

UNIVERSITI PUTRA MALAYSIA

NITRIFICATION AND DENITRIFICATION OF PARTIALLY TREATED LANDFILL LEACHATE

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By

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Faculty : Food Science and Biotechnology

In this study, biological removal of ammonia, nitrite and nitrate nitrogen of partially treated landfill leachate (PTLL) was conducted by nitrification and denitrification processes. The experiments were conducted by batch treatment using 16L stirred tank reactor in which 8 L of PTLL was treated with 0%, 1%, 5% and 10% (v/v) of centrifuged landfill leachate sludge and the pH was adjusted to 7 at every 12 hour interval. The treatment systems were kept above 80% saturated with oxygen (0.06-0.19 vvm).

It was found that the treatment with 10% centrifuged landfill leachate sludge was sufficient to reduce 93% and 63% of the PTLL's ammonia and nitrite, respectively, under aerobic condition. It was also observed that the level of nitrate can be reduced by 56% by biological means from the PTLL's original concentration of 13,500 ppm during nitrification process. However, subsequent denitrification was not possible due to foaming which occurred during the nitrification treatment with 10% centrifuged



landfill leachate sludge. Large loss of biomass from the system was experienced, even when the flowrate of air supplied was reduced to a very low level at 0.06 vvm. Furthermore, the impeller located at the upper part of the reactor's shaft was unable to break the large amount of foam formed.

As an alternative to prevent foaming, further experiments were carried out in a 6L reactor with the use of 4L synthetic media of (a) defined media with controlled pH between 7.5 and 8.5; (b) model leachate (without organic nitrogen) with (i) pH adjusted to 7 every 12 hours (ii) controlled pH between 7.5 and 8.5; and (c) model leachate (with organic nitrogen and pH controlled between 7.5 and 8.5. These media consisting of ammonia, nitrite and nitrate concentrations of 1000 ppm, 1500 ppm and 3000 ppm, respectively, were treated with 10% of centrifuged landfill leachate sludge for complete nitrification and denitrification processes and to isolate the microbes involved. The saturated oxygen was kept above 80% (0.02 vvm) throughout the treatments.

Complete nitrification and denitrification were achieved at 120 and 168 hours, when defined media and model leachate (without organic nitrogen) were used respectively, under controlled pH between 7.5 and 8.5. The cell population of both treatments was found to increase from 10^8 to 10^{10} cell/ml and 10^9 to 10^{10} cell/ml respectively, at the end of denitrification process, under C/N ratio of 0.4 in which acetic acid was used as carbon source.



Several strains were isolated from nitrification and denitrification processes. They were strains WNZ 1, WNZ 2 and WNZ 3 (ammonia oxidizers) which were unable to be identified by Biolog Identification System, *Acinetobacter calcoaceticus* and *Acidovorax konjaci* (nitrite oxidizers) and *Pseudomonas aeruginosa* 1, *Pseudomonas aeruginosa* 2 and *Pseudomonas aeruginosa* 3 (nitrate oxidizers).



NITRIFIKASI DAN DINITRIFIKASI LELEHAN SISA PEPEJAL SEPARA RAWATAN

Oleh

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Kajian penyahan nitrogen amonia,nitrit dan nitrat nitrogen dari lelehan sisa pepejal separa rawatan secara biologi dilakukan melalui proses-proses nitrifikasi dan denitrifikasi. Eksperimen dilakukan secara rawatan 'batch' dengan menggunakan reaktor tangki pengadukan 16 L dimana lelehan sisa pepejal separa rawatan dirawat bersama 0%, 1%, 5% dan 10% (v/v) enapcemar lelehan sisa pepejal yang diempar dan pH di laraskan kepada 7 pada setiap 12 jam. Ketepuan oksigen di dalam system-sistem rawatan ini di kawal melebihi paras 80 % (0.06-0.19 vvm).

Didapati, rawatan bersama10% enapcemar lelehan sisa pepejal yang diempar adalah memadai untuk menurunkan 93% dan 63% daripada kepekatan ammonia dan nitrit awalan lelehan sisa pepejal separa rawatan iaitu 400 dan 2000 ppm, setiap satunya di bawah keadaan arobik. Didapati juga bahawa paras nitrat dapat dikurangkan sebanyak 56% daripada kepekatan asal lelehan sisa pepejal separa rawatan iaitu 13,500 ppm pada proses nitrifikasi. Walaubagaimanapun, proses dinitrifikasi seterusnya tidak



dapat dijalankan kerana berlakunya pembuihan semasa rawatan bersama 10% enapcemar lelehan sisa pepejal yang diempar yang menyebabkan kehilangan banyak biomas di dalam system walaupun kepekatan oksigen yang dibekalkan telah diturunkan kepada 0.06 vvm. Pengaduk yang berada di bahagian atas bioreaktor tidak dapat memecahkan buih-buih yang terbentuk.

Sebagai altenatif, eksperimen selanjutnya dijalankan dengan penggunaan media sintetik seperti (1) media tetap dengan kawalan pH diantara 7.5- dan 8.5; (2) model lelehan sisa pepejal (tanpa nitrogen organik) dengan (i) pelarasan pH kepada 7 pada setiap 12 jam (ii) kawalan pH di antara 7.5 dan 8.5; dan (c) model lelehan sisa pepejal (dengan nitrogen organic) dengan kawalan pH di antara 7.5 dan 8.5. Media-media ini mengandungi kepekatan-kepekatan ammonia nitrit dan nitrat pada 1000 ppm, 1500 ppm dan 3000 ppm, setiap satunya dirawat bersama 10% enapcemar sisa pepejal yang diempar untuk pemerhatian proses-proses nitrifikasi dan dinitrifikasi yang lengkap dan untuk memencilkan mikrob-mikrob yang terlibat. Kepekatan oksigen dikekalkan melebihi paras 80% (0.02 vvm) sepanjang rawatan di jalankan.

Nitrifikasi dan dinitrifikasi yang dicapai adalah pada 120 dan 168 jam apabila media tetap dan media model lelehan sisa pepejal (tanpa nitrogen organic) digunakan, setiap satunya di bawah kawalan pH diantara 7.5 dan 8.5. Populasi sel untuk kedua-dua rawatan didapati meningkat dari 10⁸ kepada10¹⁰ sel/ml dan 10⁹ kepada 10¹⁰ sel/ml, setiap satunya pada akhir proses denitrifikasi dengan nisbah C/N 0.4 dimana asid asetik digunakan sebakai punca karbon.



Beberapa strain dapat dipencilkan dari proses-proses nitrifikasi dan dinitrifikasi. Diantaranya ialah strain WNZ 1, WNZ 2 dan WNZ 3 (pengoksida-pengoksida ammonia) yang mana tidak dapat dikenalpasti oleh SIstem Pengenalpastian Biolog, *Acinetobacter calcoaceticus* dan *Acidovorax konjaci* (pengoksida-pengoksida nitrit) dan *Pseudomonas aeruginosa* 1, *Pseudomonas aeruginosa* 2 dan *Pseudomonas aeruginosa* 3 (pengoksida-pengoksida nitrat).



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TABLE OF CONTENTS

	Page
ABSTRACT	ii
ABSTRAK	v
ACKNOWLEDGEMENTS	viii
APPROVAL	ix
DECLARATION	х
LIST OF TABLES	xvii
LIST OF FIGURES	xix
LIST OF ABBREVIATIONS	xxiv

CHAPTER

I	INTRODUCTION	1
II	LITERATURE REVIEW	3
	Generation Process of Landfill Leachate	3
	Current Treatment System of Landfill Leachate	5
	Landfill Leachate Treatment in Malaysia	7
	Foaming In Biological Wastewater Treatment	9
	Composition and Characteristics of Landfill Leachate	12
	Microbiology of Landfill Leachate	17
	Landfill Leachate as Pollution	20
	Forms of Nitrogen	21
	Ammonia	21
	Nitrite	23
	Nitrate	24
	Nitrogen Cycle	25
	Nitrogen as Pollutant	26
	Effect of Nitrogen Discharged	27
	Nitrogen Removal Treatments	27
	Biological Nitrogen Removal	28
	Biological Nitrification and Denitrification	28
	Bacterial Population of Nitrification	30
	Nitrifying Bacteria	30
	Ammonia Oxidizers	31
	Nitrite Oxidizers	31
	Nitrifiers and Their Characteristics	34
	Ammonia Oxidizing Bacteria	34
	Nitrite Oxidizing Bacteria	35
	Biochemistry of Nitrification	36
	Biochemical Pathway	36
	Energy and Synthesis Relationship	40



	Effect of Environmental Factors	42
	Nitrification Inhibitors	43
	Bacterial Population of Denitrification (Nitrate Oxidizers)	49
	Biochemistry of Denitrification	50
	Biochemical Pathway	50
	Energy and Synthesis Relationship	52
	Effect of Environmental Factors of Denitrification	54
	C/N Relationship	54
	Importance of Denitrification	60
	Aerobic Denitrification	60
	Nitrification and Denitrification of Landfill Leachate	62
	Electron Microscopy (EM)	63
	Scanning Electron Microscope (SEM)	64
	Transmission Electron Microscope (TEM)	64
III	GENERAL MATERIALS AND METHODS	66
	Chemical Reagents	66
	Landfill Leachate Treatment of AirHitam Sanitary Landfill	67
	Partially Treated Landfill Leachate (PTLL) and Landfill Leachate Sludge	69
	Experimental Design	70
	Aerobic Batch Treatment of Partially Treated Landfill Leachate	71
	Sludge Preparation	71
	Dissolved Oxygen (D.O) Measurement	71
	Reactor Setup	71
	Aerobic Treatment of PTLL (Nitrification)	75
	Nitrification and Denitrification of Defined Medium	75
	Isolation of Ammonia Oxidizing Bacteria	77
	Isolation of Nitrite Oxidizing Bacteria	78
	Isolation of Nitrate Oxidizing Bacteria	78
	Biolog MicroLog Identification System	79
	Maintenance of Isolates	82
	Medium	82
	Maintenance and Growth Media	82
	Preparation of Inoculum	82
	Appropriate pH and Temperature of Isolates (Shake Flask System)	83
	Microbial Growth Study	83
	Ammonia, nitrite and nitrate removals	84
	Analytical Methods	85
	Quantitative Analyses	85
	Ammoniacal Nitrogen Determination	85
	Nitrite Nitrogen Determination	85
	Nitrate Nitrogen Determination	86
	Total Phosphate Determination	87
	Acetic Acid Determination	87
	Total Kjedahl Nitrogen (TKN)	88
	Chemical Oxygen Demand (COD)	89
	Biological Oxygen Demand (BOD)	90
	Total Solids (TS) and Suspended Solids (SS)	

	Measurements	92
	Volatile Suspended Solids (VSS)	93
	Optical Density (O.D)	93
	Cell Number	94
	Qualitative Analyses	95
	Cell Morphological Characteristics and Gram Staining	95
	Oxidase Test	96
	Catalase Test	96
	Motality of Bacteria	96
	Cultural Characteristics	97
	Specimen Preparation for Electron Microscopy	97
	Scanning Electron Microscopy (SEM) and	
	Transmission Electron Microscopy (TEM)	97
	Negative Staining	99
IV	NITRIFICATION OF PARTIALLY TREATED LANDFILL	
	LEACHATE (PTLL)	100
	Introduction	100
	Material and Methods	102
	Landfill Leachate Sludge and Partially Treated Landfill Leachate	
	Effluent (PTLL)	102
	Characteristics of PTLL and Centrifuged Landfill	
	Leachate Sludge	102
	Batch Aerobic Treatment (Nitrification)	103
	Sample Analyses	104
	Results and Discussion	104
	Characteristics of Partially Treated Landfill	
	Leachate (PTLL)	104
	Characteristics of Landfill Leachate Sludge	107
	Batch Aerobic Treatment	108
	Nitrification of PTLL at Different Percentages of	
	Centrifuged Landfill leachate Sludge	108
	pH Status on Nitrification of PTLL	113
	TS, SS, VSS and Cell Concentration on	
	Nitrification of PTLL	114
	Phosphate Consumption During Nitrification of	
	PTLL	117
	BOD ₅ and COD Removal	117
	Conclusion	119
v	NITRIFICATION AND DENITRIFICATION OF MODEL	
	LEACHATE	120
	Introduction	120
	Materials and Methods	121
	Preparation of Defined Media for Nitrification and	
	Denitrification	121
	Preparation of Model Leachate (With Organic Nitrogen)	
	Media for Nitrification and Denitrification	122

	Preparation of Model Leachate (Without Organic Nitrogen)	
	Media for Nitrification and Denitrification	122
	Sample Analyses	123
	Results and Discussion	123
	Nitrification and Denitrification of Defined Media	123
	Nitrification of Model Leachate (With Organic Nitrogen)	
	Media	130
	Nitrification and Denitrification of Model Leachate	
	(Without Organic Nitrogen) Media	136
	Conclusion	137
VI	ISOLATION, IDENTIFICATION AND CHARACTERIZATION OF	<u>.</u>
	NITRIFYING AND DENITRIFYING BACTERIA	138
	Introduction	138
	Materials and Methods	139
	Preparation on the Isolation of Ammonia, Nitrite and Nitrate	
	Oxidizers from Nitrifying and Denitrifying System	139
	Sample Preparation for TEM and SEM of Isolated Nitrifiers	
	and Denitrifiers	140
	Preparation on Biochemical and Physical Characteristics of	
	Isolated Nitrifiers and Denitrifiers	141
	Biolog Identification of Isolated Nitrifiers and Denitrifiers	141
	Results and Discussion	142
	Bacterial Isolation of Ammonia, Nitrite and Nitrate Oxidizers	
	from Nitrification and Denitrification System	142
	Identification of Isolated Ammonia, Nitrite and Nitrate	
	Oxidizers	142
	Physical Characteristics of Isolated Ammonia, Nitrite and	
	Nitrate Oxidizers	144
	Conclusion	157
VII	INFLUENCE OF CULTURE CONDITIONS ON THE GROWTH O	
	NITRIFYING AND DENITRIFYING BACTERIA	158
	Introduction	158
	Materials and Methods	161
	Preparation for Appropriate pH and Temperature Test of Isolated	
	Nitirfiers and Denitrifiers of Isolated Nitrifiers and Denitrifiers	161
	Growth Study of Isolated Nitirfiers and Denitrifiers	161
	Preparation for Different Ammonia, Nitrite and Nitrate	
	Concentrations Test of Isolated Ammonia, Nitrite and	
	Nitrate Oxidizers	163
	Preparation for Different C/N Ratios Test of Isolated Nitrate	
	Oxidizers	163
	Samples Analyses	164
	Results and Discussion	164
	Effect of pH and Temperature on Isolated Nitrifiers and	
	Denitrifiers	164
	Growth Kinetic of Logistic Model on Isolated Nitrifiers	



		and Denitrifiers	169
		Preferable C/N Ratios of Isolated Nitrate Oxidizers	174
		Removal of Ammonia, Nitrite and Nitrate at Different	
		Concentrations by Isolated Nitrifiers and Denitrifiers	178
	Conclusion		188
VIII	SUMMARY,	, CONCLUSION AND SUGGESTIONS FOR	
	FUTURE W	ORK	189
	Summary		189
	Suggestions		191
	Conclusion		191
REFE	ERENCES		193
APPE	APPENDICES		213
BIODATA OF THE AUTHOR		220	



LIST OF TABLES

Table		Page
1	Number of landfill sites and levels in Malaysia (up to March 2002)	8
2	Characteristics of landfill leachate	15
3	The most frequently observed xenobiotic organic compounds (XOCs) in landfill leachate	16
4	Microbial isolates of landfill leachate	19
5	Common ammonia oxidizers	32
6	Common nitrite oxidizers	33
7	Characteristics of ammonia oxidizers	34
8	Characteristics of nitrite oxidizers	35
9a	Inhibitory effect of organic and inorganic compounds	45
10(b-c	c) Inhibitory effect of organic and inorganic compounds	46
11	Ammonia nitrogen and nitrate nitrogen concentration range for <i>Nitrobacter</i> inhibition as function of pH at temperature 20 ⁰ C	47
12	Inorganic compounds that lead to inhibition of the nitrification process	47
13	Genera of bacteria which are abundant in sewage and capable of performing denitrification	49
14	Carbon sources in denitrifying experiments	58
15	Composition of indicator for TKN	89
16	Characteristics of raw and Partially Treated Landfill Leachate (PTLL) of AirHitam Sanitary Landfill, Puchong	106
17	Characteristics of landfill leachate sludge	107
18	Cell and phosphate concentrations in treatment of PTLL with different sludge percentages	116
19	BOD removal of model leachate	133

20 Cell numbers and phosphate concentrations in treatment of model

21	leachate (without organic nitrogen) with 10% centrifuged sludge Isolated strains detected by Biolog Identification System	134 143
22	Physical characteristics of isolated strains	147
23	Cultural and biochemical characteristics of isolated strains	156
24	Summary on growth rates of isolated strains	171

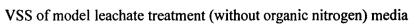


LIST	OF	FIG	URES
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Figure		Page
1	Decomposition chain: from protein to nitrate	23
2	The Nitrogen Cycle with reference to nitrogen control in wastewater treatment	25
3	Microbial nitrogen cycle	38
4(a-b)	The electron transport of ammonia and nitrite oxidizers	39
5	The electron transport of nitrate oxidizers	51
6	Schematic diagram of landfill leachate treatment plant of AirHitam Sanitary Landfill, Puchong	68
7	Partially Treated Landfill leachate (PTLL) entering settling pond before been discharged to nearby river at treatment plant of Airhitam Sanitary Landfill, Puchong	69
8	Experimental design	70
9a	Reactor set up of Partially Treated Landfill Leachate (PTLL) treatment System	72
10b	Reactor set up of Partially Treated Landfill Leachate (PTLL) treatment System	73
11c	Reactor set up of Partially Treated Landfill Leachate (PTLL) treatment System	74
12	System set up of batch synthetic medium treatments	76
13a	Removals of ammonia, nitrite and nitrate in treatment of PTLL with 0% sludge	110
14b	Removals of ammonia, nitrite and nitrate in treatment of PTLL with 1% sludge	110
15c	Removals of ammonia, nitrite and nitrate in treatment of PTLL with 5% sludge	110
16d	Removals of ammonia, nitrite and nitrate in treatment of PTLL with 10% sludge	111
17	Profile of TKN removal with different percentages of sludge	112



18	pH profile during treatment of PTLL with different percentages of leachate sludge with pH adjusted to 7 at every 12 hours.	113
19	Total solids in treatment with different sludge percentages	115
20	Suspended solids in treatment with different sludge percentages	115
21	VSS in treatment with different sludge percentages	116
22	BOD removal of PTLL in treatment with different percentages of landfill leachate sludge	118
23	The COD removals during nitrification with different sizes of sludge	119
24	Nitrification and denitrification of defined media with 10% centrifuged landfill leachate sludge	125
25	Phosphate consumption and cell accumulation during nitrification and denitrification of defined media with 10% centrifuged landfill leachate sludge	126
26	Total solids and suspended solids of nitrification and denitrification of defined media	126
27	COD and VSS of the treatment of defined media	128
28 (a-c	e)SEM micrograph of bacterial population at the end of ammonia, nitrite and nitrate removal	129
29	Ammonia removal of model leachate (without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	130
30a	Nitrite removal of model leachate(without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	132
31b	Nitrate removal of model leachate(without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	132
32	COD removal of model leachate(without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	133
33	Suspended solids of model leachate (without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	135
34	Total solids of model leachate (without organic nitrogen) media treated with 10% centrifuged landfill leachate sludge	135
35	VSS of model leachate treatment (without organic nitrogen) media	



	treated with 10% centrifuged landfill leachate sludge	136
36	Ammonia, nitrite and nitrate of Model leachate (with organic nitrogen) Media treated with 10% centrifuged landfill leachate sludge	137
37	Negative staining, SEM and TEM micrographs of isolated strain WNZ 1	148
38	Negative staining, SEM and TEM micrographs of isolated strain WNZ 2	149
39	Negative staining, SEM and TEM micrographs of isolated strain WNZ 3	150
40	Negative staining, SEM and TEM micrographs of isolated strain A. calcoaceticus	151
41	Negative staining, SEM and TEM micrographs of isolated strain <i>P. aeruginosa</i> 1	152
42	Negative staining, SEM and TEM micrographs of isolated strain <i>P. aeruginosa</i> 2	153
43	Negative staining, SEM and TEM micrographs of isolated strain <i>P. aeruginosa</i> 3	154
44	Effect of pH and temperature on growth of isolated strain WNZ 1	165
45	Effect of pH and temperature on growth of isolated strain WNZ 2	166
46	Effect of pH and temperature on growth of isolated strain WNZ 3	166
47	Effect of pH and temperature on growth of isolated strain <i>A. calcoaceticus</i>	167
48	Effect of pH and temperature on growth of isolated strain <i>P. aeruginosa</i> 1	167
49	Effect of pH and temperature on growth of isolated strain <i>P. aeruginosa</i> 2	168
50	Effect of pH and temperature on growth of isolated strain <i>P. aeruginosa</i> 3	168
51	Growth profile of isolated strain WNZ 1	169
52	Growth profile of isolated strain WNZ 2	170
53	Growth profile of isolated strain WNZ 3	170
54	Growth profile of isolated strain A. calcoaceticus	172

55	Growth profile of isolated strain P. aeruginosa 1	173
56	Growth profile of isolated strain P. aeruginosa 2	173
57	Growth profile of isolated strain P. aeruginosa 3	174
58a	Nitrate removal by P. aeruginosa 1 under different C/N ratios	175
59Ъ	Nitrate removal by P. aeruginosa 2 under different C/N ratios	175
60c	Nitrate removal by P. aeruginosa 3 under different C/N ratios	176
61	Cell number, nitrate removal, phosphate and acetic acid consumption by <i>P. aeruginosa</i> 1 under C/N ratio of 0.4	178
62	Ammonia removal at initial ammonia concentration of 50 ppm by strain WNZ 1	180
63a	Nitrite removal at initial nitrite concentration of 375 ppm by <i>A. calcoaceticus</i>	181
64b	Nitrite removal at initial nitrite concentration of 750 ppm by <i>A. calcoaceticus</i>	182
65c	Nitrite removal at initial nitrite concentration of 1500 ppm by A. calcoaceticus	182
66d	Nitrite removal at initial nitrite concentration of 3000 ppm by <i>A. calcoaceticus</i>	182
67e	Nitrite removal at initial nitrite concentration of 6000 ppm by <i>A. calcoaceticus</i>	183
68f	Nitrite removal at initial nitrite concentration of 12,000 ppm by <i>A. calcoaceticus</i>	183
69	Nitrate removal by A. calcoaceticus	185
70a	Nitrate removal at initial nitrite concentration of 2000 ppm by <i>P. aeruginosa</i> 1	185
71b	Nitrate removal at initial nitrite concentration of 4000 ppm by	186
72c	P. aeruginosa 1 Nitrate removal at initial nitrite concentration of 8000 ppm by P. aeruginosa 1	186
73d	Nitrate removal at initial nitrite concentration of 12,000 ppm by <i>P. aeruginosa</i> 1	187



74e Nitrate removal at initial nitrite concentration of 24,000 ppm by *P. aeruginosa* 1

187



LIST OF ABBREVIATIONS

v/v	Volume per volume
C/N ratio	Carbon to nitrogen ratio of medium ppm
μmax	Maximum or initial specific growth rate (h ⁻¹)
BOD	Biological oxygen demand
COD	Chemical oxygen demand
rpm	Rotation per minute
TKN	Total kjedahl nitrogen
TS	Total solids
SS	Suspended solids
VSS	Volatile suspended solids
SBR	Sequencing batch reactor
ppm	Parts per million
mmol	Millimol
SEM	Scanning electron microscopy
TEM	Transmission electron microscopy
μm	Micrometer
O.D	Optical density
М	Molarity

