



***FACILITATIVE RECOVERY OF CYCLODEXTRIN  
GLUCANOTRANSFERASE USING CHROMATOGRAPHIC STRATEGIES***

**MAGARET A/P SIVAPRAGASAM**

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**By**

**MAGARET A/P SIVAPRAGASAM**

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,  
in Fulfilment of the Requirements for the Degree of Doctor of Philosophy**

**January 2014**

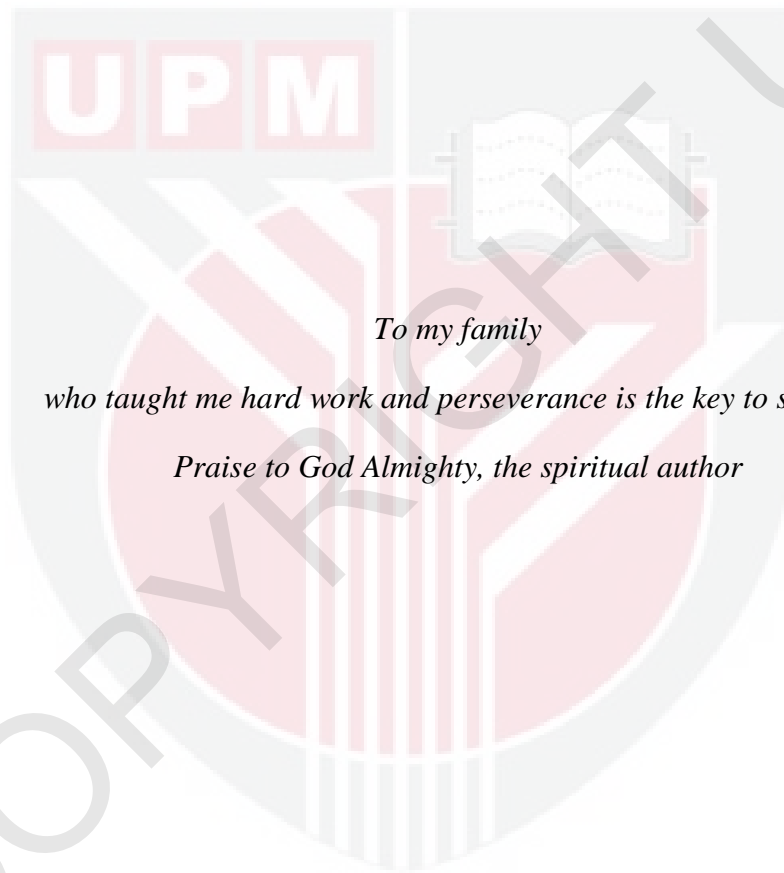
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## DEDICATION



*To my family*

*who taught me hard work and perseverance is the key to success*

*Praise to God Almighty, the spiritual author*

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Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfillment of the requirement for the degree of Doctor of Philosophy

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GLUCANOTRANSFERASE USING CHROMATOGRAPHIC STRATEGIES**

By

**MAGARET A/P SIVAPRAGASAM**

**January 2014**

**Chairman : Associate Professor Norhafizah Abdullah, PhD**  
**Institute : Bioscience**

Cyclodextrin glucanotransferase (CGTase), are monomeric enzymes that are secreted extracellularly which catalyzes transglycosylation reactions via its glucosyl residues and are used as an acceptor in forming cyclodextrins (CD). CD's, are widely used in the pharmaceutical, medicine, food, textile, agriculture and the cosmetic industries. Purifying CGTase is often a complicated task due to its heterogeneity, complexity and instability. To harness, it requires a set of downstream processing which typically consist of a cascade of recovery steps. The CGTase used in this study originated from *Bacillus sp* G1, which was successfully cloned and expressed in *E.coli* BL21. Recombinant CGTase was found to be growth related with maximum enzyme production at 167 U/mL after 10 hours of culture at 37<sup>0</sup>C in an orbital shaker with constant speed of 175 rpm. A series of pre purification strategies were carried out to determine the best method to concentrate the enzyme for subsequent purification procedures. Ammonium sulphate precipitation (70% saturation point) and dialysis tubing (SnakeSkin and flat tubing-with MWCO 3.5k) were investigated for concentrating the CGTase from *E.coli* culture. Results showed dialysis using SnakeSkin method to be superior to ammonium sulphate precipitation with CGTase yield of 148 U/mL and 19 U/mL respectively. Adsorbents used were mixed mode (of hydrophobic and ion exchange) ion exchangers, and immobilised metal affinity chelating. These adsorbents packed in a Tricorn 10/50 column, were screened for their suitability to purify CGTase by buffer optimization, frontal analysis and static binding evaluations. Purification yields using mixed mode chromatography were observed by using the mixed mode resin, PPA HyperCel which obtained 97% of CGTase enzyme recovery. Recovery performance were compared with other chromatography methods which is the ion exchange chromatography at 78% recovery and immobilised metal affinity chromatography at 87% recovery.

Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk ijazah Doktor Falsafah

**PEMULIHAN DIPERMUDAHKAN SIKLODEKSTRIN  
GLUKANOTRANFERASE MENGGUNAKAN STRATEGI  
KROMATOGRAFI**

Oleh

**MAGARET A/P SIVAPRAGASAM**

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Siklodekstrin glukanostransferase (CGTase) merupakan satu kelas enzim monomerik yang dirembeskan di luar sel yang memangkinkan tindakbalas pentransglikosilan melalui sisa glukosilnya yang bertindak sebagai penerima dalam pembentukan siklodekstrin (CD). CD digunakan secara meluas di dalam industri farmaseutikal, perubatan, makanan, tekstil, pertanian dan kosmetik. Penulenan CGTase adalah satu tugas yang sukar disebabkan oleh kepelbagaian, kerumitan dan ketidakstabilannya. Untuk mendapatkannya, ia memerlukan satu set pemprosesan hiliran yang biasanya terdiri daripada satu rangkaian langkah-langkah pemulihan. CGTase yang digunakan dalam kajian ini berasal daripada *Bacillus sp.* G1, yang telah berjaya diklon ke dalam *E.coli* BL21. CGTase rekombinan didapati berkait rapat dengan kadar pertumbuhan dan pengeluaran enzim maksimum adalah sebanyak 167 U/mL selepas 10 jam pengkulturan pada 37°C di dalam penggoncang orbital dengan kelajuan malar 175 putaran per minut. Sebagai enzim luar sel, satu siri pra-penulenan telah dilakukan bagi menentukan kaedah yang terbaik untuk memekatkan enzim dalam prosedur penulenan yang berikutnya. Pemendakan ammonium sulfat (70% tahap tepu) dan tiub dialisis (*SnakeSkin* dan tiub pipih dengan potongan berat molekul 35000) telah diuji untuk pemekatan CGTase dari kultur *E.coli*. Keputusan menunjukkan dialisis menggunakan kaedah *SnakeSkin* adalah lebih baik berbanding pemendakan ammonium sulfat dengan hasil CGTase, masing-masing sebanyak 148 U/mL dan 19 U/mL. Penjerap yang digunakan terdiri daripada mod campuran (hidrofobik dan pertukaran ion), penukar ion, dan pengkelatan afiniti logam tersekat gerak. Penjerap ini dipadatkan di dalam turus Tricorn 10/50 dan telah disaring untuk kesesuaian bagi penulenan CGTase dengan mengoptimumkan penimbal, analisis depan dan keupayaan pengikatan statik. Hasil penulenan terbaik telah diperolehi melalui resin mod campuran, PPA HyperCel, dengan 97% pemulihan CGTase. Prestasi kadar pemulihan telah dibandingkan dengan kaedah kromatografi yang lain seperti kromatografi penukaran ion dengan rekoveri 78% dan pengkelatan afiniti logam tersekat dengan kadar rekoveri 87%.

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This thesis would have remained a dream had it not been for God. All praise and thanks due.

I certify that a Thesis Examination Committee has met on 9th January 2014 to conduct the final examination of Magaret a/p Sivapragasam on her thesis entitled "Facilitative Recovery of Cyclodextrin Glucanotransferase using Chromatographic Strategies" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U.(A) 106] 15 March 1998. The Committee recommends that the student be awarded the Doctor of Philosophy.

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## TABLE OF CONTENTS

	<b>Page</b>
<b>ABSTRACT</b>	<b>i</b>
<b>ABSTRAK</b>	<b>ii</b>
<b>ACKNOWLEDGEMENT</b>	<b>iii</b>
<b>DECLARATION</b>	<b>v</b>
<b>LIST OF TABLES</b>	<b>xvi</b>
<b>LIST OF FIGURES</b>	<b>xvii</b>
<b>LIST OF APPENDICES</b>	<b>xix</b>
<b>LIST OF ABBREVIATION</b>	<b>xx</b>
<b>CHAPTER</b>	
<b>1 INTRODUCTION</b>	<b>1</b>
1.1 Background study	1
1.2 Problem statement	1
1.3 Research objectives	2
1.4 Thesis layout and research strategy	2
<b>2 LITERATURE REVIEW</b>	<b>4</b>
2.1 Background of protein purification	4
2.2 Pre purification strategies	4
2.2.1 Types of pre-purification strategies	4
2.3 Theory of adsorption chromatography	11
2.3.1 Adsorption isotherm	11
2.3.2 Static binding capacity for the adsorption of protein from suspensions	13
2.3.3 Dynamic Binding Capacity	14
2.4 Column configuration and performance	20
2.5 Types of ligand and their design	21
2.5.1 Ion Exchange Chromatography (IEC)	21
2.5.2 Hydrophobic Interaction Chromatography (HIC)	22
2.5.3 Reversed Phase Chromatography (RPC)	24
2.5.4 Size Exclusion Chromatography (SEC)	25
2.5.5 Affinity Chromatography (AF)	26
2.5.6 Mixed Mode Chromatography (MMC)	27
2.6 Mode of chromatographic operations	28
2.6.1 Fluidized Bed Adsorption (FBA)	28
2.6.2 Packed Bed Adsorption (PBA)	29
2.6.3 Expanded Bed Adsorption (EBA)	30
2.7 Cyclodextrin Glucanotransferase (CGTase)	31
2.7.1 Substrate and reactions	31
2.7.2 CGTase producers	32
2.7.3 Purification strategies of CGTase	37
2.8 Concluding remarks	45
<b>3 GENERAL METHODOLOGY</b>	<b>46</b>
3.1 Materials	

3.1.1	Strain	46
3.1.2	Chemicals	46
3.1.3	Adsorbents used for the column purification of CGTase	46
3.1.4	Chromatography adsorption column	46
3.1.5	Sodium Dodecyl Sulfate Polyacrylamide Gel Electrophoresis (SDS PAGE)	46
3.2	Methods	
3.2.1	Preparation of feedstock	47
3.2.2	Halozone detection for CGTase growth on iodine flooded plates	47
3.2.3	Preparation of homogenate	48
3.2.4	Buffer preparation	48
3.2.5	Static binding capacity using an adsorption isotherm model for CGTase	49
3.2.6	Dynamic binding capacity (DBC) for CGTase	49
3.2.7	Purification of recombinant CGTase from clarified <i>E.coli</i> homogenate in a packed bed adsorption chromatography column	50
3.2.8	Analytical procedures	50
<b>4</b>	<b>ASSESSMENT OF MIXED MODE ADSORBENT FOR THE PURIFICATION OF RECOMBINANT PROTEIN USING COLUMN ADSORPTION CHROMATOGRAPHY</b>	<b>53</b>
4.1	Introduction	53
4.2	Material and Methods	54
4.2.1	Culture conditions of CGTase	54
4.2.2	Halozone detection for CGTase growth on starch plates	54
4.2.3	Evaluation of the buffer exchange step using SnakeSkin dialysis tubing and regular dialysis tubing for pre concentration performance	54
4.2.4	Ammonium sulphate precipitation of the extracellular CGTase	54
4.2.5	Screening of washing and elution buffers for CGTase purification using HEA and PPA HyperCel resins	55
4.2.6	Static binding capacity of CGTase onto HEA and PPA HyperCel using an adsorption isotherm model	56
4.2.7	Preparation of chromatography column and evaluation of column performance	57
4.2.8	Dynamic binding capacity for CGTase onto mixed mode adsorbents, PPA and HEA HyperCel using frontal analysis	57
4.2.9	Purification of CGTase via packed bed adsorption chromatography using mixed mode resins	58
4.2.10	Analytical procedures	58
4.3	Results and Discussion	

4.3.1	CGTase homogenate preparation	59
4.3.2	CGTase enzyme concentration approaches	60
4.3.3	Buffer formulation for the adsorption of CGTase onto PPA and HEA HyperCel	62
4.3.4	Buffer Formulation for desorption of CGTase from HEA and PPA HyperCel adsorbents	65
4.3.5	Static binding capacity of CGTase from <i>E.coli</i> homogenate using an adsorption isotherm analysis	69
4.3.6	Tricorn 10/50 column performance packed with HEA and PPA HyperCel	70
4.3.7	Dynamic binding capacity of CGTase onto mixed mode resins via column adsorption chromatography	71
4.3.8	Purification of CGTase from <i>E.coli</i> homogenate using HEA and PPA HyperCel resin loaded in a packed bed adsorption column chromatography	72
4.4	Concluding remarks on the efficiency of mixed mode adsorbent, HEA and PPA HyperCel	77
<b>5</b>	<b>CGTase PURIFICATION USING A CONVENTIONAL ION-EXCHANGE CHROMATOGRAPHY (IEC) TECHNIQUE</b>	<b>78</b>
5.1	Introduction	78
5.2	Materials and Methods	79
5.2.1	Organism and culture conditions of CGTase	79
5.2.2	Pre concentration of CGTase using SnakeSkin dialysis tubing	80
5.2.3	Adsorbent used for the column purification of CGTase	80
5.2.4	Screening of washing and elution buffers for CGTase purification using DEAE Sepharose resin	80
5.2.5	Static binding capacity of CGTase onto DEAE Sepharose using an adsorption isotherm model	82
5.2.6	Dynamic binding capacity for CGTase onto ion exchange adsorbent, DEAE Sepharose via frontal analysis	82
5.2.7	Purification of CGTase via packed bed adsorption chromatography using DEAE Sepharose	82
5.2.8	Analytical procedure	80
5.3	Results and Discussion	
5.3.1	Buffer formulation for the adsorption of CGTase onto DEAE Sepharose	80
5.3.2	Buffer formulation for the elution of CGTase from DEAE Sepharose	84
5.3.3	Static binding capacity of CGTase from <i>E.coli</i> homogenate using an adsorption isotherm analysis	84

5.3.4	Dynamic binding capacity for CGTase onto DEAE Sepharose via column adsorption chromatography	86
5.3.5	Purification of CGTase from <i>E.coli</i> homogenate using DEAE Sepharose resin loaded in a packed bed adsorption column chromatography	87
5.4	Conclusion	91

## 6 COLUMN PURIFICATION OF CGTase VIA AFFINITY CHROMATOGRAPHY (AF)

6.1	Introduction	92
6.2	Materials and Methods	94
6.2.1	Organism and Culture Conditions of CGTase	94
6.2.2	Pre concentration of CGTase from <i>E.coli</i> feedstock via SnakeSkin dialysis tubing	94
6.2.3	Preparation of Ni <sup>2+</sup> Loaded Sepharose chelating	
6.2.4	Column preparation	94
6.2.5	Screening of washing and elution buffers for CGTase purification via IMAC	95
6.2.6	Static binding capacity of CGTase onto Ni <sup>2+</sup> -Sepharose IMAC resin using an adsorption isotherm model	96
6.2.7	Dynamic binding capacity of CGTase onto Ni <sup>2+</sup> -Sepharose IMAC resin	97
6.2.8	Column purification of CGTase via packed bed adsorption approach using Ni <sup>2+</sup> -Sepharose IMAC resin	97
6.2.9	Analytical procedure	97
6.3	Results and Discussion	
6.3.1	E-L-W buffer formulation for the adsorption of CGTase onto Ni <sup>2+</sup> -Sepharose	97
6.3.2	Elution buffer formulation for the desorption of CGTase from Ni <sup>2+</sup> -Sepharose	100
6.3.3	Static binding capacity of CGTase from <i>E.coli</i> homogenate onto the Ni <sup>2+</sup> -Sepharose IMAC resin using an adsorption isotherm analysis	101
6.3.4	Dynamic binding capacity (DBC) for CGTase onto Ni <sup>2+</sup> -Sepharose IMAC resins via column adsorption chromatography	103
6.3.5	Purification of CGTase from <i>E.coli</i> homogenate using Ni <sup>2+</sup> -Sepharose IMAC resin loaded in a packed bed adsorption column chromatography	103
6.4	Conclusion	110

## 7 GENERAL DISCUSSION, CONCLUSIONS AND SUGGESTIONS FOR FURTHER WORK

7.1	Introduction	111
7.2	Discussion	111
7.2.1	Comparison of Langmuir values for different	

	chromatography resins	111
7.2.2	Comparison of dynamic binding capacity values of different chromatography resins	113
7.2.3	Comparison of various purification strategies of CGTase	114
7.3	Conclusion and recommendation for future research	118
7.3.1	Conclusion	118
7.4	Recommendations for future research	118

<b>REFERENCES</b>	<b>120</b>
<b>APPENDICES</b>	<b>149</b>
<b>BIODATA OF STUDENT</b>	<b>153</b>
<b>LIST OF PUBLICATION</b>	<b>154</b>





## LIST OF TABLES

<b>Table</b>	<b>Page</b>
2.1 Examples of mechanical and non-mechanical cell disruption methods	5
2.2 Mechanisms of cell disruption methods for the release of intracellular proteins	6
2.3 Examples of ionic and non-ionic protein precipitation techniques	8
2.4 Extracellular protein precipitation techniques	8
2.5 DBC values of various commercial chromatographic resins commonly used for the purification of proteins	16
2.6 Properties of CGTase from various producers	34
2.7 Purification and pre purification methods employed for the recovery of CGTase	40
3.1 Block diagram of research work	52
4.1 Pre purification of the enzyme CGTase using various techniques	61
4.2(A) Washing buffer parameters tested for PPA HyperCel (PBS: Sodium Phosphate Buffer), SAB: Sodium Acetate Buffer, SCA: Sodium Citrate Buffer	63
4.2(B) Washing buffer parameters tested for HEA HyperCel (PBS: Sodium Phosphate Buffer), SAB: Sodium Acetate Buffer, SCA: Sodium Citrate Buffer)	64
4.3 Elution buffer parameters tested for both ligands (SAB: Sodium Acetate Buffer, SCA: Sodium Citrate Buffer)	67
4.4 Evaluation of column packing performance, number of plates per meter (N/m), height equivalent to a theoretical plate (HETP) and asymmetry factor (AF)	71
4.5 Purification table for CGTase recovery using PPA HyperCel	74
4.6 Purification table for CGTase recovery using HEA HyperCel	77
5.1 Washing buffer parameters tested for DEAE Sepharose	84
5.2 Elution buffer parameters tested for DEAE Sepharose	85
5.3 Purification table for CGTase recovery using DEAE Sepharose	88
6.1 Washing buffer parameters tested for Ni <sup>2+</sup> -Sepharose	98
6.2 Elution buffer parameters tested for Ni <sup>2+</sup> -Sepharose	101
6.3 Purification table for CGTase using Ni <sup>2+</sup> -Sepharose IMAC resin via Strategy A	105
6.4 Purification table for CGTase using Ni <sup>2+</sup> -Sepharose IMAC resin via Strategy B	107
6.5 Purification table for CGTase using Ni <sup>2+</sup> -Sepharose IMAC resin via Strategy C	110
7.1 Comparison of static binding results using a Langmuir approach	113
7.2 Comparison of dynamic binding capacity values	114
7.3 Comparison of parameters for various purification strategies of CGTase	117

## LIST OF FIGURES

Figure	Page
2.1 Breakthrough curve for the adsorption of protein from suspension	14
2.2 Principle of anion and cation exchanger	22
2.3 Principle of hydrophobic interaction chromatography	23
2.4 Principle of RPC	24
2.5 Schematic representation of a size exclusion column	25
2.6 Schematic operation of antibody-antigen affinity binding	27
2.7 Schematic mechanism of a type mixed mode adsorbent (Adapted from Pall Life Science)	28
2.8 Difference between the packed bed and expanded bed mode of operation (Adapted from Chase, 1994)	30
2.9 (a) Structural representation of wild type CGTase from <i>Bacillus Circulans</i> [EC:2.4.1.19] coloured differently to represent the five Domains (A-E) (b) Structure of the three main types of cyclodextrins as a product of intramolecular transglycosylation CGTase on starch (Adapted from Tachibana et al., 1999)	32
2.10 Representation of CGTase G1. Green represents the 22 amino acids, magenta; catalytic residues, orange; substrate (starch), blue dots; calcium binding sites, Domain A is represented by the grey ribbon structures (Adapted and edited from Goh et al., 2008)	37
4.1 <i>rE.coli</i> harbouring the <i>Bacillus</i> sp. G1 insert	60
4.2 Growth Curve of <i>E.coli</i> cell culture showing CGTase expression profile after IPTG induction at 5th hour	60
4.3 Graph of experimental data of equilibrium isotherm of CGTase onto HEA and PPA HyperCel and the least square fit to the Langmuir equation	69
4.4 DBC of CGTase onto PPA and HEA HyperCel in column adsorption chromatography	72
4.5 Chromatogram of CGTase separation via PPA HyperCel at 1mL/min Buffers used: equilibration buffer: 100 mM sodium phosphate buffer pH 8, washing buffer 100 mM sodium phosphate buffer pH 8, step elution 100 mM sodium acetate step pH 5-3. Column regeneration with 1 M NaOH.	75
4.6 Chromatogram of CGTase separation via HEA HyperCel at 1mL/min. Buffers used: equilibration buffer: 100 mM sodium phosphate buffer pH 7, washing buffer 100 mM sodium phosphate buffer pH 7, 100 mM sodium citrate buffer pH 5-3 gradient elution. Column regeneration with 1M NaOH	76
5.1 Graph of experimental data of equilibrium isotherm of CGTase onto DEAE Sepharose and the least square fit to the Langmuir equation	86

5.2	DBC of CGTase onto DEAE Sepharose in column adsorption chromatography	87
5.3	Chromatogram of CGTase separation via DEAE Sepharose at 1mL/min. Buffers used: equilibration buffer: 20 mM Tris-HCl pH7, washing buffer 20 mM Tris-HCl pH7, elution buffer: 20 mM Tris-HCl, 1 M NaCl, pH7 (0-1 M) gradient elution. Column regeneration with 1M NaOH	90
6.1	Graph of experimental data of equilibrium isotherm of CGTase onto to Ni <sup>2+</sup> -Sepharose IMAC adsorbent and the least square fit to the Langmuir equation.	102
6.2	Breakthrough curve of CGTase onto the Ni <sup>2+</sup> -Sepharose IMAC resin	103
6.3	Chromatogram of CGTase separation via Ni <sup>2+</sup> -Sepharose IMAC resin at 1mL/min. Buffers used: equilibration buffer: 20 mM sodium phosphate pH 7 washing buffer: 20 mM sodium phosphate buffer pH7, gradient elution 20 mM sodium phosphate, 50mM EDTA pH 7.	105
6.4	Chromatogram of CGTase separation via Ni <sup>2+</sup> IMAC resin at 1mL/min. Buffers used: equilibration buffer: 20 mM sodium phosphate, pH 7 washing buffer: 20 mM sodium phosphate buffer pH 7, gradient elution 20 mM sodium phosphate, 0.1 M Imidazole, pH 7	107
6.5	Chromatogram of CGTase separation via Ni <sup>2+</sup> IMAC resin at 1mL/min. Buffers used: equilibration buffer: 20 mM sodium phosphate, pH 7 washing buffer: 20 mM sodium phosphate buffer pH 7, single step elution 20 mM sodium phosphate, 45 mM Imidazole, pH 7.	109
7.1	DBC of CGTase onto various adsorbents in column adsorption chromatography	114
A	CGTase Standard Curve	150

## LIST OF APPENDICES

Appendix		Page
A	CGTase enzyme assay	149
B	SDS PAGE	151



## LIST OF ABBREVIATIONS

BSA	bovine serum albumin
CIP	cleaning-in-place
EBA	expanded bed adsorption
HEA	hexylamine
FBA	fluidized bed adsorption
PBA	packed bed adsorption
PPA	phenylpropylamine
IEC	ion exchange chromatography
HIC	hydrophobic interaction chromatography
AC	affinity chromatography
SEC	size exclusion chromatography
RPC	reversed phase chromatography
MMC	mixed-mode chromatography
IgG	immunoglobulin G
MW	molecular weight
IMAC	immobilized metal affinity chromatography
BPER	Bacterial Protein Extraction Reagent
MWCO	Molecular weight cut off
$q^*$	concentration of the adsorbent phase to the adsorbent per unit volume of settled adsorbent
$q_m$	maximum adsorption capacity of adsorbent
$C^*$	equilibrium concentration of protein in bulk solution
$K_d$	dissociation constant for the mixture with the adsorbent.
$K$	Constant, refers to the capacity of the adsorbent for the adsorbate
$1/n$	Constant, measures the strength of adsorption
$x$	mass of adsorbate
$m$	mass of adsorbent
$p$	the equilibrium pressure of adsorbate
$v$	volume of gas adsorbed at STP (0°C, 760 mmHg)
$c$	constant related to the heat of adsorption
$v_m$	volume of monomolecular layer of gas adsorbed at STP
$P_o$	vapor pressure of adsorbate at test temperature
$C_{UO}$	initial solute concentration in the feed solution
$C_{BO}$	initial solute concentration in the adsorbent
$S$	quantity of feed solution
$A$	quantity of adsorbent
$N$	number of theoretical plate
$t_R$	retention time
$\sigma_t$	standard deviation of chromatographic peak
$d$	peak width at half height expressed in units of time, volume or measured distance on chromatogram
$L$	column length (in units of cm)
$t$	retention value of acetone or NaCl peak expressed in volume, time or measured distance on chromatogram
$N$	number of theoretical plates
$t_R$	retention time

- $w_h$  peak width at half height (in units of time)  
a the distance from the leading edge of the peak to the mid-point of the peak  
b the distance from the mid-point of the peak to the trailing edge



# CHAPTER 1

## INTRODUCTION

### 1.1 Background Study

Product recovery involves processing steps in which product such as proteins are captured, concentrated and purified from biological feedstock such as bacteria, yeast, fungal or mammalian cells culture. Purifying protein is often a complicated task due to proteins' heterogeneity, instability and complexity, in particular when not in their native environment. For process engineers, the challenges are not only associated with the task to recover protein in its active form, but also to achieve high yields that are expressed intrinsically at low concentration of feedstock containing many components of host organism and culture medium. This challenge is addressed in different approaches, such as the use of multi-steps process and integration of two or more techniques. For example, combining clarification steps (involving centrifugation and filtration) followed by product concentration steps (via ultrafiltration/diafiltration) and finally purification step, achieved typically via forms of chromatography techniques.

In this present study, a protein called cyclodextrin glucanotransferase (CGTase) is used. CGTase belongs to the  $\alpha$ -amylase enzyme family which catalyzes the degradation of starch via cleavage of  $\alpha$ -1,4-glycosidic bonds to form saccharides such as maltose, glucose and cyclodextrin (CD). With the increasing interest and application of cyclodextrin- the product of CGTase catalyzed reaction, there are great demands for its production for food and biotechnology industries at large. Hence creating a demand for the production of CGTase at a reasonable, economic value. CGTase is expressed natively as extracellular metabolites by variety of alkalophilic, mesophilic and thermophilic *Bacillus* genus bacteria (Letsididi et al., 2011; Alves-Prado et al., 2007). The cloning of CGTase gens into bacterial expressing host has been made in recent years, from which its expression and stability was improved significantly (Tesfai et al., 2012; Kweon et al., 2004).

### 1.2 Problem statement

The current strategy for the purification of CGTase incorporates a many-step procedure that is tedious and time-consuming. Typically, cascades of unit operations involving precipitation, filtration and different mode of adsorption chromatography are employed (Mirka et al., 2012; Savergave et al., 2008). It has been estimated that the overall cost of downstream processing is closely correlated to the number of purification steps employed (Spalding, 1991) and in fact, it represents the most significant expense in protein manufacturing by accounting for 40-65% total manufacturing cost (Orr et al.,

2012). Hence it is essential for the development of purification strategies tailor-made for CGTase, aiming at maximizing the yield, maintaining its biological properties, while minimizing the time and cost of production without compromising the final product purity.

The general approach for any protein purification is usually via exploitation of their physicochemical differences and interactions in charge, hydrophobicity, size or affinity with different separation technique employed (Kweon et al., 2004). The use of combination of more than one type of interaction, also known as mixed-mode has also been used in the past. The fundamental understanding of these interactions is necessary for the development of protein purification with a good industrial compliance. This includes investigation on the static adsorption and desorption behavior with the adsorbents of choice, dynamic behavior during protein loading, washing and elution in the column operation as well as the product integrity (activity, purity and yield).

### **1.3 Research objectives**

The research objectives are listed as follows;

- i) To develop a mixed mode chromatographic process for CGTase recovery.
- ii) To develop an ion exchange chromatographic process for CGTase recovery.
- iii) To develop an affinity chromatographic process for CGTase recovery.
- iv) To compare and select the most suitable chromatographic process for CGTase recovery.

### **1.4 Thesis Layout and Research Strategy**

The thesis is organized into eight chapters which conclude with the conclusion and recommendations for future research. This chapter (Chapter 1) highlights the background study of the current purification phenomenon, the problem statements and research objectives. Chapter 2 reviews the background of protein purification, purification and pre-purification strategies as well as various modes of adsorption chromatography. Also thoroughly reviewed are the enzyme CGTase, its origin, sources, applications and current purification strategies which are currently employed. Chapter 3 introduces general methodology used throughout the study. Chapter 4 includes purification of CGTase using mixed mode ligands upon which its suitability was tested with buffer optimizations and column adsorption conditions. Chapter 5 focuses on the purification of CGTase using affinity chromatography method in which a pseudo-type affinity (immobilized metal affinity chromatography) was assessed in its suitability to purify the protein CGTase. Chapter 6 investigates the efficiency of an anion exchanger to stand as a one-step chromatography purification scheme for CGTase recovery. Chapter 7 ties all methods together and concludes the efficiency of all the methods as a



one-step chromatography technique for the successful purification of the enzyme CGTase.



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## LIST OF PUBLICATION

- 1) "Cell disruption strategies for the release of intracellular Glutathione S-Transferase (GST) from *E.coli* homogenate" - Proceeding in National Symposium of Fermentation Technology 2009, UniKL, (MiCET), Melaka
- 2) Sivapragasam, M. & Abdullah, N. (2014) "Purification of Glutathione S-transferase using mixed mode chromatography", February, vol. 3 issue 2, International Journal of Engineering Research and Technology.

