeolite ZSM-5 Catalyst	19
 3 MATERIALS AND METHODOLOGY	20
3.1 Chemicals and Materials	20
3.2 Catalyst Preparation	20
3.3 Characterization of Catalyst	22
3.3.1 X-Ray Diffraction Analysis (XRD)	22
3.3.2 X-Ray Fluorescence Spectroscopy (XRF)	23

3.3.3	Brunauer-Emmer-Teller Surface Area Measurement (S_{BET})	23
3.3.4	Temperature-Programmed-Desorption of Ammonia (TPD-NH ₃)	23
3.3.5	Field Emission Scanning Electron Microscopy/Energy Dispersive X-Ray (FE-SEM/EDX)	24
3.4	Characterization of Biomass	24
3.5	Bio-oil Synthesis	24
3.6	Bio-oil Characterization	26
3.6.1	Gas Chromatography Mass Spectrometry (GC/MS)	26
4	RESULTS AND DISCUSSION	27
4.1	Catalyst Characterization	27
4.1.1	X-Ray Diffraction Analysis (XRD)	27
4.1.2	X-Ray Fluorescence Spectroscopy (XRF)	28
4.1.3	Brunauer-Emmer-Teller Surface Area Measurement (S_{BET})	29
4.1.4	Temperature-Programmed-Desorption of Ammonia (TPD-NH ₃)	30
4.1.5	Field Emission Scanning Electron Microscopy/Energy Dispersive X-Ray (FE-SEM/EDX)	33
4.2	Biomass Characterization	40
4.3	Catalytic Activity	41
4.3.1	Pre-optimization	42
4.3.2	Effect of Catalyst Composition on Yield	43
4.3.3	Effect of Temperature on Yield	46
4.3.4	Effect of Reaction Time on Yield	48
4.3.5	Effect of Catalyst Loading on Yield	49
4.4	Analysis of The Composition of Bio-oil by GC-MS	51
4.4.1	Uncatalyzed Reaction	51
4.4.2	Catalyzed Reaction at Optimum Condition	53
5	CONCLUSIONS AND RECOMMENDATIONS FOR FUTURE RESEARCH	55
5.1	Conclusion	55
5.2	Future Research Recommendation	56
	REFERENCES	57
	APPENDICES	65
	BIODATA OF STUDENT	68
	LIST OF PUBLICATIONS	69

LIST OF TABLES

Table	Page
2.1 Oil palm biomass collected in 2005 (Shuit <i>et al.</i> , 2009)	9
2.2 Analysis of EFB generated from Malaysian palm oil mills (Hosseini and Wahid, 2014).	11
2.3 Operational parameters and products for direct liquefaction, flash pyrolysis, pyrolysis and gasification (Behrendt <i>et al.</i> , 2008).	15
3.1 List of chemicals used.	20
3.2 Actual weight of zinc sulphate heptahydrate ($\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$) added to parent catalyst zeolite ZSM-5.	22
4.1 Metal composition (%) from XRF analysis.	29
4.2 Specific surface area of each catalyst.	30
4.3 The acid strength of all the catalysts	33
4.4 Distribution of elements in catalysts.	38
4.5 Weight percentage (%) of each element for each modified catalysts.	40
4.6 The composition analysis of EFB fiber.	41
4.7 Compound found in bio-oil converted without the presence of catalyst under 180°C for 90 mins.	52
4.8 Composition of bio-oil obtained under optimum condition	53

LIST OF FIGURES

Figure	Page
1.1 World total primary energy supply from 1971 to 2013 by fuel (Mtoe) (Key World Energy Statistics, OECD/IEA, 2015)	1
1.2 1971 and 2013 fuel shares of total final consumption (Key World Energy Statistics, OECD/IEA, 2015)	2
1.3 Biomass produced from different industry in Malaysia (Shuit <i>et al.</i> , 2009)	3
1.4 Comparison of activation energy between catalyzed and uncatalyzed reaction (Clark, 2012)	5
2.1 World's oil production in 2007 (MPOC, 2007)	9
2.2 The conversion technologies of oil palm biomass (Shuit <i>et al.</i> , 2009; Hosseini and Wahid, 2014)	12
3.1 Flowchart of $\chi\%$ Zn/ZSM-5 catalyst preparation and characterization	21
3.2 Schematic Diagram for the liquefaction of the biomass	25
4.1 X-Ray Diffraction pattern of the synthesized catalyst of different composition	28
4.2 TPD-NH ₃ profile of ZSM-5, 5%Zn/ZSM-5, 10%Zn/ZSM-5, 15%Zn/ZSM-5 and 20%Zn/ZSM-5	32
4.3 FESEM of (a) ZSM-5, (b) 5%Zn/ZSM-5, (c) 10%Zn/ZSM-5, (d) 15%Zn/ZSM-5 and (e) 20%Zn/ZSM-5.	34
4.4 (a) EDX spectrum for ZSM-5. (b) EDX spectrum for 5%Zn/ZSM-5, (c) EDX spectrum for 10%Zn/ZSM-5, (d) EDX spectrum for 15%Zn/ZSM-5, (e) EDX spectrum for 20%Zn/ZSM-5.	35
4.5 Effect of temperature on the bio-oil yield without the presence of catalyst. Reaction condition: EFB amount of 5.0g, reaction temperature from 140°C to 220°C, reaction time of 90 min.	43
4.6 Effect of zinc oxide concentration on yield. Reaction condition: EFB amount of 5.0g, reaction temperature of 180°C, catalyst amount of 0.5w/w%, reaction time of 90 min.	44

4.7	Proposed mechanism for biomass derived furfural formation over ZnO supported zeolite catalyst. (Choudhary <i>et al.</i> , 2011)	45
4.8	Effect of temperature on yield. Reaction condition: EFB amount of 5.0g, reaction time of 90 min, catalyst amount of 0.5w/w%, Zn amount of 15wt% of ZSM-5.	47
4.9	Effect of reaction time on yield. Reaction condition: EFB amount of 5.0g, reaction temperature of 180°C, catalyst amount of 0.5w/w%, Zn amount of 15wt% of ZSM-5.	48
4.10	Effect of catalyst loading on yield. Reaction conditions: EFB amount 5.0g, reaction temperature of 180°C, reaction time of 90 min, Zn amount of 15wt% ZSM-5.	50
4.11	GC-MS graph of bio-oil obtained without the presence of catalyst at optimum condition. Reaction conditions: EFB amount of 5.0g, reaction time of 90 min, reaction temperature of 180°C.	52
4.12	GC-MS graph of bio-oil obtained with the presence of catalyst under optimum condition. Reaction conditions: EFB amount of 5.0g, reaction time of 90 min, reaction temperature of 180°C, catalyst loading of 0.5w/w%, Zn amount of 15wt% of ZSM-5.	54

LIST OF ABBREVIATIONS

DEG	Diethylene glycol
DES	Diethyl Ether Soluble
E _a	Activation energy
EC	Ethylene carbonate
EFB	Empty Fruit Bunch
EG	Ethylene glycol
FE-SEM	Field Emission Scanning Electron Microscopy
GC-MS	Gas Chromatography Mass Spectrometry
JCPDS	Joint Committee of Powder Diffraction Standards
LPY	Liquid Product Yield
MFI	Mordenite Framework Inverted
PG	Propylene glycol
RES	Renewable Energy Sources
S _{BET}	<i>Brunauer-Emmett-Teller</i> Surface Area Measurement
TPD-NH ₃	Temperature Programmed Desorption of Ammonia
WS	Water Soluble
XRD	X-Ray Diffraction
XRF	X-Ray Fluorescence Spectroscopy
ZC	Calcined Zeolite ZSM-5
Zn	Zinc

CHAPTER 1

INTRODUCTION

1.1 Background and definitions

1.1.1 Worldwide Energy Consumption and Consequences

Energy is economically and socially required to improve and enhance the quality of human life. Energy could be found in many forms, such as electrical, thermal, chemical, gravitational, mechanical, nuclear, motion and sound. Generally, energy resources that are available in this world have been categorized natural fossils fuels, renewable resources and nuclear resources (Demirbas A, 2000).

In older days, natural fossil fuels such as coal, petroleum and natural gas have been the main source of energy to supply worldwide energy needs. Energy is needed for almost all kind of operations and activities such as economic developments, agriculture, industrialization, transportation and others. **Fig. 1.1** shows the world total primary energy supply from 1971 to 2013 by fuel. The demand for energy from natural fossil fuels such as coal, oil and natural gas is in an almost steady ascending trend from year 1971 to 2013.

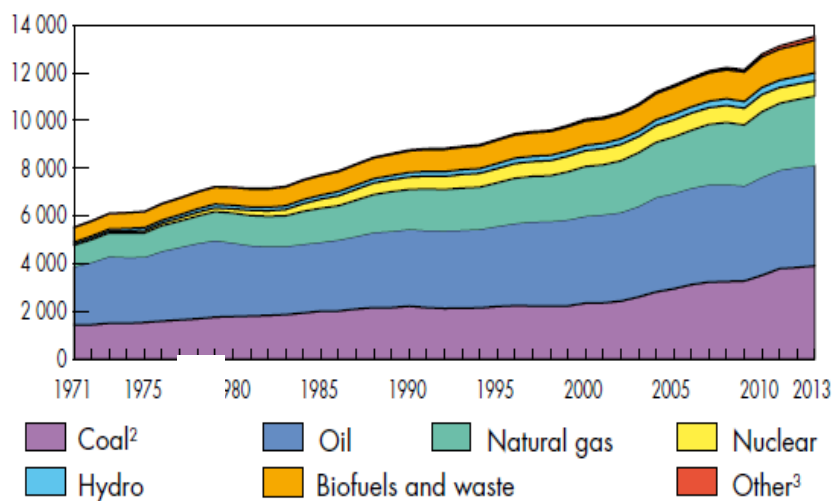


Figure 1.1 : World total primary energy supply from 1971 to 2013 by fuel (Mtoe)
(Key World Energy Statistics, OECD/IEA, 2015)

The role of natural fossil fuel as energy supply is still very important even until today. However, rapid increment in world's population and economic developments increases the demand for energy supply. Furthermore, the large dependence on the usage of fossil fuels to sustain the need of energy supply leads to the occurrence of global environmental issues. Some of the common environmental issues resulting from the utilization of fossil fuel include global warming, ozone depletion, acid rain and greenhouse effect. Due to the negative effects given by fossil fuels, this have stirred up the attention of finding alternatives or substituents to restore the energy source structure and promote greater efficiency of energy, as well as to satisfy the existing energy consumption in this world.

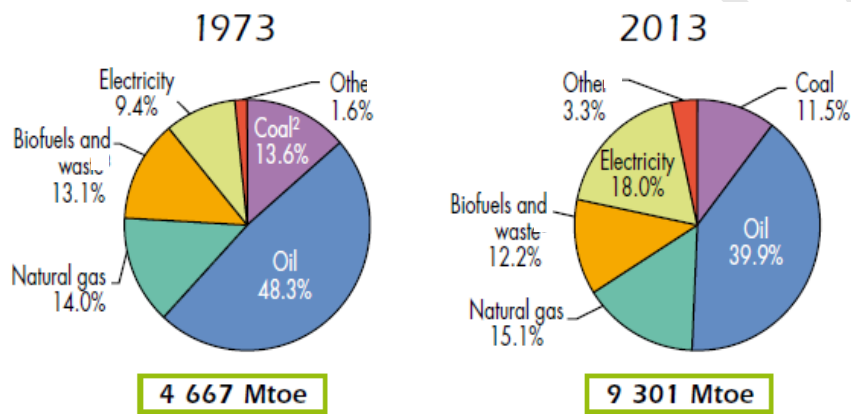


Figure 1.2 : 1971 and 2013 fuel shares of total final consumption
(Key World Energy Statistics, OECD/IEA, 2015)

The fuel shares of total final consumption for 1973 and 2013 are shown in **Fig. 1.2**. According to the statistics above, the total final consumption by fuel increased almost up to 50% in 4 decades time from 1973. This has come to pin point to the importance of the renewable energy as energy supply source in coming decades.

1.1.2 Biomass: The Promising Renewable Energy Source and Its Advantages

Due to the depletion of the natural energy source, renewable energy sources (RES) have been revealing their potential as a substituent for natural fossil fuel as these renewable energy sources offer some advantages over energy produced from fossil fuel. Common RES that are in use include wind, solar, biomass and geothermal (Shuit *et al.*, 2009). Among all the existing renewable energy sources, biomass has attracted a lot of interests as the promising substituent for fossil fuel. The abundance of biomass all around the world has increased its utilization in many aspects, thus replacing crude-based non-renewable energy resources. It is highly remarked that biomass has an important role in future energy supply.

Biomass mainly consists of carbon, hydrogen and oxygen, and is an organic substance from living which mainly includes agricultural crops, forestry residues and sea products. It provides significant environmental advantages and at the same time appears to be the best solution for the substitution of fossil resources in many applications such as heat production, power and fuels for transportation. Apart from being a source of energy supply, chemical and biomaterials production from the biomass is also getting more and more common. In other words, biomass can help to control environmental issues that are related to fossil fuels despite its main function as the source of energy supply.

The source of biomass includes agricultural crops, forestry residues, municipal and solid wastes and others. All these wastes could be converted and are very useful in various applications such as transportation fuels, value-added chemicals, fertilizers and agro-chemicals (Demirbas, 2001; Chan *et al.*, 2014). In Malaysia, biomass produced from different industries is shown in **Fig. 1.3**.

Biomass Produced from Different Industry in Malaysia

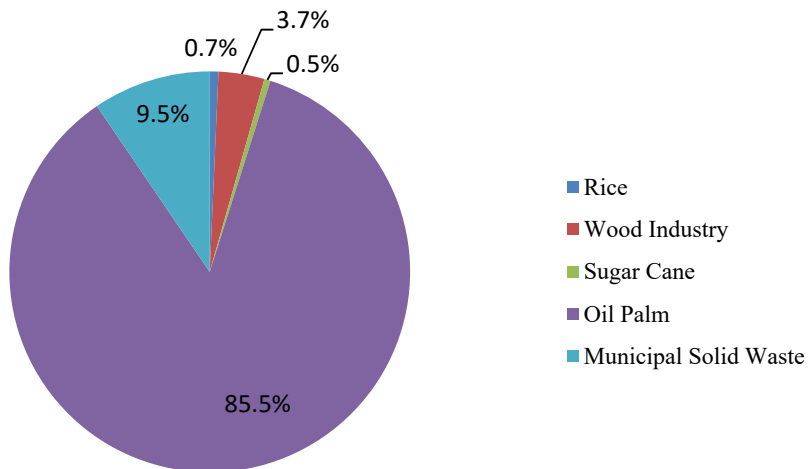


Figure 1.3 : Biomass produced from different industry in Malaysia
(Shuit *et al.*, 2009)

Malaysia is one of the major producers of palm oil in the world. Hence, as shown in the chart above, the biomass produced from oil palm industry has the highest percentage among all the industries in Malaysia, summing up to approximately 85.5% of the total biomass produced. It was reported that as in 2010, Malaysia contributed an incredible amount of oil palm biomass waste, approximately 86.9Mt/year (Ng *et al.*, 2012). As such, the abundance of oil palm biomass waste can be served as feedstock for biomass to biofuel conversion. Looking deep into the biomass produced from oil palm industry, types of biomass produced includes oil palm empty fruit bunch (EFB),

trunks, fronds, fiber, shell, wet shell and palm kernel (Shuit *et al.*, 2009). As a result of that, oil palm empty fruit bunch (EFB) has become a great option to be used as the feedstock of biomass-to-biofuel conversion.

The conversion of biomass into fuel products could be done either biologically or thermochemically. Fermentation and anaerobic digestion are two of the examples of biological conversion of biomass. Meanwhile, examples for thermochemical conversion are gasification, liquefaction and pyrolysis (Pan *et al.*, 2010; Mohan *et al.*, 2006; Demirbaş, 2001; Collard and Blin, 2014). Among these two routes of methods, thermochemically-converted biomass appears to be more promising in obtaining products in three phases: low molecular weight liquid, gas fuel and solid residue (Yaman, 2004).

Biomass could be converted into valuable high energy products effectively such as biofuels, gas and char (Mohan *et al.*, 2006). It is remarked that the liquid fuel from biomass has an important role in future energy supply. There are several advantages offered by biofuel as energy product. Biofuels produced from biomass are environmentally friendly as they do not produce toxic gases such as SO_x and NO_x . Apart from that, these biofuels are renewable, bio-degradable and able to reduce greenhouse effect (Puppan, 2002; Sensöz and Kaynar, 2006; Iliopoulou *et al.*, 2007).

The thermochemically-generated liquid product produced from biomass is called bio-oil. Bio-oil appears to be a dark brown organic liquid with distinctive smoky odor. Another typical property of bio-oil is that bio-oil generated from biomass consists of different size of molecules (Peacocke *et al.*, 1994). One of the biggest advantages offered by bio-oil is the ability to function as liquid fossil fuel substituent (Abdullah and Gerhauser, 2008; Sulaiman *et al.*, 2011). In addition, bio-oil contains valuable chemicals and chemicals extracted from bio-oil are used as food flavorings, resins, adhesives, agrichemicals, and fertilizers (Liu and Zhang, 2008; Yip *et al.*, 2009). Not only that, bio-oil is also used for power generation for diesel engines and turbines.

1.1.3 Catalyst

Catalyst is any substance that accelerates the rate of chemical reaction by lowering activation energy of a specific reaction without itself participating or being consumed in the reaction. The function of a catalyst is best described in **Fig. 1.3**. A catalyst works by providing an alternative pathway with lower activation energy (E_a) compared to non-catalyzed system (Farnetti *et al.*, 2009).

Thermodynamically, reactant must obtain energy that is greater than the activation energy in order for reactants to be able to react and become products. Otherwise, reactants with energy lower than E_a will remain unreacted and unable to go through transition state to react and become products. In this case, the function of the catalyst is magnified as catalyst provides an alternative pathway with lower activation energy

that helps reactant to overcome the energy barrier and able to transform into products successfully. The difference of the activation energy between catalyzed and uncatalyzed reaction is clearly shown in **Fig. 1.4**.

There are two categories of catalyst: homogeneous and heterogeneous catalyst. Homogeneous catalyst can be distinguished from heterogeneous catalyst by the difference of phases in a particular reaction. In homogenous catalyst, the catalyst has the same phase with the reactant or sample feedstock. Meanwhile in heterogeneous catalyst, the reactants and catalyst are not of the same phase.

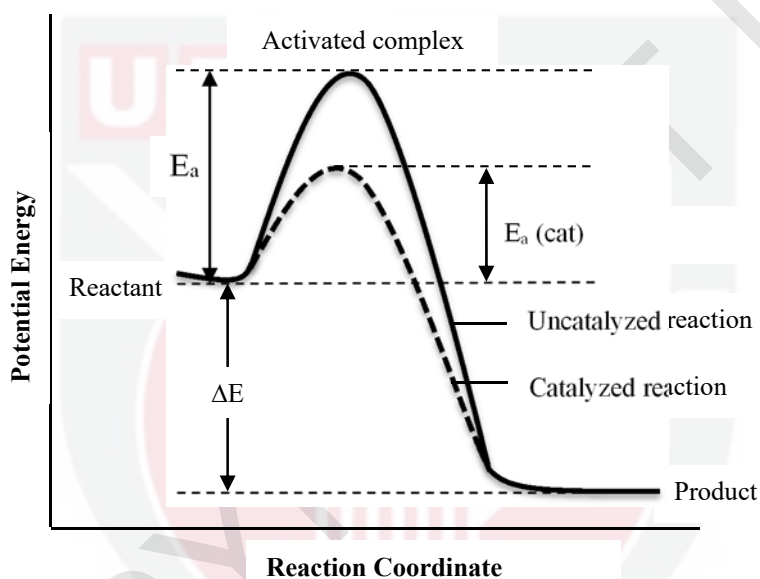


Figure 1.4 : Comparison of activation energy between catalyzed and uncatalyzed reaction (Clark, 2012)

1.2 Problem Statement

In the past two decades, pyrolysis has always been selected as the thermochemical method for the production of bio-oil. Although pyrolysis technology is a promising way to give high yield product, it has become less favorable as reaction time needed is long and temperature needed for this method is high. High operating temperature of pyrolysis gives forth to a very big problem: cross-linking and re-combination reaction between hydrocarbons and aromatics. This may further lead to tar and char formation which eventually causes difficulty in decomposition.

In addition, pyrolysis requires dry biomass in basis prior every treatment and this will lead to substantial energy consumption due to high heat of water vaporization. Moreover, the reaction time for pyrolysis is longer. It is therefore unfeasible from the view of economy. To overcome these matters, solvolysis was used in this research, a method which does not have the disadvantages resulting from pyrolysis.

In most of the biomass conversion, homogeneous catalysts were used instead of heterogeneous catalyst. Effect of heterogeneous catalyst on the yield of the liquid product and chemical components derived from the biomass via liquefaction on the other hand is not common. There are limited studies reporting on the biomass-to-bio-oil conversion via liquefaction.

In this work, zinc (in oxide form) supported on zeolite solid acid catalysts was introduced to enhance the production of the bio-oil production. It was reported that zeolite ZSM-5 provides many advantages such as shape selectivity, limited coke deactivation and high thermal activity. Zinc oxide on the other hand has found to be a mild catalyst and the use of zinc oxide as a catalyst has testified to have insignificant effect on the water-insoluble fraction. Zn-supported zeolite catalyst is used to ease the separation of liquid product and the catalyst, in which with the application of heterogeneous catalyst in this study, the problem arising from homogeneous catalyst is overcome.

Conversion of biomass into bio-oil via catalytic solvolysis is dependent on many factors, which includes the choice of biomass, solvent, catalyst, reaction parameters etc. Sources of biomass to be used are such as rice straw, wood, oil palm biomass and municipal solid waste. While different feedstock may vary the final product of the bio-oil, empty fruit bunch has been chosen to be used to convert biomass into bio-oil is due to its main advantage: abundance availability of this feedstock. However the utilization of EFB for biomass-to-biofuel conversion is not very common especially with the enhancement of solid acid catalyst although it has been reported that EFB that has been generated is able to be used as biofuel. It is therefore one of the interest in this study to further expand the utilization of EFB in biomass-to-biofuel conversion.

1.3 Objectives

Generally, there are three objectives in this study:

1. To synthesize a suitable catalyst for the bio-oil production via catalytic solvolysis of oil palm empty fruit bunch fiber.
2. To produce bio-oil from oil palm empty fruit bunch (EFB) fiber via catalytic solvolysis.
3. To optimize the yield of bio-oil by manipulating various parameters, such as temperature, amount of catalyst and reaction time.

1.4 Scope of study

There were two highlights of this study: (1) to prepare Zn/ZSM-5 in an appropriate composition of zinc deposited on zeolite ZSM-5 successfully via wet impregnation method; (2) to produce and optimize the bio-oil produced from EFB fiber with the enhancement of the catalyst synthesized by varying parameters such as temperature, reaction time etc. Characterization tests such as XRD analysis, FE-SEM/EDX, TPD-NH₃ and BET were employed to further analyze the synthesized catalyst, while the chemical composition on the bio-oil produced was determined by GC-MS analysis.

REFERENCES

- Abdullah, N., & Gerhauser, H. (2008). Bio-oil derived from empty fruit bunches. *Fuel*, 87(12), 2606–2613.
- Ahmadzadeh, A. & Zakaria, S. (2007). Kinetics of oil palm empty fruit bunch phenolysis in the presence of sulfuric acid as a catalyst. *Journal of Applied Polymer Science* 106: 3529-3533.
- Aho, A., Kumar, N., Eränen, K., Salmi, T., Hupa, M., & Murzin, D. Y. (2008). Catalytic pyrolysis of woody biomass in a fluidized bed reactor: Influence of the zeolite structure. *Fuel*, 87(12), 2493-2501.
- Akhtar, J., & Amin, N. A. S. (2011). A review on process conditions for optimum bio-oil yield in hydrothermal liquefaction of biomass. *Renewable and Sustainable Energy Reviews*, 15(3), 1615–1624.
- Akhtar, J., Kuang, S. K., & Amin, N. S. (2010). Liquefaction of empty palm fruit bunch (EPFB) in alkaline hot compressed water. *Renewable Energy*, 35(6), 1220–1227.
- Alswata, A. A., Ahmad, M. Bin, Al-Hada, N. M., Kamari, H. M., Hussein, M. Z. Bin, & Ibrahim, N. A. (2017). Preparation of Zeolite/Zinc Oxide Nanocomposites for toxic metals removal from water. *Results in Physics*, 7, 723–731.
- Awalludin, M. F., Sulaiman, O., Hashim, R., & Nadhari, W. N. A. W. (2015). An overview of the oil palm industry in Malaysia and its waste utilization through thermochemical conversion, specifically via liquefaction. *Renewable and Sustainable Energy Reviews*, 50, 1469–1484.
- Badin, J. & Kirschner, J. (1980). Biomass greens US power production. *Renewable Energy World*, 1, 40-45.
- Batistela, V. R., Fogaça, L. Z., Fávaro, S. L., Caetano, W., Fernandes-Machado, N. R. C., & Hioka, N. (2017). ZnO supported on zeolites: Photocatalyst design, microporosity and properties. *Colloids and Surfaces A: Physicochemical and Engineering Aspects*, 513, 20–27.
- Behrendt, F., Neubauer, Y., Oevermann, M., Wilmes, B., & Zobel, N. (2008). Direct liquefaction of biomass. *Chemical Engineering and Technology*, 31(5), 667–677.
- Bi, Y., Wang, Y., Chen, X., Yu, Z., & Xu, L. (2014). Methanol aromatization over HZSM-5 catalysts modified with different zinc salts. *Chinese Journal of Catalysis*, 35(10), 1740–1751.

- Butler, E., Devlin, G., Meier, D., & McDonnell, K. (2011). A review of recent laboratory research and commercial developments in fast pyrolysis and upgrading. *Renewable and Sustainable Energy Reviews*, 15(8), 4171–4186.
- Chai, F., Cao, F., Zhai, F., Chen, Y., Wang, X., & Su, Z. (2007). Transesterification of Vegetable Oil to Biodiesel using a Heteropolyacid Solid Catalyst. *Advanced Synthesis & Catalysis*, 349(7), 1057–1065.
- Chan, Y. H., Dang, K. V., Yusup, S., Lim, M. T., Zain, A. M., & Uemura, Y. (2014). Studies on catalytic pyrolysis of empty fruit bunch (EFB) using Taguchi's L9 Orthogonal Array. *Journal of the Energy Institute*, 87(3), 227–234.
- Chan, Y. H., Yusup, S., Quitain, A. T., Tan, R. R., Sasaki, M., Lam, H. L., & Uemura, Y. (2015). Effect of process parameters on hydrothermal liquefaction of oil palm biomass for bio-oil production and its life cycle assessment. *Energy Conversion and Management*, 104, 180–188.
- Chan, Y. H., Yusup, S., Quitain, A. T., Uemura, Y., & Sasaki, M. (2014). Bio-oil production from oil palm biomass via subcritical and supercritical hydrothermal liquefaction. *Journal of Supercritical Fluids*, 95, 407–412.
- Chang, S. H. (2014). An overview of empty fruit bunch from oil palm as feedstock for bio-oil production. *Biomass and Bioenergy*, 62, 174–181.
- Chen, Y., Mu, R., Yang, M., Fang, L., Wu, Y., Wu, K., Liu, Y., Gong, J. (2017). Catalytic hydrothermal liquefaction for bio-oil production over CNTs supported metal catalysts. *Chemical Engineering Science*, 161, 299–307.
- Chen, Y., Wu, Y., Zhang, P., Hua, D., Yang, M., Li, Chen, Z., Liu, J. (2012). Direct liquefaction of *Dunaliella tertiolecta* for bio-oil in sub/supercritical ethanol–water. *Bioresource Technology*, 124, 190–198.
- Chew, T. L., & Bhatia, S. (2008). Catalytic processes towards the production of biofuels in a palm oil and oil palm biomass-based biorefinery. *Bioresource Technology*, 99(17), 7911–7922.
- Chin, S. X., Chia, C. H., Zakaria, S., Fang, Z., & Ahmad, S. (2015). Ball milling pretreatment and diluted acid hydrolysis of oil palm empty fruit bunch (EFB) fibres for the production of levulinic acid. *Journal of the Taiwan Institute of Chemical Engineers*, 52, 85–92.
- Choudhary V., Pinar, A. B., Sandler, S. I., Vlachos, D. G. & Lobo, R. F. (2011). Xylose isomerization to xylulose and its dehydration to furfural in aqueous media. *Acs Catalysis*, 1(12), 1724–1728.
- Choudhary, V., Sandler, S. I., & Vlachos, D.G. (2012). Conversion of xylose to furfural using Lewis and Brønsted acid catalysts in aqueous media. *Acs Catalysis*, 2(9), 2022–2028.

- Clark, C. (2012). Principles of General Chemistry. Chapter 14: Chemical Kinetics 1766: *Creative Commons*.
- Clark, J. H. (2002). Solid acids for green chemistry. *Accounts of Chemical Research*, 35(9), 791-797.
- Clausen, B. S., Topsøe, H., & Frahm, R. (1998). Application of Combined X-Ray Diffraction and Absorption Techniques for *in Situ* Catalyst Characterization. *Advances in Catalysis*, 42, 315–344.
- Collard, F. X., & Blin, J. (2014). A review on pyrolysis of biomass constituents: Mechanisms and composition of the products obtained from the conversion of cellulose, hemicelluloses and lignin. *Renewable and Sustainable Energy Reviews*, 38, 594–608.
- Demirbaş, A. (2001). Biomass resource facilities and biomass conversion processing for fuels and chemicals. *Energy Conversion and Management*, 42(11), 1357–1378.
- Demirbas, A. 2000a. Recent advances in biomass conversion technologies. *Energy Education Science and Technology* 6:19–40.
- Demirbas, A., Pehlivan, E., & Altun, T. (2006). Potential evolution of Turkish agricultural residues as bio-gas, bio-char and bio-oil sources. *International Journal of Hydrogen Energy*, 31(5), 613–620.
- Duan, P., & Savage, P. E. (2010). Hydrothermal liquefaction of a microalga with heterogeneous catalysts. *Industrial & Engineering Chemistry Research*, 50(1), 52-61.
- Farnetti, E., Monte, R. D. and Kaspar, J. (2009). Homogeneous and heterogeneous catalysis. In *Inorganic and Bio-inorganic Chemistry Vol 2*. pp. 50-86, Encyclopedia of Life Support Systems
- Fermoso, J., Hernando, H., Jana, P., Moreno, I., Přech, J., Ochoa-Hernández, C., Pizarro, P., Coronado, J. M., Čejka, J., Serrano, D. P. (2016). Lamellar and pillared ZSM-5 zeolites modified with MgO and ZnO for catalytic fast-pyrolysis of eucalyptus woodchips. *Catalysis Today*, 277, 171–181.
- French, R., & Czernik, S. (2010). Catalytic pyrolysis of biomass for biofuels production. *Fuel Processing Technology*, 91(1), 25–32.
- Gayubo, A. G., Aguayo, A. T., Atutxa, A., Prieto, R., & Bilbao, J. (2004). Deactivation of a HZSM-5 zeolite catalyst in the transformation of the aqueous fraction of biomass pyrolysis oil into hydrocarbons. *Energy & fuels*, 18(6), 1640-1647.
- Goyal, H. B., Seal, D., & Saxena, R. C. (2008). Bio-fuels from thermochemical conversion of renewable resources: A review. *Renewable and Sustainable Energy Reviews*, 12(2), 504–517.

- Hasanog, A., Irmak, S., & Erbatur, O. (2014). Bioresource Technology Biofuel production by li quefaction of kenaf (*Hibiscus cannabinus* L .) biomass, *151*, 278–283.
- Hosseini, S. E., & Wahid, M. A. (2014). Utilization of palm solid residue as a source of renewable and sustainable energy in Malaysia. *Renewable and Sustainable Energy Reviews*, *40*, 621–632.
- Huang, J., Long, W., Agrawal, P. K., & Jones, C. W. (2009). Effects of Acidity on the Conversion of the Model Bio-oil Ketone Cyclopentanone on H–Y Zeolites. *The Journal of Physical Chemistry C*, *113*(38), 16702–16710.
- Ibrahim, M. F., Abd-Aziz, S., Yusoff, M. E. M., Phang, L. Y., & Hassan, M. A. (2015). Simultaneous enzymatic saccharification and ABE fermentation using pretreated oil palm empty fruit bunch as substrate to produce butanol and hydrogen as biofuel. *Renewable Energy*, *77*, 447–455.
- Iliopoulou, E. F., Antonakou, E. V., Karakoulia, S. A., Vasalos, I. A., Lappas, A. A., & Triantafyllidis, K. S. (2007). Catalytic conversion of biomass pyrolysis products by mesoporous materials: Effect of steam stability and acidity of Al-MCM-41 catalysts. *Chemical Engineering Journal*, *134*(1–3), 51–57.
- Jackson, M. A., Compton, D. L., & Boateng, A. A. (2009). Screening heterogeneous catalysts for the pyrolysis of lignin. *Journal of Analytical and Applied Pyrolysis*, *85*(1), 226–230.
- Jena, U., & Das, K. C. (2011). Comparative Evaluation of Thermochemical Liquefaction and Pyrolysis for Bio-Oil Production from Microalgae. *Energy & Fuels*, *25*(11), 5472–5482.
- Jung, Y. H., Kim, I. J., Kim, H. K., & Kim, K. H. (2013). Dilute acid pretreatment of lignocellulose for whole slurry ethanol fermentation. *Bioresource Technology*, *132*, 109–114.
- Karagöz, S., Bhaskar, T., Muto, A., & Sakata, Y. (2005). Catalytic hydrothermal treatment of pine wood biomass: Effect of RbOH and CsOH on product distribution. *Journal of Chemical Technology and Biotechnology*, *80*(10), 1097–1102.
- Karagöz, S., Bhaskar, T., Muto, A., Sakata, Y., & Uddin, M. A. (2004). Low-temperature hydrothermal treatment of biomass: Effect of reaction parameters on products and boiling point distributions. *Energy and Fuels*, *18*(1), 234–241.
- Key world Energy Statistics 2015, OCED/IEA
- Kim, S., & Kim, C. H. (2013). Bioethanol production using the sequential acid/alkali-pretreated empty palm fruit bunch fiber. *Renewable Energy*, *54*, 150–155.

- Kržan, A., Kunaver, M., & Tišler, V. (2005). Wood liquefaction using dibasic organic acids and glycols. *Acta Chim. Slov*, 52, 253-258.
- Kumar, D., & Ali, A. (2012). Nanocrystalline K–CaO for the transesterification of a variety of feedstocks: Structure, kinetics and catalytic properties. *Biomass and Bioenergy*, 46, 459–468.
- Lew, C. M., Rajabbeigi, N., & Tsapatsis, M. (2012). Tin-containing zeolite for the isomerization of cellulosic sugars. *Microporous and Mesoporous Materials*, 153, 55-58.
- Lin, L., Yao, Y., Yoshioka, M., & Shiraishi, N. (2004). Liquefaction mechanism of cellulose in the presence of phenol under acid catalysis. *Carbohydrate Polymers*, 57(2), 123–129.
- Liu, Z., & Zhang, F. S. (2008). Effects of various solvents on the liquefaction of biomass to produce fuels and chemical feedstocks. *Energy Conversion and Management*, 49(12), 3498–3504.
- Lu, Q., Dong, C., Zhang, X., Tian, H., Yang, Y., & Zhu, X. (2011). Selective fast pyrolysis of biomass impregnated with ZnCl₂ to produce furfural: Analytical Py-GC/MS study. *Journal of Analytical and Applied Pyrolysis*, 90(2), 204–212.
- Marland, G., Boden, T. A., & Andres, R. J.(2008). Global, Regional, and National Fossil Fuel CO₂ Emissions. In Trends: A Compendium of Data on Global Change. Carbon Dioxide Information Analysis Center, Oak Ridge National Laboratory, U.S. Department of Energy, Oak Ridge, Tenn., U.S.A.
- McKendry, P. (2002). Energy production from biomass (Part 1): overview of biomass. *Bioresource Technology*, 83:37-46.
- Medina, J. D. C., Woiciechowski, A. L., Filho, A. Z., Bissoqui, L., Nosedá, M. D., Vandenberghe, L.P.S.; Zawadzki, S.F.; Soccol, C.R. 2016 Biological activities and thermal behavior of lignin from oil palm empty fruit bunches as potential source of chemicals of added value. *Industrial Crops and Products* 94:630-637.
- Mihalcik, D. J., Mullen, C. A., & Boateng, A. A. (2011). Screening acidic zeolites for catalytic fast pyrolysis of biomass and its components. *Journal of Analytical and Applied Pyrolysis*, 92(1), 224–232.
- Milne, T., Agblevor, F., Davis, M., Deutch, S., & Johnson, D. (1997). A review of the chemical composition of fast-pyrolysis oils from biomass. In *Developments in thermochemical biomass conversion* (pp. 409-424). Springer Netherlands.
- Mohan, D., Pittman, C. U., & Steele, P. H. (2006). Pyrolysis of Wood / Biomass for Bio-oil : A Critical Review. *Energy & Fuesl*, 20(4), 848–889.

- MPOB, Malaysian Palm Oil Board (2010). Malaysian Oil Palm Industry Statistics 2009, 29th Ed. MPOC. World's oil production in 2007.
- Mun, S. P., & Hassan, E. B. M. (2004). Liquefaction of lignocellulosic biomass with mixtures of ethanol and small amounts of phenol in the presence of methanesulfonic acid catalyst. *Journal of Industrial and Engineering Chemistry*, 10(5), 722-727.
- Muraza, O., & Galadima, A. (2014). Isomerization and alkylation of biomass-derived compounds in aqueous media over hydrophobic solid acid catalysts: a mini review. *Industrial & Engineering Chemistry Research*, 53(46), 17869-17877.
- Nakajima, K., Baba, Y., Noma, R., Kitano, M., N. Kondo, J., Hayashi, S., & Hara, M. (2011). Nb₂O₅·nH₂O as a heterogeneous catalyst with water-tolerant Lewis acid sites. *Journal of the American Chemical Society*, 133(12), 4224-4227.
- Ng, W. P. Q., Lam, H. L., Ng, F. Y., Kamal, M., & Lim, J. H. E. (2012). Waste-to-wealth: Green potential from palm biomass in Malaysia. *Journal of Cleaner Production*, 34 (September 2011), 57-65.
- Ogi, T., Yokoyama, S. Y., & Koguchi, K. (1985). Direct liquefaction of wood by alkali and alkaline earth salt in an aqueous phase. *Chemistry letters*, (8), 1199-1202.
- Othmer, K. (1980). Encyclopedia of chemical technology. 3rd ed, 347-60.
- Pan, P., Hu, C., Yang, W., Li, Y., Dong, L., Zhu, L., Tong, D., Qing, R., Fan, Y. (2010). The direct pyrolysis and catalytic pyrolysis of *Nannochloropsis sp.* residue for renewable bio-oils. *Bioresource Technology*, 101(12), 4593-4599.
- Pattiya, A., Titiloye, J. O., & Bridgwater, A. V. (2008). Fast pyrolysis of cassava rhizome in the presence of catalysts. *Journal of Analytical and Applied Pyrolysis*, 81(1), 72-79.
- Peacocke, G. V. C., Russell, P. A., Jenkins, J. D., & Bridgwater, A. V. (1994). Physical properties of flash pyrolysis liquids. *Biomass and Bioenergy*, 7(1-6), 169-177.
- Puppan, D. (2002). Environmental evaluation of biofuels. *Periodica Polytechnica Ser. Soc. Man. Sci.* 10:95-116.
- Pütün, E. (2010). Catalytic pyrolysis of biomass: Effects of pyrolysis temperature, sweeping gas flow rate and MgO catalyst. *Energy*, 35(7), 2761-2766.
- Qian, Y., Zuo, C., Tan, J., & He, J. (2007). Structural analysis of bio-oils from sub-and supercritical water liquefaction of woody biomass. *Energy*, 32(3), 196-202.
- Ren, Y., Zhang, F., Hua, W., Yue, Y., & Gao, Z. (2009). ZnO supported on high silica HZSM-5 as new catalysts for dehydrogenation of propane to propene in the presence of CO₂. *Catalysis Today*, 148(3-4), 316-322.

- Rezzoug, S. A., & Capart, R. (1996). Solvolysis and hydrotreatment of wood to provide fuel. *Biomass and Bioenergy*, 11(4), 343–352.
- Riemann, U. (2007). BTL biomass-to-liquid for dummies. In: Solution Provider for Next Generation Biofuel Technologies (Biomass & Waste to Diesel), Syracuse, New York Area.
- Román-Leshkov, Y., Moliner, M., Labinger, J. A., & Davis, M. E. (2010). Mechanism of glucose isomerization using a solid Lewis acid catalyst in water. *Angewandte Chemie International Edition*, 49(47), 8954–8957.
- Saber, M., Golzary, A., Hosseinpour, M., Takahashi, F., & Yoshikawa, K. (2016). Catalytic hydrothermal liquefaction of microalgae using nanocatalyst. *Applied Energy*, 183, 566–576.
- Sairan, S., & Aman, M. I. (2007). CO₂ reduction opportunity – power generation perspective. Research Paper on TNB Research Sdn. Bhd.
- Savage, P. E., Levine, R. B., Huelsman, C. M. (2010). Hydrothermal processing of biomass. In Thermochemical Conversion of Biomass to Liquid Fuels and Chemicals. *Royal Society of Chemistry*, 192–221.
- Şensöz, S. and Kaynar, I. (2006). Bio oil production from soybean (*Glycine max* L.); fuel properties of Bio-oil. *Industrial Crops and Products* 23:99-105.
- Shuit, S. H., Tan, K. T., Lee, K. T., & Kamaruddin, A. H. (2009). Oil palm biomass as a sustainable energy source: A Malaysian case study. *Energy*, 34(9), 1225–1235.
- Sulaiman, F., Abdullah, N., Gerhauser, H., & Shariff, A. (2011). An outlook of Malaysian energy, oil palm industry and its utilization of wastes as useful resources. *Biomass and Bioenergy*, 35(9), 3775–3786.
- Tan, K. T., Lee, K. T., Mohamed, A. R., & Bhatia, S. (2009). Palm oil: Addressing issues and towards sustainable development. *Renewable and Sustainable Energy Reviews*, 13(2), 420–427.
- Tan, L., Yu, Y., Li, X., Zhao, J., Qu, Y., Choo, Y. M., & Loh, S. K. (2013). Pretreatment of empty fruit bunch from oil palm for fuel ethanol production and proposed biorefinery process. *Bioresource Technology*, 135, 275–282.
- Teoh, C.H. (2002). The palm oil industry in Malaysia – from seed to frying pan. Malaysia: Plantation Agriculture, WWF.
- Valdez, P. J., Nelson, M. C., Wang, H. Y., Lin, X. N., & Savage, P. E. (2012). Hydrothermal liquefaction of *Nannochloropsis* sp.: Systematic study of process variables and analysis of the product fractions. *Biomass and Bioenergy*, 46, 317–331.

- Wang, C., Du, Z., Pan, J., Li, J., & Yang, Z. (2007). Direct conversion of biomass to bio-petroleum at low temperature. *Journal of Analytical and Applied Pyrolysis*, 78(2), 438–444.
- Wang, C., Pan, J., Li, J., & Yang, Z. (2008). Comparative studies of products produced from four different biomass samples via deoxy-liquefaction. *Bioresource Technology*, 99(8), 2778–2786.
- Wang, F., Chang, Z., Duan, P., Yan, W., Xu, Y., Zhang, L., Miao, J., Fan, Y. (2013). Hydrothermal liquefaction of *Litsea cubeba* seed to produce bio-oils. *Bioresource Technology*, 149, 509–515.
- Wang, L., Han, C., Nadagouda, M. N., & Dionysiou, D. D. (2016). An innovative zinc oxide-coated zeolite adsorbent for removal of humic acid. *Journal of Hazardous Materials*, 313, 283–290.
- Wang, T., Zhang, L., Li, D., Yin, J., Wu, S., & Mao, Z. (2008). Mechanical properties of polyurethane foams prepared from liquefied corn stover with PAPI. *Bioresource Technology*, 99(7), 2265–2268.
- White, L. P. & Plasket, L.G. (1981). Biomass as fuel. New York: Academic Press.
- Xu, F., Xu, Y., Lu, R., Sheng, G.-P., & Yu, H.-Q. (2011). Elucidation of the Thermal Deterioration Mechanism of Bio-oil Pyrolyzed from Rice Husk Using Fourier Transform Infrared Spectroscopy. *Journal of Agricultural and Food Chemistry*, 59(17), 9243–9249.
- Yaman, S. (2004). Pyrolysis of biomass to produce fuels and chemical feedstocks. *Energy Conversion and Management*, 45(5), 651–671.
- Yan, Y., Xu, J., Li, T., & Ren, Z. (1999). Liquefaction of sawdust for liquid fuel. *Fuel Processing Technology*, 60(2), 135–143.
- Yang, Y., Hu, C. W., & Abu-Omar, M. M. (2012). Synthesis of furfural from xylose, xylan, and biomass using $\text{AlCl}_3 \cdot 6 \text{H}_2\text{O}$ in biphasic media via xylose isomerization to xylulose. *ChemSusChem*, 5(2), 405–410.
- Yip, J., Chen, M., Szeto, Y. S., & Yan, S. (2009). Comparative study of liquefaction process and liquefied products from bamboo using different organic solvents. *Bioresource Technology*, 100(24), 6674–6678.
- Zhao, X., Wei, L., Cheng, S., Huang, Y., Yu, Y., & Julson, J. (2015). Catalytic cracking of camelina oil for hydrocarbon biofuel over ZSM-5-Zn catalyst. *Fuel Processing Technology*, 139, 117–126.