

# **UNIVERSITI PUTRA MALAYSIA**

CHEMICAL OXYGEN DEMAND REMOVAL USING ARTIFICIALLY CONSTRUCTED BIOFILM BY DIELECTROPHORESIS ON WIRECLOTH ELECTRODE

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By

WAI YORK CHOW

Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in Fulfilment of the Requirements for the Degree of Master of Science.

**June 2014** 

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Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfilment of the requirement for the degree of Master of Science.

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#### WAI YORK CHOW

**June 2014** 

#### Chairman: Associate Prof. Zurina Zainal Abidin, PhD

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Artificial structured biofilm constructed (ASB) by dielectrophoresis (DEP) principle using wirecloth electrode was explored for its potential in wastewater treatment. The wirecloth produced by adopting textile technology, utilised 100 µm stainless steel wire and 83 decitex polyester yarns. The wirecloth is highly flexible and able to be fixed in most treatment system. The ASB was then immobilized using polyethylenimine (PEI) solution. The biofilm formation time was greatly shortened as the DEP attraction can result in an effective immobilization process. Micrococcus sp., Rhodococcus sp. and Bacillus sp. isolated from pharmaceutical wastewater was used. A lab scale reactor was used to determine the optimum conditions and the ability of DEP-constructed biofilm in wastewater treatment. The experiment parameters included wirecloth surface area, pH, temperature and HRT. 2 types of medium; low strength and high strength synthetic wastewater were used in the experiments. The treatment process showed a good potential in treating both type of synthetic wastewater where almost 90% COD reduction was achieved at the optimum conditions for each parameter. The larger the wirecloth surface area used the better the COD reduction can be achieved. The restriction may only cause by insufficient of nutrient in a given medium's volume. The performance of the artificial biofilm was dependent on the pH value. The optimum pH value for both mediums was found to be pH 8. Lower pH and higher pH value tend to inhibit the activity of microorganisms and decrease the COD reduction to 62.4% in low strength and 75.1% in high strength synthetic wastewater, respectively. The best temperature chosen was 40 °C. This is due to higher COD removal rate achieved and the COD reduction was nearly 90% for both mediums. The suitable HRT for low strength synthetic wastewater are around 1 to 3 days and the HRT for high strength synthetic wastewater was 4 to 7 days. As the COD value was higher, shorter retention time will result in an incomplete treatment where COD reduction was just 56.3%. The built up of artificial biofilm (increase of active biomass) can eventually shorten the treatment time which shown in the experiment results of HRT. ESEM and SEM images revealed the surface morphology

of ASB. The layers of EPS proved to be interconnected and support the nutrient diffussion and the build up of microcolonies for a better COD removal.



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#### PENGYINGKIRAN PERMINTAAN OKSIGEN KIMIA (COD) DENGAN MENGGUNAKAN KONSTRUKSI BIOFILEM BUATAN YANG DIBINA DARIPADA PROSES DEP PADA TENUNAN KAIN WAYAR

Oleh

#### WAI YORK CHOW

**Jun 2014** 

#### Pengerusi: Professor Madya Zurina Zainal Abidin, PhD

Fakulti Kejuruteraan

Biofilem berstruktur tiruan (ASB) dibina dengan prinsip dielectrophoresis (DEP) dengan menggunakan kain tenunan wayar telah diterokai untuk mengetahui potensinya dalam rawatan air sisa. Cara in dapat dicapai dengan menyekat gerakan mikroorganisma tertentu pada kain tenunan wayar dan memulakan proses pembentukan biofilem buatan. Kain tenunan wayar ini dihasilkan oleh teknologi tekstil dengan menggunakan wayar berdiameter 100 µm dan benang poliester 83 desiteks. Kain tenunan wayar ini sangat fleksibel dan dapat digunakan dalam kebanyakan sistem rawatan. Seterusnya, penyekatan gerakan mikroorganisma dapat dihasil dengan menggunakan polyethylenimine (PEI). Masa pembentukan biofilem dapat dikurangkan dengan ketara kerana tarikan DEP dapat menghasilkan proses penyekatan yang lebih sempurna. Mikroorganisma yang tumbuh dalam air sisa farmaseutikal telah diasingkan dengan kaedah mengkultur dan dikenal pasti sebagai Micrococcus sp., Rhodococcus sp. dan Bacillus sp. Sebuah reactor yang berskala makmal telah dibina untuk menentukan keadaan yang optima dan keupayaan biofilem konstruksi-DEP semasa rawatan. Parameter eksperimen termasuk luas kawasan permukaan, pH, suhu dan HRT. Perantara yang digunakan dalam eksperimen ini ialah sisa kumbahan sintetik kekuatan tinggi dan kekuatan rendah. Proses rawatan menunjukkan potensi yang baik semasa merawat kedua-dua jenis air sisa sintetik di mana hampir 90% pengurangan COD dapat dicapai bagi keadaan-keadaan optimum dalam setiap parameter. Kawasan permukaan kain tenunan wayar yang lebih besar adalah lebih berkesan dalam rawatan air sisa sintetik. Sebab ini adalah tidak benar apabila tiada nutrien yang mencukupi dalam air sisa sintetik tersebut. Nilai pH yang optima bagi kedua-dua medium adalah pH 8. pH yang rendah dan pH yang tinggi dapat menghalang aktiviti mikroorganisma dan mengurangkan COD kepada 62.4% dalam air sisa sintetik berkekuatan rendah dan 75.1% dalam air sintetik berkekuatan tinggi. Suhu terbaik yang dipilih adalah 40 ℃. Ini adalah kerana kadar keturunan COD yang lebih tinggi dan pengurangan COD dicapai pada hampir 90% bagi keduadua medium. Dalam parameter HRT, masa yang sesuai untuk air sisa sintetik

berkekuatan rendah adalah sekitar 1 hingga 3 hari, dan HRT untuk air sisa sintetik berkekuatan tinggi adalah 4 hingga 7 hari. COD yang tinggi dan masa penahanan yang pendek akan menyebabkan rawatan yang tidak lengkap di mana hanya 56.3% COD dapat disinkirkan. Pembinaan biofilem tiruan (peningkatan biomas aktif) boleh memendekkan masa rawatan seperti mana yang ditunjukkan dalam keputusan eksperimen HRT. Imej daripada ESEM dan SEM mendedahkan morfologi permukaan biofilm buatan dengan DEP proses. Lapisan EPS adalah saling bergabung dan dapat menyokong diffussi nutrien dan membina microcolonies dengan lebih baik serta meningkakan kecekapan rawatan air sisa.



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I certify that a Thesis Examination Committee has met on [date] to conduct the final examination of Wai York Chow on his thesis entitled "Chemical Oxygen Demand Removal Using Artificially Constructed Biofilm by Dielectrophoresis on Wirecloth Electrode" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U.(A) 106] 15 March 1998. The committee recommends that the student be awarded the degree of Master of Science.

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# LIST OF ABBREVIATIONS

ω	Angular Frequency
$\Delta E^2$	Square of the Electric Field Gradient
ASB	Artificial Structured Biofilm
ASMC	Artificial Structured Microbial Consortia
BOD	Biochemical Oxygen Demand
COD	Chemical Oxygen Demand
CSLM	Confocal Scanning Laser Microscopy
DEP	Dielectrophoresis
EPS	Extracellular polymeric substances
ESEM	Environment Scanning Electron Microscope
ε	Permittivity
ε <sub>m</sub>	Medium's conductivity
εο	Free Space Permittivity
FEMLAB	Comsol Multiphysics
GDD	Gaseous Detection Device
HRT	Hydraulic Retention Time
OD	Optical Density
ORP	Oxidation Reduction Potential
PEI	Polyethylenimine
pk-pk	Peak to Peak
r	Radius
$R_e(f_{cm})$	Clausius-Mossotti Factor
r <sub>o</sub>	Radius Vector
SA	Surface Area
SEM	Scanning Electron Microscope

SS	Suspended Solids
TDS	Total Dissolved Substance
TOC	Total Organic Carbon
TSS	Total Suspended Solid
V	Potential
VOC	Volatile Organic Compounds
VSS	Volatile Suspended Substance
α	Particle's Efective Polarisability

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#### **CHAPTER 1**

#### **INTRODUCTION**

#### 1.1 Background

Water is one of the most important elements to support almost all of the living creatures, hence, wastewater treatment has become a crucial topic which gains attention from human beings. Water contamination has become a major issue in the global context as a result of globalization, population growth, urbanization, industrialization and more extravagant life.

Due to increasing industrial activity from all over the world, discharging of untreated wastewater has become a significant issue. The wastewater effluent can pollute surface, and underground water and soil. Hence, the discharging of produced water on environment has become a crucial challenge that need to be solved immediately. The impacts of wastewater need to be reduced and this results in a more stringent regulatory standard for discharging wastewater. In Malaysia, national water quality standards can be divided to 5 classes and the value of some parameters such as COD, BOD, pH, TDS are strictly controlled before the wastewater can be discharged into the river (Environmental Quality Reports, 2011). For example, discharging limit of COD and BOD in class IIA are 25 and 3 mg/L.

Environmental microbiology can be related to the studies of municipal waste treatment and waste degradation and during the last ten years biofilms have become an important subject in microbiological inquiry. This can be considered as a critical element in the preservation of water quality systems as well as a key component of biological reactions in wastewater treatment (Flemming et al., 2000). Many natural and engineered systems are influenced by biofilms such as microorganisms firmly attached to surfaces (Lewandowski and Beyenal, 2007). The effects of biofilms may be vary from desirable, through undesirable, even to a bad situation, depending on the specific locations where the biofilms are deposited (International Water Assn, 2008).

One of the significant elements in biofilms is naturally occurred microbial consortia where it is used widely in industry, for example in wastewater treatment, bioremediation, metal leaching, silage production and various food fermentations (Rebac et al., 1995; James, 1993). Biofilm treatment process can act as a safer biological control method when we compare to a chemically modification method (Woolard, 1997). Microbial consortia in nature tend to exist in highly organized macroscopic structures with extensive internal organization where the macroscopic structuring also provides protection against exogenous toxic substrates (Alp et al., 2002).

To treat wastewater using biofilms, different methods have been studied including aerobic submerged biofilm (Gonz aez-Mart nez and Duque-Luciano, 1992),

multistage biofilm reactors (Ghaniyari-Benis et al., 2009), immobilization of bacteria (Li et al., 2013), and biofilm hybrid system (Qi et al., 2007). Most of the biofilm formations are time dependent and require a suitable amount of nutrients to initiate the growth. However, a better and more efficient wastewater treatment method should be developed in order to turn those disadvantages into benefits.

#### **1.2 Problem statement**

Severe waterborne diseases such as cholera and typhoid fever were discovered and spread through contaminated water (Yates et al., 2004). This posed a threat to human beings which greatly increased the environmental attention and resulted in the construction of sewer system as well as the needs of wastewater treatment. The emerging knowledge of wastewater treatment resulted in the development of many new treatment methods include anaerobic digestion, trickling filter, biological treatment and etc. (Metcalf et al., 1979). Despite recent studies advance in wastewater treatment, the development of new and better method is still a big concern. In this study, a new method of artificial constructed biofilm using DEP is able to open a new chapter in wastewater treatment process.

In previous studies, some problems occurred while using DEP processes such as the difficulties in producing large surface area microelectrodes and the electrodes are less flexible to fix in selected treatment system. From the development of a novel microelectrode by using weaving technology (Abidin et al., 2007), the application of DEP can be further developed such as the construction of biofilm in wastewater treatment. Biofilm is a biological treatment method which is environmental friendly and efficient. This method can significantly reduce the chemical usage that needed by other wastewater treatment methods.

Time is an important parameter in biological fix-film treatment system as natural biofilm takes time to develop; i.e. a few weeks or even months need to be used to develop biofilm which also means a higher preparation cost. However, the construction of biofilm using DEP technique can provide a better and faster way of biofilm formation which significantly reduces the waiting time of natural biofilm formation. This is because the DEP technique can efficiently attract the microorganisms on the wirecloth electrode and form an effective bonding after the immobilization process.

The flexibility of biofilm's attached medium is always a great concern as the treatment tank varies in different sizes. Wirecloth constructed using weaving technology enables one to fold it into various type of shape in order to fix in required pattern. The additional advantage of using wirecloth is that it provides a larger surface area which also theoretically means a higher active biomass generation in biofilm construction. During wastewater treatment, greater treatment efficiency can be achieved if the active biomass (biofilm) is higher. The flexibility is due to the elasticity of polyester yarns and the larger surface area is generated by using weaved microelectrodes.

In order to treat wastewater, the removal of organic and inorganic constituents is needed. Suitable parameter should be chosen in order to determine the wastewater treatment efficiency. The value of COD and BOD has been used as an important indicator to show the evidence for biodegradability. There are several factors that limit the biodegradation process, including nutrient availability and chemical composition of selected wastewater (Metcalf et al., 1979). Biodegradation patterns can fluctuate over the long term. Sometimes the value of COD and BOD might fall within certain limits, then suddenly spike up again (Leeson and Hinchee, 1997).

Due to the rising concern about environmental issues, stringent effluent limitations have been set up to control wastewater treatment plants. Thus, finding a new environmental friendly in a most effective and less time consuming way which can treat wastewater efficiently is crucial in this research.

#### **1.3** Objectives of the Study

The main goal of this research is to use wirecloth as a matrix to form artificial structured biofilm (ASB) using dielectrophoresis (DEP) technique and utilized this ASB for wastewater treatment. Specific objectives of the research are listed as below:

a. To construct and morphologically characterize artificial constructed biofilm on wirecloth electrode using DEP and also immobilization.

b. To investigate and evaluate the efficiency of the immobilized constructed biofilm for COD removal of the synthetic wastewater based on different operating parameters, such as surface area of wirecloth, pH, temperature and HRT.

#### **1.4** Scope of the study

The fabrication of wirecloth electrode was done by research teammate by using weaving machine at Swiftech Sdn. Bhd. The wirecloth was weaved using polyester yarn and stainless steel wire in plain weave pattern. The diameter of stainless steel wires were 100  $\mu$ m and the diameter of polyester yarn was 83 decitex.

The selected microorganisms were separated by culture method and the microorganisms were cultured by incubating in an incubator shaker and separated using centrifugation method. Further details and method were discussed in chapter 3.

The synthetic wastewater for wastewater treatment was prepared freshly when needed. Two types of synthetic wastewater are prepared which are low strength and high strength synthetic wastewater. Whereas for artificial bioflm construction, the selected microorganisms were separated out from inoculum, mixed together and ready to use on following process. The wirecloth electrode was connected by a frequency generator and the mixed microorganisms were introduced on the surface of wirecloth. Once the frequency generator was turned on, the microorganisms were be attracted towards the wirecloth by DEP process, and forming artificial consortia which later developed into an artificial biofilm. During the immobilizing process, the attracted microorganisms were immobilized on wirecloth by using polyethylenimine (PEI). After the process was completed, the wirecloth was ready to use for wastewater treatment where the artificial biofilms develop on the wirecloth in the wastewater.

Performance and evaluation of the constructed biofilm were based on the initial and final values of COD that were calculated in order to observe the treatment efficiency. The selected parameters were, surface area, pH, temperature and HRT. After the treatment ended, the biofilm was send to Institute of Bioscience to obtain the image of ESEM and SEM.



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APPENDICES

#### Appendix A

#### Wirecloth's Gap Calculation and Reagents' Preparation

#### 1. Calculation of Gap Between Electrodes

80 picks per inch = 80 wires in inch (length og wire cloth), 79 gaps

Total 80 wires with the diameter  $71 \,\mu\text{m} = 80 \text{ x} 71 \,\mu\text{m} = 5680 \,\mu\text{m}$ 

1 inch =  $0.0254 \text{ m} = 5680 \mu\text{m} + \text{total length of gaps between electrodes}$ 

Gap between each electrode,

 $=\frac{0.0254m-0.00568m}{79}$  $=250 \times 10^{-6} \ \mu m$ 

#### 2. BOD and COD Reagent Preparation

#### **Iodine Azide Solution**

500 g of Sodium Hydroxide, NaOH + 150 g of Potassium Iodide KI + 10 g of

Sodium Azide, NaN<sub>3</sub>

Mix all and let them dissolve in 1000 ml of distilled water.

#### **Starch Indicator**

Use either an aqueous solution or soluble starch powder mixtures. To prepare an aqueous solution, dissolve 2g laboratory-grade soluble starch and 0.2g salicylic and as a preservative, in 100ml hot distilled water.

#### **Standard Sodium Thiosulfat Titrant**

Dissolve 6.205g Sodium thiosulfate  $Na_2S_2O_3.5H_2O$  in distilled water. Add 1.5 ml 6N Sodium hydroxide NaOH or 0.4 g solid NaOH and dilute to 1000ml. Standardize with bi-iodite solution, 0.0021M; Dissolve 812.4 mg Potassium hydride KH(IO<sub>3</sub>)<sub>2</sub> in distilled water and dilute to 1000ml.

#### **Manganous Sulfate Solution**

Dissolve 480g MnSO<sub>4</sub>.4H<sub>2</sub>O, 400g MnSO<sub>4</sub>.2H<sub>2</sub>O OR 364g MnSO<sub>4</sub>.H<sub>2</sub>O in distilled water, filter and dilute to 1L. The MnSO<sub>4</sub> solution should not give a colour with starch when added to an acidified potassium iodide (KI) Solution.

#### **Preparation of Dilution Water**

For 8 liter distilled water

8ml Magnesium Sulphate, MgSO<sub>4</sub>.7H<sub>2</sub>O

8ml Calcium Chloride, CaCl<sub>2</sub>

8ml Ferum Chloride, FeCl<sub>3</sub>.6H<sub>2</sub>O

8ml Phosphate buffer solution

Aerate the dilution water for minimum 8 hours.

#### Preparation:

- a. MgSO<sub>4</sub>.7H<sub>2</sub>O (Manganese sulfate solution)
- Dissolve 22.5g MgSO<sub>4</sub>.7H<sub>2</sub>0 in distilled water and dilute until 1 liter.
- b. CaCl<sub>2</sub> (Calcium chloride solution)
   Dissolve 27.5g CaCl<sub>2</sub> in distilled water and dilute to 1 liter.
- c. FeCl<sub>3</sub>.6H<sub>2</sub>O (Ferric chloride solution)
  - Dissolve 0.25g FeCl<sub>3</sub>.6H<sub>2</sub>O in distilled water and dilute to 1 liter.
- d. Phosphate buffer solution

Dissolve

8.5g	$KH_2PO_4$
21.75g	$K_2HPO_4$
33.4g	Na <sub>2</sub> .HPO <sub>4</sub> .7H <sub>2</sub> O
1.7g	NH <sub>4</sub> Cl

For Phosphate buffer solution, dissolve all in 500 ml of distilled water.

#### **Preparation of Sulfuric Acid Reagent**

Dissolve 5.5g of Argentum Sulphate, AgSO<sub>4</sub> in each kg of concentrate sulphuric acid.

This means, 1000g H<sub>2</sub>SO<sub>4</sub> will need to use 5.5g Silver Sulphate.

In standard solution of  $H_2SO_4$ , 1L = 1000kg

So, for 1.84kg H<sub>2</sub>SO<sub>4</sub>, use =  $1.84/1 \ge 5.5$ g AgSO<sub>4</sub>

 $= 10.12 \text{g AgSO}_4$ 

So, 10.12g AgSO<sub>4</sub> in 1L H2SO4 (concentrate)

#### Preparation of Standard Ferrous Ammonium Sulfate Titrant (FAS) (0.10M)

Dissolve 39.2g Ferrous Ammonium Sulfate,  $Fe(NH_4)_2(SO_4)_2.6H_2O$  in distilled water.

Add 20ml concentrated H<sub>2</sub>SO<sub>4</sub>, Cool and dilute to 1000ml.

Standardize solution daily against standard K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> digestion solution as follow:

-Pipette 5ml digestion solution into a small beaker.

-Add 10ml reagent water to substitute for sample.

-Cool to room temperature

-Add 1 to 2 drops diluted ferroin indicator and titrate with FAS titrant.

#### Preparation of Standard Potassium Dichromate Digestion Solution 0.01667M

Add 500ml distilled water to 4.903g K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub> (primary standard grade), which dried at 150 °C for 2 hours. Next, add in 167 ml concentration H<sub>2</sub>SO<sub>4</sub> and 33.3 g HgSO<sub>4</sub>. Dissolve, cool to room temperature and dilute to 1000ml.

# Appendix B

## **COD Profiles**

Set	Avg. used FAS, ml	COD value, mg/L
blank	1.50	246
0	0.70	246
1	0.70	246
2	0.70	246
3	0.70	246
4	0.60	276
5	0.60	276
6	0.60	276
7	0.50	307
8	0.50	307
9	0.50	307
10	0.45	323

# Table B1 Effect of PEI in COD reduction for low strength synthetic wastewater

# Table B2 Effect of PEI in COD reduction for high strength synthetic wastewater

Set	Avg. Used FAS, ml	COD value, mg/L
blank	1.50	1230
0	1.10	1230
1	1.10	1230
2	1.10	1230
3	1.10	1230
4	1.10	1230
5	1.10	1230
6	1.10	1230
7	1.10	1230
8	1.10	1230
9	1.10	1230
10	1.10	1230

Time, hrs	Type C	Type B	type A
0	0.021	0.021	0.021
3	0.085	0.055	0.055
6	0.102	0.067	0.068
9	0.244	0.102	0.092
12	0.382	0.168	0.162
15	0.487	0.214	0.283
18	0.576	0.284	0.364
21	0.674	0.316	0.451
24	0.776	0.387	0.495
27	0.871	0.445	0.525
30	0.976	0.582	0.589
33	0.988	0.684	0.647
36	0.988	0.809	0.759
39	0.986	0.818	0.874
42	0.976	0.811	0.901
45	0.978	0.828	0.911
48	0.979	0.826	0.924
51	0.956	0.821	0.928
54	0.950	0.802	0.928
57	0.945	0.791	0.928
60	0.945	0.786	0.899
63	0.943	0.779	<mark>0.8</mark> 86
66	0.940	0.775	<mark>0.8</mark> 77
69	0.937	0.770	<mark>0.</mark> 870
72	0.935	0.770	0.870

Table B3 Growth rate curve, OD600

Time,	Туре А	Туре В	Type C
days	COD removal, %	COD removal, %	COD removal, %
0	0	0	0
1	18.10	18.11	18.11
2	30.10	30.1	24.58
3	55.45	55.45	55.45
4	67.05	65.45	67.05
5	76.75	74.21	74.21
6	80.41	80.41	82.1
7	80.41	82.32	82.1
8	88.76	88.76	85.21
9	88.76	88.76	89.89
10	88.76	88.76	89.89
11	88.76	88.76	89.89
12	88.76	88.76	89.89
13	88.76	88.76	89.89
14	88.76	88.76	89.89

Table B4 Wastewater treatment ability test for selected microorganisms

Time	SA,	64 cm2	SA,	56 cm2	SA,	48 cm2	SA, 40 cm2		
dav	COD,		COD,		COD		COD		
uay	mg/L	Reduction %	mg/L	Reduction %	mg/L	Reduction %	mg/L	Reduction %	
0	237	0	237	0	237	0	237	0	
1	59	75.11	59	75.11	88	62.87	118	50.21	
2	29	87.76	29	87.76	59	75.11	88	62.87	
3	29	87.76	29	87.76	29	<mark>8</mark> 7.76	29	87.76	
4	29	87.76	29	87.76	29	87.76	29	87.76	
5	29	87.76	2 <mark>9</mark>	87.76	29	87.76	29	87.76	
6	29	87.76	29	87.76	29	87.76	29	87.76	
7	29	87.76	29	87.76	29	87.76	29	87.76	

 Table B5 Effect of SA for low strength synthetic wastewater

Time,	ne, SA, 64 cm2		SA, 5	56 cm2	SA, 4	8 cm2	SA, 40 cm2			
day	COD, mg/L	<b>Reduction %</b>	COD, mg/L	<b>Reduction %</b>	COD mg/L	<b>Reduction %</b>	COD mg/L	<b>Reduction %</b>		
0	1259	0	1259	0	1259	0	1259	0		
1	1027	18.43	1027	18.43	1173	6.83	1173	6.83		
2	880	30.10	880	30.10	1027	12.45	1173	6.83		
3	733	41.78	733	41.78	880	24.98	880	24.98		
4	586	53.45	586	53.45	586	53.45	586	53.45		
5	440	65.05	440	65.05	440	65.05	586	53.45		
6	440	65.05	440	65.05	440	65.05	440	65.05		
7	146	88.4	176	86.02	293	76.73	440	65.05		
8	117	90.7	117	90.7	293	76.73	293	76.73		
9	117	90.7	117 <mark></mark>	90.7	234	81.41	234	81.41		
10	117	90.7	117	90.7	176	86.02	205	83.72		
11	146	88.4	117	90.7	146	88.4	146	88.4		
12	117	90.7	146	88.4	146	88.4	146	88.4		
13	117	90.7	117	90.7	117	90.7	117	90.7		
14	117	90.7	117	90.7	117	90.7	117	90.7		
15	117	90.7	117	90.7	146	88.4	146	88.4		
16	117	90.7	146	88.4	117	90.7	117	90.7		
17	117	90.7	117	90.7	117	90.7	117	90.7		
18	117	90.7	117	90.7	117	90.7	117	90.7		
19	117	90.7	117	90.7	117	90.7	117	90.7		
20	117	90.7	117	90.7	117	90.7	117	90.7		
	$(\mathbf{G})$									

# Table B6 Effect of SA for low strength synthetic wastewater

	pH2 pH4		pH4		pH6	рН8		pH10		
Day	COD, mg/L	Reduction, %	COD, mg/L	Reduction, %	COD, mg/L	Reduction, %	COD, mg/L	Reduction, %	COD, mg/L	Reduction, %
0	250	0	250	0	250	0	250	0	250	0
1	250	0.00	250	0.00	250	0	109	56.4	250	0
2	250	0.00	188	24.80	125	50.00	31	87.60	220	12
3	250	0.00	156	37.60	31	87.60	31	87.60	156	37.6
4	125	50.00	94	62.40	31	87.60	62	75.20	125	50.00
5	94	62.40	94	62.40	62	75.20	31	87.60	125	50.00
6	94	62.40	62	75.20	31	87.60	31	87.60	94	62.40
7	94	62.40	31	87.60	31	87.60	31	87.60	94	62.40
8	94	62.40	31	87.60	31	87.60	31	87.60	62	75.20
9	94	62.40	31	87.60	31	87.60	31	87.60	62	75.20
10	94	62.40	31	87.60	31	87.60	31	87.60	62	75.20

# Table B7 Effect of pH for low strength synthetic wastewater

pH2		pH4		рН6		pH8		pH10		
Day	COD,		COD,		COD,		COD,		COD,	
	mg/L	Reduction, %	mg/L	Reduction, %	mg/L	<b>Reduction</b> , %	mg/L	Reduction, %	mg/L	Reduction, %
0	1207	0	1207	0	1207	0	1207	0	1207	0
1	1207	0.00	1207	0	1207	0	1207	0.00	1207	0
2	1056	12.51	1056	12.51	1056	12.51	1056	12.51	1056	12.51
3	1056	12.51	1056	12.51	754	37.53	<mark>7</mark> 54	37.53	1056	12.51
4	1056	12.51	1056	12.51	754	37.53	<mark>7</mark> 54	37.53	1056	12.51
5	1056	12.51	603	50 <mark>.04</mark>	452	62.55	301	75.06	754	37.53
6	1056	12.51	603	50 <mark>.04</mark>	452	62.55	120	90.05	603	50.04
7	1056	12.51	301	7 <mark>5.06</mark>	150	87.57	<mark>1</mark> 20	90.05	301	75.06
8	754	37.52	150	87.57	150	87.57	<mark>1</mark> 20	90.05	301	75.06
9	301	75.06	150	87 <mark>.57</mark>	120	90.05	120	90.05	301	75.06
10	301	75.06	150	87.57	150	87.57	150	87.57	301	75.06
11	301	75.06	150	87.57	120	90.05	120	90.05	301	75.06
12	301	75.06	150	87.57	120	90.05	120	90.05	301	75.06
13	301	75.06	150	87.57	120	90.05	120	90.05	301	75.06
14	301	75.06	150	87.57	120	90.05	120	90.05	301	75.06

# Table B8 Effect of pH for high strength synthetic wastewater

		26 °C	4	40 ℃	50 ℃		60 °C		70 °C	
Day	COD,	Reduction,	COD,	Reduction,	COD,	Reduction,	COD,	Reduction,	COD,	Reduction,
	mg/L	%	mg/L	%	mg/L	%	mg/L	%	mg/L	%
0	261	0	261	0	261	0	261	0	261	0
1	232	11.11	87	66.67	232	11.11	261	0	261	0
2	174	33.33	29	88.89	189	27.58	261	0	261	0
3	58	77.77	29	88.89	145	44.44	<mark>2</mark> 61	0	261	0
4	29	88.89	29	88.89	145	44.44	<b>26</b> 1	0	261	0
5	29	88.89	29	88. <mark>89</mark>	145	44.44	261	0	261	0
6	29	88.89	29	88 <mark>.89</mark>	145	44.44	261	0	261	0
7	29	88.89	29	8 <mark>8.89</mark>	145	44.44	<mark>2</mark> 61	0	261	0

# Table B9 Effect of Temperature for low strength synthetic wastewater

	26 °C 40 °C 50 °C		60 °C		70 °C					
Day	COD,		COD,		COD,		COD,		COD,	
	mg/L	Reduction, %	mg/L	<b>Reduction</b> , %	mg/L	Reduction, %	mg/L	Reduction, %	mg/L	Reduction, %
0	1305	0	1305	0	1305	0	1305	0	1305	0
1	1305	0.00	1160	11.11	1305	0	1305	0	1305	0
2	1160	11.11	870	33.33	1305	0.00	130 <mark>5</mark>	0	1305	0
3	1160	11.11	870	33.33	870	33.33	130 <mark>5</mark>	0	1305	0
4	870	33.33	586	55.56	580	55.56	<u>1305</u>	0	1305	0
5	725	44.44	435	66.6 <mark>7</mark>	870	33.33	1305	0	1305	0
6	580	55.56	290	77.7 <mark>8</mark>	580	55.56	1305	0	1305	0
7	580	55.56	145	88. <mark>89</mark>	870	33.33	1305	0	1305	0
8	290	77.78	145	88. <mark>89</mark>	580	33.33	1305	0	1305	0
9	290	77.78	145	88. <mark>89</mark>	580	55.56	<mark>130</mark> 5	0	1305	0
10	145	88.89	145	88.89	580	55.56	1305	0	1305	0
11	145	88.89	145	88.89	870	33.33	1305	0	1305	0
12	145	88.89	145	88.89	580	55.56	1305	0	1305	0
13	145	88.89	145	88.89	580	55.56	1305	0	1305	0
14	145	88.89	145	88.89	580	55.56	1305	0	1305	0
15	145	88.89	145	88.89	580	55.56	1305	0	1305	0
16	145	88.89	145	88.89	580	55.56	1305	0	1305	0
17	145	88.89	145	88.89	580	33.33	1305	0	1305	0
18	145	88.89	145	88.89	580	55.56	1305	0	1305	0
19	145	88.89	145	88.89	580	55.56	1305	0	1305	0
20	145	88.89	145	88.89	580	55.56	1305	0	1305	0
		$\bigcirc$								

# Table B10 Effect of Temperature for high strength synthetic wastewater

Time,	COD,	Reduction %
day	mg/L	Actuation, 70
0	276	0
1	123	55.43
2	61	77.89
3	30	89.13
4	30	89.13
5	30	89.13
6	30	89.13
7	30	89.13
8	30	89.13
9	30	89.13
10	30	89.13
12	30	89.13
14	30	89.13
16	30	89.13
18	30	89.13
20	30	89.13
22	30	89.13
24	30	89.13
26	30	89.13
28	30	89.13
30	30	89.13
33	30	89.13
36	61	77.89
39	30	89.13
42	30	89.13
45	61	77.89

 Table B11 Effect of HRT for low strength synthetic wastewater

	Time,	COD,	Reduction. %			
	day	mg/L	Reduction: 70			
	48	61	89.13			
	51	30	89.13			
	54	30	89.13			
	57	30	89.13			
	60	30	89.13			
	64	30	89.13			
	68	123	55.43			
	72	184	33.33			
	76	123	55.43			
	80	215	22.10			
	84	184	33.33			
	88	184	33.33			
A.	92	184	33.33			
	96	215	22.10			
4	100	123	55.43			
	105	215	22.10			
1	110	215	22.10			
1	115	<mark>18</mark> 4	33.33			
	120	<mark>24</mark> 6	10.87			
	125	<mark>2</mark> 15	22.10			
	130	184	33.33			
	135	215	22.10			
	140	123	55.43			
	145	184	33.33			
	150	215	22.10			

Time, day	COD, mg/L	Reduction, %		
0	1230	0		
3	923	24.95		
6	538	56.26		
9	461	62.52		
12	538	56.26		
15	538	56.26		
18	538	56.26		
21	538	56.26		
25	538	56.26		
29	<mark>538</mark>	56.26		
33	153	87.56		
37	153	87.56		
41	153	87.56		
45	153	87.56		
49	153	87.56		
54	153	87.56		
59	307	75.04		
64	153	87.56		

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Table B12 Effect of HRT	for high strength	synthetic wastewater

Time.	COD,	Doduction 0/
day	mg/L	Keduction, 76
69	153	87.56
74	153	87.56
79	153	87.56
84	153	87.56
90	153	87.56
96	307	75.04
102	307	75.04
108	153	87.56
114	153	87.56
120	153	87.56
126	153	87.56
133	- 307	75.04
140	307	75.04
147	153	87.56
154	307	75.04
161	153	87.56
168	153	87.56
175	153	87.56

#### **BIODATA OF STUDENT**

Wai York Chow was born in Kluang on 09<sup>th</sup> April 1988. He completed his primary education at SJK (C) Layang-Layang at the year of 2000. Thus, He furthered his secondary education at SMK Layang-Layang at where he accomplished his SPM (Sijil Pelajaran Malaysia) examination at the year of 2006. Then, he decided to take a pre-university study, STPM (Sijil Tinggi Persekolahan Malaysia) at Sekolah Tinggi Kluang. At 2009, he enrolled in the degree course of Industrial Chemistry (Honors) in Universiti Putra Malaysia (UPM), and graduated with upper second-class honours degree at 2011. At the same year, he entered his degree of Master in Science to further his postgraduate life in UPM under supervise of Assoc. Prof. Dr Zurina Zainal Abidin.



## PUBLICATIONS

## **Book Chapter (Published)**

Abidin, Z. Z., Wai, Y. C., Haffifudin, N., & Ahmadun, F. (2013). Construction of ASMC by Dielectrophoresis Using Wirecloth Electrode for the Treatment of Wastewater. In R. Pogaku, A. Bono & C. Chu (Eds.). *Developments in Sustainable Chemical and Bioprocess Technology* (pp. 65-71). Springer US.

