



UNIVERSITI PUTRA MALAYSIA

***SYNTHESIS AND CHARACTERIZATION OF HETEROGENEOUS MIXED
OXIDE CATALYSTS BASED ON EGG SHELL FOR BIODIESEL
PRODUCTION FROM WASTE COOKING OIL***

NASAR MANSIR

FS 2018 25



**SYNTHESIS AND CHARACTERIZATION OF HETEROGENEOUS MIXED
OXIDE CATALYSTS BASED ON EGG SHELL FOR BIODIESEL
PRODUCTION FROM WASTE COOKING OIL**

By

NASAR MANSIR

**Thesis submitted to the School of Graduate Studies, Universiti Putra Malaysia,
in Fulfilment of the Requirement for the Degree of Doctor of Philosophy**

February 2018

COPYRIGHT

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



DEDICATION

The thesis is wholly dedicated to my loving parents Alh Mansir Lawal and Hajiya Safiya Muhammad for their support and encouragement throughout my life.



Abstract of thesis submitted to the Senate of Universiti Putra Malaysia in fulfilment of the requirements for the degree of Doctor of Philosophy

**SYNTHESIS AND CHARACTERIZATION OF HETEROGENEOUS MIXED
OXIDE CATALYSTS BASED ON EGG SHELL FOR BIODIESEL
PRODUCTION FROM WASTE COOKING OIL**

By

NASAR MANSIR

February 2018

Chairman : Professor Taufiq-Yap Yun Hin, PhD
Faculty : Science

Biodiesel is one of the most promising biofuel alternatives to conventional fossil fuel, considering its number of advantages particularly environmental benign and availability of feedstock. Conventionally, homogeneous catalytic system is used for the production of biodiesel in commercial scale using high grade feedstock such as soybean oil, palm oil and sunflower oil. However, the current biodiesel production process is no longer sustainable considering the high cost of feedstock and other environmental related issues associated to homogeneous catalyst system. Newly developed calcium oxide based catalysts doped with mixed bimetallic oxides were synthesized using simple wet impregnation method. The synthesized mixed oxide catalysts were used for the transesterification of waste cooking oil using normal reflux method to produce fatty acid methyl ester (FAME). The catalysts (Molybdenum Zirconia Calcium oxide (Mo-Zr/CaO), Manganese Zirconia Calcium oxide (Mn-Zr/CaO), Tungsten Zirconia Calcium oxide (W-Zr/CaO), and Tungsten Molybdenum Calcium oxide (W-Mo/CaO) were characterized to investigate their physico-chemical properties using various characterization techniques such as XRD, TPD, BET, SEM, EDX, TGA and FTIR. The basicity and acidity of the catalysts determined their activity towards transesterification reaction. The Mo-Zr/CaO and Mn-Zr/CaO catalysts achieved 90.1% and 92.1% FAME yield under the reaction temperature of 80 °C and reaction time of 3 h in both cases. W-Zr/CaO catalyst recorded biodiesel yield of 94.1% at 80 °C reaction temperature, & 1 h reaction time. W-Mo/CaO catalyst achieved the biodiesel yield of 96.2% at reaction temperature of 70 °C, & 2 h reaction time. The order of activity of the synthesized catalyst for FAME production is W-Mo/CaO > W-Zr/CaO > Mn-Zr/CaO > Mo-Zr/CaO. The Ca^{2+} leaching has reduced significantly with the increase in transition metal mixed oxide loading over the CaO surface. Additionally, all the synthesized catalysts could convert high FFA waste cooking oil to FAME at mild reaction conditions and be

reused and regenerated for subsequent biodiesel production cycle. The most stable catalyst (W-Mo/CaO) achieved 90 % FAME yield at 70 °C temperature and 2 h reaction time in the 5th reusability cycle. The synthesized biodiesel was tested and met the biodiesel standard quality parameters according to ASTM D67751 and EN 14214.



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan ijazah Doktor Falsafah

**SINTESIS DAN PENCIRIAN MANGKIN HETEROGEN OKSIDA
CAMPURAN BERASASKAN KULIT TELUR UNTUK PENGHASILAN
BIODIESEL DARIPADA SISA MINYAK MASAK**

Oleh

NASAR MANSIR

Februari 2018

Pengerusi : Professor Taufiq-Yap Yun Hin, PhD
Fakulti : Sains

Biodiesel merupakan salah satu bahan api bio yang menjanjikan alternatif kepada bahan api fosil, disebabkan oleh beberapa kelebihan terutamanya mersa alam dan sumber yang boleh diperbaharui. Sistem pemangkinan homogenus digunakan secara konvensional untuk penghasilan biodiesel bagi skala komersial menggunakan sumber bahan mentah bergred tinggi seperti minyak kacang soya, minyak sawit dan minyak bunga matahari. Walaubagaimanapun, penghasilan biodiesel semasa tidak lagi mampan berikutan peningkatan kos sumber bahan mentah dan isu-isu berkaitan alam sekitar yang melibatkan sistem pemangkinan homogenus. Mangkin berasaskan kalsium oksida yang baru dibangunkan didopkan bersama campuran oksida dwilogam yang disintesis menggunakan kaedah pengisitepuan basah. Mangkin oksida campuran yang disintesis digunakan untuk transesterifikasi sisa minyak masak menggunakan kaedah refluks normal untuk menghasilkan asid lemak metil ester (FAME). Mangkin (Molibdenum Zirkonia Kalsium oksida (Mo-Zr/CaO), Mangan Zirkonia Kalsium oksida (Mn-Zr/CaO), Tungsten Zirkonia Kalsium oksida (W-Zr/CaO), and Tungsten Molibdenum Kalsium oksida (W-Mo/CaO) dicirikan untuk mengenalpasti sifat fiziko-kimia menggunakan pelbagai teknik pencirian seperti XRD, TPD, BET, SEM, EDX, TGA dan FTIR. Sifat kebesan dan keasidan menentukan aktiviti mangkin terhadap tindak balas transesterifikasi. Mangkin Mo-Zr/CaO dan Mn-Zr/CaO menghasilkan 90.1% dan 92.1% FAME pada suhu tindak balas 80 °C dan 3 jam masa tindak balas untuk kedua-duanya. Mangkin W-Zr/CaO mencatatkan hasil biodiesel sebanyak 94.1 % pada suhu tindak balas 80 °C dan 1 jam masa tindak balas. Mangkin W-Mo/CaO menghasilkan biodiesel 96.2% pada suhu tindak balas 70 °C dan 2 jam tindak balas. Susunan aktiviti mangkin yang disintesis untuk penghasilan FAME adalah W-Mo/CaO > W-Zr/CaO > Mn-Zr/CaO > Mo-Zr/CaO. Perlunturan ion Ca^{2+} menunjukkan pengurangan yang ketara dengan peningkatan kandungan logam peralihan campuran oksida pada permukaan CaO.

Tambahan pula, semua mangkin yang disintesis mampu menukarkan FFA yang tinggi dalam sisa minyak masak kepada FAME pada keadaan sederhana dan boleh digunasesmula untuk beberapa kitaran penghasilan biodiesel. Mangkin yang paling stabil (W-Mo/CaO) menghasilkan 90 % FAME pada suhu 70 °C dan 2 jam masa tindak balas dalam 5 kitaran. Biosiesel yang disintesis diuji dan mencapai parameter kualiti piawai berdasarkan kepada ASTM D67751 dan EN 14214



ACKNOWLEDGEMENTS

All praise is to Allah for sustaining my life and giving me the opportunity to carry out this project successfully.

My profound gratitude goes to my supervisor Professor Dr Taufiq-Yap Yun Hin for his supervision and tireless parental guidance throughout the period of my PhD research and my entire stay at Malaysia, I appreciate. Similar gratitude goes to my co-supervisors; Tan Yen Ping, Mohd Izham Saiman and Umer Rashid, may God reward them abundantly.

Appreciation goes to the entire technical and teaching staff of chemistry department Universiti Putra Malaysia for their guidance and support during my PhD research work.

My profound appreciation goes to Federal University, Dutse Nigeria, for releasing me to pursue a PhD degree in chemistry from Universiti Putra Malaysia, may Allah elevate the statues of the university ameen.

My special appreciation goes to Siow Hwa Teo, who is a post doctoral assistant to my supervisor, Mr Surahim, Abdulkareem Al-sultan, Mahashanon, Nurshazwani, Ms Shikin Minaj, Jali Sham, Arfaeza Annur, who have helped me in one way or the other during this journey despite their commitments, I appreciate.

I would like to thank for my guardian, mentor and of course a father Dr Badamasi Lawal Charanchi who always stand for me in thin and thick situations for my success, I appreciate.

Immense gratitude goes to my wife Mrs. Maryam Sada Lawal and my three loving children Mansir (Daddy), Mahamud and Ahmad for their support and encouragement throughout my stay in Malaysia may God fulfil their good dreams.

My Profound gratitude and appreciation goes to my Parents Hajiya Safiya and Alh Mansir for their support and parental guidance I appreciate.

Appreciation goes to my brothers for their support and encouragement particularly, Bello Mansir, Sani Mansir, Bishir Mansir and Abubakar Mansir, thank you very much.

Profound gratitude goes to my friends for their support and encouragement more especially Idris Rabi'u, Jamilu Haruna Funtua, Salisu Nasir Babura, Muhammad Salisu Khalil, Sani Suleiman Isah Maiadua, Dr Aminu Musa Yar'adua, Ibrahim Abdullahi Ubale, Musa Abdullahi, Saifullahi Lawal, Engr. Nasiru Bello Kadandani, Babangida Ibrahim Babura, Ibrahim Muhammad Dutsinma, Maharazu Mamman Danmusa, Bashir Mukhtar, many but few to mention.



This thesis was submitted to the Senate of the Universiti Putra Malaysia and has been accepted as a fulfilment of the requirement for the degree of Doctor of Philosophy. The members of the supervisory committee were as follows:

Taufiq-Yap Yun Hin, PhD

Professor
Faculty of Science
University Putra Malaysia
(Chairman)

Muhamad Izham Saiman, PhD

Senior Lecturer
Faculty of Science
Universiti Putra Malaysia
(Member)

Tan Yen Ping, PhD

Senior Lecturer
Faculty of Science
Universiti Putra Malaysia
(Member)

Umer Rashid, PhD

Research Fellow
Institute of Advanced Technology
Universiti Putra Malaysia
(Member)

ROBIAH BINTI YUNUS, PhD

Professor and Dean
School of Graduate Studies
Universiti Putra Malaysia

Date :

Declaration by Members of Supervisory Committee

This is to confirm:

- that the research conducted and the thesis writing was under our supervision;
- supervision responsibilities as stated in the Universiti Putra Malaysia (Graduate Studies) Rules 2003 (Revised 2012-2013) are adhered

Signature: _____

Name of
Chairman of
Supervisory
Committee:

Professor Dr. Taufiq-Yap Yun Hin

Signature: _____

Name of
Member of
Supervisory
Committee:

Dr. Muhamad Izham Saiman

Signature: _____

Name of
Member of
Supervisory
Committee:

Dr. Tan Yen Ping

Signature: _____

Name of
Member of
Supervisory
Committee:

Dr. Umer Rashid

TABLE OF CONTENTS

	Page
ABSTRACT	i
ABSTRAK	iii
ACKNOWLEDGEMENTS	v
APPROVAL	vii
DECLARATION	ix
LIST OF TABLES	xv
LIST OF FIGURES	xvii
LIST OF ABBREVIATIONS	xxi

CHAPTER

1	INTRODUCTION	1
	1.1 Background	1
	1.2 Problem statement	3
	1.3 The scope of the research	4
	1.4 Objectives of the research	4
2	LITERATURE REVIEW	5
	2.1 Introduction	5
	2.2 Combustibility of vegetable oil	5
	2.3 Biodiesel as a promising alternative renewable fuel	5
	2.4 Feedstock for Biodiesel production	6
	2.4.1 Edible oils	7
	2.4.2 Non-edible oils	8
	2.4.3 Composition of vegetable based oils	9
	2.5 Waste cooking oil as viable feedstock for biodiesel	10
	2.6 Biodiesel production process	11
	2.7 Catalytic system for biodiesel production	13
	2.7.1 Homogeneous Catalysts for biodiesel production	15
	2.7.2 Drawbacks of homogeneous base catalyst	17
	2.7.3 Mechanism of the transesterification reaction using base catalyst	18
	2.7.4 Drawbacks of homogeneous acid catalyst	19
	2.7.5 Mechanism of esterification reactions using acid catalyst	20
	2.8 Heterogeneous catalysts for biodiesel production	21
	2.8.1 Solid acid catalysts for biodiesel production	23
	2.8.2 Solid base catalysts for biodiesel production	27
	2.8.3 Solid Modified waste egg shell derived bifunctional catalyst	28
	2.8.4 Limitations of Solid catalysts	31

2.8.5	Properties of catalysts for biodiesel production	31
2.9	Factors influencing biodiesel yield	31
2.9.1	Methanol to oil molar ratio	32
2.9.2	Catalyst loading	32
2.9.3	Reaction temperature	33
2.9.4	Reaction Time	33
2.10	Alternative techniques for biodiesel production	33
2.10.1	Conventional reflux method	33
2.10.2	Autoclave reactor	34
2.11	Current status and challenges for biodiesel production	34
3	MATERIALS AND METHODS	35
3.1	Materials	35
3.2	Preliminary investigation and pre-treatment of waste cooking oil	35
3.2.1	Gas Chromatography-mass spectrometric analysis	36
3.2.2	Acid value determination	36
3.2.3	Saponification value evaluation	36
3.3	Catalysts synthesis processes	37
3.4	Physico-chemical properties analysis	39
3.4.1	X- ray diffraction	39
3.4.2	Brunauer-Emmett-Teller	39
3.4.3	Scanning electron microscopy	40
3.4.4	Energy dispersive X-ray	40
3.4.5	Temperature programmed desorption	40
3.4.6	Fourier transform infrared spectroscopy	41
3.4.7	Thermo-gravimetric analysis	41
3.5	Catalytic production of biodiesel and yield evaluation	41
3.5.1	Biodiesel production using normal reflux	41
3.5.2	Biodiesel yield evaluation process	42
3.6	Catalyst stability determination	42
3.6.1	Stability analysis of molybdenum-zirconium/calcium mixed oxide	42
3.6.2	Stability test of manganese-zirconium/calcium mixed oxide	43
3.6.3	Reusability test of Tungsten-zirconium/calcium mixed oxide	43
3.6.4	Recyclability study of Tungsten-molybdenum/calcium mixed oxide	43
3.7	Biodiesel characterization and fuel properties evaluation	43
3.7.1	Kinematic viscosity analysis	44
3.7.2	Flash point analysis	44
3.7.3	Pour point analysis	44

4	RESULTS AND DISCUSSION	46
4.1	Properties of high FFA waste cooking oil	46
4.2	Physico-chemical properties evaluation of Mo-Zr/CaO catalyst	47
4.2.1	Structure and crystallography of the catalyst	47
4.2.2	Surface area analysis	48
4.2.3	Surface morphology analysis	48
4.2.4	Elemental composition of the Mo-Zr/CaO catalyst	49
4.2.5	Basicity of the Mo-Zr/CaO catalyst	50
4.3	Activity of Mo-Zr/CaO mixed oxide catalyst on waste cooking oil	51
4.3.1	Effect of methanol to oil molar ratio	52
4.3.2	Effect of catalyst loading	53
4.3.3	Effect of temperature of the reaction	54
4.3.4	Reaction Time	55
4.3.5	Effect of Mo-Zr bimetallic oxide on Ca^{2+} leaching in FAME	56
4.3.6	Reusability Evaluation	57
4.3.7	Metal leaching determination in FAME	57
4.4	Physico-chemical properties evaluation of Mn-Zr/CaO catalyst	59
4.4.1	BET Surface area analysis	60
4.4.2	Surface morphology evaluation	61
4.4.3	Elemental composition analysis	62
4.4.4	Basicity level evaluation	63
4.5	Catalytic activity of Mn-Zr/CaO catalyst for biodiesel production	64
4.5.1	Effect of Methanol to oil molar ratio	66
4.5.2	Effect of catalyst loading	67
4.5.3	Effect of temperature of the reaction	67
4.5.4	Effect of Reaction Time	68
4.5.5	Catalyst Reusability evaluation	69
4.6	Physico-chemical evaluation of W-Zr/CaO mixed oxide catalyst	70
4.6.1	Structure and crystallography	70
4.6.2	Brunauer-Emmet-Teller (BET) Surface area analysis	71
4.6.3	Acidity and basicity of the catalyst	72
4.6.4	Morphology of the catalyst	74
4.6.5	Elemental composition analysis of W-Zr/CaO catalyst	75
4.7	Catalytic activity evaluation of W-Zr/CaO catalyst	76
4.7.1	Effect of methanol to oil molar ratio	77
4.7.2	Effect of catalyst loading	78
4.7.3	Effect of reaction temperature	79
4.7.4	Effect of reaction time	80
4.7.5	Reusability test	81
4.7.6	Catalyst leaching test	82
4.8	Physico-chemical properties analysis of W-Mo/CaO catalyst	83
4.8.1	Structure & Crystallography	83
4.8.2	Surface area measurement	84
4.8.3	Temperature programmed desorption	85

4.8.4	Surface morphology characteristic	88
4.8.5	Thermo gravimetric analysis	89
4.8.6	Fourier transform infrared spectroscopy	90
4.9	Stoichiometric composition analysis of W_x-Mo_y/CaO catalyst	91
4.9.1	Evaluation of catalyst stability and reusability	93
4.10	Biodiesel Fuel properties and Evaluation	95
4.10.1	Kinematic viscosity	95
4.10.2	Pour point	95
4.10.3	Flash point	95
4.10.4	Acid value and Moisture content	95
5	CONCLUSION AND RECOMMENDATIONS	97
5.1	Transesterification of waste cooking oil using synthesized catalysts	97
5.2	Recommendation for future research	98
	BIBLIOGRAPHY	100
	APPENDICES	111
	BIODATA OF STUDENT	118
	LIST OF PUBLICATIONS	119

LIST OF TABLES

Table		Page
2.1	Comparison of standards between biodiesel and fossil diesel according to American Standard for Testing and Materials	6
2.2	Oil content of some edible feedstocks for biodiesel	7
2.3	Oil content of some non edible feedstocks for biodiesel	9
2.4	Fatty acid composition (%) of different vegetable oils	10
2.5	Common fatty acid composition of plant based oil	11
2.6	Comparison between homogeneous and heterogeneous catalysts for biodiesel production	13
2.7	A literature report on biodiesel production from different feedstocks using solid acid catalysts at severe reaction condition	25
2.8	A literature report on biodiesel production from high FFA feedstocks using bifunctional catalysts under mild conditions	30
3.1	Some globally accepted vegetable oil analysis and their standard methods	37
4.1	Physico-chemical properties of waste cooking oil	46
4.2	BET surface area, pore volume and pore size of Mo-Zr/CaO catalyst samples	48
4.3	Elemental composition analysis of the Mo-Zr/CaO catalyst	50
4.4	Concentration of leached Ca^{2+} (mg/L) in different FAME samples by AA	58
4.5	Surface area and crystallite size analysis of the Mn-Zr/CaO sample	61
4.6	EDX Analysis of the synthesized Mn-Zr/CaO catalyst samples	63
4.7	Basic site density and biodiesel yield of Mn-Zr/CaO catalyst sample	65
4.8	BET surface area, pore volume and pore size of W-Zr/CaO catalyst samples	72

4.9	Acid and basic site densities of W-Zr/CaO catalyst samples	74
4.10	Elemental composition of W-Zr/CaO catalyst samples	76
4.11	Leaching test of Ca^{2+} from different W-Zr loadings on CaO	83
4.12	BET surface area, pore volume and pore size and crystal size of W-Mo/CaO catalyst samples	85
4.13	Acid and basic site densities of the synthesized catalyst samples	88
4.14	Summary of the related studies using different catalysts	93
4.15	Comparison of fuel standards between biodiesel obtained in this study and the ASTM biodiesel standard values	96

LIST OF FIGURES

Figure		Page
2.1	Expected distributions of vegetable oil exports by the year 2022	8
2.2	Schematic block of homogeneous catalyst reaction for biodiesel production	14
2.3	Schematic block of heterogeneous catalyst reaction for biodiesel production	15
2.4	Mechanism of transesterification reaction for FAME production	19
2.5	Mechanism of esterification reaction for FAME production	21
2.6	Simultaneous esterification and transesterification of solid acid catalyst for biodiesel production	24
3.1	The overall research activities flow chart	45
4.1	XRD patterns of (a) CaO, (b) 5wt Mo-Zr/CaO, (c) 10wt Mo-Zr/CaO, d=15wt Mo-Zr/CaO, e=20wt Mo-Zr/CaO, f=25wt Mo-Zr/CaO calcined at 650 °C (5 °C/min) for 5h. •CaO *MoCaO, ♣MoZrO, ♦ZrCaO	47
4.2	(a) SEM image of un-doped CaO (b) SEM image of 5Mo-Zr/CaO (c) SEM image of 10Mo-Zr/CaO (d) SEM image of 15Mo-Zr/CaO (e) SEM image of 20Mo-Zr/CaO and (f) SEM image of 25Mo-Zr/CaO	49
4.3	TPD-CO ₂ of synthesized Mo-Zr/CaO mixed oxide catalyst samples showing absorption peaks at different temperature range	51
4.4	Correlation between basicity and FAME yield production of different catalyst samples under the same reaction conditions of 15:1 methanol oil ratio, 80°C reaction temperature, 3 wt% catalyst loading and 3 h reaction time	52
4.5	Optimization of effect of methanol to oil molar ratio for transesterification reaction of waste cooking oil to FAME	53
4.6	Optimization of effect of catalyst loading on FAME production from waste cooking oil using 10Mo-Zr/CaO catalyst samples	54

4.7	Optimization of effect of reaction temperature for FAME production from 10Mo-Zr/CaO catalyst samples	55
4.8	Optimization of effect of reaction time for FAME production using 10Mo-Zr/CaO catalyst sample	56
4.9	Reusability of 10Mo-Zr/CaO catalyst at 3 h reaction time, 80 °C reaction temperature, 3 wt% catalyst loading and 15:1 methanol to oil ratio	57
4.10	The XRD patterns of fresh (a) and spent (b) 10Mo-Zr/CaO catalyst after four successive reaction cycles	59
4.11	XRD patterns of synthesized catalyst samples; (a) CaO, (b) 3Mn-7Zr/CaO, (c) 4Mn-Zr/CaO, (d) 5Mn-5Zr/CaO, (e) 6Mn-4Zr/CaO, (f) 7Mn-3Zr/CaO calcined at 650 °C (5 °C/min) for 5h. ♣CaO ♦MnCaO ★ZrCaO, *MnZrO	60
4.12	SEM micrograms of the synthesized Mn-Zr/CaO catalyst samples; (a) CaO, (b) 3Mn-7Zr/CaO, (c) 4Mn-6Zr/CaO, (d) 5Mn-5Zr/CaO, (e) 6Mn-4Zr/CaO, (f) 7Mn-3Zr/CaO	62
4.13	TPD-CO ₂ of synthesized Mn-Zr/CaO catalyst samples; (a) CaO, (b) 7Mn-3Zr/CaO, (c) 6Mn-4Zr/CaO, (d) 5Mn-5Zr/CaO, (e) 4Mn-6Zr/CaO, (f) 3Mn-7Zr /CaO	63
4.14	Correlation between the CO ₂ absorption and the biodiesel yield of the Mn-Zr/CaO catalyst samples under the optimized 15:1 methanol oil ratio, 3 wt% catalyst loading, 80 °C reaction temperature and 3 h reaction time	65
4.15	Optimization of effect of methanol to oil molar ratio for biodiesel production from waste cooking oil using 4Mn-6Zr/CaO catalyst sample	66
4.16	Optimization of effect of catalyst loading for biodiesel production from waste cooking oil using 4Mn-6Zr/CaO catalyst sample	67
4.17	Optimization of effect of reaction temperature for the production of biodiesel from waste cooking oil using 4Mn-6Zr/CaO catalyst sample	68
4.18	Optimization of effect of reaction time for the production of biodiesel from waste cooking oil using 4Mn-6Zr/CaO catalyst sample	69
4.19	Biodiesel yield and reusability cycles of the synthesized 4Mn-6Zr/CaO catalyst under the optimized reaction condition of 15:1	70

methanol oil ratio, 3 wt% catalyst loading, 80 °C reaction temperature, 3 h reaction time

4.20	XRD Patterns of synthesized catalyst samples; a=CaO, b=1W-Zr/CaO, c=3W-Zr/CaO, d=5W-Zr/CaO, e=7W-Zr/CaO, f=W-Zr/CaO calcined at 650 °C (5 °C/min) for 5 h *CaO, ♣WCaO, ♥ZrCaO, •WZrO	71
4.21	TPD-CO ₂ profile of synthesized W-Zr/CaO mixed oxide catalysts samples with CO ₂ absorptions at different temperature range	73
4.22	TPD-NH ₃ profiles of synthesized W-Zr/CaO mixed oxide catalyst samples with NH ₃ absorptions at different temperature range	74
4.23	Micrograms of the synthesized W-Zr/CaO catalyst samples; (a) SEM image of CaO, (b) SEM image of 1W-Zr/CaO, (c) SEM image of 3W-Zr/CaO, (d) SEM image of 5W-Zr/CaO, (e) SEM image of 7W-Zr/CaO, (f) SEM image of 9W-Zr/CaO	75
4.24	Correlation between the acidity, basicity and the biodiesel yield of W-Zr/CaO catalyst samples	77
4.25	Optimization of effect of methanol to oil ratio using 7W-Zr/CaO catalyst on biodiesel production from waste cooking oil	78
4.26	Optimization of effect of catalyst loading using 7W-Zr/CaO catalyst for biodiesel production from waste cooking oil	79
4.27	Optimization of effect of reaction temperature using 7W-Zr/CaO catalyst sample for the production of biodiesel from waste cooking oil	80
4.28	Optimization of effect of reaction time using 7W-Zr/CaO catalyst sample for biodiesel production from waste cooking oil	81
4.29	Reusability cycles of 7W-Zr/CaO catalyst under optimized condition of 15:1 methanol oil ratio, 80 °C reaction temperature, 2 wt% catalyst loading and 1 h reaction time	82
4.30	XRD patterns of synthesized W-Mo/CaO catalyst samples calcined at 650°C. ♣CaO, ★WCaO, ♥MoCaO and ♦WMO	84
4.31	TPD-CO ₂ profile of synthesized W-Mo/CaO catalysts samples with CO ₂ absorption at different temperature ranges	86
4.32	TPD-NH ₃ profile of synthesized W-Mo/CaO catalyst samples	87

with NH₃ absorptions at different temperature ranges

4.33	SEM Micrographs of synthesized W-Mo/CaO catalyst samples	89
4.34	Thermal gravimetric analysis of synthesized W-Mo/CaO catalyst samples a=W _{0.3} -Mo _{0.7} /CaO, b=W _{0.4} -Mo _{0.6} /CaO, c=W _{0.5} -Mo _{0.5} /CaO, d=W _{0.6} -Mo _{0.4} /CaO and e=W _{0.7} -Mo _{0.3} /CaO	90
4.35	FTIR spectra of the synthesized W-Mo/CaO catalyst samples; a=W _{0.3} -Mo _{0.7} /CaO b=W _{0.4} -Mo _{0.6} /CaO c=W _{0.5} -Mo _{0.5} /CaO, d=W _{0.6} -Mo _{0.3} /CaO and e=W _{0.7} -Mo _{0.3} /CaO	91
4.36	Correlation between the acidity, basicity and the biodiesel yield of W-Mo/CaO catalyst samples	92
4.37	Reusability cycles of the synthesized W _{0.6} -Mo _{0.4} /CaO catalyst sample for biodiesel production under optimized reaction conditions of 15:1 methanol to oil molar ratio, 2 wt% catalyst loading, 70 °C reaction temperature and 2 h reaction time	94
4.38	The SEM images of W _{0.6} -Mo _{0.4} /CaO catalyst sample before and after reaction cycles (a) Virgin catalyst (b) Used catalyst	94

LIST OF ABBREVIATIONS

AAS	Atomic Absorption Spectroscopy
AOAC	Association of Official Analytical Chemists
ASTM	American Society for Testing Materials
AV	Acid Value
P	Actual gas pressure
v	Adsorbed gas quality
BET	Brunauer Emmett Teller
R_1, R_2, R_3	Carbon chain of fatty acid
C_{IS}	Concentration of Internal Standard
CO_2 –TPD	Temperature Programmed Desorption of Carbon dioxide
CP	Cloud Point
DG	Diglycerides
EDX	Energy Dispersive X-ray
FAME	Fatty Acid Methyl Ester
FFA	Free Fatty Acid
FID	Flame Ionization Detector
FP	Flash Point
FTIR	Fourier Transform Infrared
FWHM	Full Width of Half Maximum
GC-MS	Gas chromatogram – mass spectroscopy
ICDD	International Centre for Diffraction Data
A_{IS}	Internal standard peak area
JCPDS	Joint Committee on Powder Diffraction Standard
MPOB	Malaysian Palm Oil Board
μm	Monolayer adsorbed gas quality
$MW_{fatty\ acid}$	Average molecular weight of fatty acid

MW _{glycerol}	Average molecular weight glycerol
MW _{water}	Average molecular weight of water
MW _{oil}	Average molecular weight of waste cooking oil
PME	Palm oil Methyl Ester
PP	Pour Point
P/P _o	Relative Pressure
ΣA	Total peak area of fatty acid methyl esters
S _{BET}	Total surface area
SEM	Scanning Electron Microscopy
SFA	Saturated Fatty Acid
SV	Saponification Value
TCD	Thermal Conductivity Detector
TG/DTA	Thermogravimetric and Differential Thermal Analysis
V _{IS}	Volume of the internal standard
WCO	Waste Cooking Oil
WFO	Waste Frying Oil
WES	Waste Egg Shell
WCPO	Waste Cooking Palm Oil
XRD	X-Ray Diffraction

CHAPTER 1

INTRODUCTION

1.1 Background

Conventional fossil fuel will continue to be a relevant key player as an energy source for human activities such as production of goods and transport services for decades to come (Galadima & Muraza, 2014). However, the global energy crisis and the possible future depletion of conventional fossil fuel, environmental problems as a result of poisonous gases especially carbon monoxide (CO) from automobile exhausts and industries are the greatest challenges of fossil fuel today. The aforementioned are the major drivers prompting the search for alternative renewable source of energy that could replace the conventional fossil fuel (Chouhan & Sarma, 2011; Muhammad *et al.*, 2015).

The current global economy depends solely on the production of goods and services, including transportation, which depends solely on petroleum based sources of energy. Apart from coal, nuclear power, natural gas and hydroelectricity that serve at different capacity in the provision of energy, transportation of goods and services sector alone is more than 90% dependence on fossil fuels (petroleum) with more than 60% annual global fuel consumption (Borges & Díaz 2012; Avhad & Marchetti 2015). Renewable sources of energy such as bio-fuels are generally considered as replaceable options alternative to traditional fossil fuel due to their environmental friendly and feedstock availability (Rabiah Nizah *et al.*, 2014; Shajaratun Nur *et al.*, 2014).

Biofuel is generally referred to as fuel either in liquid or gaseous form produced from biomass and used as fuel for internal combustion engines (cars, generators, ships and airplanes). Biofuels has proved to be economically viable considering the availability of feedstocks and eco-friendly as a result of biodegradability and less toxicity (Nigam & Singh, 2011). Other advantages of biodiesel over Petro-diesel include; the provision of independent economy that would employ rural people and reduce over dependence on fossil fuel economy. Biodiesel has improved combustion due to high oxygen content and could easily be blended with fossil based diesel in different proportions.

Biodiesel is one of the promising alternative source of energy considering its biodegradability and low emission of carbon dioxide, free sulphur and non-toxic nature (Fauzi & Amin., 2013; Mardhiah *et al.*, 2017). Another interesting thing about biodiesel is that it possesses all the chemical properties of traditional fossil fuel such as improved cetane number, high flash point low cloud point and good pour point (Galadima & Muraza, 2014).

As a result of rapid growth in human population, scientific and technological advancements in developing countries, the biodiesel demand is estimated to either doubled or tripled by the year 2020 and beyond (Galadima & Muraza, 2014). However, relevant studies have fully verified number of issues regarding biodiesel that is not convincingly addressed yet. Conversion of triglycerides into fatty acid methyl ester requires a reaction of the former with monohydric alcohol (methanol). Most of the researchers recommended that the short chain monohydric alcohol, typically methanol, ethanol and propanol with no distinct justification of which provides the best viscosity requirements in line with specifications by American Society of Testing and Materials (ASTM) and European standard (EN) (Galadima & Muraza, 2014).

Technically, biodiesel is not yet considered as a popular alternative source of energy to conventional fossil fuel worldwide considering issues related to feedstock and catalyst system. High cost of food grade oil, which covers more than 80% of total biodiesel production, and conventional homogeneous catalyst system that require large amounts of water and energy during separation after the reaction, makes biodiesel production difficult and expensive. Inadequate of raw material and effective catalytic system, are the major problems facing commercialization of biodiesel to meet the global demand and the united nation millennium environmental policy. Hence the fundamental policy of biodiesel is not yet achieved.

Biodiesel production in commercial scale at low cost and environmentally benign condition is the only way to make biodiesel globally accepted fuel for industrial and transport services. This can only be achieved through diversifying and utilization of different low cost feedstock for biodiesel synthesis. The low cost feedstock for biodiesel include palm fatty acid distillate (PFAD), waste cooking oil, *jatropha curas oil* etc (Bhuiya *et al.*, 2014). Considering the free fatty acid (FFA) content of these feedstock, separation difficulty and environmental issues of homogeneous catalyst system after reaction, heterogeneous catalyst is regarded as the best option for sustainable commercial production of biodiesel with less difficulty.

Generally a catalyst is defined as any material or substance that speeds up the rate of chemical reaction by lowering its activation energy (Peter & Julio, 2010). It is usually added in a minute amount in comparison to the quantity of the reactants, which is not consumed during the chemical reaction; it is also known as an initiator. However, in some cases the catalyst inhibits the reaction by being consumed and regenerated, while in other cases it seems not to include in the process and functions by high calibre of surface characteristics (Ertl *et al.*, 2008). Catalysis generally represents the vital technology for accelerating the essential chemical conversion, which is a key to recognize environmentally friendly and commercially feasible reactions for transforming energy carriers to direct usable energy. However, the use of heterogeneous catalysts for chemical conversions not only decreases the total energy input needed for production processes, but also improves two considerable catalyst aspects, i.e. selectivity and thermal stability, thus leading to ecologically benign green technology.

1.2 Problem statement

The extensively available feedstocks make biodiesel production a striking field to invest in and enlarge. Nevertheless, current employed manufacturing processes produced an expensive renewable-based fuel in contrast to conventional fossil-based fuel, which is attributed to feedstock and manufacturing costs.

A conventional catalytic system (homogeneous catalyst) adopted for the production of biodiesel in commercial scale is only fitting for the higher grade vegetable oils. Continual use of such oil as feedstock for fuel may pose hunger threat due to food versus fuel competition in the near future. Besides, continual usage of liquid catalysts will make biodiesel not only difficult, but pollute the environment through the generated waste water during washing of catalyst.

Sustainable biodiesel production should employ the usage of low grade feedstock such as waste cooking oil, palm fatty acid distillate (PFAD), which would maintain a new route being cheap and accessible to overcome the associated problems with food grade oil. Heterogeneous catalyst has revealed less marked operational difficulty when compared to homogeneous catalysts, as they have the advantages of easy separation after use, reused severally, environmentally benign, low cost and easy to dispose after use.

However, most of heterogeneous catalysts for biodiesel production are associated to severe reaction conditions during the reaction process, which are considered as one of the main obstacles to this category of catalyst. This project will focus more on developing new heterogeneous catalyst system that could convert the low grade feedstock specifically waste cooking oil with high free fatty acid (FFA) and some impurities such as water content at mild conditions (low reaction temperature ≤ 80 °C, short reaction time ≤ 3 h, low catalyst loading and moderate methanol to oil molar ratio). The catalytic activity of these catalysts would be improved to achieve high biodiesel yield at reduced severe reaction conditions by providing the appropriate basic and acid site densities in the catalysts samples. Leaching of catalyst active sites of most heterogeneous catalysts is another problem that greatly affects the final biodiesel yield. The newly synthesized catalysts should also made to be highly stable and reduced in leaching of active sites and therefore record high yield and reused severally before losing the catalytic activity.

Mixed metal oxides catalysts from CaO, a highly basic material and transition metals oxides were developed (Mo-Zr/CaO, Mn-Zr/CaO, W-Zr/CaO, and W-Mo/CaO) via wet impregnation method. The CaO was synthesised from egg shell. Physico-chemical properties of the mixed oxide catalysts were determined through different characterization techniques. The catalyst synthesis was optimized by varying transition metal oxide composition over the CaO surface. The catalytic activity of the synthesized catalysts was determined via transesterification reaction of waste

cooking oil to biodiesel. The prepared catalysts could have reduced leaching of Ca^{2+} metal ions in the produced biodiesel. The catalysts reusability was evaluated, which further ascertained the stability of the newly developed catalysts.

1.3 The scope of the research

The scope of this study includes the synthesis and characterizations of mixed metal oxides supported CaO from the egg shell for the transesterification of high FFA waste cooking oil to biodiesel. The catalyst was synthesized by simple wet impregnation method. The transition metal oxides such as WO_3 , ZrO_2 , MnO_3 and MoO_3 were made to bimetallic oxide and then impregnated on to the egg shell powder (CaO). The prepared catalysts were characterized to investigate their physico-chemical properties using XRD, TPD, SEM, EDX, TGA BET and FTIR techniques. The bimetallic oxide supported CaO displayed excellent physico-chemical properties that enhanced their catalytic performance on the high FFA waste cooking oil for biodiesel production. Catalysts in different stoichiometric composition were synthesized and tested for transesterification reaction of waste cooking oil. The best catalyst system was optimized for biodiesel production under four independent reaction parameters, which includes reaction temperature (60-100°C), methanol to oil molar ratio (5-25 wt%) reaction time (1-5h), and catalyst loading (1-5wt%). The catalyst reusability, stability and yield were investigated. Leaching of catalytic active phase is the major drawback of CaO based catalysts. The leaching of catalyst active sites was investigated by studying the effect of bimetallic mixed oxide loading on CaO.

1.4 Objectives of the research

The main objectives of this research are itemized as follows;

1. To synthesize and characterized the mixed metal oxides modified eggshell derived catalysts.
2. To investigate the catalytic activity of the synthesized catalysts for biodiesel production from waste cooking oil.
3. To optimize the reaction conditions for biodiesel production.
4. To evaluate the reusability and leaching of the synthesized catalysts.
5. To compare the physico-chemical properties of the produced biodiesel with the standard biodiesel fuel properties according to the ASTM and EN standards

BIBLIOGRAPHY

- Agarwal, D., & Agarwal, A. K. (2007). Performance and emissions characteristics of Jatropa oil (preheated and blends) in a direct injection compression ignition engine. *Applied Thermal Engineering*, 27, 2314–2323.
- Alhassan, F. H., Yunus, R., Rashid, U., Sirat, K., Islam, A., Lee, H. V., & Yup, H. (2013). Production of biodiesel from mixed waste vegetable oils using ferric Catal., sulphate as an effective reusable heterogeneous solid acid catalyst. *Applied Catalysis A: General*, 456(4), 182–187.
- Alves, C. T., Oliveira, A., Carneiro, S. A. V, Silva, A. G., Andrade, H. M. C., Melo, S. A. B. V. De, & Torres, E. A. (2013). Transesterification of waste frying oil using a zinc aluminate catalyst. *Fuel Processing Technology*, 106, 102–107.
- Amani, H., Ahmad, Z., Asif, M., & Hameed, B. H. (2014). Transesterification of waste cooking palm oil by MnZr with supported alumina as a potential heterogeneous catalyst. *Journal of Industrial and Engineering Chemistry*, 20(6), 4437–4442.
- Amani, H., Ahmad, Z., & Hameed, B. H. (2014). Highly active alumina-supported Cs – Zr mixed oxide catalysts for low-temperature transesterification of waste cooking oil. “*Applied Catalysis A, General*,” 487, 16–25.
- Amigun, B., Sigamoney, R., & Blottnitz, H. V. (2008). Commercialization of biofuel industry in Africa: A review. *Renewable and Sustainable Energy Reviews*, 12, 690–711.
- Ardizzone, S., Bianchi, C. L., Cappelletti, G., & Porta, F. (2004). Liquid-phase catalytic activity of sulfated zirconia from sol – gel precursors : the role of the surface features. *Journal of Catalysis*, 227, 470–478.
- Arifin, A. A., Bakar, J., Tan, C. p., Rahman, R. A., Krim, R., & Loi, C. C. (2009). Essential fatty acids of Pitaya (Dragon fruit) seed oil. *Food Chemistry*, 114, 561–564.
- Avhad, M. R., & Marchetti, J. M. (2015). A review on recent advancement in catalytic materials for biodiesel production. *Renewable and Sustainable Energy Reviews*, 50, 696–718.
- Banković-Ilić, I. B., Stamenković, O. S., & Veljković, V. B. (2012). Biodiesel production from non-edible plant oils. *Renewable and Sustainable Energy Reviews*, 16(6), 3621–3647.
- Bet-moushoul, E., Farhadi, K., Mansourpanah, Y., Mohammad, A., Molaei, R., & Forough, M. (2016). Application of CaO-based / Au nanoparticles as heterogeneous nanocatalysts in biodiesel production. *Fuel*, 164, 119–127.

- Bhaskar, S., Abhishek, G., Ismail, R., & Faizal, B. (2014). Towards a sustainable approach for development of biodiesel from plant and microalgae : A review. *Renewable and Sustainable Energy Reviews*, 29, 216–245.
- Bhaumik, P., & Dhepe, P. L. (2016). Solid acid catalyzed synthesis of furans from carbohydrates. *Catalysis Reviews*, 58(May), 36–112.
- Bhuiya, M. M. K., Rasul, M. G., Khan, M. M. K., Ashwath, N., Azad, A. K., & Hazrat, M. A. (2014). Second Generation Biodiesel: Potential Alternative to-edible Oil-derived Biodiesel. *Energy Procedia*, 61, 1969–1972.
- Birla, A., Singh, B., Upadhyay, S. N., & Sharma, Y. C. (2012). Kinetics studies of synthesis of biodiesel from waste frying oil using a heterogeneous catalyst derived from snail shell. *Bioresource Technology*, 106, 95–100.
- Borges, M. E., & Díaz, L. (2012). Recent developments on heterogeneous catalysts for biodiesel production by oil esterification and transesterification reactions : A review. *Renewable and Sustainable Energy Reviews*, 16(5), 2839–2849.
- Canakci, M., & Van Gerpen, J. (2004). A pilot plant to produce biodiesel from high free fatty acid feedstocks. *Transactions of the American Society of Agricultural Engineers*, 46, 945–955.
- Chen, G., & Fang, B. (2011). Preparation of solid acid catalyst from glucose-starch mixture for biodiesel production. *Bioresource Technology*, 102, 2635–2640.
- Chouhan, A. P. S., & Sarma, A. K. (2011). Modern heterogeneous catalysts for biodiesel production : A comprehensive review. *Renewable and Sustainable Energy Reviews*, 15(9), 4378–4399.
- Correia, L. M., Saboya, R. M. A., de Sousa Campelo, N. Cecilia, J. A., Rodríguez-Castellón, E. Cavalcante Jr, C. L., & Vieira, R. S. (2014). Characterization of calcium oxide catalysts from natural sources and their application in the transesterification of sun- flower oil. *Bioresource Technology*, 151, 207–213.
- Cullity, B. D. (1978). *Elements of X-ray diffraction*. London: Addison-Wesley.
- Damyanova, S., Pawelec, B., & Arishtirova, K. (2008). Study of the surface and redox properties of ceria – zirconia oxides. *Applied Catalysis A: General*, 337(1), 86–96.
- Dehkordi, A. M., & Ghasemi, M. (2012). Transesterification of waste cooking oil to biodiesel using Ca and Zr mixed oxides as heterogeneous base catalysts. *Fuel Processing Technology*, 97, 45–51.
- Demirbas, A. (2003). Biodiesel fuels from vegetable oils via catalytic and non-catalytic supercritical alcohol transesterification and other methods: A survey. *Energy Conversion and Management*, 44(13), 2093–2109.

- Demirbas, A., & Kara, H. (2006). New options for conversion of vegetable oils to alternative fuels. *Energy source part A. Recovery Utilization and Environment Effects*, 28, 619–626.
- Deng, X., Fang, Z., Liu, Y. hu, & Yu, C. L. (2011). Production of biodiesel from Jatropha oil catalyzed by nanosized solid basic catalyst. *Energy*, 36(2), 777–784.
- Dias, J. M., Alvim-Ferraz, M. C. M., & Almeida, M. F. (2008). Comparison of the performance of different homogeneous alkali catalysts during transesterification of waste and virgin oils and evaluation of biodiesel quality. *Fuel*, 87, 3572–3578.
- Ertl, G., Knözinger, H., & Weitkamp, J. (2008). *Preparation of solid catalysts*. John Wiley & Sons.
- Escobar, J. C., Lora, E. S., Venturini, O. J., Yáñez, E. E., Castillo, E. F., & Almazan, O. (2009). Biofuels: Environment, technology and food security. *Renewable and Sustainable Energy Reviews*, 13(6-7), 1275–1287.
- Ezebor, F., Khairuddean, M., Zuhairi, A., & Lim, P. (2014). Oil palm trunk and sugarcane bagasse derived solid acid catalysts for rapid esterification of fatty acids and moisture-assisted transesterification of oils under pseudo-infinite methanol. *BIORESOURCETECHNOLOGY*, 157, 254–262.
- Fadhil, A. B., & Ali, L. H. . (2013). Alkaline-catalyzed transesterification of Silurus triostegus Heckel fish oil: Optimization of transesterification parameters. *Renewable Energy*, 60, 481–488.
- FAO. (2014). Food and Agriculture Organization. Oil seeds market summary Trade and Markets Division, Food outlook. Retrieved April 20, 2014, from http://www.fao.org/fileadmin/templates/est/COMM_M
- Farooq, M., Ramli, A., & Subbarao, D. (2013). Biodiesel production from waste cooking oil using bifunctional heterogeneous solid catalysts. *Journal of Cleaner Production*, 59, 131–140.
- Fauzi, A. H. M., & Amin., N. A. S. (2013). Optimization of oleic acid esterification catalyzed by ionic liquid for green biodiesel synthesis. *Energy Conversion and Management*, 76, 818–827.
- Felizardo, P., Neiva Correia, M. J., Raposo, I., Mendes, J. F., Berkemeier, R., & Bordado, J. . (2006). Production of biodiesel from waste frying oils. *Waste Management*, 26, 487–494.
- Furuta, S., Hiromi, M., & Kazushi, A. (2004). Biodiesel fuel production with solid superacid catalysis in fixed bed reactor under atmospheric pressure. *Catalysis Communications*, 5, 721–723.
- Furuta, S., Matsushashi, H., & Arata, K. (2006). Biodiesel fuel production with solid

- amorphous-zirconia catalysis in fixed bed reactor. *Biomass and Bioenergy*, 30, 870–873.
- Galadima, A., & Muraza, O. (2014). Biodiesel production from algae by using heterogeneous catalysts: A critical review. *Energy*, 78, 0–11.
- Gole, V. L., & Gogate, P. R. (2013). Intensification of synthesis of biodiesel from non-edible oil using sequential combination of microwave and ultrasound. *Fuel Process Technology*, 106, 62–69.
- Grandos, M. L., Alonso, D. M., Mariscal, R., Galisteo, F. C., & Moreno-Tost, R. (2007). Biodiesel from sunflower oil by using activated calcium oxide. *Applied Catalysis B : Environmental*, 73(3-4), 317–326.
- Gryglewicz, S. (1999). Rapeseed oil methyl oil esters preparation using heterogeneous catalysts. *Bioresource Technology*, 70, 249–253.
- Hua, Y., Omar, M., Nolasco-hipolito, C., & Taufiq-yap, Y. H. (2015). Waste ostrich- and chicken-eggshells as heterogeneous base catalyst for biodiesel production from used cooking oil: Catalyst characterization and biodiesel yield performance. *Applied Energy*, 160, 58–70.
- Islam, A., Eng-Seng Chan, N. B., Taufiq-Yap, Y. H., Alam, M. D., Mondal, H., & Moniruzzaman, M. D. (2014). Energy security in Bangladesh Perspective - Assessment and Implication. *Renewable and Sustainable Energy Reviews*, 32, 154–171.
- Islam, A., & Hui, Y. (2012). Synthesis and characterization of millimetric gamma alumina spherical particles by oil drop granulation method. *Journal of Porous Material*, 19, 807–817.
- Islam, A., Taufiq-yap, Y. H., Chan, E., Moniruzzaman, M., & Islam, S. (2014). Advances in solid-catalytic and non-catalytic technologies for biodiesel production. *Energy Conversion and Management*, 88, 1200–1218.
- Islam, A., Yun Hin, T.-Y., Ravindra, P., & Siow, H. T. (2015). Biodiesel synthesis over millimetric g-Al₂O₃/KI catalyst. *Energy*, 89, 965–973.
- Issariyakul, T., & Dalai, A. K. (2014). Biodiesel from vegetable oils. *Renewable and Sustainable Energy Reviews*, 31, 446–471.
- Jacobson, K., Gopinath, R., Meher, L. C., & Dalai, A. K. (2008). Solid acid catalyzed biodiesel production from waste cooking oil. *Applied Catalysis B: Environmental*, 85, 86–91.
- Jitputti, J., Kitiyanan, B., Rangsunvigit, P., Bunyakiat, K., Attanatho, L., & Jenvanitpanjakul, P. (2006). Transesterification of crude palm kernel oil and crude coconut oil by different solid catalysts. *Chemical Engineering Journal*, 116(1), 61–66.

- Kaur, N., & Ali, A. (2015). Preparation and application of $\text{Ce} = \text{ZrO}_2 \cdot \text{TiO}_2 = \text{SO}_2$ as solid catalyst for the esterification of fatty acids. *Renew Energy*, 81, 421–431.
- Kawashima, A., Matsubara, K., & Honda, K. (2009). Acceleration of catalytic activity of calcium oxide for biodiesel production. *Bioresource Technology*, 100, 696–700.
- Kazemian, H., Turowec, B., Siddiquee, M. N., & Rohani, S. (2013). Biodiesel production using cesium modified mesoporous ordered silica as heterogeneous base catalyst. *Fuel*, 103, 719–724.
- Knothe, G. (2005). The history of vegetable oil based diesel fuel. In G. Knothe, J. V. Garpen, & J. Krahel (Eds.), *The biodiesel handbook*. Illinois: AOCS.
- Kouzu, M., & Hidaka, J. (2011). Transesterification of vegetable oil into biodiesel catalyzed by CaO: A review. *Fuel*, 93, 1–12.
- Lakhaya, J. K., Jutika, B., & Dhanapati, D. (2014). Review on the latest developments in biodiesel production using carbon based catalysts. *Renewable and Sustainable Energy Reviews*, 29, 546–564.
- Lam, M. K., Lee, K. L., & Mohamed, A. R. (2010). Homogeneous, heterogeneous and enzymatic catalysis for transesterification of high free fatty acid oil (waste cooking oil) to biodiesel: A review. *Biotechnology Advances*, 28(4), 500–518.
- Lam, M. K., Lee, K. T., & Mohamed, A. R. (2009). Sulfated tin oxide as solid superacid catalyst for transesterification of waste cooking oil: An optimization study. *Applied Catalysis B: Environmental*, 93, 134–139.
- Lee, A. F., Bennett, J. A., Manayil, J. C., & Wilson, K. (2014). Heterogeneous catalysis for sustainable biodiesel production via esterification and transesterification. *Royal Society of Chemistry*, 1–30.
- Lee, A. F., Bennett, J. A., Manayil, J. C., & Wilson, K. (2014). Heterogeneous catalysis for sustainable biodiesel production via esterification and transesterification. *Chemical Society Reviews*, 43, 7887–7916.
- Lee, D. W., Park, Y. M., & Lee, K. Y. (2009). Heterogeneous base catalysts for transesterification in biodiesel synthesis. *Catalysis Survey from Asia*, 13, 63–77.
- Leung, D. Y. C., & Guo, Y. (2006). Transesterification of neat and used frying oil: Optimization for biodiesel production. *Fuel Processing Technology*, 87, 883–890.
- Li, Y., Zhang, X. D., Sun, L., Xu, M., Zhou, W. G., & Liang, X. H. (2010). Solid superacid catalyzed fatty acid methyl esters production from acid oil. *Applied Energy*, 87(7), 2369–2373.

- Li, Y., Zhang, X., Sun, L., Zhang, J., & Xu, H. (2010). Fatty acid methyl ester synthesis catalyzed by solid superacid catalyst. *Applied Energy*, 87(1), 156–159.
- Liu, L., Wang, B., Du, Y., Zhong, Z., & Borgna, A. (2015). Bifunctional $\text{Mo}_3\text{VO}_x/\text{H}_4\text{SiW}_{12}\text{O}_{40}/\text{Al}_2\text{O}_3$ catalysts for one-step conversion of glycerol to acrylic acid: Catalyst structural evolution and reaction pathways. *Applied Catalysis B, Environmental*, 174–175, 1–12.
- Lokman, I. M., Rashid, U., & Yun Hin, T. (2015a). Chinese Journal of Chemical Engineering Production of biodiesel from palm fatty acid distillate using sulfonated-glucose solid acid catalyst: Characterization and optimization. *Chinese Journal of Chemical Engineering*, 23, 1857–1864.
- Lokman, I. M., Rashid, U., & Yun Hin, T.-Y. (2015b). Meso- and macroporous sulfonated starch solid acid catalyst for esterification of palm fatty acid distillate. *ARABIAN JOURNAL OF CHEMISTRY*. <http://doi.org/10.1016/j.arabjc.2015.06.034>
- Lokman, I. M., Rashid, U., Yunus, R., & Taufiq, Y. H. (2014). Carbohydrate-derived Solid Acid Catalysts for Biodiesel Production from Low-Cost Feedstocks: A Review. *Catalysis Reviews: Science and Engineering*, 56(July 2015), 187–219.
- Lotero, E., Liu, Y., Lopez, D. E., Suwannakarn, K., Bruce, D. A., & Goodwin, J. G. (2005). Synthesis of Biodiesel via Acid Catalysis. *Industrial and Engineering Chemistry Research*, 44, 5353–5363.
- Ma, F., & Hanna, H. A. (1999). Biodiesel production: A review. *Bioresource Technology*, 70, 1–15.
- Mahesh, S. E., Ramanathan, A., Begum, K. M. M. S., & Narayanan, A. (2015). Biodiesel production from waste cooking oil using KBr impregnated CaO as catalyst. *Energy Conversion and Management*, 91, 442–450.
- Manoilova, O., Podkolzin, S., Tope, B., Lercher, J., Stangland, E., & Goupil, J.-M. (2004). Surface acidity and basicity of La_2O_3 , LaOCl , and LaCl_3 characterized by IR spectroscopy, TPD, and DFT calculations. *Journal of Physical Chemistry B*, 108, 1577–1581.
- Marchetti, J. M., & Errazu, A. F. (2008). Esterification of free fatty acids using sulfuric acid as catalyst in the presence of triglycerides. *Biomass Bioenergy*, 32, 892–895.
- Mardhiah, H. H., Ong Chyuan, H., Masjuki, H. H., Lim, S., & Lee, H. V. (2017). A review on latest developments and future prospects of heterogeneous catalyst in biodiesel production from non-edible oils. *Renewable and Sustainable Energy Reviews*, 67, 1225–1236.
- Meher, L. C., Churamani, C. P., Ahmed, Z., & Naik, S. N. (2013). *Jatropha curcas* as

- a renewable source for bio-fuels — A review. *Renewable and Sustainable Energy Reviews*, 26, 397–407.
- Motasemi, F., & Ani, F. N. (2012). A review on microwave-assisted production of biodiesel. *Renewable and Sustainable Energy Reviews*, 16(7), 4719–4733.
- Muhammad, Y., Adeniyi, P., Raji-yahya, A. O., Aziz, A. R. A., Mohd, W., & Wan, A. (2015). Acidity and catalytic performance of Yb-doped SO₂ for biodiesel production. *Journal of the Taiwan Institute of Chemical Engineers*, 000, 1–10.
- Muhammad, Y., Mohd, W., Wan, A., & Aziz, A. R. A. (2014). Activity of solid acid catalysts for biodiesel production: A critical review. *Applied Catalysis A, General*, 470, 140–161.
- Muppaneni, T., Reddy, H. K., Ponnusamy, S., Patil, P. D., Sun, Y. Q., Dailey, P., & Deng, S. G. (2013). Optimization of biodiesel production from palm oil under supercritical ethanol conditions using hexane as co-solvent: a response surface methodology approach. *Fuel*, 107, 633–640.
- Nakajima, K., & Hara, M. (2012). Amorphous Carbon with SO₃H Groups as a Solid Brønsted Acid Catalyst. *American Chemical Society Catalysis*, 2, 1296–1304.
- Nakatani, N., Takamori, H., Takeda, K., & Sakugawa, H. (2009). Transesterification of soybean oil using combusted oyster shell waste as a catalyst. *Bioresource Technology*, 100, 1510–1513.
- Nakpong, P., & Wootthikanokkhan, S. (2010). High free fatty acid coconut oil as a potential Energy, feedstock for biodiesel production in Thailand. *Renewable Energy*, 35, 1682–1687.
- Navajas, A., Issariyakul, T., Arzamendi, G., Gandía, L. M., & Dalai, A. K. (2013). Development of eggshell derived catalyst for transesterification of used cooking oil for biodiesel production. *Asia-Pacific Journal of Chemical Engineering*, 8, 742–748.
- Nigam, P. S., & Singh, A. (2011). Production of liquid biofuels from renewable sources. *Progress in Energy and Combustion Science*, 37, 52–68.
- Nur Syazwani, O., Rashid, U., & Taufiq Yap, Y. H. (2015). Low-cost solid catalyst derived from waste *Cyrtopleura costata* (Angel Wing Shell) for biodiesel production using microalgae oil. *Energy Conversion and Management*, 101, 749–756.
- Park, Y.-M., Lee, D., Kim, D., Lee, J., & Lee, K. (2008). The heterogeneous catalyst system for the continuous conversion of free fatty acids in used vegetable oils for the production of biodiesel. *Catalysis Today*, 131, 238–243.
- Pesaresi, L., Brown, D. R., Lee, A. F., Montero, J. M., Williams, H., & Wilson, K.

- (2009). Cs-doped $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ catalysts for biodiesel applications. *Applied Catalysis A : General*, 360, 50–58.
- Peter, A., & Julio, D. P. (2010). *Physical Chemistry*. (Oxford, Ed.) (Ninth). New York: W,H Freeman and Company New York.
- Pua, F., Fang, Z., Zakaria, S., Guo, F., & Chia, C. (2011). Direct production of biodiesel from high-acid value *Jatropha* oil with solid acid catalyst derived from lignin. *Biotechnology for Biofuels*, 56(4), 2–9.
- Rabiah Nizah, M. F., Taufiq-Yap, Y. H., Rashid, U., Teo, S. H., Shajaratun Nur, Z. A., & Islam, A. (2014). Production of biodiesel from non-edible *Jatropha curcas* oil via transesterification using $\text{Bi}_2\text{O}_3\text{-La}_2\text{O}_3$ catalyst. *Energy Conversion and Management*, 88, 1257–1262.
- Ramachandran, K., Suganya, T., Nagendra Gandhi, N., & Renganathan, S. (2013). recent developments for biodiesel production by ultrasonic assist transesterification using different heterogeneous catalyst Areview. *Renewable and Sustainable Energy Reviews*, 22, 410–418.
- Rashid, U., & Anwar, F. (2008). Production of biodiesel through optimized alkalinecatalyzed Oil., transesterification of rapeseed oil. *Fuel*, 87(3), 265–273.
- Rashid, U., Ibrahim, M., Yasin, S., Yunus, R., Taufiq-Yap, Y. H., & Knothe, G. (2013). Biodiesel from *Citrus reticulata* (Mandarin orange) seed oil, a potential non-food feedstock. *Industrial Crops Production*, 45, 355–359.
- Rathore, V., & Madras, G. (2007). Synthesis of biodiesel from edible and non-edible oils in supercritical alcohols and enzymatic synthesis in supercritical carbon dioxide. *FUEL*, 86, 2650–2659. <http://doi.org/10.1016/j.fuel.2007.03.014>
- Rattanaphra, D., & Harvey, A. (2010). Simultaneous Conversion of Triglyceride / Free Fatty Acid Mixtures into Biodiesel Using Sulfated Zirconia. *Top Catalysis*, 53, 773–782.
- Rezaei, R., Mohadesi, M., & Moradi, G. R. (2013). Optimization of biodiesel production using waste mussel shell catalyst. *FUEL*, 109, 534–541.
- Robels-Medina, A., Gonzales-Moreno, P. A., Esteban-Cerdan, L., & Molina-Grima, E. (2009). Biocatalysis: Towards ever greener biodiesel production. *Biotechnology Advances*, 27(4), 389–408.
- Sánchez-Cantú, M., Pérez-Díaz, L. M., Pala-Rosas, I., Cadena-Torres, E., Juárez-Amador, L., & Rubio-Rosas, E. Rodríguez-Acosta, M. Valente, J. S. (2013). Hydrated lime as Methanol., an effective heterogeneous catalyst for the transesterification of castor oil and Methanol. *Fuel*, 110, 54–62.
- Sarin, M., Arora, R., N.P., S., Sarin, R., & Malhotra, R. . (2010). Blends of biodiesel synthesized from non-edible and edible oils: influence on the OS (oxidation

- stability). *Energy*, 35, 3449–3453.
- Sarin, R., Sharma, M., Sinharay, S., & Malhotra, R. K. (2007). Jatropha – Palm biodiesel blends : An optimum mix for Asia. *FUEL*, 86, 1365–1371.
- Shajaratun Nur, Z. A., Taufiq-Yap, Y. H., Rabiah Nizah, M. F., Teo, S. H., Syazwani, O. N., & Islam, A. (2014). Production of biodiesel from palm oil using modified Malaysian natural dolomites. *Energy Conversion and Management*, 78, 738–744.
- Sheikh, R., Choi, M., Im, J., & Park, Y. (2013). Study on the solid acid catalysts in biodiesel production from high acid value oil. *Journal of Industrial and Engineering Chemistry*, 19(4), 1413–1419.
- Sherbiny, S. A. El, Refaat, A. A., & Elsheltawy, S. T. (2010). Production of biodiesel using the microwave technique. *Journal of Advanced Research*, 1, 309–314.
- Shin, H., An, S., Sheikh, R., Park, Y. H., & Bae, S. (2012). Transesterification of used vegetable oils with a Cs-doped heteropolyacid catalyst in supercritical methanol. *Fuel*, 96, 572–578.
- Shu, Q., Nawaz, Z., Gao, J., Liao, Y. ., Zhang, Q., Wang, D., & Wang, J. (2010). Synthesis of biodiesel from a model waste oil feedstock using a carbon-based solid acid Catalyst:, Reaction and separation. *Bioresource Technology*, 101, 5374–5384.
- Singh, A. K., & Fernando, S. D. (2007). Reaction kinetics of soybean oiltransesterification using heterogeneous metal oxide catalysts. *Chemical Engineering Technology*, 30, 1716–1720.
- Siow, H. T., Motonobu, G., & Taufiq-yap, Y. H. (2015). Biodiesel production from Jatropha curcas L . oil with Ca and La mixed oxide catalyst in near supercritical methanol conditions. *The Journal of Supercritical Fluids*, 104, 243–250.
- Sirisomboonchai, S., Abuduwayiti, M., Guan, G., Samart, C., Abliz, S., Hao, X., ... Abudula, A. (2015). Biodiesel production from waste cooking oil using calcined scallop shell as catalyst. *Energy Conversion and Management*, 95, 242–247.
- Soriano, N. U., Venditti, R., & Argyropoulos, D. S. (2010). Biodiesel synthesis via homogeneous Lewis acid-catalyzed transesterification. *Fuel*, 88, 560–565.
- Sunita, G., Devassy, B. M., Vinu, A., Sawant, D. P., Balasubramanian, V. V., & Halligudi, S. B. (2008). Synthesis of biodiesel over zirconia-supported isopoly and heteropoly tungstate catalysts. *Catalysis Communications*, 9, 696–702.
- Suryaputra, W., Winata, I., Indraswati, N., & Ismadji, S. (2013). Waste capiz (Amusium crista- tum) shell as a new heterogeneous catalyst for biodiesel production. *Renewable Energy*, 50, 795–799.

- Taufiq-yap, Y. H., Hwa, S., Rashid, U., Islam, A., & Zobir, M. (2014). Transesterification of *Jatropha curcas* crude oil to biodiesel on calcium lanthanum mixed oxide catalyst : Effect of stoichiometric composition. *Energy Conversion and Management*, 88, 1290–1296.
- Thitsartarn, W., & Kawi, S. (2011). Transesterification of Oil by Sulfated Zr-Supported Silica., Mesoporous. *Industrial Engineering Chemical Research*, 50, 7857–7865.
- Tonetto, G. M., & Marchetti, J. M. (2010). Transesterification of soybean oil over Me/Al₂O₃ (Me = Na Ba, Ca, and K) catalysts and monolith K/Al₂O₃-cordierite. *Topics Catalysis*, 53, 755–762.
- Trakarnpruk, W. (2012). Biodiesel production from palm fatty acids distillate using tungstophosphoric acid- and Cs-salt immobilized-silica. *Walailak Journal of Science and Technology*, 9(1), 37–47.
- Ulgen, A., & Hoelderich, W. (2009). Conversion of Glycerol to Acrolein in the Presence of WO₃/ZrO₂ Catalysts. *Catalysis Letters*, 131(1-2), 122–128.
- Uzun, B. B., Kılıç, M., Özbay, N., Pütün, A. E., & Pütün, E. (2012). Biodiesel production from waste frying oils: Optimization of reaction parameters and determination of fuel properties. *Energy*, 44, 347–351.
- Van Gerpen, J., Shanks, B., & Pruszko, R. (2004). *National Renewable Energy Laboratory Biodiesel Analytical methods*.
- Verziua, M., Comana, S. M., Ryan Richardsb, V., & asile I. Parvulescua. (2011). Transesterification of vegetable oils over CaO catalysts. *Catalysis Today*, 167(December 2015), 64–70.
- Weckhuysen, B. M., Mestl, G., Rosynek, M. P., Krawietz, T. R., Haw, J. F., & Lunsford, J. H. (1998). Destructive adsorption of carbon tetrachloride on alkaline earth metal oxides. *Physical Chemistry B*, 102, 3773–3778.
- Wilson, K., & Clark, J. H. (2000). Solid acids and their use as environmentally friendly catalysts in organic synthesis *. *Pure & Applied Chemistry*, 72(7), 1313–1319.
- Wong, Y. C., Tan, Y. P., Ramli, I., & Tee, H. S. (2015). Biodiesel production via transesterification of palm oil by using CaO – CeO₂ mixed oxide catalysts. *Fuel*, 162, 288–293.
- Xie, W., & Li, H. (2006). Alumina-supported potassium iodide as a heterogeneous catalyst for biodiesel production from soybean oil. *Journal of Molecular Catalysis A:Chemical*, 255, 1–9.
- Yaakob, Z., Mohammad, M., Alherbawi, M., Alam, Z., & Sopian, K. (2013). Overview of the production of biodiesel from Waste cooking oil. *Renewable*

and Sustainable Energy Reviews, 18, 184–193.

Yan, S., Salley, S. O., & Ng, K. Y. S. (2009). Simultaneous transesterification and esterification of unrefined or waste oils over ZnO-La₂O₃ catalysts. *Applied Catalysis A : General*, 353(2), 203–212.

Yujaroen, D., Goto, M., Sasaki, M., & Shotipruk, A. (2009). Esterification of palm fatty Reaction, acid distillate (PFAD) in supercritical methanol: Effect of hydrolysis on reactivity. *Fuel*, 88, 2011–2016.

Zhang, J., & Jiang, L. (2008). Acid Catalysed Esterification of Zanthoxylum bungeanum Oil With High Free Fatty Acids for Biodiesel Production. *Bioresource Technology*, 99, 8995–8998.

