



**UNIVERSITI PUTRA MALAYSIA**

***PERFORMANCE OF A COMBINED SYSTEM OF ELECTROLYSIS AND  
GRANULAR ACTIVATED CARBONS FOR LEACHATE TREATMENT OF  
JERAM SANITARY LANDFILL, MALAYSIA***

**MOHAMMED RIYADH KHALEEL**

**FK 2015 38**



**PERFORMANCE OF A COMBINED SYSTEM OF ELECTROLYSIS AND  
GRANULAR ACTIVATED CARBONS FOR LEACHATE TREATMENT OF  
JERAM SANITARY LANDFILL, MALAYSIA**

**By**

**MOHAMMED RIYADH KHALEEL**

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in  
Fulfillment of the Requirements for the Degree of Master of Science**

**September 2015**

## **COPYRIGHT**

All material contained within the thesis, including without limitation text, logos, icons, photographs and all other artwork, is copyright material of Universiti Putra Malaysia unless otherwise stated. Use may be made of any material contained within the thesis for non-commercial purposes from the copyright holder. Commercial use of material may only be made with the express, prior, written permission of Universiti Putra Malaysia.

Copyright © Universiti Putra Malaysia



Abstract of the thesis presented to the senate of Universiti Putra Malaysia in fulfillment of the requirement for the degree of Master of Science.

**PERFORMANCE OF A COMBINED SYSTEM OF ELECTROLYSIS AND GRANULAR ACTIVATED CARBONS FOR LEACHATE TREATMENT OF JERAM SANITARY LANDFILL, MALAYSIA**

By

**MOHAMMED RIYADH KHALEEL**

**September 2015**

**Chairman : Amimul Ahsan, PhD**  
**Faculty : Engineering**

In this study, raw leachate collected from Jeram Sanitary Landfill (JSL) was characterized. The landfill leachate is a complex substance that contains toxic compounds, organic matter, ammonium, heavy metals and colloidal solids and a variety of pathogens potentially contaminate surface water and groundwater. The effluents are complicated to deal with and biological processes are totally inefficient for the toxic nature of stabilized leachate. Hence, there are coagulation-flocculation and adsorption process used to treat leachate. The coagulation-flocculation does by electrolysis process and adsorption by activated carbon. The raw leachate was treated using electrolysis treatment technique in which iron and stainless steel electrodes were utilized. In the electrolysis process, different voltages of 3, 6, 12, 18 and 24 volt and different retention times (RT) of 5, 10, 15, 20, 30, 40 and 50 min were used. The filtration process by quartz filter is subsequent treatment after electrolysis process. The adsorption process by using granular activated carbon (GAC) obtained from coconut shell (GACC) and oil palm shell (GACP) was final treatment after electrolysis and filtration processes. In the adsorption process, different AC dosages of 2, 4, 6, 8 and 10 g/l and different contact times (CT) of 1, 2, 3, 4, 5, 6, 8, 10 and 13 hr were used.

In electrolysis, the biochemical oxygen demand ( $BOD_5$ ) removal efficiency was 68% and the chemical oxygen demand (COD) removal efficiency of 56% was achieved using the iron electrode. Total dissolved solids (TDS) removal efficiency of 55% was obtained at 20 min RT. Optimum total suspended solids (TSS) removal efficiencies of 69 and 75% were obtained using iron and stainless steel electrodes, respectively. Salinity removal efficiency was 53% and turbidity removal efficiency was 96%. The pH value was 9.4 at 40 min RT using iron electrode. The lowest electrical conductivity (EC) value was recorded as 156 $\mu$ s/cm using iron electrode.

In adsorption process, the  $BOD_5$  removal efficiency was 95%, while the COD removal efficiency was 88%. Total nitrogen (TN) removal efficiency was recorded as 98.7%, while phosphate ( $PO_4$ ) removal efficiencies of 84 and 82% were obtained at CT of 4 (GACC) and 2 hr, (GACP) respectively. TDS removal efficiency was obtained as of 66 and 75% at 4 hr CT of GACC and GACP, respectively. Optimum TSS removal

efficiency was 90%. Salinity removal efficiencies using GACC and GACP were 81 and 74%, respectively. Turbidity removal efficiency of 95% was the highest removal efficiency recorded at 6 hr. The pH was 8.93 for both GACC and GACP. Using GACC and GACP, EC values were recorded as 102 and 83 $\mu$ s/cm, respectively.

After several combinations of voltage were used for the electrolysis process, where, 40 min RT and 24 volt were selected as the best combination for the highest removal efficiency. Also, GAC dosage of 10 g/l at 6 hr CT yielded the highest removal efficiency.

Generally, iron electrode is the cheaper and more resistant to corrosion than stainless steel. The results obtained from the iron electrode were close to stainless steel results. On the other hand, GACP is the cheaper than GACC. Also, GACP is abundantly produced in Malaysia as a biomass waste generated from agricultural activities. In conclusion, GACP can be considered a promising environmental-friendly adsorbent for the treatment of landfill leachate.

Abstrak tesis yang dikemukakan kepada senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk Ijazah Master Sains

**PRESTASI SISTEM GABUNGAN ELEKTROLISIS DAN BERBUTIR  
DIAKTIFKAN KARBON BAGI LEACHATE RAWATAN JERAM SANITARY  
TAPAK PELUPUSAN SAMPAHOLEH, MALAYSIA**

Oleh

**MOHAMMED RIYADH KHALEEL**

**September 2015**

**Pengerusi : Amimul Ahsan, PhD**  
**Fakulti : Kejuruteraan**

Dalam kajian ini, larutan resap mentah yang dikutip dari Jeram Sanitary Landfill (JSL) telah digubal. Sampel larutan resap tapak pelupusan adalah bahan kompleks yang mengandungi sebatian toksik, bahan organik, ammonium, logam berat dan pepejal koloid dan pelbagai patogen yang berpotensi mencemarkan air permukaan dan air bawah tanah. Efluen yang rumit untuk menangani dan proses biologi adalah betul-betul tidak cekap untuk sifat toksik larutan resap stabil. Oleh itu, terdapat pembekuan-pemberbukan dan proses penjerapan digunakan untuk merawat larutan resap. Pembekuan-pemberbukan tidak melalui proses elektrolisis dan penjerapan oleh karbon diaktifkan. Larutan resap mentah telah dirawat dengan menggunakan teknik rawatan elektrolisis di mana besi dan keluli tahan karat elektrod yang digunakan. Dalam proses elektrolisis, voltan yang berbeza 3, 6, 12, 18 dan 24 volt dan masa tahanan yang berbeza (RT) sebanyak 5, 10, 15, 20, 30, 40 dan 50 min telah digunakan. Proses penapisan oleh penapis kuarza adalah rawatan berikutnya selepas proses elektrolisis. Proses penjerapan dengan menggunakan karbon berbutir diaktifkan (GAC) yang diperolehi daripada tempurung kelapa (GACC) dan tempurung kelapa sawit (GACP) adalah rawatan akhir selepas elektrolisis dan penapisan proses. Dalam proses penjerapan, AC dos yang berbeza 2, 4, 6, 8 dan 10 g / l dan masa hubungan yang berbeza (CT) 1, 2, 3, 4, 5, 6, 8, 10 dan 13 jam digunakan.

Dalam elektrolisis, permintaan oksigen biokimia ( $BOD_5$ ) kecekapan penyingkiran adalah 68% dan kecekapan keperluan oksigen kimia (COD) penyingkiran 56% telah dicapai dengan menggunakan elektrod besi. Jumlah kecekapan pepejal terlarut (TDS) penyingkiran 55% telah diperolehi pada 20 min RT. Jumlah pepejal terampai Optimum (TSS) kecekapan penyingkiran 69 dan 75% telah diperolehi dengan menggunakan besi dan keluli tahan karat elektrod, masing-masing. Kecekapan penyingkiran kemasinan adalah 53% dan kecekapan penyingkiran kekeruhan adalah 96%. Nilai pH adalah 9.4 pada 40 min RT menggunakan elektrod besi. Kekonduksian elektrik (EC) Nilai terendah yang dicatatkan sebagai  $156\mu s / cm$  menggunakan elektrod besi.

Dalam proses penjerapan, kecekapan penyingkiran  $BOD_5$  adalah 95%, manakala kecekapan penyingkiran COD adalah 88%. Jumlah nitrogen (TN) kecekapan

penyingkiran dicatatkan sebagai 98.7%, manakala kecekapan fosfat ( $PO_4$ ) penyingkiran 84 dan 82% telah diperolehi di CT 4 masing-masing (GACC) dan 2 jam, (GACP). TDS kecekapan penyingkiran telah diperolehi pada 66 dan 75% pada 4 jam CT GACC dan GACP, masing-masing. TSS Optimum kecekapan penyingkiran adalah 90%. Kecekapan penyingkiran kemasinan menggunakan GACC dan GACP adalah 81 dan 74% masing-masing. Kekeruhan kecekapan penyingkiran sebanyak 95% adalah penyingkiran tertinggi kecekapan direkodkan pada 6 jam. PH adalah 8.93 untuk kedua-dua GACC dan GACP. Menggunakan GACC dan GACP, nilai SPR telah direkodkan sebagai 102 dan 83 $\mu$ s / cm, masing-masing.

Selepas beberapa kombinasi voltan digunakan untuk proses elektrolisis, di mana, 40 min RT dan 24 volt telah dipilih sebagai kombinasi yang terbaik untuk penyingkiran kecekapan tertinggi. Juga, GAC dos 10 g / l pada 6 hr CT menghasilkan penyingkiran kecekapan tertinggi.

Secara umumnya, elektrod besi adalah lebih murah dan lebih tahan kakisan daripada keluli tahan karat. Keputusan yang diperolehi daripada elektrod besi yang rapat dengan keputusan keluli tahan karat. Sebaliknya, GACP adalah lebih murah daripada GACC. Juga, GACP banyaknya dihasilkan di Malaysia sebagai sisa biojisim yang dihasilkan daripada aktiviti pertanian. Kesimpulannya, GACP boleh dianggap sebagai penjerap mesra alam menjanjikan untuk rawatan leachate tapak pelupusan.

## ACKNOWLEDGEMENTS

I would like to extend my earnest and sincere gratitude to Almighty Allah for His guidance throughout my study period.

I wish to express my deepest gratitude to my supervisor, Dr. Aimul Ahsan, for his excellent guidance, caring, patience, and providing me with an excellent atmosphere for conducting the study. I would also like to thank my committee members; Prof. Dr. Thamer Ahmed Muhammed and Dr. Nik Norsyahariati Nik Daud, who let me experience this research journey by making important suggestions and advices, I actually found it extremely useful.

I would like to express my utmost gratitude, indebtedness and appreciation to my parents and my wife for their love, support and encouragement that inspired me to accomplish this study.



This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfillment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

**Amimul Ahsan, PhD**  
Senior Lecturer  
Faculty of Engineering  
Universiti Putra Malaysia  
(Chairman)

**Thamer Ahmed Muhammed, PhD**  
Professor  
Faculty of Engineering  
Universiti Putra Malaysia  
(Member)

**Nik Norsyahariati Nik Daud, PhD**  
Lecturer  
Faculty of Engineering  
Universiti Putra Malaysia  
(Member)

---

**BUJANG BIN KIM HUAT, PhD**  
Professor and Dean  
School of Graduate Studies  
Universiti Putra Malaysia

Date:

## TABLE OF CONTENTS

	<b>Page</b>
<b>ABSTRACT</b>	i
<b>ABSTRAK</b>	iii
<b>ACKNOWLEDGEMENTS</b>	v
<b>APPROVAL</b>	vi
<b>DECLARATION</b>	viii
<b>LIST OF FIGURES</b>	xii
<b>LIST OF TABLES</b>	xvii
<b>LIST OF ABBREVIATIONS</b>	xviii
<b>CHAPTER</b>	
<b>1 INTRODUCTION</b>	
1.1 Background	1
1.2 Problem Statement	4
1.3 Research Objectives	5
1.4 Scope of study	5
<b>2 LITERATURE REVIEW</b>	
2.1 Introduction	7
2.2 Preparing landfill place and specification	8
2.3 Composition of leachate and influencing factors	11
2.3.1 Leachate composition	11
2.3.2 Leachate management	12
2.3.3 Standards of leachate discharge	14
2.3.4 Influencing factors	15
2.3.4.1 Age of Landfill	15
2.3.4.2 Climate variation	16
2.3.4.3 Kind of waste deposited	16
2.4 Landfill leachate treatment methods	17
2.4.1 Conventional techniques	17
2.4.1.1 Recycling	17
2.4.1.2 Combined treatment with municipal waste water	17
2.4.1.3 Biological treatment	18
2.4.1.4 Physical- chemical methods	22
2.4.2 Advanced techniques	24
2.4.2.1 Membrane techniques	24
2.4.2.2 Oxidation processes	26
2.4.2.3 Electrolysis techniques	26
2.5 Preparation of Activated Carbon	28
2.5.1 Physical Activation	30
2.5.2 Chemical Activation	30
<b>3 METHODOLOGY</b>	
3.1 Introduction	32
3.2 Raw leachate collected from Jeram sanitary landfill	35

3.3	Experimental setup	35
3.3.1	Electrolysis process	36
3.3.2	Filtration	37
3.3.3	Granular activated carbon adsorption	39
3.3.4	Modification of GAC	40
3.3.5	AC adsorption process	42
3.4	Landfill leachate quality parameters	43
3.4.1	Biochemical Oxygen Demand (BOD <sub>5</sub> )	43
3.4.2	Chemical Oxygen Demand (COD)	45
3.4.3	Total nitrogen (TN) and phosphate (PO <sub>4</sub> )	46
3.4.4	TSS and TDS	46
3.4.5	Turbidity (NTU)	49
3.4.6	pH, salinity (mg/l), electrical conductivity (μs/cm)	49
3.5	Calculation of removal efficiency	50
<b>4</b>	<b>RESULTS AND DISCUSSION</b>	
4.1	Electrolysis treatment	52
4.1.1	Effect of electrolysis on removal of COD and BOD <sub>5</sub>	54
4.1.2	Effect of electrolysis on removal of TSS and TDS	56
4.1.3	Effect of electrolysis on removal of turbidity	59
4.1.4	Effect of electrolysis on pH	60
4.1.5	Effect of electrolysis on salinity and conductivity	61
4.2	Granular Activated Carbon	63
4.2.1	Effect of adsorption on removal of COD and BOD <sub>5</sub>	64
4.2.1.1	Adsorbent contact time	64
4.2.1.2	Adsorbent dosage	69
4.2.2	Effect of adsorption on removal of TN and PO <sub>4</sub>	72
4.2.2.1	Adsorbent contact time	72
4.2.2.2	Adsorbent dosage	74
4.2.3	Effect of GACC and GACP on pH	78
4.2.4	Effect of GACC and GACP on removal of TSS	78
4.2.5	Effect of GACC and GACP on TDS removal	80
4.2.6	Effect of GACC and GACP on removal of turbidity	81
4.2.7	Effect of GACC and GACP on removal of Salinity	81
4.2.8	Effect of GACC and GACP on electrical conductivity	83
4.3	Optimum conditions for electrolysis	84
4.4	Optimum conditions for activated carbon dosage	89
4.5	Cost analysis of electrical energy consumed	98
4.6	Cost analysis of granular activated carbon	100
<b>5</b>	<b>CONCLUSIONS AND RECOMMENDATIONS</b>	
5.1	Conclusions	102
5.2	Recommendations	103
	<b>REFERENCES</b>	104
	<b>APPENDICES</b>	118
	<b>BIODATA OF STUDENT</b>	134
	<b>PUBLICATION</b>	135

## LIST OF FIGURES

<b>Figure</b>	<b>Page</b>
1.1 Cross-section of a Sanitary landfill showing the composition of layers	3
2.1 Cross section of Sanitary landfill showing network of pipes through layers	10
2.2 Schematic overview of the water cycle at constructed landfill with impermeable liner	10
2.3 Plants currently used in reed bed systems at Imog, Moen	21
2.4 Transmission electron	29
2.5 Chemical reaction at electrodes	29
3.1 Flowchart of research steps	33
3.2 Flowchart of methodology process	34
3.3 Location of Jeram Sanitary Landfill, Jeram, Kuala Selangor, Malaysia	35
3.4 Schematic diagram of electrolysis process with filtration and adsorption	37
3.5 (a) Reaction and oxidation at anode and cathode (b) Solid residues on electrodes	38
3.6 (a) Quartz filter (b) Filter media (Quartz) size (i) 1-1.2 mm (ii) 0.8-1 mm (iii) 0.6-0.8 mm	38
3.7 Modification of AC (a) Sieving (b) Deionized water (c) GACP soaked with deionized water to remove black spots (d) Wash GACP with H <sub>2</sub> SO <sub>4</sub> at 110°C for 24 hr (e) Sample were dried overnight in an oven at 110°C (f) Stored in a desiccator	42
3.8 (a) Weighting GAC dose (b) Treated leachate with GAC dose shaking at 100 rpm	42
3.9 (a) Pipette 1 ml leachate into BOD bottle (b) BOD bottle covered by aluminum and incubate in incubator at 20°C for 5 days	44
3.10 Determination of DO (a) add MnSO <sub>4</sub> and Alkaline- Iodide Azide reagent, (b) add H <sub>2</sub> SO <sub>4</sub> , (c) add 2-3 drops of starch indicator, (d) samples become colourless	44
3.11 Determination of COD (a) COD reactor at 150°C for 2 hr (b) COD measurement by colorimeter	46
3.12 (a) The TN reagent (b) Adjust the pH (6-8) of stored samples for PO <sub>4</sub> calculation by colorimeter	46
3.13 Determination of TSS (a) Put the filter paper in the vacuum filtration apparatus (b) Filter paper in evaporating dish (c) Weight the clean filter paper (d) Filter paper (Whatman GFC 47mm Ø)	48
3.14 TRACER POCKETESTER	49
3.15 (a) Turbidimeter (b) Sample preparation	49

3.16	pH measured by (a) TRACER POCKETESTER (b) pH meter	50
4.1	Deposition on electrodes at end of electrolysis process	53
4.2	Sedimentation at the end of electrolysis process	53
4.4	COD removal efficiency with different voltages and retention times by using iron electrode	54
4.5	COD removal efficiency with different voltages and retention times by using stainless steel electrode	55
4.6	BOD <sub>5</sub> removal efficiency with different voltages and retention times by using iron electrode	56
4.7	BOD <sub>5</sub> removal efficiency with different voltages and retention times by using stainless steel electrode	56
4.8	TSS removal efficiency with different voltages and retention times by using iron electrode	57
4.9	TSS removal efficiency with different voltages and retention times by using stainless steel electrode	58
4.10	TDS removal efficiency with different voltages and retention times by using iron electrode	58
4.11	TDS removal efficiency with different voltages and retention times by using stainless steel electrode	58
4.12	Turbidity removal efficiency with different voltages and retention times by using iron electrode	59
4.13	Turbidity removal efficiency with different voltages and retention times by using stainless steel electrode	60
4.14	pH of leachate by using iron electrode with different voltages and different retention times	61
4.15	pH of leachate by using stainless steel electrode with different voltages and different retention times	61
4.16	Salinity removal efficiency with different voltages and retention times by using iron electrode	62
4.17	Salinity removal efficiency with different voltages and retention times by using stainless steel electrode	62
4.18	Electrical removal efficiency with different voltages and retention times by using iron electrode	63
4.19	Electrical removal efficiency with different voltages and retention times by using stainless steel electrode	63
4.20	BOD <sub>5</sub> removal efficiency with different dosages and contact times by using GACC	65
4.21	BOD <sub>5</sub> removal efficiency with different dosages and contact times by using GACP	66
4.22	COD removal efficiency with different dosages and contact times by using GACC	66

4.23	COD removal efficiency with different dosages and contact times by using GACP	66
4.24	Langmuir isotherm for BOD <sub>5</sub> removal by GACP at 6 hr	69
4.25	Langmuir isotherm for BOD <sub>5</sub> removal by GACC at 6 hr	69
4.26	Freundlich isotherm for BOD <sub>5</sub> removal by GACP at 6 hr	70
4.27	Freundlich isotherm for BOD <sub>5</sub> removal by GACC at 6 hr	70
4.28	Langmuir isotherm for COD removal by GACP at 6 hr	70
4.29	Langmuir isotherm for COD removal by GACC at 6 hr	71
4.30	Freundlich isotherm for COD removal by GACP at 6 hr	71
4.31	Freundlich isotherm for COD removal by GACC at 6 hr	71
4.32	TN removal efficiency with different dosages and contact times by using GACC	73
4.33	TN removal efficiency with different dosages and contact times by using GACP	73
4.34	PO <sub>4</sub> removal efficiency with different dosages and contact times by using GACC	73
4.35	PO <sub>4</sub> removal efficiency with different dosages and contact times by using GACP	74
4.36	Langmuir isotherm for TN removal by GACC at 6 hr	75
4.37	Langmuir isotherm for TN removal by GACP at 6 hr	75
4.38	Freundlich isotherm for TN removal by GACC at 6 hr	75
4.39	Freundlich isotherm for TN removal by GACP at 6 hr	77
4.40	Langmuir isotherm for PO <sub>4</sub> concentration removal by GACC at 4 hr	77
4.41	Langmuir isotherm for PO <sub>4</sub> concentration removal by GACP at 3 hr	77
4.42	Effect of GACC on pH value	78
4.43	Effect of GACP on pH value	78
4.44	TSS removal efficiency with different dosages and contact times by using GACC	79
4.45	TSS removal efficiency with different dosages and contact times by using GACP	79
4.46	TDS removal efficiency with different dosages and contact times by using GACC	80
4.47	TDS removal efficiency with different dosages and contact times by using GACP	80
4.48	Turbidity removal efficiency with different dosages and contact times by using GACC	81
4.49	Turbidity removal efficiency with different dosages and contact times by using GACP	82
4.50	Salinity removal efficiency with different dosages and contact times by using GACC	82

4.51	Salinity removal efficiency with different dosages and contact times by using GACP	82
4.52	Electrical conductivity removal efficiency with different dosages and contact times by using GACC	83
4.53	Electrical conductivity removal efficiency with different dosages and contact times by using GACP	83
4.54	Effect of electrical potential on removal efficiency for tested parameters by using iron electrode	84
4.55	Effect of electrical potential on removal efficiency for tested parameters by using stainless steel electrode	84
4.56	Variations of removal efficiency with different voltages for BOD <sub>5</sub> using (a) Iron electrode and (b) Stainless steel electrode	85
4.57	Variations of removal efficiency with different voltages for COD using (a) Iron electrode and (b) Stainless steel electrode	86
4.58	Variations of removal efficiency with different voltages for TSS using (a) Iron electrode and (b) Stainless steel electrode	87
4.59	Variations of removal efficiency with different voltages for TDS using (a) Iron electrode and (b) Stainless steel electrode	87
4.60	Variations of removal efficiency with different voltages for Turbidity using (a) Iron electrode and (b) Stainless steel electrode	88
4.61	Variations of removal efficiency with different voltages for Salinity using (a) Iron electrode and (b) Stainless steel electrode	89
4.62	Effect of GACC dosage on removal efficiency for tested parameters	92
4.63	Effect of GACP dosage on removal efficiency for tested parameters	92
4.64	Variations of removal efficiency with GACC and GACP dosage for BOD <sub>5</sub>	93
4.65	Variations of removal efficiency with GACC and GACP dosage for COD	93
4.66	Variations of removal efficiency with GACC and GACP dosage for TN	94
4.67	Variations of removal efficiency with GACC and GACP dosage for PO <sub>4</sub>	95
4.68	Variations of removal efficiency with GACC and GACP dosage for TSS	95
4.69	Variations of removal efficiency with GACC and GACP dosage for TDS	96
4.70	Variations of removal efficiency with GACC and GACP dosage for Turbidity	97
4.71	Variations of removal efficiency with GACC and GACP dosage for Salinity	97
4.72	The comparison among the correlation analysis for TSS, TDS and turbidity by using GACC	98



4.73	The comparison among the correlation analysis for TSS, TDS and turbidity by using GACP	98
4.74	Electricity cost increasing pattern for different voltages and retention times	100





## LIST OF TABLES

<b>Table</b>		<b>Page</b>
2.1	Compositions of landfill leachate (mg/L)	14
2.2	Limiting concentration to discharge of landfill leachate in Malaysia	15
2.3	Classification of landfill leachate according to age	16
2.4	Typical performance of attached growth biological treatment systems	21
3.1	Number of times use iron electrode for the electrolysis process	36
3.2	Number of times use stainless steel electrode for the electrolysis process	36
3.3	Chemical and physical properties of filter media	39
3.4	Properties of granular activated carbon based on coconut shell	40
3.5	Properties of granular activated carbon based on palm shell	41
4.1	Properties of raw leachate sample	53
4.2	Comparison of GAC with other adsorbents for COD remediation	67
4.3	Comparison of GAC with other adsorbents for BOD <sub>5</sub> remediation	68
4.4	Comparison of GAC with other adsorbents for TN remediation	76
4.5	Comparison of GAC with other adsorbents for PO <sub>4</sub> remediation	76
4.6	Comparison of GAC with other adsorbents for TDS remediation	90
4.7	Comparison of GAC with other adsorbents for Turbidity remediation	90
4.8	Comparison of GAC with other adsorbents for electrical conductivity remediation	90
4.9	The summary of removal efficiency for ten measured parameters Electricity consumed (KWh) for values RTs	91
4.10	Cost comparison of optimum conditions for AC adsorption.	99
4.11	Cost savings comparison based on flow rates	101
4.12	Cost savings comparison based on flow rates	101

## LIST OF ABBREVIATIONS

AC	Activated Carbon
AOP	advanced oxidation processes
BOD5	Biological Oxygen Demand
CAS	Conventional activated sludge systems
COD	Chemical Oxygen Demand
CT	Contact Time
DC	Direct Electric Current
DOC	Dissolved Organic Carbon
DOM	Dissolved Organic Matter
EC	Electrical Conductivity
GAC	Granular Activated Carbon
GACC	Granular Activated Carbon based on coconut shell
GACP	Granular Activated Carbon based on palm shell
GHG	Green House Gas
HA	Humic Acid
HRT	Hydraulic Retention Time
IUPAC	International Union of Pure and Applied Chemistry
JSL	Jeram Sanitary Landfill
LR	Loading Rate
MAP	magnesium ammonium phosphate
MF	Microfiltratio
MSW	Municipal Solid Waste
N	Nitrogen
NF	nan filtration
NTU	Nephelometric Turbidity Units
PAC	Powder Activated Carbon
RO	Reversed osmosis
rpm	Revolution per minute
RT	Retention Time
SBR	Sequential Batch Reactor
SS	Suspended Solids

TCOD	Total Chemical Oxygen Demand
TDS	Total Dissolved Solids
TKN	Total Kjeldahl Nitrogen
TOC	Total Organic Carbon
TSS	Total Suspended Solids
UASB	Upflow Anaerobic Sludge Blanket
UF	ultrafiltration
VFA	Volatile Fatty Acids
WWTP	Waste Water Treatment Plant



# CHAPTER 1

## INTRODUCTION

### 1.1 Background

Sanitary landfills are defined as a place where the solid waste has been isolated from an exact environment till the mentioned solid waste is totally safe. It degrades biologically, chemically as well as physically. Solid waste in the landfill is a type of solid waste generated from community, commercial and agricultural operations. This includes wastes from households, offices, stores and other non-manufacturing activities. A site is a subject to be regarded as sanitary landfill after four basic conditions should be met, longer term aim should be introduced in order to meet them finally in full. Basic requirements are: partial or full hydrogeological isolation, Permanent control, planned waste emplacement and covering as well as formal engineering presentation.

The location of landfills for the deposition of domestic and industrial solid waste in remote areas is for health reasons. This is because of the emission of green house gas GHG (methane and carbon dioxide) from decomposing waste within the landfills that can be harmful to health and also pose major environmental problems. Additionally, there is the production of a liquid known as leachate when precipitation infiltrates the solid waste. Due to the high content of organic compounds and ammonium ions, leachate is highly polluted (Welander et al., 1997).

Leachate is generated from the garbage decomposition as well as precipitation which infiltrates and percolates throughout the waste material volume and settles down to the bottom of the landfill and generates chemical reaction as well as physical mixing together with ingredients that found in the subjected waste. Leachate commonly has high level of toxic compounds concentration together with matter of organic, heavy metals and ammonium. Inappropriate geological material under the landfill is the main cause of risk of leachate leakage to the groundwater. A long term humans health issues may be caused by heavy metals and toxic materials in leachate (Thörneby et al., 2003).

Leachate in landfill frequently exceeds standard for surface water and municipal waste water, often for several decades. Landfill leachate has the high possibility to pollute surface water and groundwater caused by pathway for leachate to the bottom of the landfill through the unsaturated soil layers to the groundwater, then by groundwater through hydraulic connections to surface water. Nevertheless, pollution may also outcome from the discharge of leachate through direct discharge of untreated leachate or by treatment plants. The main factors influencing the pollution chance from landfill leachate are the flux of the leachate and concentration. The landfill sitting such as the hydro geological setting and the degree of protection provided and the basic quality, volume, sensitivity of the receiving groundwater and surface water (Ghafari et al., 2009).

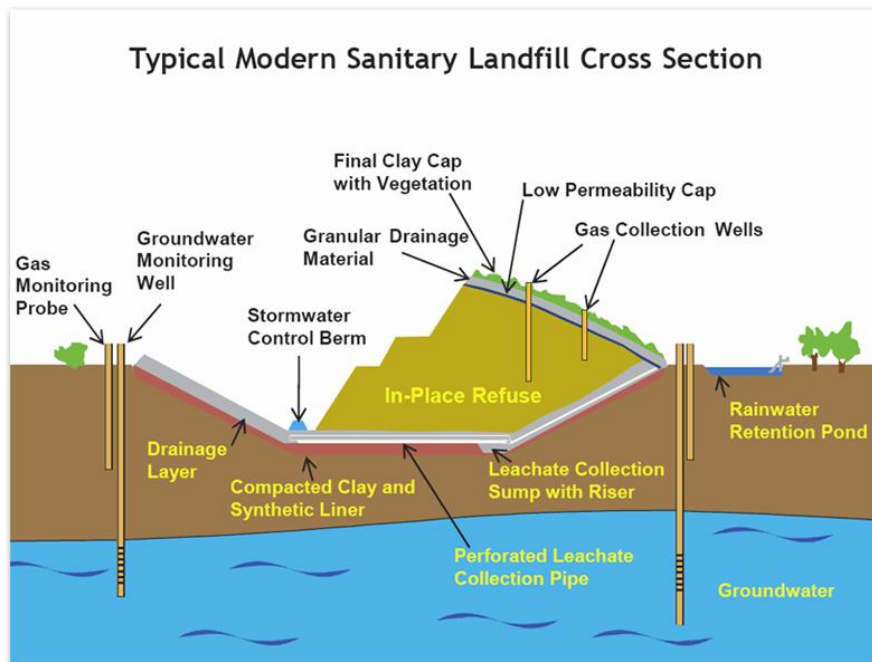
One of the methods to control leachate generation is to control the water infiltration in the sanitary landfill by solid waste compaction. This method reduces the infiltration rate while growing plants on the soil covers of the solid waste can also have the same effect. The sanitary landfill leachate properties are controlled by temperature, pH, solid waste properties, moisture content, redox potential, etc. Temperature has a significant effect on the decomposition process in a sanitary landfill. Besides, moisture is needed for the biological conversion and stabilization within the sanitary landfill. The redox and pH potential set the conditions for the different phases of decomposition and biological processes within the sanitary landfill. Thus, the microbial composition within the sanitary landfill effectively contributes to the sanitary landfill stabilization (Pokhrel et al., 2005).

Ground-water becomes contaminated due to buried solid waste that is above the level of water table. Ground-water gets contaminated likewise if leachate moves downwards from the sanitary landfill into the ground-water table as a result of precipitation infiltration (Madu, 2008).

The survey by O'Leary et al.(1995) investigates the objectives and factors that need to be considered in the design of a sanitary landfill that is related to biological, physical and chemical reactions at municipal solid waste landfills that occur simultaneously and result in waste decomposition leachate and gases (O'Leary et al., 1995).

The design procedure entails alternating layers of compacted municipality solid waste (MSW) with cover material when waste is disposed. This can be compost, soil, or any other approved material, where wastes are compacted after dumping by special bulldozers and the fresh layer of MSW is laid over with cover material to start another layer. This method helps to reduce odor problems, and prevents exposure to health hazards. All sanitary landfills are supplied leachate collection systems. A typical liner is composed of layers of synthetic material, plastic, gravel, and clay to prevent leachate from escaping as shown in Figure 1.1. A lined landfill is also fitted with a pipeline network to collect and drain the leachate. Leachate recirculation is practiced at a solid waste landfill, or it is treated and discharged (Nora, 2006).

The design of the sanitary landfill location would prevent, or it also might reduce any undesirable outcomes on the environment and the effect on human health. It is very important to adopt methods, standards and operational systems based on current best practices in the design, which reflects progress in management techniques and containment standards. Protecting the environment and health should be the main aims when designing a landfill. The findings of the environmental assessment, risk assessment and the conceptual design proposals are interactive process in landfill design. The main aim behind waste management is sustainability (Manandhar, 2009).



**Figure 1.1: Cross-section of a Sanitary landfill showing the composition of layers** (<http://runcoenv.com/landfill.htm>)

The central objective of waste policy is to reduce the harmful health and environmental impacts of waste. In order to meet this objective, it is particularly important to:

- prevent the generation of waste
- promote reuse of waste
- promote biological recovery of waste and recycling of materials
- promote energy use of waste not suited for recycling
- ensure that the treatment and disposal of waste does not cause any harmful impacts

The main climate-related objective of waste policy is to reduce the greenhouse gas emissions generated by waste, particularly by reducing the methane emissions resulting from treatment at landfills. In order to reach the objective, the amount of landfilled biodegradable waste will be substantially reduced, while at the same time measures will be taken to increase the recovery rates of methane generated at landfills (Graveland et al., 2003).

It is a known fact that all living plants and beings need nutrients which are essential for development. However, excessive use can cause adverse effects. As an example, aquatic life is affected by excess nutrient discharge in natural water bodies, as it increases oxygen demand and eutrophication, while human beings will suffer various health problems from excess nutrients. Human daily activities produce a high concentration of phosphorous and nitrogen and due to the discharge of wastewater that causes eutrophication in water bodies. Therefore, there is an urgent need to improve wastewater treatment technology to a level when it can efficiently remove organic



matter, nutrients and other harmful constituents. These problems have led to the realization that there is an urgent need to think of solutions and alternative methods and available materials in the process of wastewater treatment. One of the natural methods and substances available to treat leachate are electrolysis treatment and activated carbon (AC).

The process of circulating direct current (DC) through an ionic substance is known as electrolysis; the user substance in the electrolysis process is either molten or dissolved in a suitable solvent, which produces a chemical reaction at the electrodes and separates the materials (Morimitsu, 2000).

In 1990, the world production of AC to meet demand was estimated to be 375,000 tons, except Eastern Europe and China. In the United States the demand for activated carbon reached 200,000 tons per year. In 2002, demand further increased and market growth for these materials for various applications was estimated at 4.6% per year (Mozammel et al., 2002). AC performance in water applications showed low cost compared to the use of other possible competitive inorganic materials such as zeolites and this has an effect on the positive market position.

## **1.2 Problem Statement**

The JSL produces huge amount of the update every day. The landfill leachate is a complex substance which generated when water is absorbed into the solid waste disposal site that contains toxic compounds, organic matter, ammonium, heavy metals and colloidal solids and a variety of pathogens potentially contaminate surface water and groundwater. The landfill leachate properties are different and these differences are caused by several factors such as availability of oxygen and moisture content, design and life expectancy of the solid waste and operational of the sanitary landfill (Tzoupanos et al., 2010).

The important potential pollution source of surface and ground water is landfill leachate. Leachate are not correctly collected, treated and safely disposed, causing extensive contamination of water wells, creeks and streams (Li et al., 2010). The effluents are complicated to deal with and biological processes are totally inefficient for the toxic nature of stabilized leachate. Hence, there are requirement to physical, chemical and biological treatment and alternative technology. Coagulation-flocculation and adsorption process are widely used in wastewater treatment plants because of implementation and operation simplicity (Rivas et al., 2004).

The electrolysis is applied for landfill leachate treatment (Peng 2013; Tsai et al.1997). It had higher performance than classical chemical coagulation process and it can be applied as a step of a joint treatment. Kabuk et al. (2013) investigated on leachate treatment with electrolysis and optimization by response surface methodology. At optimum working conditions, 60.5 % COD removal, 92.4 % total suspended solids (TSSs) removal, 60.8 % total organic carbon (TOC) removal, 28.3 % total Kjeldahl nitrogen (TKN) removal, 99 % PO4-P removal, and 28.9 % NH3-N removal results were obtained.

Therefore, in this study, a novel low-cost process integrating electrocoagulation with an activated carbon (AC) contactor is developed for the first time to improve the treatment of the increasing volume of leachate. The optimum pollutant removal efficiencies (for BOD<sub>5</sub>, COD, TDS, TSS, and pH) are identified by extensive laboratory analysis. The proposed process is an ecofriendly, sustainable technique for leachate treatment, which reduces treatment cost and saves energy, and which also helps in protecting the environment.

The optimal conditions of electrolysis for landfill leachate treatment have not been investigated in Malaysia. In addition the optimal conditions of AC dosage for landfill leachate treatment have not been studied in Malaysia. Moreover, a combined system of electrolysis and AC have not been studied until now. It is hope that by applying the combined system; we can get high removal efficiency for various parameters (BOD<sub>5</sub>, COD, TN, PO<sub>4</sub>, TDS, TSS, Turbidity, pH, Salinity and electrical conductivity).

### **1.3 Research Objectives**

The main objective of the current study is to examine the performance of a combined system of electrolysis and granular activated carbon adsorption to treat landfill leachate collection from Jeram Sanitary Landfill.

The specific objectives of this study can summarize as bellow:

1. To evaluate the performance of iron and stainless steel electrodes to treat landfill leachate by electrolysis.
2. To evaluate the pollutants removal efficiency from landfill leachate by using the granular activated carbons based on coconut and oil palm shells.
3. To determine the optimum conditions of hydraulic retention time, voltage and AC dosage for electrolysis process followed by AC adsorption.

### **1.4 The scope of the study**

In this study, leachate samples were collected from JSL, followed by laboratory testing procedures in order to evaluate and determine the levels biochemical oxygen demand (BOD), chemical oxygen demand (COD), total nitrogen (TN), phosphate (PO<sub>4</sub>), total suspended solid (TSS), total dissolved solids (TDS), turbidity, pH, salinity and electrical conductivity (EC) in these samples. In January 2007, the landfill started operations. The landfill leachate was collected without any pre-treatment performed. To keep the properties of the wastewater unchanged, the leachate of the collected landfill was stored in refrigerator at 4°C. The type of leachate landfill is medium leachate. The treatment process is divided into three stages: Firstly; the electrolysis process for leachate treatment was conducted using iron and stainless steel electrodes at various retention time (5, 10, 15, 20, 30, 40 and 50 min) and different voltages (3, 6, 12, 18 and 24 volt). Secondly; quartz filters were employed to remove the particles. Finally, GAC commercial coconut shells were used in leachate treatment with different contact time (1, 2, 3, 4, 5, 6, 8, 10 and 13 hr) and dosage (2, 4, 6, 8 and 10 g/l) to



determine the treatment efficiency of leachate. Furthermore a commercial GAC based on palm shells was also used in leachate treatment with different contact times in order to compare the treating efficiency outputs of leachate for each GAC type using laboratory testing techniques; BOD, COD, TN, PO<sub>4</sub>, TSS, TDS, turbidity, pH, salinity and EC, to find the optimal one with preminent quality and determine the HRT, voltage, CT, AC dosage, etc.



## REFERENCES

- Abbas, A. A., Jingsong, G., Ping, L. Z., Pan, Y. Y., and Al-Rekabi, W. S. (2009). Review on Landfill Leachate Treatments. *American Journal of Applied Sciences*, 6(4), 672-684.
- Abdoli M. A., Karbassi A. R., Samiee-Zafarghandi R., Rashidi Z., Gitipour S. and Pazoki, M. (2012). Electricity generation from leachate treatment plant. *International Journal of Environmental Research*, 6, 493-498.
- Abuzaid, N. S., Bukhari, A. A., and Al-Hamouz, Z. M. (1998). Removal of bentonite causing turbidity by electro-coagulation. *Journal of Environmental Science & Health Part A*, 33(7), 1341-1358.
- Ademiluyi, F. T., Amadi, S. A., and Amakama, N. J. (2009). Adsorption and Treatment of Organic Contaminants using Activated Carbon from Waste Nigerian Bamboo. *Journal of Applied Sciences and Environmental Management*, 13(3).
- Adhoum, N., and Monser, L. (2004). Decolourization and removal of phenolic compounds from olive mill wastewater by electrocoagulation. *Chemical Engineering and Processing: Process Intensification*, 43(10), 1281-1287.
- Ahmadpour, A., and Do, D. D. (1996). The preparation of active carbons from coal by chemical and physical activation. *Carbon*, 34(4), 471-479.
- Ahn, H., Chae, S., Kim, S., Wang, C., and Summers, R. (2007). Efficient taste and odour removal by water treatment plants around the Han River water supply system. *Water Science & Technology*, 55(5), 103-109.
- Ahn, W. Y., Kang, M. S., Yim, S. K., & Choi, K. H. (2002). Advanced landfill leachate treatment using an integrated membrane process. *Desalination*, 149(1), 109-114.
- Alade, A. O., Amuda, O. S., & Ibrahim, A. O. (2012). Isothermal studies of adsorption of acenaphthene from aqueous solution onto activated carbon produced from rice (*Oryza sativa*) husk. *Desalination and Water Treatment*, 46(1-3), 87-95.
- Alfajara, C. G., Nakano, K., Nomura, N., Igarashi, T., and Matsumura, M. (2002). Operating and scale-up factors for the electrolytic removal of algae from eutrophied lakewater. *Journal of Chemical Technology and Biotechnology*, 77(8), 871-876.
- Alinsafi, A., Khemis, M., Pons, M. N., Leclerc, J. P., Yaacoubi, A., Benhammou, A., and Nejmeddine, A. (2005). Electro-coagulation of reactive textile dyes and textile wastewater. *Chemical Engineering and Processing: Process Intensification*, 44(4), 461-470.

- Alkalay D., Guerrero L., Lema J.M., Mendez R. and Chamy R. (1998). Review: Anaerobic treatment of municipal sanitary landfill leachates: the problem of refractory and toxic components. *World Journal of Microbiology and Biotechnology*, 14, 309-320.
- Amokrane, A., Comel, C., and Veron, J. (1997). Landfill leachates pretreatment by coagulation-flocculation. *Water research*, 31(11), 2775-2782.
- Andreozi R., Caprio V., Insola A. and Marotta R. (1999). Advanced oxidation processes (AOP) for water purification and recovery. *Catalysis Today*, 53, 51–59.
- Arriagada, R., Garcia, R., Molina-Sabio, M., & Rodriguez-Reinoso, F. (1997). Effect of steam activation on the porosity and chemical nature of activated carbons from Eucalyptus globulus and peach stones. *Microporous Materials*, 8(3), 123-130.
- Ayoub, G. M., Hamzeh, A., and Semerjian, L. (2011). Post treatment of tannery wastewater using lime/bittern coagulation and activated carbon adsorption. *Desalination*, 273(2), 359-365.
- Aziz, H. A., Adlan, M. N., Zahari, M. S. M., and Alias, S. (2004). Removal of ammoniacal nitrogen (N-NH<sub>3</sub>) from municipal solid waste leachate by using activated carbon and limestone. *Waste management & research*, 22(5), 371-375.
- Babel, S., and Kurniawan, T. A. (2004). Cr (VI) removal from synthetic wastewater using coconut shell charcoal and commercial activated carbon modified with oxidizing agents and/or chitosan. *Chemosphere*, 54(7), 951-967.
- Balasubramanian, N., and Madhavan, K. (2001). Arsenic removal from industrial effluent through electrocoagulation. *Chemical Engineering & Technology*, 24(5), 519-521.
- Banerjee, S., and Dastidar, M. G. (2005). Use of jute processing wastes for treatment of wastewater contaminated with dye and other organics. *Bioresource technology*, 96(17), 1919-1928.
- Bansal, R.C., Donnet, J.B., Stoeckli, H.F. Active carbon. Marcel Dekker, 1988, New York.
- Bansode, R. R., Losso, J. N., Marshall, W. E., Rao, R. M., and Portier, R. J. (2004). Pecan shell-based granular activated carbon for treatment of chemical oxygen demand (COD) in municipal wastewater. *Bioresource technology*, 94(2), 129-135.
- Bayramoglu, M., Kobya, M., Eyvaz, M., and Senturk, E. (2006). Technical and economic analysis of electrocoagulation for the treatment of poultry slaughterhouse wastewater. *Separation and Purification Technology*, 51(3), 404-408.

- Berrios, M., Martín, M. Á., and Martín, A. (2012). Treatment of pollutants in wastewater: Adsorption of methylene blue onto olive-based activated carbon. *Journal of Industrial and Engineering Chemistry*, 18(2), 780-784.
- Bian, D., Ren, Q., Ai, S., Zuo, Y., and Liu, J. (2011, April). Study on treatment of wastewater from the production of PolyTHF with adsorption method. In *Electric Information and Control Engineering (ICEICE), 2011 International Conference on* (pp. 6188-6190). IEEE.
- Board, E. (2007). Clean Development Mechanism Project Design Document Form (CDM-PDD), Version 03-in effect as of: 28 July 2006, PT Navigat Energy Indonesia Integrated Solid Waste Management (GALFAD) Project in Bali, Indonesia.
- Boni, M. R., Chiavola, A., and Saffroni, S. (2006). Pretreated waste landfilling: Relation between leachate characteristics and mechanical behaviour. *Waste Management*, 26(10), 1156-1165.
- Borghi A. D., Binaghi L., Converti A., and Borghi M. D. (2003). Combined treatment of leachate from sanitary landfill and municipal wastewater by activated sludge. *Chemical and Biochemical Engineering Quarterly*, 17, 277–283.
- Butler, E., Hung, Y. T., Yeh, R. Y. L., and Suleiman Al Ahmad, M. (2011). Electrocoagulation in wastewater treatment. *Water*, 3(2), 495-525.
- Butkovskiy, A. (2009). Leachate treatment at Filborna Landfill with focus on nitrogen removal (Doctoral dissertation, Masters Thesis, Department of Chemical Engineering, Lund University, Sweden.[Links]).
- Calli B., Mertoglu B., Roest K., and Inan B. (2006). Comparison of long-term performances and final microbial compositions of anaerobic reactors treating landfill leachate. *Bio-resource Technology*, 97, 641–647.
- Castillo E., M. Vergara, and Y. Moreno (2007). Landfill leachate treatment using a rotating biological contactor and an upward-flow anaerobic sludge bed reactor. *Waste Management*, 27, 720–726.
- Çeçen, F., and Aktaş, Ö. (2011). Water and Wastewater Treatment: Historical Perspective of Activated Carbon Adsorption and its Integration with Biological Processes. *Activated Carbon for Water and Wastewater Treatment: Integration of Adsorption and Biological Treatment*, 1-11.
- Chang, P. Y., Wei, Y. L., Yang, Y. W., and Lee, J. F. (2003). Removal of copper from water by activated carbon. *Bulletin of environmental contamination and toxicology*, 71(4), 0791-0797.
- Chen, G. (2004). Electrochemical technologies in wastewater treatment. *Separation and purification Technology*, 38(1), 11-41.

- Chianese, A., Ranauro, R., and Verdone, N. (1999). Treatment of landfill leachate by reverse osmosis. *Water Research*, 33(3), 647-652.
- Chiu-Yue L., Feng-Yi B., and Jen C. (1999). Anaerobic co-digestion of septage and landfill leachate. *Bioresource Technology*, 68, 275-282.
- Chopra, A. K., Sharma, A. K., and Kumar, V. (2011). Overview of electrolytic treatment: an alternative technology for purification of wastewater. *Archives of Applied Science Research*, 3(5), 191-206.
- Cleasby, J.L., 1990. Filtration. In: *American Water Work Association Water quality and Treatment: A Handbook of Public Water Supplies*, Fourth ed. McGraw-Hill, Inc, New York.
- Cossu, R., Polcaro, A. M., Lavagnolo, M. C., Mascia, M., Palmas, S., and Renoldi, F. (1998). Electrochemical treatment of landfill leachate: oxidation at Ti/PbO<sub>2</sub> and Ti/SnO<sub>2</sub> anodes. *Environmental science and technology*, 32(22), 3570-3573.
- Crutcher, A. J., and Yardley, J. R. (1991). Implications of Changing Refuse Quantities and Characteristics on Future Landfill Design and Operations. *Municipal solid waste management: making decisions in the face of uncertainty*, 171.
- Cusick, R. D., Bryan, B., Parker, D. S., Merrill, M. D., Mehanna, M., Kiely, P. D., and Logan, B. E. (2011). Performance of a pilot-scale continuous flow microbial electrolysis cell fed winery wastewater. *Applied microbiology and biotechnology*, 89(6), 2053-2063.
- Daneshvar, N., Oladegaragoze, A., and Djafarzadeh, N. (2006). Decolorization of basic dye solutions by electrocoagulation: an investigation of the effect of operational parameters. *Journal of hazardous materials*, 129(1), 116-122.
- Daud, W. M. A. W., and Houshamnd, A. H. (2010). Textural characteristics, surface chemistry and oxidation of activated carbon. *Journal of Natural Gas Chemistry*, 19(3), 267-279.
- Deng Y. (2007). Physical chemical removal of organic contaminants in municipal landfill leachate. E.C. Lehmann ed. *Landfill research focus*, Nova publishers, New York.
- Deng Y. (2009). Advanced Oxidation Processes (AOPS) for Reduction of Organic Pollutants in Landfill Leachate: A Review. *International Journal of Environment and Waste Management*, 4, 367-384.
- Department of Environment (DOE). 2020. *Environmental Requirements: A Guide For Investors in Malaysia*.
- Dho, N. Y., Koo, J. K., and Lee, S. R. (2002). Prediction of leachate level in Kimpo metropolitan landfill site by total water balance. *Environmental monitoring and assessment*, 73(3), 207-219.

- Di Laconi C., Pagano M., Ramadori R., and Lopez A. (2010). Nitrogen recovery from a stabilized municipal landfill leachate. *Bioresource Technology*, 101, 1732–1736.
- Dialynas, E., and Diamadopoulos, E. (2008). Integration of immersed membrane ultrafiltration with coagulation and activated carbon adsorption for advanced treatment of municipal wastewater. *Desalination*, 230(1), 113-127.
- Diamadopoulos, E. (1994). Characterization and treatment of recirculation-stabilized leachate. *Water Research*, 28(12), 2439-2445.
- Duran-Ros, M., Puig-Bargués, J., Arbat, G., Barragán, J., and Ramírez de Cartagena, F., 2009. Performance and backwashing efficiency of disc and screen filters in microirrigation systems. *Biosystem Engineering* 103 (1), 35-42.
- El-Hendawy, A. N. A., Alexander, A. J., Andrews, R. J., and Forrest, G. (2008). Effects of activation schemes on porous, surface and thermal properties of activated carbons prepared from cotton stalks. *Journal of Analytical and Applied Pyrolysis*, 82(2), 272-278.
- El Nemr, A., Khaled, A., Abdelwahab, O., and El-Sikaily, A. (2008). Treatment of wastewater containing toxic chromium using new activated carbon developed from date palm seed. *Journal of Hazardous Materials*, 152(1), 263-275.
- Encinar, J. M., Beltran, F. J., Ramiro, A., and Gonzalez, J. F. (1998). Pyrolysis/gasification of agricultural residues by carbon dioxide in the presence of different additives: influence of variables. *Fuel Processing Technology*, 55(3), 219-233.
- EPA, N. (1996). Environmental guidelines: solid waste landfills. NSW Environment Protection Authority.
- Enzminger J.D., Robertson D., Ahlert R.C., and Kosson D.S. (1987). Treatment of Landfill Leachates. *Journal of Hazardous Materials*, 14, 83-101.
- Fangyue L., Knut W., and Wilhelm H. (2009). Treatment of the methanogenic landfill leachate with thin open channel reverse osmosis membrane modules. *Waste Management*, 29, 960–964.
- Feng, C., Sugiura, N., Shimada, S., and Maekawa, T. (2003). Development of a high performance electrochemical wastewater treatment system. *Journal of hazardous materials*, 103(1), 65-78.
- Fernandes H., Aline V., Martins C. L., Antonio R. V., and Costa R. H. R. (2012). Microbial and chemical profile of a ponds system for the treatment of landfill leachate. *Waste Management*, Article In Press
- Foo K.Y., and Hameed B.H. (2009). An overview of landfill leachate treatment via activated carbon adsorption process. *Journal of Hazardous Materials*, 171, 54–60.



- Foo, K. Y., Lee, L. K., and Hameed, B. H. (2013). Batch adsorption of semi-aerobic landfill leachate by granular activated carbon prepared by microwave heating. *Chemical Engineering Journal*, 222, 259-264.
- Forgie, D.J.L. (1988). Selection of the most appropriate leachate treatment methods. Part 3: A decision model for the treatment train selection. *Water Pollution Research Journal Canada*, 23, 341-355.
- Gourdon R., Comel C., Vermande P., and Veron J., (1989). Fractionation of the organic matter of a landfill leachate before and after aerobic or anaerobic biological treatment. *Water Research*, 23, 167-173.
- Graveland, C., Bouwman, A. F., Eickhout, B., and Strengers, B. J. (2003). Projections of multi-gas emissions and carbon sinks, and marginal abatement cost functions modelling for land-use related sources.
- Ghafari, S, Aziz, H.A, Isa, M.H. and Zinatizadeh, A.A. (2009), Application of response surface methodology (RSM) to optimize coagulation-flocculation treatment of leachate using poly-aluminium chloride (PAC) and alum. *Journal of Hazardous Materials*, 163, pp. 650-656.
- Hamaidi-Maouche, N., Bourouina-Bacha, S., and Oughlis-Hammache, F. (2009). Design of experiments for the modeling of the phenol adsorption process. *Journal of Chemical & Engineering Data*, 54(10), 2874-2880.
- Halize AR (2011). *Climate Change Phenomena: Is Human in Danger?*, Health and the Environment Journal, Vol.2, No.1
- Hong, K., Chang, D., Bae, H., Sunwoo, Y., Kim, J., and Kim, D. (2013). Electrolytic removal of phosphorus in wastewater with noble electrode under the conditions of low current and constant voltage. *Int. J. Electrochem. Sci*, 8, 8557-8571.
- Hongjiang L., Youcai Z., Lei S., and Yingying G. (2009). Three-stage aged refuse biofilter for the treatment of landfill leachate. *Journal of Environmental Sciences*, 21, 70–75.
- Hu, A. Y., and Stuckey, D. C. (2007). Activated carbon addition to a submerged anaerobic membrane bioreactor: effect on performance, transmembrane pressure, and flux. *Journal of environmental engineering*, 133(1), 73-80.
- Hu, C. Y., Lo, S. L., Kuan, W. H., and Lee, Y. D. (2005). Removal of fluoride from semiconductor wastewater by electrocoagulation–flotation. *Water research*, 39(5), 895-901
- Ihara, I., Kanamura, K., Shimada, E., and Watanabe, T. (2004). High gradient magnetic separation combined with electrocoagulation and electrochemical oxidation for the treatment of landfill leachate. *Applied Superconductivity, IEEE Transactions on*, 14(2), 1558-1560.

- Ilhan, F., Kurt, U., Apaydin, O., and Gonullu, M. T. (2008). Treatment of leachate by electrocoagulation using aluminum and iron electrodes. *Journal of hazardous materials*, 154(1), 381-389.
- Imena S., Ismail T., Sami S., Fathi A., Khaled M., Ahmed G., and Latifa B.; 2008. Characterization and anaerobic batch reactor treatment of Jebel Chakir Landfill leachate. *Desalination*, 246, 417-424.
- Inan, H., Dimoglo, A., Şimşek, H., and Karpuzcu, M. (2004). Olive oil mill wastewater treatment by means of electro-coagulation. *Separation and purification technology*, 36(1), 23-31.
- Ince M., Senturk E., Engin G. O., Keskinler B. (2010). Further treatment of landfill leachate by nanofiltration and microfiltration-PAC hybrid process. *Desalination*, 255, 52-60.
- Ioannidou, O., and Zabaniotou, A. (2007). Agricultural residues as precursors for activated carbon production—a review. *Renewable and Sustainable Energy Reviews*, 11(9), 1966-2005.
- Jokela J.P.Y., Kettunen R.H., Sormunen K.M., and Rintala J.A. (2002). Biological nitrogen removal from municipal landfill leachate: low-cost nitrification in biofilters and laboratory scale in-situ denitrification. *Water Research*, 36, 4079-4087.
- Kabuk, H. A., İlhan, F., Avsar, Y., Kurt, U., Apaydin, O., and Gonullu, M. T. (2014). Investigation of leachate treatment with electrocoagulation and optimization by response surface methodology. *CLEAN-Soil, Air, Water*, 42(5), 571-577.
- Kargi F., and Pamukoglu M. Y. (2003). Aerobic biological treatment of pre-treated landfill leachate by fed-batch operation. *Enzyme and Microbial Technology*, 33, 588-595.
- Kautto, P., and Melanen, M. (2004). How does industry respond to waste policy instruments—Finnish experiences. *Journal of Cleaner production*, 12(1), 1-11.
- Kawai M., Purwanti I.F., Nagao N., Slamet A., Hermana J., and Tod T. (2012). Seasonal variation in chemical properties and degradability by anaerobic digestion of landfill leachate at Benowo in Surabaya, Indonesia. *Journal of Environmental Management*, 110, 267-275.
- Kennedy K. J. and Lentz E. M. (2000). Treatment of landfill leachate using sequencing batch and continuous flow upflow anaerobic sludge blanket (UASB) Reactors. *Water Research*, 34, 3640-3656.
- Kettunen R. H., Hoilijoki T. H., and Rintala J. A. (1996). Anaerobic and sequential anaerobic-aerobic treatments of municipal landfill leachate at low temperature. *Bio-resource Technology*, 58, 31-40.



- Khalili, N. R., Campbell, M., Sandi, G., and Golaś, J. (2000). Production of micro-and mesoporous activated carbon from paper mill sludge: I. Effect of zinc chloride activation. *Carbon*, 38(14), 1905-1915.
- Khan, M. A., Kim, S. W., Rao, R. A. K., Abou-Shanab, R. A. I., Bhatnagar, A., Song, H., and Jeon, B. H. (2010). Adsorption studies of Dichloromethane on some commercially available GACs: Effect of kinetics, thermodynamics and competitive ions. *Journal of hazardous materials*, 178(1), 963-972.
- Kheradmand S., Karimi-Jashni A., and Sartaj M. (2010). Treatment of municipal landfill leachate using a combined anaerobic digester and activated sludge system. *Waste Management*, 30, 1025–1031.
- Kim, D., Kim, W., Yun, C., Son, D., Chang, D., Bae, H., ... and Hong, K. (2013). Agro-industrial wastewater treatment by electrolysis technology. *Int. J. Electrochem. Sci*, 8, 9835-9850.
- Kima D., Hong-Duck R., Man-Soo K., Jinhyeong K., and Sang-Il L. (2007). Enhancing struvite precipitation potential for ammonia nitrogen removal in municipal landfill leachate. *Journal of Hazardous Materials*, 146, 81–85.
- Kjeldsen P., Barlaz M. A., Rooker A. P., Baun A., Ledin A., and Christensen T. H. (2002). Present and Long-Term Composition of MSW Landfill Leachate: A Review. *Critical Reviews in Environmental Science and Technology*, 32, 297-336.
- Kumar, P. R., Chaudhari, S., Khilar, K. C., and Mahajan, S. P. (2004). Removal of arsenic from water by electrocoagulation. *Chemosphere*, 55(9), 1245-1252.
- Kuokkanen, V., and Kuokkanen, T. (2013). Recent applications of electrocoagulation in treatment of water and wastewater—A review.
- Kurniawan T. A., Wai-Hung L., and Chan G.Y.S. (2006). Degradation of recalcitrant compounds from stabilized landfill leachate using a combination of ozone-gac adsorption treatment. *Journal of Hazardous Materials*, B137, 443–455.
- Kurniawan, T. A., and Lo, W. H. (2009). Removal of refractory compounds from stabilized landfill leachate using an integrated H<sub>2</sub>O<sub>2</sub> oxidation and granular activated carbon (GAC) adsorption treatment. *Water research*, 43(16), 4079-4091.
- Kurniawan, T. A., Lo, W. H., and Sillanpää, M. E. (2011). Treatment of Contaminated Water Laden with 4-Chlorophenol using Coconut Shell Waste-Based Activated Carbon Modified with Chemical Agents. *Separation Science and Technology*, 46(3), 460-472.
- Kurt, U., Apaydin, O., and Gonullu, M. T. (2007). Reduction of COD in wastewater from an organized tannery industrial region by Electro-Fenton process. *Journal of hazardous materials*, 143(1), 33-40.

- Laitinen N., Luonsi A., and Vilen J. (2006). Landfill leachate treatment with sequencing batch reactor and membrane bioreactor. *Desalination*, 191, 86–91.
- Lehtomäki, A., and Björnsson, L., 2006. Two-stage anaerobic digestion of energy crops: methane production, nitrogen mineralisation and heavy metal mobilisation. *Environmental technology*, 27(2), 209-218.
- Li, W, Hua, T, Zhou, Q.X, Zhang, S.G. and Li, F.X. (2010). Treatment of stabilized landfill leachate by the combined process of coagulation/flocculation and powder activated carbon adsorption. *Desalination* 264, pp. 56-62.
- Lin, C. C., and Liu, H. S. (2000). Dye Adsorption by Activated Carbon in Centrifugal Field. *Progress in Biotechnology*, 16, 25-28.
- Lin, S. H., and Peng, C. F. (1994). Treatment of textile wastewater by electrochemical method. *Water research*, 28(2), 277-282.
- Liu X., Xiao-Ming L., Qi Y., Xiu Y., Ting-Ting S., Wei Z., Kun L., Yi-Hu S., and Guang-Ming Z. (2012). Landfill leachate pretreatment by coagulation–flocculation process using iron-based coagulants: Optimization by response surface methodology. *Chemical Engineering Journal*, 200-202, 39-50.
- Liyan, S., Youcai, Z., Weimin, S., and Ziyang, L. (2009). Hydrophobic organic chemicals (HOCs) removal from biologically treated landfill leachate by powder-activated carbon (PAC), granular-activated carbon (GAC) and biomimetic fat cell (BFC). *Journal of hazardous materials*, 163(2), 1084-1089.
- Lua, A. C., and Guo, J. (2001). Microporous oil-palm-shell activated carbon prepared by physical activation for gas-phase adsorption. *Langmuir*, 17(22), 7112-7117.
- Madu, J. I. (2008). New leachate treatment methods. Doctoral dissertation, Water and Environmental Engineering, Department of Chemical Engineering. Lund University, SWEDEN.
- Manandhar, D. R., Krishnamurthy, V., and Kasaju, Y. S. (2009). Quantitative leachate estimation from a pilot-scale lysimeter study. *International Journal of Environment and Waste Management*, 4(3), 322-330.
- Mehmood M.K., Adetutu E., Nedwell D.B., and Ball A.S. (2009). In situ microbial treatment of landfill leachate using aerated lagoons. *Bioresource Technology*, 100, 2741–2744.
- Min, K. S., Yu, J. J., Kim, Y. J., and Yun, Z. (2004). Removal of ammonium from tannery wastewater by electrochemical treatment. *Journal of Environmental Science and Health, Part A*, 39(7), 1867-1879.
- Mohan, D., Singh, K. P., and Singh, V. K. (2008). Wastewater treatment using low cost activated carbons derived from agricultural byproducts—a case study. *Journal of Hazardous materials*, 152(3), 1045-1053.

- Mohanty, K., Das, D., and Biswas, M. N. (2008). Treatment of phenolic wastewater in a novel multi-stage external loop airlift reactor using activated carbon. *Separation and Purification Technology*, 58(3), 311-319.
- Mollah, M. Y. A., Schennach, R., Parga, J. R., and Cocke, D. L. (2001). Electrocoagulation (EC)—science and applications. *Journal of hazardous materials*, 84(1), 29-41.
- Morimitsu, Y., Hayashi, K., Nakagawa, Y., Fujii, H., Horio, F., Uchida, K., and Osawa, T. (2000). Antiplatelet and anticancer isothiocyanates in Japanese domestic horseradish, wasabi. *Mechanisms of ageing and development*, 116(2), 125-134.
- MWA Design Guidelines for Water Supply Systems. Malaysian Water Association, 1994
- Mozammel, H. M., Masahiro, O., and Bhattacharya, S. C. (2002). Activated charcoal from coconut shell using ZnCl<sub>2</sub> activation. *Biomass and Bioenergy*, 22(5), 397-400.
- Muhammad U., Hamidi A. A., Mohd S. and Yusoff, 2010. Variability of Parameters Involved in Leachate Pollution Index and Determination of LPI from Four Landfills in Malaysia. *International Journal of Chemical Engineering*, 2010, 56-61.
- Neczaj E., Okoniewska E., and Malgorzata K. (2005). Treatment of landfill leachate by sequencing batch reactor. *Desalination*, 185, 357–362.
- Nora K. (2006) Assessment of Aeration and Leachate Recirculation In Open Cell Landfill Operation With Leachate Management Strategies. Unpublished Master dissertation, Asian Institute of Technology, School of Environment, Resources and Development Thailand.
- Nowicki, P., Pietrzak, R., and Wachowska, H. (2008). Siberian anthracite as a precursor material for microporous activated carbons. *Fuel*, 87(10), 2037-2040.
- Nurul'ain, B. J. (2007). The production and characterization of activated carbon using local agricultural waste through chemical activation process. *International journal of environment and bioenergy-research gate*, 1-24.
- O'Leary, P. R., and Walsh, P. W. (1995). *Decision Maker's Guide to Solid Waste Management, Volume II. Solid and Hazardous Waste Education Center, University of Wisconsin, Milwaukee.*
- Oller I., Malato S., and Sánchez-Pérez J.A. (2011). Combination of advanced oxidation processes and biological treatments for wastewater decontamination—A review. *Science of the Total Environment*, 409, 4141–4166.
- Öman, C. B., and Junestedt, C. (2008). Chemical characterization of landfill leachates—400 parameters and compounds. *Waste management*, 28(10), 1876-1891.

- Othman, E., Yusoff, M. S., Aziz, H. A., Adlan, M. N., Bashir, M. J., and Hung, Y. T. (2010). The Effectiveness of Silica Sand in Semi-Aerobic Stabilized Landfill Leachate Treatment. *Water*, 2(4), 904-915.
- Othman, F., Ni'am, M. F., Sohaili, J., and Fauzia, Z. (2007). Electrocoagulation technqeu in enhancing COD and suspended solids removal to improve wastewater quality. *Water Science & Technology*, 56(7), 47-53.
- Peters, T. A. (1998). Purification of landfill leachate with membrane filtration. *Filtration & separation*, 35(1), 33-36.
- Pokhrel, D., and Viraraghavan, T. (2005). Municipal solid waste management in Nepal: practices and challenges. *Waste Management*, 25(5), 555-562.
- Prahas, D., Kartika, Y., Indraswati, N., and Ismadji, S. (2008). Activated carbon from jackfruit peel waste by H<sub>3</sub>PO<sub>4</sub> chemical activation: pore structure and surface chemistry characterization. *Chemical Engineering Journal*, 140(1), 32-42.
- Qu, Y., Sun, J., Li, F., Zhang, C., and Zhou, Q. (2009, June). Feasibility Study on Adsorption of PFOA from Reuse Water by Powdered Activated Carbon. In *Bioinformatics and Biomedical Engineering, 2009. ICBBE 2009. 3rd International Conference on* (pp. 1-3). IEEE.
- Quarterly Metals Report January 2015 Analysis & forecasts for Base & Precious Metals, Iron Ore & Steel.
- Raghab, S. M., El Meguid, A. M. A., and Hegazi, H. A. (2013). Treatment of leachate from municipal solid waste landfill. *HBRC Journal*, 9(2), 187-192.
- Rajeshwar, K., and Ibanez, J. G. (1997). *Environmental electrochemistry: Fundamentals and applications in pollution sensors and abatement*. Academic Press.
- Rao, N. N., Somasekhar, K. M., Kaul, S. N., and Szpyrkowicz, L. (2001). Electrochemical oxidation of tannery wastewater. *Journal of Chemical Technology and Biotechnology*, 76(11), 1124-1131.
- Ren, L., Siegert, M., Ivanov, I., Pisciotta, J. M., and Logan, B. E. (2013). Treatability studies on different refinery wastewater samples using high-throughput microbial electrolysis cells (MECs). *Bioresource technology*, 136, 322-328.
- Renoua S., Givaudan J.G., Poulain S., Dirassouyan F., and Moulin P., 2008. Landfill leachate treatment: Review and opportunity. *Journal of Hazardous Materials*, 150(3), pp. 468-493.
- Rengaraj, S., Moon, S. H., Sivabalan, R., Arabindoo, B., and Murugesan, V. (2002). Agricultural solid waste for the removal of organics: adsorption of phenol from water and wastewater by palm seed coat activated carbon. *Waste Management*, 22(5), 543-548.

- Robinson H. D., and Grantham G. (1988). The treatment of landfill leachates in on-site aerated lagoon plants: experience in Britain and Ireland. *Water Research*, 22, 733-747.
- Rubio J., Souza M.L., and Smith R.W. (2002). Overview of flotation as a wastewater treatment technique. *Minerals Engineering*, 15, 139–155.
- Rivas, F.J, Beltran, F, Carvalho, F, Acedo, B. and Gimeno, O. (2004). Stabilized leachate: sequential coagulation-flocculation + chemical oxidation process. *Journal of Hazardous Materials B116*, pp. 95-102.
- Rivera-Utrilla, J., Méndez-Díaz, J., Sánchez-Polo, M., Ferro-García, M. A., and Bautista-Toledo, I. (2006). Removal of the surfactant sodium dodecylbenzenesulphonate from water by simultaneous use of ozone and powdered activated carbon: Comparison with systems based on O<sub>3</sub> and O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>. *Water research*, 40(8), 1717-1725.
- Saito, N., Aoki, K., Usui, Y., Shimizu, M., Hara, K., Narita, N., ... and Endo, M. (2011). Application of carbon fibers to biomaterials: a new era of nano-level control of carbon fibers after 30-years of development. *Chemical Society Reviews*, 40(7), 3824-3834.
- Schrank, S. G., José, H. J., Moreira, R. F. P. M., and Schröder, H. F. (2004). Elucidation of the behavior of tannery wastewater under advanced oxidation conditions. *Chemosphere*, 56(5), 411-423.
- Shivayogimath, C. B., and Jahagirdar, R. (2013). TREATMENT OF SUGAR INDUSTRY WASTEWATER USING ELECTROCOAGULATION TECHNIQUE. *International Journal of Research in Engineering and Technology*, 262-265.
- Sir M., Podhola M., Patočka T., Honzajková Z., Kocurek P., Kubal M., and Kura M. (2012). The effect of humic acids on the reverse osmosis treatment of hazardous landfill leachate. *Journal of Hazardous Materials*, 207–208, 86–90.
- Smil, V. (2000). Phosphorus in the environment: natural flows and human interferences. *Annual review of energy and the environment*, 25(1), 53-88.
- Spellman, F. R. (2013). *Handbook of water and wastewater treatment plant operations*. CRC Press.
- Srivastava, S. K., Gupta, V. K., Mohan, D., and Pant, N. (1993). Removal of COD from reclaimed rubber factory effluents by using the activated carbon (developed from fertilizer waste material) and activated slag (developed from the blast furnace waste material)- a case study. *Fresenius Environmental Bulletin*, 2(7), 394-401.

- Szpyrkowicz, L., Kaul, S. N., and Neti, R. N. (2005). Tannery wastewater treatment by electro-oxidation coupled with a biological process. *Journal of Applied Electrochemistry*, 35(4), 381-390.
- Thörneby, L., Hogland, W., Stenis, J., Mathiasson, L., and Somogyi, P. (2003). Design of a reverse osmosis plant for leachate treatment aiming for safe disposal. *Waste management & research*, 21(5), 424-435.
- Tubtimthai, O. (2003). Landfill lysimeter studies for leachate characterization and top cover methane oxidation (Doctoral dissertation, Asian Institute of Technology).
- Timur H., Ozturk I. (1999). Anaerobic Sequencing Batch Reactor Treatment of Landfill Leachate. *Water Research*, 33, 3225-3230.
- Tränkler, J., Visvanathan, C., Chiemchaisri, C. H. A. R. T., and Shöll, W. (2005). The open cell landfill-a suitable approach for landfill design and operation in the tropical region. In *Proceedings Sardinia*.
- Trebouet D., Schlumpf J. P., Jaouen P., and Quemeneur F. (2001). Stabilized Landfill Leachate Treatment by Combined Physicochemical–Nanofiltration Processes. *Water Research*, 35, 2935–2942
- Tsai, C. T., Lin, S. T., Shue, Y. C., and Su, P. L. (1997). Electrolysis of soluble organic matter in leachate from landfills. *Water research*, 31(12), 3073-3081.
- Tzoupanos, N.D. and Zouboulis, A.I. (2010). Characterization and application of novel coagulant reagent (polyaluminium silicate chloride) for the post treatment of landfill leachates. *Water Treatment Technologies for the Removal of High Toxicity Pollutants*, pp. 247-252.
- Un, U.T., Ugur, S., Koparal, A.S., and Ogutveren, U.B., (2006) Electrocoagulation of olive mill wastewaters. *Separation and Purification Technology* 52(1), 136-141.
- Ushikoshi K., Kobayashi T., Uematsu K., Toji A., Kojima D., and Matsumoto K. (2002). Leachate treatment by the reverse osmosis system. *Desalination*, 150, 121-129
- Uygur A., and Kargı F. (2004). Biological nutrient removal from pre-treated landfill leachate in a sequencing batch reactor. *Journal of Environmental Management*, 71, 9–14.
- Violet, A. O. (2013). Ozonation of biologically treated landfill leachate. Master's dissertation, Faculty of Bioscience Engineering. GENT University, Belgium.
- Walker, G. M., and Weatherley, L. R. (1999). Biological activated carbon treatment of industrial wastewater in stirred tank reactors. *Chemical Engineering Journal*, 75(3), 201-206.
- Wang, G., Li, W., Huang, L., and Gao, Y. (2010, June). Study on Active Carbon as Emergency Treatment of Songhua River Polluted by Nitrobenzene.



InBioinformatics and Biomedical Engineering (iCBBE), 2010 4th International Conference on (pp. 1-3). IEEE.

- Wei L., Qixing Z., and Tao H., 2010. Removal of Organic Matter from Landfill Leachate by Advanced Oxidation Processes: A Review. *International Journal of Chemical Engineering*, 2010, 46-55.
- Welander, U., Henrysson, T., and Welander, T. (1997). Nitrification of landfill leachate using suspended-carrier biofilm technology. *Water Research*, 31(9), 2351-2355.
- Williams, C. J. (2005). Characterization of the spatial and temporal controls on soil moisture and streamflow generation in a semi-arid headwater catchment. Doctoral dissertation, Boise State University, United States.
- Wu, J. J., Wu, C. C., Ma, H. W., and Chang, C. C. (2004). Treatment of landfill leachate by ozone-based advanced oxidation processes. *Chemosphere*, 54(7), 997-1003.
- Yıldız, Y. Ş., Koparal, A. S., and Keskinler, B. (2008). Effect of initial pH and supporting electrolyte on the treatment of water containing high concentration of humic substances by electrocoagulation. *Chemical Engineering Journal*, 138(1), 63-72.
- Zhang C., Wang Y. (2009). Removal of dissolved organic matter and phthalic acid esters from landfill leachate through a complexation–flocculation process. *Waste Management*, 29, 110–116
- Zhang, H., Zhang, D., and Zhou, J. (2006). Removal of COD from landfill leachate by electro-Fenton method. *Journal of hazardous materials*, 135(1), 106-111.
- Zhao R., Novak J. T., and Goldsmith C. D. (2012). Evaluation of on-site biological treatment for landfill leachates and its impact: A size distribution study. *Water research*, 46, 3837-3848.