

# **UNIVERSITI PUTRA MALAYSIA**

PREPARATION OF La2O3-CaO MIXED OXIDE CATALYSTS SUPPORTED ON NANOSTRUCTURED ACTIVATED CARBON FOR BIODIESEL PRODUCTION FROM WASTE COOKING OIL

ABDULKAREEM GHASSAN ABDULKREEM

FS 2016 58



## PREPARATION OF La<sub>2</sub>O<sub>3</sub>-CaO MIXED OXIDE CATALYSTS SUPPORTED ON NANOSTRUCTURED ACTIVATED CARBON FOR BIODIESEL PRODUCTION FROM WASTE COOKING OIL



ABDULKAREEM GHASSAN ABDULKREEM

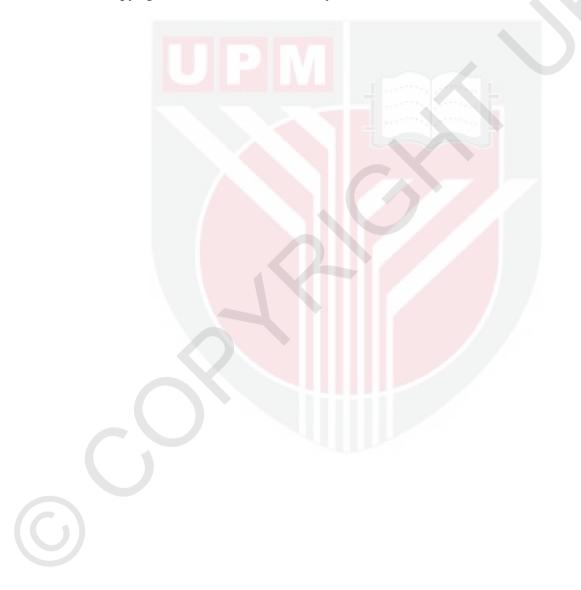
Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in Fulfillment of the Requirements for the Degree of Master of Science

October 2016

## COPYRIGHT

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfillment of the requirement for the degree of Master of Science

## PREPARATION OF La<sub>2</sub>O<sub>3</sub>-CaO MIXED OXIDE CATALYSTS SUPPORTED ON NANOSTRUCTURED ACTIVATED CARBON FOR BIODIESEL PRODUCTION FROM WASTE COOKING OIL

By

#### ABDULKAREEM GHASSAN ABDULKREEM

October 2016

Chairman : Professor Taufiq Yap Yun Hin, FASc, PhD Faculty : Science

Advanced carbon nanorod promoted binary La2O3-CaO system with improved physical properties, tailored surface morphology and chemistry were developed in vacuum-impregnating methods. The nanostructured catalyst (CaO-La<sub>2</sub>O<sub>3</sub>/AC nanocatalyst) was prepared to convert waste cooking oil with high FFA into biodiesel via one step esterification-transesterification reaction. The novel catalyst was characterized by XRF, FTIR, HRTEM, FESEM, XRD, TGA, BET, TPD-CO<sub>2</sub> and TPD-NH<sub>3</sub>. The high catalytic activity of the nanocatalyst was mainly depended on the high acid and basic density of active sites that contributed from the synergic effect between mesoporous carbon and binary metallic system, which allowed more occurrence of simultaneous esterification-transesterification process of high FFA waste oil without additional pretreatment step. Results showed a maximum triglyceride conversion of 98.6  $\pm$  0.5% with acid value 0.4  $\pm$  0.5 mg KOH/g of triglyceride conversion under optimal condition at 3% of catalyst, methanol: oil ratio of 16:1, 100 °C within 4 h of reaction. Furthermore, bi-metallic catalysts with stable carbon nanorod support were capable to maintained high reusability with high FAME yield (> 98%) with low acid value (<0.5 mg KOH/g) for 5 cycles. Several physicochemical properties of WCO-based biodiesel produced were tested and in good agreement to ASTM D6751 standards.

Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk ijazah Master Sains

## PENYEDIAAN PEMANGKIN OKSIDA CAMPURAN La<sub>2</sub>O<sub>3</sub>-CaO YANG DISOKONG ATAS KARBON YANG DIAKTIFKAN DAN BERNANOSTRUKTUR UNTUK PENGELUARAN BIODIESEL DARIPADA SISA MINYAK MASAK

Oleh

#### ABDULKAREEM GHASSAN ABDULKREEM

Oktober 2016

Pengerusi : Profesor Taufiq Yap Yun Hin, FASc, PhD Fakulti : Sains

Sistem binari CaO-La<sub>2</sub>O<sub>3</sub> yang digalakkan oleh nanorod karbon yang maju, dengan ciri-ciri fizikal yang lebih baik and morfologi permukaan dan kimia yang disesuaikan, telah dibangunkan dengan menggunakan kaedah resapan vakum. Pemangkin bernanostruktur (CaO-La<sub>2</sub>O<sub>3</sub>/AC pemangkin nano) disediakan untuk menukar sisa minyak masak yang tinggi FFA kepada biodiesel melalui tindakbalas selangkah pengesteran-transesterifikasi. Pemangkin dicirikan baru tersebut oleh XRF,FTIR,HRTEM, FESEM, XRD, TGA, BET, TPD-CO<sub>2</sub> dan TPD-NH<sub>3</sub>. Aktiviti bermangkin tinggi pemangkin nano tersebut banyak bergantung kepada keasidan dan kepadatan asas yang tinggi pada tapak aktif yang menyumbang daripada kesan bersinergi antara karbon berliang meso dan sistem logam binari, yang membolehkan lebih banyak berlakunya proses pengesteran-transesterifikasi serentak terhadap sisa minyak dengan FFA tinggi tanpa tambahan langkah rawatan awal. Keputusan menunjukkan maksimum sebanyak 98.6  $\pm 0.5\%$  dengan nilai asid 0.4  $\pm 0.5$  mg KOH/g dalam penukaran trigliserida di bawah keadaan optimum pada 3% daripada pemangkin, dengan nisbah metanol:minyak sebanyak 16:1, pada suhu 100 °C dalam masa tindakbalas 4 jam. Tambahan pula, pemangkin bi-logam dengan sokongan nanorod karbon yang stabil mampu mengekalkan kebolehan gunapakai tinggi dengan alah FAME yang tinggi (> 98%) dengan nilai asid yang rendah (<0.5 mg KOH/g) untuk 5 kitaran. Beberapa ciri-ciri fizikokimia biodiesel berasaskan WCO yang diuji adalah bertepatan juga dengan piawai ASTM D6751.



### ACKNOWLEDGEMENTS

Bismillah Ar-Rahman Ar-Rahim. Alhamdullilah, Thanks to Allah S.W.T the almighty for giving me the strength, patience and faith to pursue my dream and also his blessings which led me through the journey of completing this research.

First and foremost, I have to thank my parents for their love and support throughout my life. Thank you both for giving me strength to reach for the stars and chase my dreams. My sisters and my brothers deserve my wholehearted thanks as well. I would like to sincerely thank my supervisor, Prof. Dr. Taufiq Yap Yun Hin, for his guidance and support throughout this study, and especially for his confidence in me. I would also like to thank, Dr. Mohd Izham Bin Saiman for serving as a member on my thesis committee. Thanks also to Dr. Lee Hwei Voon. I would also like to thank miss Nurul Asikin Bt Mijan, in a special way, I express my heartfelt gratefulness for her guide and support that I believed I learned from the best.

To all my friends, thank you for your understanding and encouragement in my many, many moments of crisis. Your friendship makes my life a wonderful experience. I cannot list all the names here, but you are always on my mind. Thank you, Mr. Mahashanon Arumugam, for always being there for me. This thesis is only a beginning of my journey. I certify that a Thesis Examination Committee has met on 5 October 2016 to conduct the final examination of Abdulkareem Ghassan Abdulkareem on his thesis entitled "Preparation of  $La_2O_3$ -CaO Mixed Oxide Catalysts Supported on Nanostructured Activated Carbon for Biodiesel Production from Waste Cooking Oil" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U.(A) 106] 15 March 1998. The Committee recommends that the student be awarded the Master of Science.

Members of the Thesis Examination Committee were as follows:

Gwendoline Ee Cheng Lian, PhD

Professor Faculty of Science Universiti Putra Malaysia (Chairman)

Tan Yen Ping, PhD Senior Lecturer Faculty of Science Universiti Putra Malaysia (Internal Examiner)

Aishah Abdul Jalil, PhD Associate Professor University of Technology, Malaysia Malaysia (External Examiner)

NOR AINI AB. SHUKOR, PhD Professor and Deputy Dean School of Graduate Studies Universiti Putra Malaysia

Date: 3 November 2016

This thesis was submitted to the Senate of the Universiti Putra Malaysia and has been accepted as fulfillment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

## Taufiq Yap Yun Hin, FASc, PhD

Professor Faculty of Science Universiti Putra Malaysia (Chairman)

## Mohd Izham Bin Saiman, PhD Lecturer Faculty of Science Universiti Putra Malaysia

(Member)

# BUJANG BIN KIM HUAT, PhD

Professor and Dean School of Graduate Studies Universiti Putra Malaysia

Date:

## **Declaration by graduate student**

I hereby confirm that:

- this thesis is my original work;
- quotations, illustrations and citations have been duly referenced;
- this thesis has not been submitted previously or concurrently for any other degree at any institutions;
- intellectual property from the thesis and copyright of thesis are fully-owned by Universiti Putra Malaysia, as according to the Universiti Putra Malaysia (Research) Rules 2012;
- written permission must be obtained from supervisor and the office of Deputy Vice-Chancellor (Research and innovation) before thesis is published (in the form of written, printed or in electronic form) including books, journals, modules, proceedings, popular writings, seminar papers, manuscripts, posters, reports, lecture notes, learning modules or any other materials as stated in the Universiti Putra Malaysia (Research) Rules 2012;
- there is no plagiarism or data falsification/fabrication in the thesis, and scholarly integrity is upheld as according to the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) and the Universiti Putra Malaysia (Research) Rules 2012. The thesis has undergone plagiarism detection software

Signature:	Date:

Name and Matric No: Abdulkareem Ghassan Abdulkreem, (GS40570)

# **Declaration by Members of Supervisory Committee**

This is to confirm that:

- the research conducted and the writing of this thesis was under our supervision;
- supervision responsibilities as stated in the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) were adhered to.

Signature: Name of Chairman	
of Supervisory	
Committee:	Professor Dr. Taufiq Yap Yun Hin, FASc
Signature:	
Name of Member of Supervisory	
Committee:	Dr. Mohd Izham Bin Saiman

# TABLE OF CONTENTS

		I	Page
APPRO DECL LIST ( LIST (	RAK OWLE OVAL ARATI OF TAB OF FIG	BLES	i iii iv vi xi xii xv
СНАР	TER		
1	1.1 1.2 1.3 1.4 1.5 1.6	RODUCTION Catalyst Catalysts for Energy Background Biodiesel Problem Statement Objectives Scope of Study	1 2 2 3 4 5 5
2	2.1 2.2 2.3 2.4 2.5 2.6	RATURE REVIEWTransesterification of Vegetable Oil Using Homogeneous Acidand Base Catalysts2.1.1Homogeneous Base Catalysts2.1.2Heterogeneous Base CatalystsAcid Catalysts for Triglyceride Transesterification2.2.1Homogeneous Acid Catalysts2.2.2Heterogeneous Acid Catalysts2.2.3Heterogeneous Acid Catalysts for Free Fatty Acids (FFAs) Esterification2.3.1Homogeneous Acid Catalysts for Free Fatty Acids (FFAs) Esterification2.3.2Heterogeneous Acid Catalysts for Free Fatty Acids (FFAs) EsterificationMetal Oxide and Mixed Metal OxidesCatalyst Support2.5.1Alumina2.5.2Silicate2.5.3Zirconium Oxide2.5.4Activated CarbonPreparation of Activated Carbon2.6.1Physical Activation2.6.2Chemical Activation2.6.2Chemical Activation2.6.2Chemical ActivationWaste Cooking Oil (WCO) as Fuel	6 6 7 8 10 11 12 12 13 14 14 14 18 18 19 19 20 20 21 24
3		HODOLOGY Materials	25 25

# viii

3.2	Preparation of La2O3-CaO Supported Activated Carbon Catalyst	26	
3.3	talyst Characterization 2		
0.0	3.3.1 Thermogravimetric Analysis (TGA)	$\frac{1}{26}$	
	3.3.2 X-Ray Diffraction Analysis (XRD)	26	
	3.3.3 Brunauer-Emmet-Teller (BET) Surface Area	27	
	Measurement 3.3.4 Temperature Programmed Desorption Of Carbon	28	
	Dioxide (TPD-CO <sub>2</sub> )	20	
	3.3.5 Temperature Programmed Desorption of ammonia	28	
	(TPD-NH <sub>3</sub> )		
	3.3.6 Field Emission Scanning Electron Microscope (FESEM)	29	
	3.3.7 High Resolution Transmission Electron Microscopy	29	
	(HRTEM)		
	3.3.8 Inductively Coupled Plasma-Atomic Emission	29	
2.4	Spectrometer (ICP-AES)	20	
3.4 3.5	Determination Of Saponification Value Transesterification-Esterification Reaction	29 30	
3.5 3.6	Catalyst Reusability Study	30 31	
3.7	Biodiesel Quantitative Analysis	32	
5.7	3.7.1 Biodiesel Conversion Measurement by Using Acid	32	
	Value	52	
	3.7.2 Determining The Fatty Acid Methyl Ester Content to	32	
	Comply With En 14103		
	3.7.3 Determining the Chemical Functional Group of	33	
	Biodiesel		
	3.7.4 Biodiesel Quality Evaluations	34	
RES	SULTS AND DISCUSSION	35	
4.1	Physical properties of nanorod activated carbon	35	
	4.1.1 Field Emission Scanning Electron Microscopy (FESEM)	35	
	4.1.2 X-Ray Diffraction Analysis (XRD)	36	
	4.1.3 Fourier Transform Infrared (FTIR) Fourier	37	
	4.1.4 Temperature Programme Desorption – Ammonia	38	
	(TPD–NH <sub>3</sub> )		
	4.1.5 Brunauer–Emmett–Teller Surface Area Measurement	39	
	(BET)		
	4.1.6 High-resolution transmission electron microscopy	40	
	Microscopy (HRTEM)	4.1	
1 2	4.1.7 Ash Content Mixed Of CoO, And Lo2O2 Supported Nanoroda Carbon	41	
4.2	Mixed Of CaO And La2O3 Supported Nanorode Carbon Catalyst	42	
	4.2.1 Field Emission Scanning Electron Microscopy	42	
	(FESEM)	.2	
	4.2.2 Thermal Gravimetric Analysis (TGA)	44	
	4.2.3 X-Ray Diffraction (XRD)	45	
	4.2.4 Fourier Transform Infrared (FTIR)	46	

4

		4.2.5 Brunauer–Emmett–Teller Surface Area Measurement (BET)	47
		4.2.6 Temperature Programme Desorption – Ammonia (TPD–NH <sub>3</sub> )	47
		4.2.7 Temperature Programme Desorption – Carbon Dioxide (TPD–CO <sub>2</sub> )	48
	4.3	One Step Esterification–Transesterification Reaction Of WCO	51
		4.3.1 Chemical Composition of WCO and Biodiesel	51
		4.3.2 Catalytic Reactivity	52
		4.3.3 Optimization of Process Parameters	54
		4.3.3.1 Effect of Catalyst Loading	54
		4.3.3.2 Effect of Methanol to Oil Molar Ratio	55
		4.3.3.3 Effect of Reaction Temperature	56
		4.3.3.4 Effect of Reaction Time	57
	4.4	Assessment of Reusability	58
		4.4.1 Catalytic Activity (Reusability)	58
		4.4.2 Leaching Study By ICP-AES	59
	4.5	Comparison Study	60
	4.6	Characterization of Synthesized Biodiesel	62
5	CON	NCLUSIONS	64
	5.1	Conclusion	64
	5.2	Suggestion and Recommendation for Future Study	64
REFEI APPEN			66 77
		<b>F</b> STUDENT	82
			83

C

# LIST OF TABLES

Т	able		Page
1		Comparison of biodiesel and diesel according to the American Standard for Testing and Materials (ASTM).	3
2		Comparison of pure metal oxides, mixed metal oxides and supported metal oxides used in biodiesel production.	16
3		Carbonization and activation condition of various lignocellulose biomass.	23
4		Details of the materials used in whole research study	25
5		parameters study for biodiesel optimization	31
6		Instrument parameters (EN 14103).	32
7		Fuel Quality testing.	34
8		TPD-NH <sub>3</sub> profile of synthesized nanorods.	39
9		Ash content of synthesized nanorods and commercial carbon.	41
10	C	Element composition of the catalysts.	43
1	1	Physicochemical properties of the catalyst.	50
12	2	Summary of recent studies for $La_2O_3$ -CaO doped catalyst for biodiesel production.	61
13	3	Fuel properties of synthesized biodiesel.	63

# LIST OF FIGURES

Figure		Page
1	Illustration of the effect of a catalyst in reducing the activation energy required for the exothermic reaction $X + Y \longrightarrow Z$ (Robertson 1070)	1
	(Robertson, 1970).	
2	a) Reaction mechanism of base-catalyzed transesterification. b) Reaction mechanism of acid catalyzed transesterification reaction	7
3	Mechanism of acid catalysed transesterification	11
4	Mechanism of Brønsted-typed acid sites catalysed esterification.	13
5	Mechanism of Lewis-typed acid sites catalyzed esterification	13
6	Distribution of biodiesel production cost, %	24
7	Morphological and their corresponding particle size distribution of the walnut shell after carbonization (A); refluxing under vacuum (B); activation of refluxed walnut shell	36
8	The preferential organization of the carbon precursors according to Grotthuss mechanism.	36
9	XRD diffraction peak for all carbon samples: A, B, C denoting the walnut shell after carbonization, refluxed under vacuum and activated of the refluxed walnut shell, respectively.	37
10	FTIR for all carbon samples; A, B, C denoting the walnut shell after carbonization, refluxed under vacuum and activated of the refluxed walnut shell, respectively.	38
11	Acidity for all carbon samples; A, B, C denoting the walnut shell after carbonization, refluxed under vacuum and activated of the refluxed walnut shell, respectively.	39
12	N <sub>2</sub> adsorption/desorption isotherms all carbon based; A, B, C denoting the walnut shell after carbonization, refluxed under vacuum and activated of the refluxed walnut shell, respectively.	40
13	(A)TEM image of the synthesized nanorods; (B) the point of contact of the synthesized nanorods. A, B, C denoting the walnut shell after carbonization, refluxed under vacuum and activated of the refluxed walnut shell, respectively.	41

	14	FESEM images for AC and La <sub>2</sub> O <sub>3</sub> -CaO doped AC catalysts: A-AC La5 Ca15, B- AC La10 Ca15, C- AC La15 Ca15, D- AC La20 Ca15, E- AC La25 Ca15, F- AC La30 Ca15 and G- EDX result.	44
	15	Thermal gravimetric analysis for AC and La <sub>2</sub> O <sub>3</sub> -CaO doped AC catalysts.	45
	16	XRD diffractogram for AC and La <sub>2</sub> O <sub>3</sub> -CaO / AC catalysts.	46
	17	FTIR spectrum for AC and La <sub>2</sub> O <sub>3</sub> -CaO/ AC catalysts.	47
	18	TPD-NH <sub>3</sub> profile for AC and La <sub>2</sub> O <sub>3</sub> -CaO/AC catalysts.	48
	19	TPD-CO <sub>2</sub> profile for AC and La <sub>2</sub> O <sub>3</sub> -CaO doped AC catalysts.	49
	20	GCMS spectrum of WCO (A) and biodiesel (B): 1- Myristic acid methyl ester, 2- Palmitic acid methyl ester, 3- Linoleic acid methyl ester, 4- Oleic acid methyl ester, 5- Stearic acid methyl ester, 6- Oleic acid methyl ester.	51
	21	FTIR spectrum for WCO and produced biodiesel.	52
	22	Transesterification of WCO using AC and La <sub>2</sub> O <sub>3</sub> -CaO doped AC. Reaction conditions: reaction temperature 60 °C; reaction time 2h; methanol to oil ratio 1:12 and catalyst loading 0.5% wt.	53
	23	The relationship between chemical properties (acidity and basicity) of the catalyst with the FAME yield	54
	24	Effect of catalyst concentration on biodiesel yield and acid value (methanol to oil molar ratio 12:1, temperature 60 $^{\circ}$ C, 2h reaction time).	55
	25	Effect of methanol to oil ratio on biodiesel yield and acid value (catalyst loading 1%, 2h reaction time, temperature 60 °C).	56
	26	Effect of temperature on biodiesel yield and acid value (methanol to oil molar ratio 16:1, catalyst concentration 3% (wt.) and 2h reaction time).	57
	27	Effect of reaction time on biodiesel yield and acid value (methanol to oil molar ratio 16:1, catalyst concentration 3% (wt.) and reaction temperature 100 °C).	58
	28	Effect of reusability study on ACLa20Ca15 catalyst for FAME yield. Reaction conditions; methanol to oil molar ratio 1:16, catalyst concentration 3% of WCO, reaction temperature 100 °C within 4h.	59

29 Effect of reusability study on ACLa20Ca15 catalyst for concentration of the CaO and La<sub>2</sub>O<sub>3</sub>. Reaction conditions; methanol to oil molar ratio 1:16, catalyst concentration 3% of WCO, reaction temperature 100 °C within 4h.



# LIST OF ABBREVIATIONS AND SYMBOLS

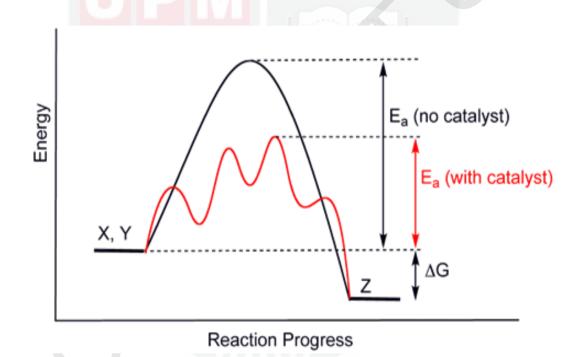
ASTM	American society for testing and materials
AC	Activated carbon
WCO	Waste cooking oil
EN	European Standard
ATZ	5-AMINOTETRAZOLE-HYDRATE
ATB	6-methoxy-α-methyl-2-naphthaleneacetic acid, 4- (aminothioxomethyl)phenyl ester
BET	Brunauer-Emmett-Teller
EDX	Energy-dispersive X-ray spectroscope
FAME	Fatty acid methyl ester
FFA	Free fatty acid
FT-IR	Fourier transform infrared
GC	Gas chromatograph
GC-MS	Gas chromatograph mass spectrometry
HRTEM	High-resolution TEM
TPD- NH3	Ammonia-temperature programmed desorption
TPD-CO <sub>2</sub>	Carbon dioxide- temperature programmed desorption
FESEM	Field emission scanning electron microscope.
TGA	Thermogravimetric analysis
XRD	X-ray power diffraction

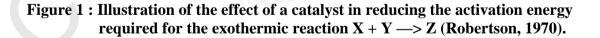
#### **CHAPTER 1**

#### **INTRODUCTION**

#### 1.1 Catalyst

The word 'catalysis' derives from the Greek word meaning 'to dissolve'. A catalyst is typically defined as a substance which enhances the rate at which a chemical reaction proceeds by reducing the activation energy required (Figure 1). It is able to act in very small quantities as an initiator for the transformation and is not used up itself in the process (Ertl *et al.*, 2008). Ertal *et al.* (2008) also refer to Laidler (1986) Ostawld's (1895), the alternative definition of a catalyst is a substance which is able to enhance a chemical reaction without affecting its equilibrium.





Since catalysis represents a means for facilitating chemical reactions with lower energy requirements, it can therefore be viewed as a process with environmental as well as commercial benefits. In addition, it also offers two significant technical advantages: selectivity and thermal stability which again contribute to improved outcome for environmental or 'green' considerations.

Roebuck in 1746, whilst producing sulphuric acid was the first to use a catalyst — a development which the chemical industry quickly picked up with wide application.

Initially, only pure elements were utilised a catalysts, however, from the start of the twentieth century, compound catalysts were developed and are widely deployed today (Leach, 1983). Examples of major industrial applications utilising the process of catalysis include those for the production of ammonia and methyl alcohol. Both these processes involve state change of reactants facilitated by solid catalysis. According to Robertson (Robertson, 1970), around 85–90 % of industrial chemical processes involve some form of catalysis, with the final products valued at around \$900bn worldwide.

## **1.2** Catalysts for Energy

Increasing population growth, economic growth and energy demand has led to concern regarding limited energy resources, particularly with regard to the overconsumption of non-sustainable fossil fuel energy sources which is now known to be responsible for global warming and climate change. This situation represents major environmental and economic challenges facing the world today and in the future. Therefore, renewable forms of energy have been proposed as a way forward, and catalysis represents renewable processes that can reduce energy requirements for chemical reactions. Furthermore, new technology is starting to examine the possibility of utilising catalysts for the production of greener and clean energy, which by its application able to reduce greenhouse gas emissions.

### 1.3 Background

Since the mid-nineteenth century, fossil fuel has been the most significant and easily available energy source in the world. Today around 90% of all vehicles are powered by fossil fuel. It is well known that petroleum products provide major source materials for the chemical industry producing plastics, pharmaceuticals, pesticides, fertilizers and solvent (Simanzhenkov *et al.*, 2003; Speight *et al.*, 2001). However, the non-renewable nature of the fossil fuel source materials has become a growing cause for concern from the latter half of the twentieth century onwards. Demand for sustainable, renewable energy sources has grown as people have sought to decrease their dependency on fossil fuels and their associated uncertainties of security of supply and price variability. Polluting gaseous emissions from burning fossil fuels are another factor driving the search for a clean energy supply (Mizsey *et al.*, 2010). Biofuel and biomass technologies have the potential to provide significant sources of energy in the next century.



Biofuel, is an alternative cleaner burning fuel that successfully been tried and used by majority of the nation to replace the use of non-sustainable fossil energy. Biofuel can be referred as liquid or gaseous fuels use in transportation sector which predominantly synthesized from biomass. Therefore, application of biofuel have been proved to be meeting wide range of social and environmental sustainable criteria including limit on deforestations, competition with food production, adverse impact on biodiversity, soil erosion and nutrient leaching. Biofuels are derived from renewable sources and include biodiesel, green diesel, bioethanol, biogas, biomethanol, synthetic biofuel and

biohydrogen( Justine *et al.*, 2009). Currently, bioethanol and biodiesel account for around 90% of the biofuel market.

#### 1.4 Biodiesel

Biodiesel is considered a viable alternative to petroleum–derived fuel. Chemically, biodiesel consists of a methyl ester with long chain fatty acids (FAME) derived from transesterification or esterification reaction of lipid feedstocks such as vegetable oils or animal fats(Narayan & Madras, 2016) and (Monirul *et al.*, 2015). Biodiesels are renewable, biodegradable, less toxic, have an environmentally friendly emission profile, a higher combustion efficiency, higher certain number, higher flash point and better lubrication than petroleum derived fuel (Alsultan *et al.*, 2016; Can *et al.*, 2016). Moreover, biodiesel and diesel share similar physicochemical properties (Table 1), so biodiesel can be used on its own or mixed with diesel in conventional compression ignition engines with some engine modifications.

# Table 1 : Comparison of biodiesel and diesel according to the American Standard for Testing and Materials (ASTM)

Property of the fuel	Biodiesel	Diesel
Standard method	ASTM D6751	ASTM D975
Fuel composition	FAME(C12-C22)	Hydrocarbon(C10-C21)
Density(g/cm <sup>3</sup> )	0.878	0.848
Pour point (°C)	-15 to 16	-30 to -15
Cloud point(°C)	-3 to 12	-15 to 5
Flash point(°C)	100-170	60-80
Cetane number	48-60	40-55
Water (vol %)	0.05	0.05
Carbon (wt. %)	77	87
Hydrogen (wt. %)	12	13
Oxygen (wt. %)	11	0
Sulphur (wt. %)	0.05	0.05

Biodiesel is considered the best candidate for petroleum derived fuel substitute in diesel engine (compression-ignition engines) due well known advantages, including following (Zhong *et al.*, 2016). Biodiesel has good combustion properties due to its high oxygen content (11%). The Lifecycle analysis indicates that biodiesel has 78% lower net carbon dioxide emissions than conventional diesel and has a lower smoke emission factor as a consequence of minimal free soot.in addition, Biodiesel is less

damaging to the environment than conventional diesel since it is biodegradable, sustainable, renewable, non-toxic and has lower sulphur content and the claimed to reduce incidence of dangerous disease by 90%. Biodiesel also offers the potential of various socioeconomic advantages such as employment, investment in rural areas and reduced negative consequences of global warming. Biodiesel has a higher cetane value than conventional diesel. The production of biodiesel is easier to produce than conventional diesel. And Biodiesel is a better lubricant than conventional diesel and therefore a better promoter of engine efficiency. Biodiesel has a higher flashpoint than conventional diesel (Table 1.1) which is a safety feature, reducing likelihood of explosive combustion. Biodiesel offers the additional environmental benefit with the potential to recycle food oils, removing them from the waste stream. Biodiesel (B20) in low blends can be used directly (without modification) in engines, although some engine modification may be required to use higher ratios of biodiesel.

## 1.5 Problem Statement

Typical feedstock used for biodiesel production mainly derived from edible oil that available abundantly around the world. These source materials have led to food vs fuel concerns as conflicts between the needs for biofuel and human food have been reported. The competition between food and fuel economics toward the same oil might bring global imbalance to the food supply and demand on the market. In addition, utilization of edible oil also surely will lead to higher production cost which unattractive for industrial scale Thus, in order to commercially viable alternative to petroleum derived fuel industry, the use of lower-cost and non-edible oil such as waste cooking oil (WCO) is taken into consideration in biodiesel production.

Nowadays, there are a lot of heterogeneous solid catalysts that have been introduced for biodiesel applications due to easy purification step and high reusability as compared to homogeneous catalysts. Different type of solid catalysts was proposed, such as base (alkaline-based and alkaline-earth-based metal oxide) and acid (functionalization of silica materials (MCM-41 and SBA-15) with organo-sulfonic acids) catalysts. Typically, transesterification catalyzed by solid base catalysts show high reactivity under the mild reacting condition as compared to solid acid catalysts. However, the WCO is an acid oil with large amounts of free fatty acids (FFAs), which the active site of base catalyst for transesterification reaction was normally inhibited by the fatty acid via saponification. Ideally, acid catalysis is a potential candidate for simultaneous esterification of the FFAs and transesterification of the triglycerides to achieve one-pot preparation of FAMEs from WCO. Therefore, heterogeneous solid acid catalyst provides an environmentally benign and cost effective process for production of biodiesel from low quality acid oil. However, challenge on developing an efficient solid acid catalyst for one-step esterification-transesterification was still on-going.

In the biodiesel production, the most important to improve the process efficiency is the catalyst. However, heterogeneous catalyst was used instead of homogeneous catalyst because of the separation and corrosion problems. On the other hand, the catalytic activity and the stability of the heterogeneous catalyst are the key factors in synthesizing a novel catalyst. To overcome this matter, the carbon-based solid acid catalysts were introduced in this research, which had proved to have high catalytic activity and good stability.

## 1.6 Objectives

The objectives of this study are:

- 1. To synthesis and characterization nanosize solid acid-base catalysts (La2O3-CaO/AC) to facilitate the manufacture of biodiesel from waste cooking oil.
- 2. To determine the catalytic activity and influential factors in esterificationtransesterification process of synthesized acid-base catalysts.
- 3. To study the reusability and catalyst stability in the esterificationtransesterification process.

## 1.7 Scope of Study

Advanced carbon nanorod promoted binary La2O3-CaO system with improved physical properties, tailored surface morphology and chemistry were developed in vacuum-impregnating methods. This nanosize mixed metal oxides supported activated carbon derived walnut shell (*juglans sp.*) are believed to consist of superior physicochemical properties than activated carbon support and enhance the one-step esterification-transesterification process of waste cooking oil. The mixed metal oxides supported on AC with in cooperation of La metal content from 5 to 30% toward one-step esterification-transesterification activity were further investigated. The highest catalytic activity from mixed metal oxides supported AC with optimum ration of Ca metal was selected and further optimize in one-step esterification-transesterification process. Besides, the reusability and catalyst stability also were studied.

#### REFERENCES

- Abdulkareem-Alsultan, G., Asikin-Mijan, N., Lee, H. V., & Taufiq-Yap, Y. H. (2016). A new route for the synthesis of La-Ca oxide supported on nano activated carbon via vacuum impregnation method for one pot esterificationtransesterification reaction. *Chemical Engineering Journal*.
- Adinata, D., Daud, W. M. A. W., & Aroua, M. K. (2007). Production of carbon molecular sieves from palm shell based activated carbon by pore sizes modification with benzene for methane selective separation. *Fuel processing technology*, 88(6), 599-605.
- Albuquerque, M. C., Jim énez-Urbistondo, I., Santamar á-Gonz ález, J., Mérida-Robles, J. M., Moreno-Tost, R., Rodr guez-Castellón, E., ... & Maireles-Torres, P. (2008). CaO supported on mesoporous silicas as basic catalysts for transesterification reactions. *Applied Catalysis A: General*,334(1), 35-43.
- Alvarez, M., Ortiz, M. J., Ropero, J. L., Niño, M. E., Rayon, R., Tzompantzi, F., & Gomez, R. (2009). Evaluation of sulfated Aluminas synthesized via the sol-gel method in the esterification of oleic acid with ethanol. *Chemical Engineering Communications*, 196(10), 1152-1162.
- Amaya, A., P fiz, J., Tancredi, N., & Cordero, T. (2007). Activated carbon pellets from eucalyptus char and tar TG studies. *Journal of Thermal Analysis and Calorimetry*, 89(3), 987-991.
- Asikin-Mijan, N., Lee, H. V., & Taufiq-Yap, Y. H. (2015). Synthesis and catalytic activity of hydration–dehydration treated clamshell derived CaO for biodiesel production. *Chemical Engineering Research and Design*, *102*, 368-377.
- Asikin-Mijan, N., Taufiq-Yap, Y. H., & Lee, H. V. (2015). Synthesis of clamshell derived Ca (OH)<sub>2</sub> nano-particles via simple surfactant-hydration treatment. *Chemical Engineering Journal*, 262, 1043-1051.
- Astruc, D., Lu, F., & Aranzaes, J. R. (2005). Nanoparticles as recyclable catalysts: the frontier between homogeneous and heterogeneous catalysis. *Angewandte Chemie International Edition*, 44(48), 7852-7872.
- Aworn, A., Thiravetyan, P., & Nakbanpote, W. (2009). Preparation of CO<sub>2</sub> activated carbon from corncob for monoethylene glycol adsorption. *Colloids and Surfaces A: Physicochemical and Engineering Aspects*, 333(1), 19-25.
- Aziz, M. A. A., Jalil, A. A., Triwahyono, S., & Ahmad, A. (2015). CO<sub>2</sub> methanation over heterogeneous catalysts: recent progress and future prospects. *Green Chemistry*, 17(5), 2647-2663.
- Babu, N. S., Sree, R., Prasad, P. S., & Lingaiah, N. (2008). Room-temperature transesterification of edible and nonedible oils using a heterogeneous strong basic Mg/La catalyst. *Energy & Fuels*, 22(3), 1965-1971.

- Bagheri, S., Muhd Julkapli, N., & Bee Abd Hamid, S. (2014). Titanium dioxide as a catalyst support in heterogeneous catalysis. *The Scientific World Journal*, 2014.
- Bancquart, S., Vanhove, C., Pouilloux, Y., & Barrault, J. (2001). Glycerol transesterification with methyl stearate over solid basic catalysts: I. Relationship between activity and basicity. *Applied Catalysis A: General*,218(1), 1-11.
- Barakos, N., Pasias, S., & Papayannakos, N. (2008). Transesterification of triglycerides in high and low quality oil feeds over an HT2 hydrotalcite catalyst. *Bioresource Technology*, 99(11), 5037-5042.
- Baskar, G., & Aiswarya, R. (2016). Trends in catalytic production of biodiesel from various feedstocks. *Renewable and Sustainable Energy Reviews*, 57, 496-504.
- Behzadi, S., & Farid, M. M. (2007). Review: examining the use of different feedstock for the production of biodiesel. *Asia-Pacific Journal of Chemical Engineering*, 2(5), 480-486.
- Bloch, M., Bournay, L., Casanave, D., Chodorge, J. A., Coupard, V., Hillion, G., & Lorne, D. (2008). Fatty acid esters in Europe: market trends and technological perspectives. *Oil & Gas Science and Technology-Revue de l'IFP*, 63(4), 405-417.
- Bo, X., Guomin, X., Lingfeng, C., Ruiping, W., & Lijing, G. (2007). Transesterification of palm oil with methanol to biodiesel over a KF/Al2O3 heterogeneous base catalyst. *Energy & Fuels*, 21(6), 3109-3112.
- BONTEMPS, J., BUREL, M., DRAGOMIR, A., & DUMITRESCU, E. (2009). Biofuels and food production Ethical issues. *Proceedings of IP Bioethics in Life Sciences and Environmental Sciences, Lublin, http://tinyurl. com/owkgbs3.*
- Can, Ö., Öztürk, E., Solmaz, H., Aksoy, F., Çinar, C., & Yücesu, H. S. (2016).
   Combined effects of soybean biodiesel fuel addition and EGR application on the combustion and exhaust emissions in a diesel engine. *Applied Thermal Engineering*, 95, 115-124.
- Canakci, M., & Van Gerpen, J. (2001). Biodiesel production from oils and fats with high free fatty acids. *Transactions of the ASAE*, 44(6), 1429.
- Cardoso, A. L., Neves, S. C. G., & Da Silva, M. J. (2008). Esterification of oleic acid for biodiesel production catalyzed by SnCl<sub>2</sub>: a kinetic investigation.*Energies*, 1(2), 79-92.
- Chen, H., Peng, B., Wang, D., & Wang, J. (2007). Biodiesel production by the transesterification of cottonseed oil by solid acid catalysts. *Frontiers of Chemical Engineering in China*, 1(1), 11-15.

- Chen, X. R., Ju, Y. H., & Mou, C. Y. (2007). Direct synthesis of mesoporous sulfated silica-zirconia catalysts with high catalytic activity for biodiesel via esterification. *The Journal of Physical Chemistry C*, 111(50), 18731-18737.
- Chhetri, A. B., Watts, K. C., & Islam, M. R. (2008). Waste cooking oil as an alternate feedstock for biodiesel production. *Energies*, *1*(1), 3-18.
- Chorkendorff, I., & Niemantsverdriet, J. W. (2006). *Concepts of modern catalysis and kinetics*. John Wiley & Sons.
- Crocker, M. (Ed.). (2010). *Thermochemical conversion of biomass to liquid fuels and chemicals* (No. 1). Royal Society of Chemistry.
- Dai, Y. M., Wu, J. S., Chen, C. C., & Chen, K. T. (2015). Evaluating the optimum operating parameters on transesterification reaction for biodiesel production over a LiAlO<sub>2</sub> catalyst. *Chemical Engineering Journal*, 280, 370-376.
- de Mattos, F. C., de Souza, J. A. D. S., Ana, B. D. A., de Macedo, J. L., Dias, J. A., Dias, S. C., & Ghesti, G. F. (2012). Lewis acid/surfactant rare earth trisdodecylsulfate catalysts for biodiesel production from waste cooking oil. *Applied Catalysis A: General*, 423, 1-6.
- de Pietre, M. K., Almeida, L. C., Landers, R., Vinhas, R. C., & Luna, F. J. (2010). H<sub>3</sub>PO<sub>4</sub>-and H2SO4-treated niobic acid as heterogeneous catalyst for methyl ester production. *Reaction Kinetics, Mechanisms and Catalysis*,99(2), 269-280.
- Delfort, B., Hillion, G., Le Pennec, D., & Lendresse, C. (2006). U.S. Patent No. 7,151,187. Washington, DC: U.S. Patent and Trademark Office.
- Demirbas, A. (2007). Biodiesel from sunflower oil in supercritical methanol with calcium oxide. *Energy Conversion and Management*, 48(3), 937-941.
- Demirbas, A. (2008). Comparison of transesterification methods for production of biodiesel from vegetable oils and fats. *Energy Conversion and Management*, 49(1), 125-130.

Demirbas, A. (2011). Competitive liquid biofuels from biomass. *Applied Energy*, 88(1), 17-28.

- Dietrich, P. J., Sollberger, F. G., Akatay, M. C., Stach, E. A., Delgass, W. N., Miller, J. T., & Ribeiro, F. H. (2014). Structural and catalytic differences in the effect of Co and Mo as promoters for Pt-based aqueous phase reforming catalysts. *Applied Catalysis B: Environmental*, 156, 236-248.
- do Nascimento, L. A. S., Tito, L. M., Ang dica, R. S., Da Costa, C. E., Zamian, J. R., & da Rocha Filho, G. N. (2011). Esterification of oleic acid over solid acid catalysts prepared from Amazon flint kaolin. *Applied Catalysis B: Environmental*, 101(3), 495-503.

- Dobrzeniecka, A., & Kulesza, P. J. (2013). Electrocatalytic Activity toward Oxygen Reduction of RuSxNy Catalysts Supported on Different Nanostructured Carbon Carriers. *ECS Journal of Solid State Science and Technology*, 2(12), M61-M66.
- Dossin, T. F., Reyniers, M. F., & Marin, G. B. (2006). Kinetics of heterogeneously MgO-catalyzed transesterification. *Applied Catalysis B: Environmental*, 62(1), 35-45.
- Erdem, M., Orhan, R., Şahin, M., & Aydın, E. (2016). Preparation and Characterization of a Novel Activated Carbon from Vine Shoots by ZnCl<sub>2</sub>.*Water, Air, & Soil Pollution, 227*(7), 1-14.
- Ertl, G., Knözinger, H., & Weitkamp, J. (Eds.). (2008). *Preparation of solid catalysts*. John Wiley & Sons.
- Farris, T. S., Coe, C. G., Armor, J. N., & Schork, J. M. (1992). U.S. Patent No. 5,164,355. Washington, DC: U.S. Patent and Trademark Office.
- Furuta, S., Matsuhashi, H., & Arata, K. (2006). Biodiesel fuel production with solid amorphous-zirconia catalysis in fixed bed reactor. *Biomass and Bioenergy*, *30*(10), 870-873.
- Gao, Y., Yue, Q., Gao, B., Sun, Y., Wang, W., Li, Q., & Wang, Y. (2013). Preparation of high surface area-activated carbon from lignin of papermaking black liquor by KOH activation for Ni (II) adsorption. *Chemical engineering journal*, 217, 345-353.
- Garcia, C. M., Teixeira, S., Marciniuk, L. L., & Schuchardt, U. (2008). Transesterification of soybean oil catalyzed by sulfated zirconia. *Bioresource Technology*, 99(14), 6608-6613.
- Granados, M. L., Alonso, D. M., Sadaba, I., Mariscal, R., & Oc ón, P. (2009). Leaching and homogeneous contribution in liquid phase reaction catalysed by solids: the case of triglycerides methanolysis using CaO. *Applied Catalysis B: Environmental*, 89(1), 265-272.
- Guan, Q., Shang, H., Liu, J., Gu, J., Li, B., Miao, R., ... & Ning, P. (2016). Biodiesel from transesterification at low temperature by AlCl<sub>3</sub> catalysis in ethanol and carbon dioxide as cosolvent: Process, mechanism and application. *Applied Energy*, *164*, 380-386.
- Guha, O. K., & Roy, J. (1995). Characterization of carbon molecular sieves by molecular probe chromatography. *Fuel processing technology*, 43(1), 61-69.
- Guo, J., & Lua, A. C. (2003). Textural and chemical properties of adsorbent prepared from palm shell by phosphoric acid activation. *Materials chemistry and physics*, 80(1), 114-119.

- Guo, M., Song, W., & Buhain, J. (2015). Bioenergy and biofuels: History, status, and perspective. *Renewable and Sustainable Energy Reviews*, 42, 712-725.
- Hagemeyer, A., Hogan, Z., Schlichter, M., Smaka, B., Streukens, G., Turner, H., ... & Yaccato, K. (2007). High surface area tin oxide. *Applied Catalysis A: General*, 317(2), 139-148.
- Hayashi, J. I., Kazehaya, A., Muroyama, K., & Watkinson, A. P. (2000). Preparation of activated carbon from lignin by chemical activation. *Carbon*,38(13), 1873-1878.
- Heidari, A., Younesi, H., Rashidi, A., & Ghoreyshi, A. A. (2014). Evaluation of CO<sub>2</sub> adsorption with eucalyptus wood based activated carbon modified by ammonia solution through heat treatment. *Chemical Engineering Journal*,254, 503-513.
- Hesas, R. H., Arami-Niya, A., Daud, W. M. A. W., & Sahu, J. N. (2013). Preparation and characterization of activated carbon from apple waste by microwaveassisted phosphoric acid activation: application in methylene blue adsorption. *BioResources*, 8(2), 2950-2966.
- HINODE, H. (2013). Comparison of Activated Carbons Prepared from Indonesian Forest and Agricultural Residues. *Asian Journal of Chemistry*,23(3), 1569-1575.
- Hu, Z., & Vansant, E. F. (1995). Carbon molecular sieves produced from walnut shell. *Carbon*, 33(5), 561-567.
- Huang, R., Cheng, J., Qiu, Y., Li, T., Zhou, J., & Cen, K. (2016). Effects of cytoplasm and reactant polarities on acid-catalyzed lipid transesterification in wet microalgal cells subjected to microwave irradiation. *Bioresource* technology, 200, 738-743.
- Islam, A., Taufiq-Yap, Y. H., Chu, C. M., Ravindra, P., & Chan, E. S. (2013). Transesterification of palm oil using KF and NaNO<sub>3</sub> catalysts supported on spherical millimetric  $\gamma$ -Al<sub>2</sub>O <sub>3</sub>. *Renewable energy*, *59*, 23-29.
- Jain, A., Ong, V., Jayaraman, S., Balasubramanian, R., & Srinivasan, M. P. (2016).
   Supercritical fluid immobilization of horseradish peroxidase on high surface area mesoporous activated carbon. *The Journal of Supercritical Fluids*, 107, 513-518.
- Jandosov, J. M., Shikina, N. V., Bijsenbayev, M. A., Shamalov, M. E., Ismagilov, Z. R., & Mansurov, Z. A. (2016). Evaluation of Synthetic Conditions for H<sub>3</sub>PO<sub>4</sub> Chemically Activated Rice Husk and Preparation of Honeycomb Monoliths. *Eurasian Chemico-Technological Journal*, 11(3), 245-252.
- Jothiramalingam, R., & Wang, M. K. (2009). Review of recent developments in solid acid, base, and enzyme catalysts (heterogeneous) for biodiesel production via transesterification. *Industrial & Engineering Chemistry Research*, 48(13), 6162-6172.

- Kawashima, A., Matsubara, K., & Honda, K. (2008). Development of heterogeneous base catalysts for biodiesel production. *Bioresource technology*, 99(9), 3439-3443.
- Kemp, W. H. (2006). *Biodiesel: basics and beyond: a comprehensive guide to production and use for the home and farm.* Tamworth, Ont.: Aztext Press.
- Kezrane, C., Awad, S., Loubar, K., Liazid, A., & Tazerout, M. (2016). Experimental assessment of performance and emissions maps for biodiesel fueled compression ignition engine.
- Knothe, G., & Steidley, K. R. (2009). A comparison of used cooking oils: a very heterogeneous feedstock for biodiesel. *Bioresource technology*, *100*(23), 5796-5801.
- Kouzu, M., Kasuno, T., Tajika, M., Sugimoto, Y., Yamanaka, S., & Hidaka, J. (2008). Calcium oxide as a solid base catalyst for transesterification of soybean oil and its application to biodiesel production. *Fuel*, 87(12), 2798-2806.
- Laidler, K. J. (1986). The development of theories of catalysis. *Archive for history of exact sciences*, *35*(4), 345-374.
- Leach, B. (Ed.). (2012). Applied industrial catalysis. Elsevier.
- Lee, D. W., Park, Y. M., & Lee, K. Y. (2009). Heterogeneous base catalysts for transesterification in biodiesel synthesis. *Catalysis Surveys from Asia*,13(2), 63-77.
- Lee, H. V., & Taufiq-Yap, Y. H. (2015). Optimization study of binary metal oxides catalyzed transesterification system for biodiesel production. *Process Safety and Environmental Protection*, 94, 430-440.
- Lee, H. V., Juan, J. C., & Taufiq-Yap, Y. H. (2015). Preparation and application of binary acid–base CaO–La<sub>2</sub>O<sub>3</sub> catalyst for biodiesel production. *Renewable Energy*, 74, 124-132.
- Lee, H. V., Juan, J. C., & Taufiq-Yap, Y. H. (2015). Preparation and application of binary acid–base CaO–La<sub>2</sub>O<sub>3</sub> catalyst for biodiesel production. *Renewable Energy*, *74*, 124-132.
- Lee, H. V., Juan, J. C., Abdullah, N. F. B., & Taufiq-Yap, Y. H. (2014). Heterogeneous base catalysts for edible palm and non-edible Jatropha-based biodiesel production. *Chemistry Central Journal*, 8(1), 1.
- Li, C., & Kumar, S. (2016). Preparation of activated carbon from un-hydrolyzed biomass residue. *Biomass Conversion and Biorefinery*, 1-13.
- Liou, T. H. (2010). Development of mesoporous structure and high adsorption capacity of biomass-based activated carbon by phosphoric acid and zinc chloride activation. *Chemical Engineering Journal*, *158*(2), 129-142.

- Liu, Y., Lotero, E., Goodwin, J. G., & Mo, X. (2007). Transesterification of poultry fat with methanol using Mg–Al hydrotalcite derived catalysts. *Applied Catalysis A: General*, 331, 138-148.
- L ópez, D. E., Goodwin, J. G., Bruce, D. A., & Furuta, S. (2008). Esterification and transesterification using modified-zirconia catalysts. *Applied Catalysis A: General*, 339(1), 76-83.
- Lotero, E., Liu, Y., Lopez, D. E., Suwannakarn, K., Bruce, D. A., & Goodwin, J. G. (2005). Synthesis of biodiesel via acid catalysis. *Industrial & engineering chemistry research*, 44(14), 5353-5363.
- Łukaszewicz, J. P., & Wesołowski, R. P. (2008). Fabrication of molecular-sieve-type carbons from Salix viminalis. *Microporous and Mesoporous Materials*, 116(1), 723-726.
- Luo, C., Zheng, Y., Ding, N., Wu, Q., Bian, G., & Zheng, C. (2010). Development and performance of CaO/La<sub>2</sub>O<sub>3</sub> sorbents during calcium looping cycles for CO2 capture. *Industrial & Engineering Chemistry Research*, 49(22), 11778-11784.
- Macala, G. S., Robertson, A. W., Johnson, C. L., Day, Z. B., Lewis, R. S., White, M. G., ... & Ford, P. C. (2008). Transesterification catalysts from iron doped hydrotalcite-like precursors: solid bases for biodiesel production. *Catalysis Letters*, 122(3-4), 205-209.
- Macedo, C., Abreu, F. R., Tavares, A. P., Alves, M. B., Zara, L. F., Rubim, J. C., & Suarez, P. A. (2006). New heterogeneous metal-oxides based catalyst for vegetable oil trans-esterification. *Journal of the Brazilian Chemical Society*, 17(7), 1291-1296.
- Meher, L. C., Sagar, D. V., & Naik, S. N. (2006). Technical aspects of biodiesel production by transesterification—a review. *Renewable and sustainable* energy reviews, 10(3), 248-268.
- Melero, J. A., Iglesias, J., & Morales, G. (2009). Heterogeneous acid catalysts for biodiesel production: current status and future challenges. *Green Chemistry*, *11*(9), 1285-1308.
- Milano, J., Ong, H. C., Masjuki, H. H., Chong, W. T., Lam, M. K., Loh, P. K., & Vellayan, V. (2016). Microalgae biofuels as an alternative to fossil fuel for power generation. *Renewable and Sustainable Energy Reviews*, 58, 180-197.
- Mizsey, P., & Racz, L. (2010). Cleaner production alternatives: biomass utilisation options. *Journal of Cleaner Production*, 18(8), 767-770.
- Mohanty, K., Das, D., & Biswas, M. N. (2006). Preparation and characterization of activated carbons from Sterculia alata nutshell by chemical activation with zinc chloride to remove phenol from wastewater. *Adsorption*, *12*(2), 119-132.

- Monirul, I. M., Masjuki, H. H., Kalam, M. A., Zulkifli, N. W. M., Rashedul, H. K., Rashed, M. M., ... & Mosarof, M. H. (2015). A comprehensive review on biodiesel cold flow properties and oxidation stability along with their improvement processes. *RSC Advances*, 5(105), 86631-86655.
- Moreno, J. I., Jaimes, R., Gómez, R., & Niño-Gómez, M. E. (2011). Evaluation of sulfated tin oxides in the esterification reaction of free fatty acids. *Catalysis Today*, *172*(1), 34-40.
- Muñoz-Gonz áez, Y., Arriagada-Acuña, R., Soto-Garrido, G., & Garc á-Lovera, R. (2009). Activated carbons from peach stones and pine sawdust by phosphoric acid activation used in clarification and decolorization processes. *Journal of chemical technology and biotechnology*, 84(1), 39-47.
- Narayan, R. C., & Madras, G. (2016). Alkylation of fatty acids in supercritical alcohols. *Energy & Fuels*, *30*(5), 4104-4111.
- Nizah, M. R., Taufiq-Yap, Y. H., Rashid, U., Teo, S. H., Nur, Z. S., & Islam, A. (2014). Production of biodiesel from non-edible Jatropha curcas oil via transesterification using Bi<sub>2</sub>O<sub>3</sub>-La<sub>2</sub> O<sub>3</sub> catalyst. *Energy Conversion and Management*, 88, 1257-1262.
- Nor, N. M., Lau, L. C., Lee, K. T., & Mohamed, A. R. (2013). Synthesis of activated carbon from lignocellulosic biomass and its applications in air pollution control—a review. *Journal of Environmental Chemical Engineering*,1(4), 658-666.
- Onyesty &, G., & B άa, A. (2009). Sorption dynamics of N<sub>2</sub> and O<sub>2</sub> in carbon monoliths from spruce, beech and oak affected by activation.*Microporous and Mesoporous Materials*, *120*(1), 84-90.

Orszulik, S. T. (Ed.). (2008). Environmental technology in the oil industry. Springer.

- Park, Y. M., Lee, D. W., Kim, D. K., Lee, J. S., & Lee, K. Y. (2008). The heterogeneous catalyst system for the continuous conversion of free fatty acids in used vegetable oils for the production of biodiesel. *Catalysis Today*, *131*(1), 238-243.
- Patil, P., Gude, V. G., Pinappu, S., & Deng, S. (2011). Transesterification kinetics of Camelina sativa oil on metal oxide catalysts under conventional and microwave heating conditions. *Chemical engineering journal*, 168(3), 1296-1300.
- Peng, Z., Guo, Z., Chu, W., & Wei, M. (2016). Facile synthesis of high-surface-area activated carbon from coal for supercapacitors and high CO<sub>2</sub> sorption. *RSC Advances*, 6(48), 42019–42028.
- Rashidi, N. A., & Yusup, S. (2016). An overview of activated carbons utilization for the post-combustion carbon dioxide capture. *Journal of CO<sub>2</sub> Utilization*, *13*, 1-16.

- Reed, A. R., & Williams, P. T. (2004). Thermal processing of biomass natural fibre wastes by pyrolysis. *International Journal of Energy Research*, 28(2), 131-145.
- Refaat, A. A. (2011). Biodiesel production using solid metal oxide catalysts.*International Journal of Environmental Science & Technology*, 8(1), 203-221.
- Robertson, A. J. B. (1970). Catalysis of gas reactions by metals.*SPRINGER-VERLAG*, *NEW YORK*. 1970, 182 P.
- Ryu, J. C., Lee, D. H., Kang, K. S., Park, C. S., Kim, J. W., & Kim, Y. H. (2008). Effect of additives on redox behavior of iron oxide for chemical hydrogen storage. *Journal of Industrial and Engineering Chemistry*, 14(2), 252-260.
- Sastry, S. V. A. R., & Murthy, C. V. R. (2012). Prospectus of biodiesel for future energy security. *Elexir, Chemical Engg*, 53, 12029-12034.
- Schuchardt, U., Sercheli, R., & Vargas, R. M. (1998). Transesterification of vegetable oils: a review. *Journal of the Brazilian Chemical Society*, 9(3), 199-210.
- Schuchardt, U., Vargas, R. M., & Gelbard, G. (1996). Transesterification of soybean oil catalyzed by alkylguanidines heterogenized on different substituted polystyrenes. *Journal of Molecular Catalysis A: Chemical*, 109(1), 37-44.
- Sercheli, R., Vargas, R. M., & Schuchardt, U. (1999). Alkylguanidine-catalyzed heterogeneous transesterification of soybean oil. *Journal of the American Oil Chemists' Society*, 76(10), 1207-1210.
- Shuit, S. H., Ng, E. P., & Tan, S. H. (2015). A facile and acid-free approach towards the preparation of sulphonated multi-walled carbon nanotubes as a strong protonic acid catalyst for biodiesel production. *Journal of the Taiwan Institute of Chemical Engineers*, *52*, 100-108.

Simanzhenkov, V., & Idem, R. (2003). Crude oil chemistry. CRC Press.

- Singh, D., Bhoi, R., Ganesh, A., & Mahajani, S. (2014). Synthesis of biodiesel from vegetable oil using supported metal oxide catalysts. *Energy & Fuels*, 28(4), 2743-2753.
- Soldi, R. A., Oliveira, A. R., Ramos, L. P., & C ésar-Oliveira, M. A. F. (2009). Soybean oil and beef tallow alcoholysis by acid heterogeneous catalysis. *Applied Catalysis A: General*, *361*(1), 42-48.

Speight, J. G., & Ozum, B. (Eds.). (2001). Petroleum refining processes. CRC Press.

Striolo, A., Chialvo, A. A., Gubbins, K. E., & Cummings, P. T. (2005). Water in carbon nanotubes: Adsorption isotherms and thermodynamic properties from molecular simulation. *The Journal of chemical physics*, 122(23), 234712.

- Su, M., Yang, R., & Li, M. (2013). Biodiesel production from hempseed oil using alkaline earth metal oxides supporting copper oxide as bi-functional catalysts for transesterification and selective hydrogenation. *Fuel*, 103, 398-407.
- Sunita, G., Devassy, B. M., Vinu, A., Sawant, D. P., Balasubramanian, V. V., & Halligudi, S. B. (2008). Synthesis of biodiesel over zirconia-supported isopoly and heteropoly tungstate catalysts. *Catalysis Communications*, 9(5), 696-702.
- Suwannakarn, K., Lotero, E., Goodwin, J. G., & Lu, C. (2008). Stability of sulfated zirconia and the nature of the catalytically active species in the transesterification of triglycerides. *Journal of Catalysis*, 255(2), 279-286.
- Taghizadeh-Alisaraei, A., Ghobadian, B., Tavakoli-Hashjin, T., Mohtasebi, S. S., Rezaei-asl, A., & Azadbakht, M. (2016). Characterization of engine's combustion-vibration using diesel and biodiesel fuel blends by time-frequency methods: A case study. *Renewable Energy*, 95, 422-432.
- Takase, M., Chen, Y., Liu, H., Zhao, T., Yang, L., & Wu, X. (2014). Biodiesel production from non-edible Silybum marianum oil using heterogeneous solid base catalyst under ultrasonication. *Ultrasonics sonochemistry*, 21(5), 1752-1762.
- Taufiq-Yap, Y. H., Lee, H. V., & Lau, P. L. (2012). Transesterification of jatropha curcas oil to biodiesel by using short necked clam (orbicularia orbiculata) shell derived catalyst. *Energy Exploration & Exploitation*, 30(5), 853-866.
- Taufiq-Yap, Y. H., Lee, H. V., Hussein, M. Z., & Yunus, R. (2011). Calcium-based mixed oxide catalysts for methanolysis of Jatropha curcas oil to biodiesel. *biomass and bioenergy*, 35(2), 827-834.
- Taufiq-Yap, Y. H., Teo, S. H., Rashid, U., Islam, A., Hussien, M. Z., & Lee, K. T. (2014). Transesterification of Jatropha curcas crude oil to biodiesel on calcium lanthanum mixed oxide catalyst: Effect of stoichiometric composition. *Energy Conversion and Management*, 88, 1290-1296.
- Temdrara, L., Addoun, A., & Khelifi, A. (2015). Development of olivestonesactivated carbons by physical, chemical and physicochemical methods for phenol removal: a comparative study. *Desalination and Water Treatment*,53(2), 452-461.
- Thitame, P. V., & Shukla, S. R. (2016). Porosity Development of Activated Carbons Prepared from Wild Almond Shells and Coir Pith Using Phosphoric Acid. *Chemical Engineering Communications*, 203(6), 791-800.
- Wen, L., Li, F., & Cheng, H. M. (2016). Carbon Nanotubes and Graphene for Flexible Electrochemical Energy Storage: from Materials to Devices. Advanced Materials.

- Wilson, K., Hardacre, C., Lee, A. F., Montero, J. M., & Shellard, L. (2008). The application of calcined natural dolomitic rock as a solid base catalyst in triglyceride transesterification for biodiesel synthesis. *Green chemistry*, *10*(6), 654-659.
- Woudhuysen, J. (Ed.). (2012). Fuel for Thought: Early June-Mid August 2012. *Energy* & *Environment*, 23(6-7), 1105-1190.
- Xie, W., & Huang, X. (2006). Synthesis of biodiesel from soybean oil using heterogeneous KF/ZnO catalyst. *Catalysis Letters*, 107(1-2), 53-59.
- Xie, W., & Zhao, L. (2013). Production of biodiesel by transesterification of soybean oil using calcium supported tin oxides as heterogeneous catalysts.*Energy Conversion and Management*, *76*, 55-62.
- Yan, S., Lu, H., & Liang, B. (2007). Supported CaO catalysts used in the transesterification of rapeseed oil for the purpose of biodiesel production.*Energy & Fuels*, 22(1), 646-651.
- Yan, S., Salley, S. O., & Ng, K. S. (2009). Simultaneous transesterification and esterification of unrefined or waste oils over ZnO-La<sub>2</sub>O<sub>3</sub> catalysts.*Applied Catalysis A: General*, *353*(2), 203-212.
- Zabeti, M., Daud, W. M. A. W., & Aroua, M. K. (2009). Activity of solid catalysts for biodiesel production: a review. *Fuel Processing Technology*,90(6), 770-777.
- Zhang, F., Xiang, X., Li, F., & Duan, X. (2008). Layered double hydroxides as catalytic materials: recent development. *Catalysis surveys from Asia*, 12(4), 253-265.
- Zhang, T., Walawender, W. P., & Fan, L. T. (2005). Preparation of carbon molecular sieves by carbon deposition from methane. *Bioresource technology*, *96*(17), 1929-1935.
- Zhang, T., Walawender, W. P., & Fan, L. T. (2005). Preparation of carbon molecular sieves by carbon deposition from methane. *Bioresource technology*, *96*(17), 1929-1935.
- Zhong, H., Watanabe, M., Enomoto, H., Jin, F., Kishita, A., Aida, T. M., & Smith, R.L. (2016). Winterization of vegetable oil blends for biodiesel fuels and correlation based on initial saturated fatty acid constituents. *Energy & Fuels*.