

UNIVERSITI PUTRA MALAYSIA

METAL OXIDE MODIFIED LIMESTONE CATALYSTS FOR GASIFICATION OF RICE STRAW IN HYDROGEN PRODUCTION

SURAHIM BIN MOHAMAD @ MAHMUD

FS 2016 55



METAL OXIDE MODIFIED LIMESTONE CATALYSTS FOR GASIFICATION OF RICE STRAW IN HYDROGEN PRODUCTION

By

SURAHIM BIN MOHAMAD @ MAHMUD

Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in fulfilment of the Requirements for the Degree of Master of Science

COPYRIGHT

All materials contained within the thesis, including without limitation text, logos, icons, photographs and all other artworks, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



DEDICATED

To my beloved parents

Mohamad @ Mahmud Bin Tahir Almarhumah Aminah Binti Harun (7.3.1955 – 8.1.2014) (may Allah grants her the highest Jannah)



METAL OXIDE MODIFIED LIMESTONE CATALYSTS FOR GASIFICATION OF RICE STRAW IN HYDROGEN PRODUCTION

By

SURAHIM BIN MOHAMAD @ MAHMUD

May 2016

Chairman : Prof. Taufiq Yap Yun Hin, PhD

Faculty : Science

Hydrogen has great potential for energy and environmental sustainability. Hydrogen is considered as a secondary source of energy, commonly referred to as an energy carrier which is used to store and transport energy in a form that can be easily used. Hydrogen does not exist freely in nature, it only produced from other sources. The potential of utilization of biomass as renewable and sustainable energy resources have attracted researchers to produce hydrogen from cheap and highly available resources such as lignocellulosic biomass waste. Biomass gasification of rice straw using modified natural limestone based catalysts has been studied to promote the production of hydrogen. This study is aimed to develop natural calcined limestone (CL) based catalysts with high activity and selectivity. Modification with addition of mono and bimetallic metal dopants (Ni, Fe, Co, NiCo, NiFe and CoFe) on CL were performed for gasification of rice straw biomass for hydrogen conversion. The catalysts were synthesized through wet impregnation method and characterized by using X-ray diffraction (XRD), Brunauer-Emmett-Teller (BET) surface area, Thermogravimetry analysis (TGA), Field emission scanning electron microscopy - Energy dispersive Xray (FESEM-EDX) and Temperature programmed desorption of carbon dioxide (TPD-CO₂) to determine the structure, physical and chemical properties of the catalysts. Temperature programmed gasification (TPG) was conducted to investigate the gasification reaction of rice straw and the product gases were analysed using online mass spectrometer. The gasification process was carried out in partial oxygen (5% O₂/Helium) environment heating from 50 to 900 °C with mass ratio of biomass to catalyst of 2:1. The results revealed that the addition of metal dopants on CL significantly improves the activity and selectivity towards hydrogen production. For monometallic doped catalysts, Ni-CL was found to give the highest H2 conversion followed by Co-CL and Fe-CL. Moreover, The CL had shown to act both as catalyst and CO₂ sorbent thus enhanced the production of hydrogen. The additions of bimetallic dopant have shown a further increment of hydrogen yield. The NiCo-CL catalyst exhibit highest hydrogen selectivity compared to other catalysts due to improvement in catalytic activity that enhanced gasification of rice straw and promoted hydrogen favoured reactions.

MANGKIN LOGAM OKSIDA MODIFIKASI BATU KAPUR BAGI PENGEGASAN JERAMI PADI DALAM PENGHASILAN HIDROGEN

Oleh

SURAHIM BIN MOHAMAD @ MAHMUD

May 2016

Pengerusi : Prof. Taufiq Yap Yun Hin, PhD

Fakulti : Sains

Hidrogen mempunyai potensi yang besar untuk kelestarian tenaga dan alam sekitar. Hidrogen dianggap sebagai sumber tenaga sekunder yang biasanya dirujuk sebagai pembawa tenaga yang digunakan untuk menyimpan dan mengangkut tenaga dalam bentuk yang mudah digunakan. Hidrogen tidak wujud secara bebas dalam alam semulajadi, ia hanya dihasilkan daripada sumber-sumber yang lain. Potensi penggunaan biojisim sebagai sumber tenaga boleh diperbaharui dan mapan telah menarik penyelidik untuk menghasilkan hidrogen dari sumber yang murah dan mudah didapati seperti daripada sisa biojisim lignoselulosa. Pengegasan biojisim daripada jerami padi dengan mnggunakan mangkin berasaskan batu kapur semula jadi yang diubahsuai telah dikaji untuk menggalakkan pengeluaran hidrogen. Kajian ini adalah bertujuan untuk membangunkan mangkin yang berasaskan batu kapur asli terkalsin (CL) yang mempunyai aktiviti dan kepilihan yang tinggi. Pengubahsuaian mangkin dengan penambahan bahan dop mono dan dwilogam (Ni, Fe, Co, NiCo, NiFe dan CoFe) ke atas CL telah digunakan dalam proses pengegasan biojisim jerami padi untuk penukaran hidrogen. Mangkin telah disintesis dengan menggunakan kaedah pengisitepuan basah dan dicirikan dengan menggunakan kaedah pembelauan sinar-X (XRD), analisis luas permukaan menggunakan kaedah Brunauer-Emmett-Teller (BET), analisis terma gravimetri (TGA), mikroskop imbasan elektron pancaran medan -Tenaga penyerakan sinar-X (FESEM-EDX) dan aturcara suhu nyahjerapan karbon dioksida (TPD-CO₂) bagi menentukan struktur serta sifat-sifat fizik dan kimia mangkin. Program-suhu-pengegasan (TPG) telah dijalan bagi menyiasat tindak balas pengegasan biojisim jerami padi dan gas yang terhasil daripada porses pengegasan ini dianalisis dengan menggunakan spektroskopi jisim secara dalam talian. Proses pengegasan dijalankan dalam keadaan separa oksigen (5 % O₂/helium) dan pemanasan pada suhu 50 - 900 ° C dengan nisbah biojisim/mangkin adalah 2:1. Hasil kajian menunjukkan bahawa penambahan bahan dop logam pada CL meningkatkan aktiviti dan kepilihan yang ketara ke atas pengeluaran hidrogen. Bagi mangkin dop monologam, Ni-CL didapati memberikan kadar penukaran hidrogen tertinggi diikuti oleh Co-CL dan Fe-CL. Selain bertindak sebagai mangkin, CL juga bertindak sebagai bahan penjerap bagi gas karbon dioksida di mana ianya telah meningkatkan lagi

pengeluaran hidrogen. Penambahan bahan dopan dwilogam telah menunjukkan peningkatan dalam penghasilan hidrogen. Mangkin NiCo-CL mempamerkan kepilihan yang tinggi terhadap hidrogen berbanding dengan mangkin yang lain. Hal ini disebabkan oleh pengingkatan dalam aktiviti mangkin tersebut yang meningkatkan lagi kadar tindak balas pengegasan biojisim jerami padi sekaligus menggalakkan tindak balas penukaran hidrogen.

ACKNOWLEDGEMENTS

In the name of Allah, the Most Gracious and the Most Merciful

I wish to express my outmost gratitude to Allah SWT for the strength and patience He bestowed on me to complete this study.

I would like to express my greatest gratitude to my main supervisor, Professor Dr. Taufiq Yap Yun Hin, for his guidance, suggestion, patience, support and encouragement throughout my study in Universiti Putra Malaysia. His valuable advices and humanitarian values have giving significant impact towards my morale and skills in conducting my research and my life. I am also grateful to my co-supervisor, Professor Dr. Mohd Zobir Hussein for his guidance and help during the study. I express my special thanks to our post-doc, Dr. Aminul Islam and research officer, Tengku Sharifah Marliza Tengku Azmi and to all the PutraCAT members for their support, expertise and valuable friendship during the period. I sincerely thanks to all staffs in Chemistry Department, Faculty of Science and Institute of Bioscience, UPM for their prompt assistant in technical issue, opinion that has helped me to complete my research.

Lastly, my deepest gratitude goes to my parents and all my family members for their endless love, prayers and continuous support throughout my study. May Allah bless all of us.

This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfilment of the requirement of the degree of Master of Science. The members of Supervisory committee were as follows:

Taufiq Yap Yun Hin, PhD

Professor Faculty of Science Universiti Putra Malaysia (Chairman)

Mohd Zobir Hussein, PhD

Professor Institute of Advanced Technology Universiti Putra Malaysia (Member)

BUJANG KIM HUAT, PhD

Professor and Dean School of Graduate Studies Universiti Putra Malaysia

Date:

Declaration by graduate student

I hereby confirm that:

- this thesis is my original work;
- quotations, illustrations and citations have been duly referenced;
- this thesis has not been submitted previously or concurrently for any other degree at any other institutions;
- intellectual property from the thesis and copyright of thesis are fully-owned by Universiti Putra Malaysia, as according to the Universiti Putra Malaysia (Research) Rules 2012;
- written permission must be obtained from supervisor and the office of Deputy Vice-Chancellor (Research and Innovation) before thesis is published (in the form of written, printed or in electronic form) including books, journals, modules, proceedings, popular writings, seminar papers, manuscripts, posters, reports, lecture notes, learning modules or any other materials as stated in the Universiti Putra Malaysia (Research) Rules 2012;
- there is no plagiarism or data falsification/fabrication in the thesis, and scholarly integrity is upheld as according to the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) and the Universiti Putra Malaysia (Research) Rules 2012. The thesis has undergone plagiarism detection software.

~.	
Signature:	Date:
•	

Name and Matric No.: Surahim Bin Mohamad @ Mahmud (GS28428)

Declaration by Members of Supervisory Committee

This is to confirm that:

- the research conducted and the writing of this thesis was under our supervision;
- supervision responsibilities as stated in the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revision 2012-2013) are adhered to.

Signature	:
Name of Chairman of	
Supervisory Committee	: Taufiq Yap Yun Hin, PhD
Signature	:
Name of Members of	
Supervisory Committee	: Mohd Zobir Hussein, PhD

TABLE OF CONTENTS

			Page
APPROV DECLAI LIST OF LIST OF	AK WLEDGI VAL RATION TTABLES	3	i ii iv v vii xii xii
CHAPTI	ER		
1	INTI 1.1 1.2 1.3	RODUCTION Background of the Study Problem Statements Objectives	1 4 5
2	2.1 2.2 2.3 2.4	RATURE REVIEW Rice Straw availability and potential Biomass Conversion Technologies Gasification Types of Catalysts for Gasification Reaction 2.4.1 Natural Mineral Catalysts 2.4.2 Alkaline metal based catalyst 2.4.3 Metal based catalyst	6 8 8 9 10 13 14
3	MAT 3.1 3.2 3.3	Introduction Sample Preparation 3.2.1 Biomass 3.2.2 Catalyst Preparation Sample Characterization 3.3.1 Carbon, Hydrogen, Nitrogen and Sulphur Analysis 3.3.2 X-Ray Fluorescence	16 18 18 18 19 19
		 3.3.2 X-Ray Fluorescence 3.3.3 Thermogravimetric Analysis (TGA) 3.3.4 X-ray Diffraction (XRD) 3.3.5 Brunauer-Emmett-Teller (BET) Surface Area Measurement 3.3.6 Field Emission Scanning Electron Microscopy-Energy Dispersive Spectroscopy 	20 20 20 20
	3.4	(FESEM-EDX) 3.3.7 Temperature Programmed Desorption of carbon dioxide (TPD- CO ₂) Catalytic Evaluation	22 22

4			ND DISCUSSION	24
	4.1		ss Characterization	24
		4.1.1	Carbon, Hydrogen, Nitrogen, Sulfur and	24
			Oxygen Analysis	
		4.1.2	X-ray Fluorescence Spectroscopy (XRF)	24
		4.1.3	Chemical Composition	25
	4.2	Limest	one Characterization	26
		4.2.1	X-ray Fluorescence Spectroscopy (XRF) of	26
			Limestone	
		4.2.2	Thermogravimetry Analysis	26
		4.2.3	X-ray Diffraction (XRD) Analysis	27
	4.3	Single	Metal – Calcined Limestone Characterization	28
		4.3.1	X-ray Diffraction (XRD) Analysis	29
		4.3.2		30
			Measurement	
		4.3.3	Field Emission Scanning Electron	30
			Microscopy - Energy Dispersive	
			Spectroscopy	
		4.3.4	Temperature Programmed Desorption of	33
		1.5.1	Carbon Dioxide (TPD-CO ₂)	33
		4.3.5	Hydrogen production from rice straw	34
		1.5.5	gasification	31
		4.3.6	Temperature programmed gasification of rice	36
		7.5.0	straw	30
	4.4	Rimeta	Il-Limestone Characterization	40
	7.7	4.4.1	X-ray Diffraction (XRD) Analysis	40
		4.4.1	Brunauer-Emmet-Teller (BET) Surface Area	40
		4.4.2	Measurement (BE1) Surface Alea	41
		1.1.2		42
		4.4.3		42
			Microscopy - Energy Dispersive	
		4.4.4	Spectroscopy	1.0
		4.4.4	Temperature Programmed Desorption of	46
		1.15	Carbon Dioxide (TPD-CO ₂)	47
		4.4.5	Temperature programmed gasification of	47
			bimetal dopant-CL catalysts	40
		4.4.6	Hydrogen production from rice straw	49
			gasification	
_	go.		0.34	
5		NCLUSIO		51
	5.1	Conclu		51
	5.2	Recom	mendations	52
DEEDE	NICEC			<i>5</i> 2
REFERE				53
	APPENDICES			61
BIODAT				63
LIST OF	PUBLIC	CATION	S	64

LIST OF TABLES

Table		Page
1.1	Typical level of cellulose, hemicellulose and lignin	3
2.1	Production quantities of paddy, rice straw and rice husk	7
2.2	Composition of rice straw and rice husk	7
2.3	Summary of the Advantages and Disadvantages of Catalysts	13
3.1	List of chemical, gases, equipment and instruments used in experiment	17
3.2	List of Prepared Catalysts	19
4.1	Ultimate analysis of rice straw	24
4.2	XRF analysis of rice straw	25
4.3	Chemical composition of rice straw	25
4.4	XRF analysis of limestone	26
4.5	BET surface area of calcined limestone, Ni-CL, Co-CL, and Fe-CL	30
4.6	Amount of CO ₂ desorbed for CL and single metal doped catalysts	34
4.7	BET surface area of calcined NiCo-CL, CoFe-CL, and NiFe-CL	42
4.8	Amount of CO ₂ desorbed	47

LIST OF FIGURES

Figure		Page
1.1	Non-renewable energy and renewable energy	2
2.1	Global Rice Paddy Production and Area	6
2.2	Diagram of approximate reaction conditions for different catalytic processes	8
2.3	Classification of catalysts used for gasification reaction	10
3.1	The overall overview of the research works	18
3.2	Schematic diagram of catalytic study	22
3.3	Schematic diagram of conventional gasification reactor	23
4.1	Thermogravimetry analysis of natural limestone	27
4.2	XRD patterns for different calcination duration of fresh limestone at 850 C a) 4 h, b) 6 h, c) 8 h, and d) 10 h	28
4.3	XRD patterns for a) CL, b) Co-CL, c) Fe-CL, and d) Ni-CL	29
4.4a	FESEM images of compounds: a) CL, b) Ni-CL, c) Co-CL and d) Fe-CL(magnification: x50K)	31
4.4b	EDX spectra of compounds: (i) CL; (ii) Ni-CL; (iii) Co-CL and (iv) Fe-CL	32
4.5	TPD-CO ₂ profiles for (a) CL; (b) Fe-CL; (c) Ni-CL, and (d) Co-CL	34
4.6	Cumulative H ₂ yield from rice straw gasification	35
4.7	Temperature programmed gasification pattern for catalytic reaction of rice straw using catalyst Ni-CL	38
4.8	XRD patterns ofa) uncalcined NiCo-CL; b) uncalcined CoFe-CL; c) uncalcined NiFe-CL; d) NiCo-CL; e) CoFe-CL and f) NiFe-CL	41
4.9a	FESEM images of compounds: (i) CL; (ii) NiCo-CL; (iii) CoFe-CL and (iv) NiFe-CL (Magnification: x50k)	43

4.9b	EDX spectra of compounds: (i) CL; (ii) NiCo-CL; (iii) CoFe-CL and (iv) NiFe-CL	45
4.10	Temperature-programmed desorption of CO ₂ profiles for (a) CL; (b) NiCo-CL; (c) CoFe-CL and (d) NiFe-CL.	46
4.11	H_2 gas evolution patterns for uncatalyzed and catalyzed gasification	48
4.12	Cumulative H ₂ yield from catalytic rice straw gasification	49



LIST OF ABBREVIATIONS

BET Brunauer Emmett Teller

BJH Barret-Joyner-Halenda

CHNS/O Carbon Hydrogen Nitrogen Sulfur and Oxygen

TCD Thermal Conductivity Detector

TGA Thermal Gravimetry Analysis

Tmax Temperature at maximum peak

TPD Temperature Programmed Desorption

XRD X-Ray Diffraction

JCPDS Joint Committee on Powder Diffraction Standards

CHAPTER 1

INTRODUCTION

1.1 Background of the study

Nowadays, human mankind on the earth is facing serious threats for their life sustainability which of energy crisis and climate change. Currently the global consumption of primary energy is still dominated by fossil fuel energy resources by 35%. It is predicted that the energy demand would be escalated significantly due to the constant growing of population and modern human activities. With the introduction of fossil fuels in the forms of coal, petroleum and natural gas, the world increasingly became dependent on these fossil fuel sources. This automatically led to much more exploitation and utilisation of fossil fuels. Thus the reserves of fossil fuel sources is being depleted in the near future and a massive increase of pollutants is being released to the atmosphere, water and soil, causing harmful effects on the environment and human health due to the fossil fuel combustion. Carbon dioxide (CO₂) as the main gas emission from the fossil fuel combustion is being known as greenhouse gas (GHG) which is considered as the main factor of global warming and climate change. Beside CO₂, methane (CH₄) easily produced in the nature is considered as the second GHG and contribute about 20% of GHG in the atmosphere respectively (Tondeur & Teng, 2008). Other consequences associated with fossil fuel use are the fossil fuel resources are not distributed evenly around the globe which makes many countries heavily dependent on imports. These tremendous increases have led to many concerns. Although it is not known how much fossil fuel is still available, it is generally accepted that it is being depleted and is non-renewable. Given these circumstances, searching for other renewable forms of energy sources is reasonable. Hence, various research fields regarding to the generation of renewable and sustainable energy sources with efficient and environmental friendly characteristic and reduction program of greenhouse gas is gaining great attention from scientist, engineers and government (Effendi et al., 2005). The example of several sources of renewable energy are solar, hydropower, wind, geothermal, biomass and biofuel energies (Ma & Hanna, 1999; Huber, 2006a).

One of the most promising and long-term solution to the future energy crisis is the production of energy from biomass. Due to wide spread availability in nature, biomass became the primary energy resource after oil and coal and has contributes about 10–14% of the world's energy supply today (McKendry, 2002). The energy utilization from biomass resources has received considerable attention since the energy crisis in the mid-1970s. The energy obtained from agricultural wastes or agricultural byproducts can be recognized as a potential source of renewable energy based on benefits of both energy recovery and environmental protection (Tsai *et al.*, 2006). In develop countries, the economy is largely based on the agricultural and forestry, so utilizations of biomass for energy purpose in these countries has a great potential to be done.

Florin & Harris (2008) defined biomass as contemporary organic matter formed by the photosynthetic capture of solar energy, which is stored as chemical energy. The main compositions in biomass are cellulose, hemicellulose, lignin and small amount of other

material. Generally, cellulose is the main component (Table 1.1) which represents 40-50% from biomass weight whereas hemicellulose represents 20-40% (Zhang *et al.*, 2010).

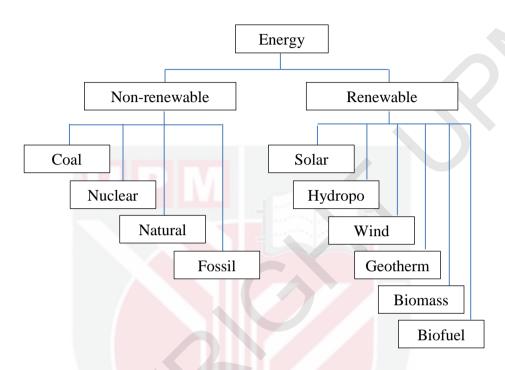


Figure 1.1: Non-renewable energy and renewable energy

Biomass can be converted into useful products including biosynthesis gas or syngas which is a mixture of CO and H₂ gases. Syngas is believed to be critical for the energy, chemical and environmental sustainability. It is very important intermediate, used as a feedstock for various fuel and chemical synthesis such as Fisher Tropsch, oxygenated compound, polycarbonate and other hydrocarbon (Gao *et al.*, 2008; Asami *et al.*, 2003). Hydrogen itself is a clean and efficient energy source which can be used for transportation and stationary power generation. It is widely used as a feedstock for the production of chemicals, hydrogenation of fats and oils in food industry, production of electronic devices, processing steel and also for desulfurization and re-formulation of gasoline in refineries.

In a large manufacture, syngas is produced via several methods include steam reforming of methane (SRM), dry reforming, partial oxidation of fossil fuels (POX) and auto-thermal reforming which combines SRM and POX. Among other methods developed to improve the existing technologies are the membrane processes, selective oxidation of methane and oxidative dehydrogenation. The detail information regarding syngas production will be discussed in Chapter 2. However, syngas is still not readily available in sufficient quantities and the production cost is still high especially for transportation purposes. (Tanksale *et al.*, 2010).

Table 1.1 : Typical level of cellulose, hemicellulose and lignin (Adapted from Mckendry, 2002)

Component	Percent dry weight (%)	Description
Cellulose	40-60	A high-molecular weight (10 ⁶ or more) linear chain of glucose linked by β-glycosidic linkage. This chain is stable and resistant to chemical attack
Hemicellulose	20-40	Consist of short, highly branched chains of sugars (five-carbon sugars such as tarabinose, p-xylose and six-carbon sugars such as p-glucose, p-galactose and p-mannose). Lower molecular weight than cellulose. Relatively easy to be hydrolysed into basic sugar.
Lignin	10-25	A biopolymer rich in three-dimensional, highly branched polyphenolic constituents that provide structural integrity to plant. More difficult to be dehydrated than cellulose and hemicellulose.

Due to increasing need of syngas, development of cost-effective and efficient hydrogen production technologies has gained significant attention in recent years. The technical challenges to achieve a stable syngas economy include improving process efficiencies, lowering the cost of production and harnessing renewable resources.

The production of syngas from biomass is expected to be particularly significant especially by using waste biomass such as rice straw as it is offer a great benefit to environment including utilizing two greenhouse gases (CO₂ and CH₄), and producing highly valuable syngas for a feedstock for other chemical and fuel processes. Besides that, it also can minimize the problem in term of waste management and health issue which related to air pollution.

A possibly good route to produce syngas is by using cheap biomass as a source through thermochemical conversion technology (Chen $et\ al.$, 2003). Gasification process is more attractive when the interest product is in the gaseous form. The gasification of biomass results in a high production of gaseous products and small quantities of char and ash and considered to be more environmentally friendly because of the lower emissions of toxic gases into the atmosphere. Gasification is basically a thermochemical process that converts lignocellulosic materials such as cellulose, hemicellulose and lignin into gaseous products. It consists of a number of elementary chemical reactions, beginning with the partial oxidation of a lignocellulosic fuel with a gasifying agent such as air, oxygen and steam (Tanksale $et\ al.$, 2010). Gasification of solid fuels to yield a mixture of H_2 and CO (syngas), followed by water-gas shift reaction to produce H_2 and CO_2 , is a well-established process (Ramzan $et\ al.$, 2011).

One of the objectives in green chemistry principle as published by United State Environmental Protection Agency (USEPA) can be achieved by using a catalyst which effective for particular reaction. Generally, catalyst is defined as any material or substance that speeds up the rate of chemical reaction by lowering it activation energy. It is added in a little amount in comparison to the quantities of the reactant and not been consumed in the chemical transformation. However, in some cases the catalyst effects the reaction by being consumed and regenerated. Related to this work, the role of catalyst (heterogeneous catalyst) is crucial for producing the syngas effectively. There are lot of studies reported that some specified catalyst can enhance the production of syngas with high activity and stability. The detail of catalyst usage in syngas production will be discussed in Chapter 2.

Limestone is a sedimentary rock composed mainly of calcium carbonate (CaCO₃), usually in the form of calcite or aragonite. It may contain considerable amounts of magnesium carbonate as well; minor constituents also commonly present include clay, iron carbonate, and quartz.

Limestone has been used in many sector including construction, chemical, agriculture and even pharmaceutical industry. For example, powdered limestone is used as filler in paper, paint, rubber and plastics and crushed limestone is used as a filter stone in onsite sewage disposal systems. Powdered limestone is also used as a sorbent (a substance that absorbs pollutants) at many coal-burning facilities. In catalytic applications, limestone is a promising heterogeneous catalyst since it promotes a nontoxic, basic catalyst which important for the reaction processes.

Similar to the other natural sources of CaCO₃ such as dolomite and seashell, the active phases of the limestone were obtained by thermal decomposition of limestone into CaO as shown in Eq. 1 below:

$$CaCO_3$$
 (s) \longrightarrow CaO (s) $+ CO_2$ (g) [Eq.1]

In Malaysia, since it is abundant and easy to get, the price of limestone is just around US\$20 - 35 per metric ton. Comparing to the price of commercial calcium oxide (CaO) which around US\$1000 - 1600 per metric ton with purity of ~95%, therefore, the application of limestone in syngas production have a high commercial prospect as the cost of material used in the reaction will be reduced.

1.2 Problem Statement

Due to dilemmas in increasing energy demand and fuel price, depletion of petroleum oil, national security and environmental problems have encouraged researchers around the world to find a new energy resources especially renewable energy which can be sustain in the future. According to Food Outlook Global Analysis in 2010, the world's production of rice straw is more than 500 million tonnes per year in last five years and expecting to be increase annually. Therefore, the use of lower-cost and non-food based

feedstock of this lignocellulosic waste biomass has been taken into consideration for syngas production.

The products gas from biomass gasification enriched mainly with H_2 , CO, CO_2 and CH_4 and also some other components such as H_2O , tar, and inorganic impurities. However, the present of PAH (PolyAromatic Hydrocarbon) in the process reduced the H_2 production and become a great challenge to deal with this tar formation to ensure the product gases is highly concentrate with H_2 at the same time minimizing the emission of CO_2 during gasification process. Thus, this study focuses on catalyst development especially from limestone based catalyst, and the influences of this limestone based catalyst with or without dopants towards the quality of syngas production.

1.3 Objectives

The objectives of this study are:

- 1. To synthesize various metal oxide modified limestone catalysts via wet impregnation method with addition of mono and bimetallic metal dopants (Ni, Fe, Co, NiCo, NiFe and CoFe).
- 2. To characterize the physico-chemical of the synthesized catalysts by various techniques such as X-ray diffraction (XRD), Brunauer-Emmett-Teller (BET) surface area, Thermogravimetry analysis (TGA), Field emission scanning electron microscopy Energy dispersive spectroscopy (FESEM-EDX) and Temperature programmed desorption of carbon dioxide (TPD-CO₂).
- 3. To carried out gasification reaction of rice straw with and without catalysts for the production of hydrogen.

REFERENCES

- Abu El-Rub, Z., Bramer, E. A., & Brem, G. (2004). Review of catalysts for tar elimination in biomass gasification processes *Ind Eng Chem Res* 43: 6911–6919.
- Abu El-Rub, Z., Bramer, E. A., & Brem, G. (2002). Tar Removal in an Entrained Flow Cracker (EFC) with aplication to Biomass Gasification. *In Pyrolysis and Gasification of Biomass and Waste, Proceedings of an Expert Meeting*: 337-346.
- Akay, G., & Jordan, C.A. (2011). Gasification of fuel cane bagasse in a downdraft gasifier: influence of lignocellulosic composition and fuel particle size on syngas composition and yield. *Energy and Fuels* 25 (5): 2274–2283.
- Alcala, M. D., & Real, C. (2006). Synthesis based on the wet impregnation method and characterization of iron and iron oxide-silica nanocomposites. Solid State Ionics 177: 955–960.
- Asadullah, M., Ito, S., Kunimori, K., Yamada, M., & Tomishige, K. (2002). Biomass Gasification to Hydrogen and Syngas at Low Temperature: Novel Catalytic System Using Fluidized-Bed Reactor. *Journal of Catalysis* 208(2): 255–259.
- Asami, K., Li, X., Fujimoto, K., Koyama, Y., Sakurama, A., Kometani, N., & Yonezawa, Y. (2003). CO₂ reforming of CH₄ over ceria-supported metal catalysts. *Catalysis Today* 84(1-2): 27–31.
- Azadi, P., Afif, E., Azadi, F., & Farnood, R. (2012). Screening of nickel catalysts for selective hydrogen production using supercritical water gasification of glucose. *Green Chemistry* 14 (6): 1766 1777.
- Barrientos, J., Lualdi, M., Boutonnet, M., & Jaras, S. (2014). Deactivation of supported nickel catalysts during CO methanation. *Applied Catalysis A: General 486*: 143–149.
- Boey, P. L., Maniam, G. P., & Hamid, S. A. (2011). Performance of calcium oxide as a heterogeneous catalyst in biodiesel production: A review. *Chemical Engineering Journal* 168(1): 15–22.
- Chaiprasert, P., & Vitidsant, T. (2009). Promotion of coconutshell gasofication by steam reforming on nickel-dolomite. *American Journal of Applied Sciences* 6(2): 332–336.
- Chandrakant, P., & Bisaria, V. (1998). Simultaneous bioconversion of cellulose and hemicellulose to ethanol. *Critical Review in Biotechnology 18*: 295–331.
- Chen, G., Andries, J., & Spliethoff, H. (2003). Catalytic pyrolysis of biomass for hydrogen rich fuel gas production. *Energy Conversion and Management*, 44(14): 2289–2296.

- Chew, T. L., & Bhatia, S. (2008). Catalytic processes towards the production of biofuels in a palm oil and oil palm biomass-based biorefinery. *Bioresource Technology*, 99(17): 7911–22.
- Chheda, J. N., Huber, G. W., & Dumesic, J. A. (2007). Liquid-phase catalytic processing of biomass-derived oxygenated hydrocarbons to fuels and chemicals. *Angewandte Chemie (International Ed. in English)*, 46(38): 7164–83.
- Chiang, K. Y., Chen, Y. S., Tsai, W. S., Lu, C. H., & Chien, K. L. (2012). Effect of calcium based catalyst on production of synthesis gas in gasification of waste bamboo chopsticks. *International Journal of Hydrogen Energy*, *37*(18): 13737–13745.
- Christensen, K. O., Chen, D., Lideng, R., & Holmen, A. (2006). Effect of supports and Ni crystal size on carbon formation and sintering during steam methane reforming. *Applied Catalysis A: General*, 314(1): 9–22.
- Corella, J., Aznar, M. P., Gill, J., Caballero, M. A. (1999). Biomass gasification in fluidized bed: where to locate the dolomite to improve gasification. *Energy Fuels* 13: 1122-1127.
- Courson, C., Makaga, E., Petit, C., & Kiennemann, A. (2000). Development of Ni catalysts for gas production from biomass gasication. Reactivity in steam- and dry-reforming. *Catalysis Today* 63: 427–437.
- Curran, G. P., Clancey, J. T., Scarpiello, D. A., Fink, C. E., Gorin, E. (1966). Carbon dioxide acceptor process. *Chemical Engineering Progress* 62: 80-86.
- Davda, R. R., Shabaker, J. W., Huber, G. W., Cortright, R. D., & Dumesic, J. A. (2005). A review of catalytic issues and process conditions for renewable hydrogen and alkanes by aqueous-phase reforming of oxygenated hydrocarbons over supported metal catalysts. *Applied Catalysis B: Environmental*, 56(1-2 SPEC. ISS.): 171–186.
- Dayton, D. (2002). A Review of the Literature on Catalytic Biomass Tar Destruction Milestone Completion Report, NREL/TP-510-32815. National Renewable Energy Laboratory (NREL) Golden, Colorado.
- Devi, L., Ptasinski, K. J., & Janssen, F. J. J. G. (2005a). Pretreated olivine as tar removal catalyst for biomass gasifiers: investigation using naphthalene as model biomass tar. *Fuel Processing Technology* 86: 707–730.
- Devi, L., Ptasinski, K. J., Janssen, F. J. J. G., van Paasen, S. V. B., Bergman, P. C. A., & Kiel, J. H. A. (2005b). Catalytic decomposition of biomass tars: use of dolomite and untreated olivine. *Renewable Energy* 30(4): 565–587.
- Di Serio, M., Ledda, M., Cozzolino, M., Minutillo, G., Tesser, R., & Santacessaria, E. (2006). Transesterification of soybean oil to biodiesel by using heterogeneous basic catalysts. *Industrial & Engineering Chemistry Research 45*: 3009–3014.

- Effendi, A., Hellgardt, K., Zhang, Z.G., & Yoshida, T. (2005). Optimising H₂ production from model biogas via combined steam reforming and CO shift reaction. *Fuel*, 84(7-8): 869-874.
- Elliott, D. C. (2008). Review Catalytic hydrothermal gasification of biomass. *Biofuels, Bioproducts and Biorefining 2* (3): 254–265.
- FAO Rice Market Monitor, October 2014, Volume XVII Issue No. 3.
- Florin, N. H., & Harris, A. T. (2008). Enhanced hydrogen production from biomass with in situ carbon dioxide capture using calcium oxide sorbents. *Chemical Engineering Science* 63 (2): 287-316.
- Food and Agriculture Organization of the United Nations, 2009.
- Gallucci, K., Stendardo, S., & Foscolo, P. U. (2008). CO₂ capture by means of dolomite in hydrogen production from syngas. *International Journal of Hydrogen Energy*, 33(12): 3049–3055.
- Gao, J., Guo, J., Liang, D., Hou, Z., Fei, J., & Zheng, X. (2008). Production of syngas via autothermal reforming of methane in a fluidized-bed reactor over the combined CeO₂–ZrO₂/SiO₂ supported Ni catalysts. *International Journal of Hydrogen Energy*, 33(20): 5493–5500.
- Garcia, L., Sanches, J. L., Salvador, M. L., Bilbao, R., & Arauzo, J. (1997). Assessment of coprecipitated nickel-alumina catalysts, for pyrolysis of biomass. *Developments in Thermochemical Biomass Conversion*. Bridgwater, A. V., & Boocok, D. G. B., Eds. Blackie Academic and Professonal. London: 1158-1169.
- Granados, M. L., Poves, M. D. Z., Alonso, D. M., Mariscal, R., Galisteo, F. C., Moreno-Tost, R., & Fierro, J. L. G. (2007). Biodiesel from sunflower oil by using activated calcium oxide. *Applied Catalysis B: Environmental* 73(3): 317–326.
- Han, J., & Kim, H. (2008). The reduction and control technology of tar during biomass gasification/pyrolysis: An overview. *Renewable and Sustainable Energy Reviews* 12(2): 397–416.
- Huang, Y. F., Kuan, W. H., Lo, S. L., & Lin, C. F. (2008). Total recovery of resources and energy from rice straw using microwave-induced pyrolysis. *Bioresource Technology* 99(17): 8252–8258.
- Huber, G. W., Iborra, S., & Corma, A. V. (2006). Synthesis of transportation fuels from biomass: chemistry, catalysts, and engineering. *Chemical Reviews* 106: 4044 4098.
- Ismail, K., Yarmo, M. A., Taufiq-Yap, Y. H., & Ahmad, A. (2012). The effect of particle size of CaO and MgO as catalysts for gasification of oil palm empty fruit bunch to produce hydrogen. *International Journal of Hydrogen Energy*, 37(4): 3639–3644.

- Chiang, K. Y., Chen, Y. S., Tsai, W. S., Lu, C. H., & Chien, K. L. (2012.). Effect of calcium based catalyst on production of synthesis gas in gasification of waste bamboo chopsticks, *International Journal of Hydrogen Energy*, 37(18): 13737– 13745.
- Kawi, S., & Ashok, J. (2013). Steam reforming of toluene as a biomass tar model compound over CeO₂ promoted Ni/CaO-Al₂O₃ catalytic systems. *International Journal of Hydrogen Energy 38*(32): 13938–13949.
- Kimura, T., Miyazawa, T., Nishikawa, J., Kado, S., Okumura, K., Miyao, T., & Tomishige, K. (2006). Development of Ni catalysts for tar removal by steam gasification of biomass. *Applied Catalysis B: Environmental*, 68(3-4): 160–170.
- Koppatz, S., Pfeifer, C., Rauch, R., Hofbauer, H., Marquard-Moellenstedt, T., & Specht, M. (2009). H₂ rich product gas by steam gasification of biomass with in situ CO₂ absorption in a dual fluidized bed system of 8 MW fuel input. *Fuel Processing Technology* 90 (7-8): 914–921.
- Kuhn, J. N., Zhao, Z., Felix, L. G., Slimane, R. B., Choi, C. W., & Ozkan, U. S. (2008). Olivine catalysts for methane- and tar-steam reforming. *Applied Catalysis B: Environmental 81*(1-2): 14–26.
- Kumar, D. & Ali, A. (2013). Transesterification of low-quality triglycerides over a zn/cao heterogeneous catalyst: kinetics and reusability studies. *Energy Fuels* 27 (7): 3758–3768.
- Lancet, M. S., & Curran, G. P. (1980). Process for gasification using a synthetic CO₂/Sub 2/ acceptor. U.S. Patent 4231760.
- Lee, W., Nam, S. S., Kim, S. B., Lee, K. W., & Choi, C. S. (2000). The effect of Na₂CO₃ on the catalytic gasification of rice straw over nickel catalysts supported on kieselguhr. *Korean Journal of Chemical Engineering* 17 (2): 174-178.
- Li, X. T., Grace, J.R., Lim, C. J., Watkinson, A. P., Chen, H. P., & Kim, J. R. (2004). Biomass gasification in a circulating fluidized bed. *Biomass and Bioenergy* 26: 171–193.
- Lin, Y. C., & Huber, G. W. (2009). The critical role of heterogeneous catalysis in lignocellulosic biomass conversion. *Energy & Environmental Science* 2(1): 68-80.
- Lind, F., Berguerand, N., Seemann, M., & Thunman, H. (2013). Ilmenite and nickel as catalysts for upgrading of raw gas derived from biomass gasification. *Energy Fuels* 27 (2): 997–1007.
- Lizzio, A. A., & Radovic, L. R. (1991). Transient kinetics study of catalytic char gasification in carbon dioxide. *Industrial Engineering and Chemical Research* 30 (8): 1735-1744.

- Ma, F. & Hanna, M. A.(1999). Biodiesel production: a review. *Bioresource Technology* 70(1): 1-15.
- McKendry, P., (2002). Energy production from biomass: overview of biomass (Part 1), *Bioresource Technology 83* (1): 37–46.
- Milne, T. A., Abatzoglou, N., & Evans, R. J. (1998). Biomass gasifier "tars": their nature, formation and conversion. Report NREL/ TP-570-25357. National Renewable Energy Laboratory (NREL) Golden, Colorado.
- Mohammed, M. A. A., Salmiaton, A., Wan Azlina, W. A. K. G., & Mohamad Amran, M. S.(2012). Gasification of oil palm empty fruit bunches: a characterization and kinetic study. *Bioresource Technology* 110: 628–636.
- Munnik, P., Jongh, P. E. D., & Jong, K. P. D. (2015). Recent Developments in the Synthesis of Supported Catalysts. Chemical Reviews 115: 6687–6718.
- Naemchanthara, K., Meejoo, S., Onreabroy, W., & Limsuwan, P. (2008). Temperature effect on chicken egg shell investigated by XRD, TGA and FTIR. *Advanced Materials Research* 55-57: 333-336.
- Ngamcharussrivichai, C., Meechan, W., Ketcong, A., Kangwansaichon, K., & Butnark, S. (2011). Preparation of heterogeneous catalysts from limestone for transesterification of vegetable oils-Effects of binder addition. *Journal of Industrial and Engineering Chemistry* 17(3): 587–595.
- Ngamcharussrivichai, C., Wiwatnimit, W., & Wangnoi, S. (2007). Modified dolomites as catalysts for palm kernel oil transesterification. *Journal of Molecular Catalysis A: Chemical* 276(1-2): 24–33.
- Olivares, A., Aznar M. P., Caballero, M. A., Gil, J., Francés. E., & Corella, J.(1997). Biomass gasification: produced gas upgrading by in-bed use of dolomite. *Industrial & Engineering Chemical Research 36* (12): 5220–5226.
- Padban, N. (2000). PFB Air Gasification of Biomass: Investigation of Product Formation and Problematic Issues Related to Ammonia, Tar and Alkali. Ph.D. Thesis, Department of Chemical Engineering II, Lund University, Lund, Sweden.
- Yu, Q. Z., Brage, C., & Nordgreen, T. (2009). Effects of chinese dolomites on tar cracking in gasification of birch, *Fuel* 88(10): 1922–1926.
- Rachman, M., Nakashimada, Y., Kakizono, T., & Nishio, N. (1998). Hydrogen production with high yield and high evolution rate by self-flocculated cells of Enterobacter aerogenes in a packed-bed reactor. Applied Microbiology and Biotechnology 49: 450–454.
- Ramzan, N., Ashraf, A., Naveed, S., & Malik, A. (2011). Simulation of hybrid biomass gasification using Aspen plus: A comparative performance analysis for food, municipal solid and poultry waste. *Biomass and Bioenergy* 35(9): 3962–3969.

- Rapagna, S., Gallucci, K., Di Marcello, M., Matt, M., Nacken, M., Heidenreich, S., & Foscolo, P. U. (2010). Gas cleaning, gas conditioning and tar abatement by means of a catalytic filter candle in a biomass fluidized-bed gasifier. *Bioresource Technology* 101(18): 7123–7130.
- Reyero, I., Arzamendi, G., & Gandía, L. M. (2014). Heterogenization of the biodiesel synthesis catalysis: CaO and novel calcium compounds as transesterification catalysts. *Chemical Engineering Research and Design* 92(8): 1519–1530.
- Richardson, S. M., Gray, M. R.(1997). Enhancement of residue hydroprocessing catalysts by doping with alkali metals. *Energy Fuels* 11 (6): 1119-1126.
- Sato, K., & Fujimoto, K. (2007). Development of new nickel based catalyst for tar reforming with superior resistance to sulfur poisoning and coking in biomass gasification. *Catalysis Communications* 8 (11): 1697–1701.
- Sheehan, J., Aden, A., Paustian, K., Killian, K., Brenner, J., Walsh, M., & Nelson K., (2003). Energy and environmental aspects of using corn stover for fuel ethanol. *Journal of Industrial Ecology* 7: 117-146.
- Shekhar, N. (2011). Popularization of biomass briquettes a means for sustainable rural development. *Asian Journal of Management Research* 2 (1): 744–761.
- Shengfu, L., Qingyuan, L., Jinyong, H., & Sai, J. (2013). Catalytic steam reforming of rice straw biomass to hydrogen-rich syngas over Ni-based catalysts, *Chinese Journal of Catalysis 34*: 1462–1468.
- Sidhu, B. S., & Beri, V, (2008). Rice residue management: farmer's perspective. *Indian* journal of air pollution control 8(1): 61-67.
- Simell, P. A., & Bredenberg, J. B. (1990). Catalytic purification of tarry fuel gas. *Fuel* 69: 1219-1225.
- Simell, P., & Kurkela, E. (1997). Tar removal from gasification gas. *Biomass Gasification and Pyrolysis*: 207-217.
- Sivasangar, S., Taufiq-Yap, Y. H., Zainal, Z., & Kitagawa, K. (2013). Thermal behavior of lignocellulosic materials under aerobic/anaerobic environments. *International Journal of Hydrogen Energy 38*(36): 16011–16019.
- Sivasangar, S., Mastuli, M. S., Islam, A., & Taufiq-Yap, Y. H. (2015). Screening of modified CaO-based catalysts with a series of dopants for the supercritical water gasification of empty palm fruit bunches to produce hydrogen. *RSC Advances* 5: 36798–36808.
- Soltani, N., Bahrami, A., Pech-Canul, M. I., & Gonzalez, L. A. (2014). Review on the physicochemical treatments of rice husk for production of advanced materials. *Chemical Engineering Journal 264*: 899–935.
- Sutton, D., Kelleher, B., Doyle, A., & Ross, J. R. H. (2001a). Investigation of nickel supported catalysts for the upgrading of brown peat derived gasification

- products. Bioresource Technology, 80(2), 111–116.
- Sutton, D., Kelleher, B., & Ross, J. R. H. (2001b) Review of Literature on Catalysts for Biomass Gasification. *Fuel Processing Technology* 73: 155-173.
- Suzuki, K., Suzuki, T., Takahashi, Y., Okimoto, M., Yamada, T., Okazaki, N., & Fujiwara, M. (2008). Nickel-catalyzed carbonization of wood for coproduction of functional carbon and fluid fuels II: improved fuel quality of oil fraction and increased heating value of gas fraction. *Journal of Wood Science* 55(1): 60–68.
- Suzuki, T., Ohme, H., & Watanabe, Y. (1992). Alkali metal catalysed carbon dioxide gasification of carbon. *Energy Fuels* 6 (4): 343-351.
- Tanksale, A., Beltramini, J. N., & Lu, G. M. (2010). A review of catalytic hydrogen production processes from biomass. *Renewable and Sustainable Energy Reviews* 14(1): 166–182.
- Tasaka, K., Furusawa, T., & Tsutsumi, A. (2007). Biomass gasification in fluidised bed reactor with Co catalyst. *Chemical Engineering Science* 62 (18–20): 5558-5563.
- Taufiq-Yap, Y. H., Sivasangar, S., Salmiaton, A. (2012). Enhancement of hydrogen production by secondary metal oxide dopants on NiO/CaO material for catalytic gasification of empty palm fruit bunches. Energy 47 (1): 158–165.
- Taufiq-Yap, Y. H., Nur-Faizal, A. R., Sivasangar, S., Hussein, M. Z., & Aishah, A. (2014). Modification of Malaysian dolomite using mechanochemical treatment via different media for oil palm fronds gasification. *International Journal of Energy Research* 38 (8): 1008–1015.
- Tondeur, D., Teng, F., & Trevor, M. L. (2008). Carbon capture and storage for greenhouse effect mitigation. In *Future Energy: Improved, Sustainable and Clean Options for our Planet*; Elsevier: Oxford, UK: 303–331.
- Tsai, W. T., Lee, M. K., & Chang, Y. M. (2006). Fast pyrolysis of rice straw, sugarcane bagasse and coconut shell in an induction-heating reactor. *Journal of Analytical and Applied Pyrolysis* 76: 230-.237.
- Umpuch, C. (2015). Removal of Yellow20 Dye from Aqueous Solution using Organorice Straw: Characteristic, Kinetic and Equilibrium Studies. *Engineering Journal* 19 (2): 59-69.
- Valverde, J. M., Sanchez-Jimenez, P. E., & Perez-Maqueda, L. A. (2014). Calcium-looping for post-combustion CO₂ capture on the adverse effect of sorbent regeneration under CO₂. *Applied Energy 126*: 161–171.
- Yang, H., Yan, R., Chen, H., Lee, D.H. & Zheng, C. (2007). Characteristic hemicelulloses, cellulose and lignin pyrolysis. *Fuel* 86:1781-1788.
- Wang, T. J., Chang, J., Wu, C. Z., Fu, Y., & Chen, Y. (2005). The steam reforming of naphthalene over a nickel-dolomite cracking catalyst. *Biomass and Bioenergy*

- 28(5): 508-514.
- Weerachanchai, P., Horio, M., & Tangsathitkulchai, C. (2009). Effects of gasifying conditions and bed materials on fluidized bed steam gasification of wood biomass. *Bioresource Technology* 100(3): 1419–1427.
- Wei, L., Xu, S., Zhang, L., Liu, C., Zhu, H., & Liu, S. (2007). Steam gasification of biomass for hydrogen-rich gas in a free-fall reactor. *International Journal of Hydrogen Energy* 32: 24–31.
- Wei, L.G., Xu, S.P., Liu, J.G., Liu, C.H., & Liu S.Q.(2008). Hydrogen production in steam gasification of biomass with CaO as a CO₂ absorbent. *Energ Fuel* 22: 1997–2004.
- Wu, C., & Williams, P. T. (2010). A novel Ni–Mg–Al–CaO catalyst with the dual functions of catalysis and CO₂ sorption for H₂ production from the pyrolysis–gasification of polypropylene. *Fuel* 89(7): 1435–1441.
- Xu, C., Donald, J., Byambajav, E., & Ohtsuka, Y. (2010). Recent advances in catalysts for hot-gas removal of tar and NH₃ from biomass gasification. *Fuel* 89(8): 1784–1795.
- Yu, H., Zhang, Q., Zhang, Q., Wang, Q., Ning, G., Luo, G., & Wei, F. (2006). Effect of the reaction atmosphere on the diameter of single-walled carbon nanotubes produced by chemical vapor deposition. *Carbon 44*(9): 1706–1712.
- Yung, M. M., Jablonski, W. S., & Magrini-bair, K. A. (2009). Review of catalytic conditioning of biomass-derived syngas. *Energy Fuels* 23(4): 1874–1887.
- Zhang, L., Xu, C., & Champagne, P. (2010). Overview of recent advances in thermochemical conversion of biomass. *Energy Conversion and Management* 51(5): 969–982.
- Zhang, R., Wang, Y., & Brown, R. C. (2007). Steam reforming of tar compounds over Ni/olivine catalysts doped with CeO₂. Energy Conversion and Management 48(1): 68–77.
- Zhao, Z., Kuhn, J. N., Felix, L. G., Slimane, R. B., Choi, C. W., & Ozkan, U. S. (2008). Thermally impregnated Ni-olivine catalysts for tar removal by steam reforming in biomass gasifiers. *Industrial & Engineering Chemistry Research* 47(3): 717-723.