

# **UNIVERSITI PUTRA MALAYSIA**

KINETICS AND PERFORMANCE OF SEWAGE SLUDGE TREATMENT USING LIQUID STATE BIOCONVERSION IN CONTINUOUS BIOREACTOR

# **ROSHANIDA BINTI A. RAHMAN**

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# DOCTOR OF PHILOSOPHY UNIVERSITI PUTRA MALAYSIA

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By

**ROSHANIDA BINTI A. RAHMAN** 

Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in Fulfilment of the Requirements for the Degree of Doctor of Philosophy

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# UPM

DEDICATION

TO MY BELOVED FAMILY

Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfilment of the requirements for the degree of Doctor of Philosophy

#### KINETICS AND PERFORMANCE OF SEWAGE SLUDGE TREATMENT USING LIQUID STATE BIOCONVERSION IN CONTINUOUS BIOREACTOR

By ROSHANIDA BINTI A. RAHMAN

December 2009

Chairman: Professor Dr Fakhru'l-Razi Ahmadun, PhD

#### **Faculty: Engineering**

Liquid state bioconversion (LSB), a novel biodegradation, bioseparation, biosolids accumulation and biodewatering process was applied for sewage sludge treatment. The LSB process has been proven to be non hazardous, safe and environmentally friendly method for ultimate sludge management and disposal. The study was developed by using mixed fungi of *Aspergillus niger* and *Penicillium corylophilum* to treat sewage sludge in a LSB bioreactor. Results of the LSB process performance in previous studies were excellent; however the studies were only conducted on a batch system. The shortfall of the LSB batch process was identified when the LSB process was about to be applied in an actual wastewater treatment plant. The continuous process is an alternative treatment to be applied due to its advantages to handle continuous sewage sludge in the wastewater treatment plant. Therefore, this research

was conducted in order to study the LSB process on the continuous system in terms of kinetic coefficients determination, process performance and process optimisation. For the continuous LSB process, a mathematical model was developed from the basic principles of material balance based on Monod equation. By investigating the kinetics of substrate utilisation and biomass growth, the kinetic coefficients of Y, K<sub>d</sub>, K<sub>s</sub> and  $\mu_{max}$  were found to be 0.79 g VSS g COD<sup>-1</sup>, 0.012 day<sup>-1</sup>, 1.78 g COD L<sup>-1</sup> and 0.357 day<sup>-1</sup>, respectively. In addition, the LSB performance was analysed by employment of the adapted fungi on a continuous basis to evaluate the bioconversion performance, bioseparation and dewaterability characteristics of sewage sludge at different hydraulic retention times (HRTs). The evaluation of the performance of LSB continuous process showed an improvement in the percentage of MLSS (mixed liquor suspended solids), COD (chemical oxygen demand), turbidity and protein in supernatant from 87 to 98%, 70 to 93%, 97 to 99% and 44 to 82%, respectively compared to the untreated sludge. The characteristics of the treated sludge from LSB continuous process in terms of settleability and dewaterability showed that the process was highly influenced by fungi entrapment with an increase of biosolids accumulation at 80% and filterability improved from 76 to 97%. The sludge volume index (SVI) in the range of 34 to 43 obtained from the treated sludge showed a good indicator of compressibility and settleability of the sludge. The LSB continuous process was modelled and analysed using response surface methodology (RSM) for optimisation purposes. Two operating factors namely HRTs and substrate influent concentrations  $(S_0)$  were optimised in terms of sewage sludge dewaterability. The optimisation result showed that the optimum values were obtained at 3.62 days and

10.12 g L<sup>-1</sup> of HRT and S<sub>0</sub>, respectively. The results were verified at a pilot scale bioreactor using the data obtained from the optimisation process. The final biosolids accumulation of 6% (w/w) obtained from the initial  $\sim$ 1% (w/w) of the untreated sludge shows that the LSB continuous process enhanced the dewaterability and hence, provide better waste management.



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk ijazah Doktor Falsafah

#### KINETIK DAN PRESTASI RAWATAN ENAPCEMAR MENGGUNAKAN BIOPENUKARAN KEADAAN CECAIR DALAM BIOREAKTOR SELANJAR

Oleh

**ROSHANIDA BINTI A. RAHMAN** 

**Disember 2009** 

Pengerusi: Profesor Dr Fakhru'l-Razi Ahmadun, PhD Fakulti: Kejuruteraan

Biopenukaran keadaan cecair (LSB) merupakan suatu proses baru bagi biodegradasi, biopemisahan, pengumpulan biopepejal dan biopenyahcairan telah digunakan untuk rawatan enapcemar. Proses LSB telah dibuktikan sebagai kaedah yang tidak berbahaya, selamat dan mesra alam bagi pengurusan dan pembuangan enapcemar akhir. Kajian ini telah dibangunkan dengan menggunakan campuran dua fungus iaitu *Aspergillus niger* dan *Penicillium corylophilum* untuk merawat sisa enapcemar di dalam sebuah bioreaktor LSB. Keputusan bagi prestasi proses LSB dalam kajiankajian terdahulu amatlah memberangsangkan, namun, kajian hanya dijalankan dalam sistem kelompok. Kekurangan yang dikenalpasti dalam proses berkelompok LSB adalah apabila proses tersebut hendak dibangunkan di loji rawatan air sisa yang

sebenar. Proses selanjar merupakan rawatan alternatif yang boleh digunakan bagi mengatasi kekurangan tersebut disebabkan kelebihannya dalam menangani enapcemar selanjar yang terdapat di loji rawatan air sisa. Oleh yang demikian, kajian ini dijalankan bagi mengkaji proses LSB pada sistem selanjar dari segi untuk mendapatkan pekali kinetik, mengkaji proses prestasi dan juga proses pengoptiman. Bagi proses LSB selanjar, satu model matematik telah dibangunkan daripada prinsip asas imbangan jisim berdasarkan persamaan Monod. Daripada kajian kinetik ke atas penggunaan substrat dan pertumbuhan biojisim, pekali kinetik bagi Y, K<sub>d</sub>, K<sub>s</sub>, dan  $\mu_{max}$  diperolehi masing-masing pada 0.79 g VSS g COD<sup>-1</sup>, 0.012 hari<sup>-1</sup>, 1.78 g COD L<sup>-1</sup> dan 0.357 hari<sup>-1</sup>. Di samping itu, prestasi LSB telah dianalisa dengan penggunaan fungus teradaptasi pada asas selanjar untuk menilai prestasi biopenukaran, biopemisahan dan ciri penyahcairan sisa enapcemar pada masa tahanan hidraulik (HRT) yang berbeza. Penilaian ke atas prestasi proses selanjar LSB telah menunjukkan peningkatan di dalam peratusan MLSS (campuran cecair pepejal terampai), COD (keperluan oksigen kimia), kekeruhan dan protein di dalam supernatan masing-masing daripada 87 kepada 98%, 70 kepada 93%, 97 kepada 99% dan 44 kepada 82%, berbanding dengan enapcemar tidak terawat. Ciri-ciri enapcemar terawat daripada proses selanjar LSB dari segi kebolehmendapan dan penyahcairan telah menunjukkan bahawa proses ini sangat dipengaruhi oleh pemerangkapan fungus dengan peningkatan pengumpulan biojisim pada 80% dan kebolehtelapan daripada 76 kepada 97%. Nilai indeks isipadu enapcemar (SVI) di antara 34 hingga 43 telah diperolehi daripada enapcemar terawat menunjukkan petanda yang baik ke atas kebolehmampatan dan kebolehmendapan enapcemar tersebut. Proses selanjar LSB

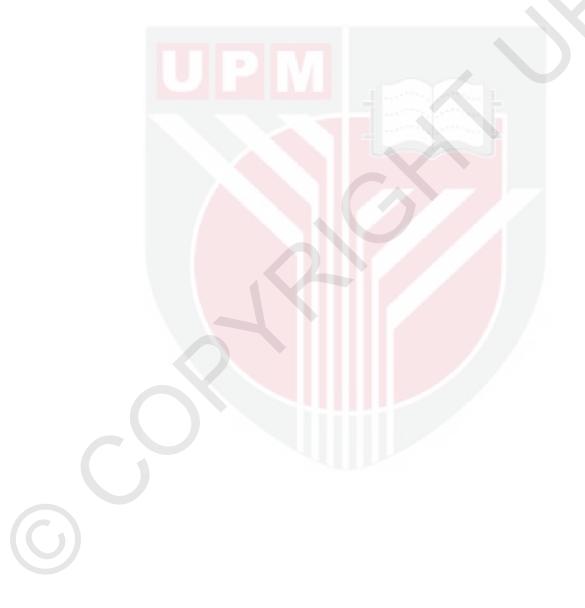
telah dimodelkan dan dianalisa dengan menggunakan kaedah rekabentuk permukaan (RSM) bagi tujuan pengoptiman. Dua faktor operasi iaitu HRTs dan kepekatan subtrat awalan (S<sub>0</sub>) telah dioptimakan dari segi kebolehnyahcairan enapcemar. Hasil pengoptiman menunjukkan HRT dan S<sub>0</sub> masing-masing mencatatkan nilai pada 3.62 hari dan 10.12 g L<sup>-1</sup>. Keputusan tersebut telah disahkan pada bioreaktor skala loji dengan menggunakan data yang diperolehi daripada proses pengoptiman. Sebanyak 6% (w/w) pengumpulan biojisim akhir telah diperolehi daripada nilai awalan sebanyak ~1% (w/w) enapcemar tidak terawat telah menunjukkan bahawa proses selanjar LSB telah meningkatkan kebolehnyahcairan dan seterusnya dapat memberi faedah kepada pengurusan sisa yang lebih baik.

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I certify that a Thesis Examination Committee has met on 23<sup>rd</sup> December 2009 to conduct the final examination of Roshanida Binti A. Rahman on her Doctor of Philosophy thesis entitled "Kinetics and Performance of Sewage Sludge Treatment using Liquid State Bioconversion in Continuous Bioreactor" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U. (A) 106] 15 March 1998. The Committee recommends that the student be awarded the Doctor of Philosophy.

Members of the Thesis Examination Committee were as follows:

#### Azni Idris, PhD

Professor Faculty of Engineering Universiti Putra Malaysia (Chairman)

#### **Robiah Yunus, PhD**

Associate Professor Faculty of Engineering Universiti Putra Malaysia (Internal Examiner)

#### Tey Beng Ti, PhD

Associate Professor Faculty of Engineering Universiti Putra Malaysia (Internal Examiner)

#### K.B Ramachandran, PhD

Professor Indian Institute of Technology (IIT) Madras India (External Examiner)

#### **BUJANG BIN KIM HUAT, PhD**

Professor and Deputy Dean School of Graduate Studies Universiti Putra Malaysia

Date: 12 April 2010

This thesis submitted to the Senate of Universiti Putra Malaysia has been accepted as fulfilment of the requirement for the degree of Doctor of Philosophy. Members of the Supervisory Committee were as follows:

## Fakhru'l-Razi Ahmadun, PhD

Professor Faculty of Engineering Universiti Putra Malaysia (Chairman)

#### Norhafizah Abdullah, PhD Associate Professor Faculty of Engineering Universiti Putra Malaysia

(Member)

# Salmiaton Ali, PhD

Associate Professor Faculty of Engineering Universiti Putra Malaysia (Member)

# HASANAH MOHD. GHAZALI, PhD

Professor and Dean School of Graduate Studies Universiti Putra Malaysia

Date: 13 May 2010

### DECLARATION

I declare that the thesis is my original work except for quotations and citations which have been duly acknowledged. I also declare that it has not been previously and is not concurrently submitted for any other degree at Universiti Putra Malaysia or at any other institution.



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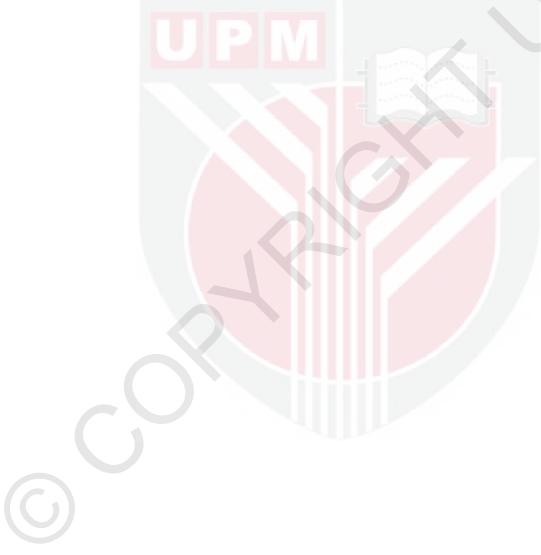
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# LIST OF ABBREVIATIONS

А	Area of the filter paper, $m^2$
Adj R <sup>2</sup>	Adjusted R <sup>2</sup>
ANOVA	Analysis of variance
APHA	Air Pollution Health Association
COD	Chemical Oxygen Demand
COD <sub>sup</sub>	COD removal in supernatant
CSTR	Completely stirred tank reactor
CV	Coefficient of Variation
D	Dilution rate, day- <sup>1</sup>
D <sub>max</sub>	Maximum dilution rate
F-test	Test for comparing model variance with residual variance
HRT	Hydraulic retention time, day
IWK	Indah Water Konsortium
Κ	Maximum specific substrate utilisation rate, g COD g VSS <sup>-1</sup> day <sup>-1</sup>
$K_d$	decay rate constant, day <sup>-1</sup>
$K_s$	Limiting substrate concentration at which $\mu$ is half $\mu_{max}$ , g COD L <sup>-1</sup>
LOF	Lack of Fit
LSB	Liquid State Bioconversion
MLSS	Mixed Liquor Suspended Solids
MLSS <sub>sup</sub>	MLSS removal in supernatant
MLVSS	Mixed Liquor Volatile Suspended Solids
OD	Optical Density
OLR	Organic Loading Rate, g COD L <sup>-1</sup> d <sup>-1</sup>
Р	Pressure of filtration, N m <sup>-2</sup>
PDA	Potato Dextrose Agar
Prob>F	Probability of seeing the observed F value if the null hypothesis was
	true

P-value	Probability value
q	Specific substrate utilization rate, g COD g VSS <sup>-1</sup> day <sup>-1</sup>
Q	Flow rate, L day <sup>-1</sup>
r	Specific resistance to filtration, m kg <sup>-1</sup>
$R^2$	A measure of the amount of variation around the mean
R <sub>m</sub>	Resistance on the medium, m <sup>-1</sup>
rpm	revolution per minute
RSM	Response Surface Methodology
$S_0$	Substrate influent, g COD L <sup>-1</sup>
S <sub>removal</sub>	Substrate removal, g COD L <sup>-1</sup>
SD	Standard Deviation
SEM	Scanning Electron Microscope
Sp.	Species
SRF	Specific Resistance to Filtration
SRT	Solid retention time, day
SSB	Solid State Bioconversion
SSV	Settled Sludge Volume, mL L <sup>-1</sup>
STP	Sewage Treatment Plant
SVI	Sludge Volume Index
t	Filtration time, sec
t	Time, day <sup>-1</sup>
V	Volume of filtration, m <sup>3</sup>
V	Reactor volume, L
VSS/SS	MLVSS to MLSS ratio
vvm	volume per volume of substrate per minute
v/v	volume/volume
w/v	weight/volume
$X, X_e$	Biomass concentration (effluent), g VSS L <sup>-1</sup>
$X_0$	Biomass in the influent, g VSS L <sup>-1</sup>
$X_1$	Hydraulic retention time (HRT)

$X_2$	Substrate influent (S <sub>0</sub> )
$X_{\text{eff}}$	Effluent biomass concentration, g VSS L <sup>-1</sup>
Y	Growth yield coefficient, g VSS g COD <sup>-1</sup>
c*	Weight of dry solids per volume of filtrate, kg m <sup>-3</sup>
μ	Viscosity of filtrate, Ns m <sup>-2</sup>
μ	Specific growth rate, day <sup>-1</sup>
θ	HRT
$\mu_{max}$	Maximum specific growth rate, day <sup>-1</sup>
2FI	Two factor interaction

C

#### **CHAPTER 1**

#### **INTRODUCTION**

#### 1.1 Background of Study

Wastewater treatment plants are considered accomplished when impurities and organic content in liquid form were transformed into solid or sludge form and followed by separation of the sludge from the liquid. The solids or sewage sludge is produced as a slurry byproduct of wastewater treatment plant (O'Kelly, 2005; Mendez et al., 2005; Uggetti et al., 2009). On average, the wastewater treatment plant is estimated to generate at about 40 to 50 g dry weight of sewage sludge per person per day and up to 60 g dry weight when incorporating a secondary treatment step (Sanchez et al., 2007; Fuentes et al., 2008). For many years, wastewater treatment plants have produced a significant increment on sewage sludge production due to an increase in civilisation, urban development and limitations in the standard of wastewater and biosolids disposal (Metcalf and Eddy, Inc. 2004). A large amount of sludge is currently generated rapidly around the world and has not stopped increasing (Romdhana et al., 2009; Hong et al., 2009). However, sewage sludge management and disposal facilities are costly and usually represent nearly 60% of the construction cost of a wastewater treatment plant and 50% of the operating cost (Peavy et al., 1985; Xing et al., 2003; Nevens et al., 2004; Cleverson et al., 2007). As a result, proper and effective sewage sludge management is needed in order to overcome this serious environmental issue.

A reduction of sewage sludge volumes can reduce the cost significantly especially for its transportation and disposal. Therefore, dewatering process is necessary to be conducted in order to reduce the moisture content of sludge. Many previous works have been identified that dewatering of sludge is one of the most costly and least understood process due to the complexity and the dynamic of the sludge matrix (Katsiris and Kouzeli-Katsiri, 1987; Bruus *et al.*, 1992; Neyens *et al.*, 2004). Sludge from sewage treatment plant usually contains less than 1% (w/w) of mixed liquor suspended solid (MLSS). Hence, the sewage sludge contains 99% or more of water. Sewage sludge which is normally considered as biological sludge is relatively hard to be dewatered compared to primary sludge in the preliminary treatment of wastewater (Chang *et al.*, 2001; Curvers *et al.*, 2009). This is probably due to the mixture of the particle, microorganisms, colloids and organic polymer in the sludge (Jorand *et al.*, 1995; Novak *et al.*, 2003).

The water within the solid compound in the sludge have different properties in terms of vapour pressure, enthalpy, entropy, viscosity, density, solid-liquid chemical interaction and many other parameters (Katsiris and Kaouzeli-Katsiri, 1987; Vaxelaire and Cezac, 2004; Northcott *et al.*, 2005). Current practices use various mechanical techniques for dewatering such as filtration, squeezing, capillary action, vacuum withdrawal and centrifuge. All of these conventional sludge treatment and dewatering technologies need intensive consumption of

energy and they are costly (Uggetti *et al.*, 2009). The cheapest method involved is the use of drying beds or lagoon but it still depends on availability of land (Hwa and Jeyaseelan, 1997). Besides the conventional process, effective dewatering requires treatment from microorganisms due to the fact that majority of these microbes live in aggregates such as films, flocs and sludges (Neyens *et al.*, 2004). Therefore, an alternative dewatering process that is environmentally friendly and safe using microorganism is a suitable method for future waste management strategy (Alam *et al*, 2003b).

Bioremediation which involves the use of microbial treatment to degrade waste contaminants has received great attention in solving the increase of sewage sludge generation. This method has been used to convert sewage sludge into valuable product or energy and to clean up a polluted environment originating from wastewater treatment plant system (Liu and Tay, 2004; Larsen et al., 2009; Xia et al., 2008; Ichinari et al., 2008; Pramanik and Khan, 2008). The employment of microbial treatment through liquid state bioconversion (LSB) process is one of the alternative options to solve the increase in sludge generation and disposal (Alam, 2002; Hind, 2008). In the past, the LSB technique functions as a multiple treatment for sewage sludge, including biodegradation, bioseparation, biodewatering and biosolids accumulation and it has also produced environmentally friendly ultimate sludge disposal (Alam *et al.*, 2001a; 2001b; 2003a; 2004a; Alam and Fakhru'l-Razi, 2003; Hind, 2008). Biodegradation and bioconversion processes involve a transformation of dissolved and organic substances by microbial communities to biomass and evolve gases. Among microbial communities, it is discovered that the fungi play

an important role in optimising waste bioconversion from secondary sludge (Molla, 2002; Alam *et al.*, 2003b). The filamentous fungi used in the LSB process is immobilised in the particle of sludge by a formation of flocs; therefore increasing the separation and filtration process significantly (Alam, 2002; Sarkar, 2006; Hind, 2008).

The LSB process of sewage treatment plant sludge has been conducted through several approaches at bench scale in a shake flask and a fermenter under sterilised condition (Alam, 2002). Subsequently, the microbial treatment of sewage treatment plant sludge or activated sludge has been evaluated by LSB batch process under non-sterilised, controlled conditions in terms of biodegradation and biodewaterability (Sarkar, 2006). Furthermore, another LSB batch process approach under natural (non-controlled) conditions has been discussed by Fakhru'l-Razi and Molla (2007) in terms of bioseparation and dewaterability using cultured inocula. Finally, the LSB batch process has been evaluated and compared between the bench and the large scale under nonsterilised, controlled conditions in terms of biodegradation, bioseparation and dewaterability (Hind, 2008). For the composting of sewage sludge or biosolids, a solid state bioconversion (SSB) process of sludge product from the LSB process has been proposed by Molla (2002). As a result, this LSB process has proven not only successful in enhancing the biodegradation, bioseparation and dewaterabilty of treated sludge but converting it into valuable biomass for compost purposes through the SSB process.

#### **1.2 Problem Statement**

Sewage sludge treatment and disposal, which are mainly of organic matter, is one of the most serious challenges environmental problems all over the world. Malaysia is not an exception where the management of the increasing volume of sewage sludge has been one of the primary environmental issues (Zain *et al.*, 2001). The increasing of the sludge volume throughout the country means a serious problem to the water resources, public health and the environment. In Malaysia, Indah Water Konsortium (IWK) Sdn. Bhd. operates and maintains most of the sewerage services. Presently, Malaysia produces approximately 7.5 million cubic meters of sewage sludge annually throughout the country. Indah Water also had spent more than RM 66 million for the sludge handling and management purpose. It is estimated that at least another RM 3.1 billion will be required to provide adequate sludge facilities by 2035 (IWK, 2007). The same increasing trend is observed all over the world, which shows the need for effective solutions for sludge management and disposal in order to overcome this problem.

An alternative sewage sludge treatment and disposal has been introduced by Alam (2002) and Molla (2002) through liquid state bioconversion (LSB) and solids states bioconversion (SSB) processes, respectively by using locally isolated fungi. The LSB is a biodegradation, bioseparation, biodewatering and biosolids accumulation process of the sewage sludge, while the SSB process produced environmentally friendly ultimate sewage sludge disposal through composting. The development of LSB process using a batch system has been studied by Alam (2002), Sarkar (2006) and Hind (2008). The LSB batch process performance also has been optimised using bench and pilot scale process and tremendous sludge volume reduction occurs by enhancing the settling and dewatering characteristics of sewage sludge (Hind, 2008). However, the main drawback of the batch process is in term of inoculums preparation. The preparation of inoculums is quite tedious due to the usage of pure culture from the mixed fungi. For every new cycle of the batch process, the inoculums has to be sub-cultured and prepared fresh before the inoculation process onto the sewage sludge. Furthermore, every inoculation for every batch process needs at least 3 days for the acclimatisation of the fungi. As a result, the process will not be practical to be implemented at an actual wastewater treatment plant which the sewage sludge is produced in huge amounts everyday.

From the economical viewpoint, the LSB batch process is not economic to be practiced at an actual treatment plant. Besides the cost of the inoculums for every cycle of the batch process, the operation cost also needs to be accounted. Every batch needs an operator to take out the LSB sludge before starting a new cycle. The process also includes feeding time for inoculums which is twice perday for 3 days for every batch. Although batch reactor is excellent on handling difficult materials and slow reactions process, however it is not economical to run the LSB process for sewage sludge treatment which is a waste and produced in a bulk at an actual wastewater treatment plant in the batch mode. Besides, a large volume of bioreactor is needed to cater the huge amount of sewage sludge at one time for batch process. To overcome the shortage from this LSB batch process in order to apply it at an actual wastewater treatment plant, the LSB continuous process is proposed in this study. A continuously stirred tank reactor proposed for this study is an adaptation of a batch reactor in which the sewage sludge is added continuously to the bioreactor while the treated sewage sludge is removed at the same time. The advantage of the continuous process is one time inoculation procedure only needed for 3 days time and re-inoculation is not required. Therefore the cost for the inoculums and operator can be reduced significantly. A smaller reactor is needed compared to batch due to the continuously flowing at the wastewater treatment plant. The output of the treated sewage sludge also can be manipulated because the continuous reactor can be altered by varying the hydraulic retention time, thus increases operating flexibility for the wastewater treatment plant operators. Besides, less operation down time is required due to no necessity for plant shut down to start the new cycle as needed by the batch process.

Despite the overwhelming performance results on the LSB process from previous studies, information on the kinetics aspect has not yet been investigated. In a continuous process, certainly some of the parameters, condition and kinetics are different compared to the batch process. In the continuous process, an equilibrium concentration of substrate is established independently from microbial density and time which allow microbes to grow at a steady state by maintaining stable environment growth conditions and hence the same physiological state. Therefore, in an ideal continuous process, more precise and statistically relevant data can be collected compared to the batch culture (Kovarova-kovar and Egli, 1998). Knowledge of kinetic coefficients is essential for biological wastewater system design, control process and optimisation of operational conditions (Nakhla *et al.*, 2006). Consequently, this research is a continuation from a previous study on the LSB process in order to develop the LSB continuous process in terms of kinetic coefficients, performances, evaluation and optimisation of the operating parameters.

#### 1.3 Objectives of Study

Based on the problem statement as discussed above, the objectives of this study are:

- 1. To develop a kinetics model for LSB process in a continuous bioreactor.
- 2. To evaluate the performance of sewage sludge using LSB continuous process.
- To optimise the LSB continuous process of sewage sludge using Response Surface Methodology (RSM).

#### 1.4 Outline and Scope of Thesis



The content of this thesis in the following chapters is divided into four parts. The first part is the literature review discussed in Chapter 2. It describes in general about sewage treatment plant sludge and in particular the LSB process. The second part of the thesis is Chapter 3 which is a discussion on the material and methods for the LSB process and analysis. The third part of the thesis deals with the results and discussions of the study. The discussions are divided into three

chapters which are Chapter 4, 5 and 6 and are related to the objectives of the study. Each chapter has its own introduction, results, discussion and summary. The last part is the overall conclusion presented as Chapter 7 which summarises all results from the findings and discusses contribution of the thesis. The details are described as below:

- i) In Chapter 2, a general introduction on aspects of sewage treatment plant sludge, problems, management and disposal is first reviewed.
  Secondly, the sludge treatment and disposal issues in Malaysia are discussed. Finally, other bioremediation techniques as well as the LSB process as an environmentally friendly sludge management and disposal is introduced and previous findings are presented.
- ii) Chapter 3 describes the materials and methods which are considered as important procedures in operating the bioreactor of the LSB continuous process. The standard analysis procedure for the influent and effluent of the bioreactor is described as well with details explained in the Appendix A.
- iii) Chapter 4 discusses the LSB continuous process and determination of the kinetic coefficients for sewage sludge. As this is a first study on the LSB continuous process of sewage sludge by applying the fungi inoculum, it is the aim of this study to provide a good overview on the microbial growth rate and substrate utilisation rate, biomass balance, substrate balance and assumption used in order to predict the

continuous process at different hydraulic retention times. The mathematical model from the basic principles of material balance and Monod equation as introduced in Chapter 2 are used. The model used has discovered that the growth or degradation phenomena can be described satisfactory with the four coefficients of  $\mu_{max}$ , K<sub>s</sub>, Y and K<sub>d</sub>. A detailed investigation of the obtained kinetic coefficients from the developed model on the experimental data is needed in order to verify the validation of the model for future design and control development applications.

- iv) Chapter 5 evaluates the LSB continuous process on the bioconversion performance, bioseparation and dewaterability characteristics. The results involve fungi adaptation, supernatant analysis of the effluent, bioseparation and dewatering characteristics of sewage sludge at different hydraulic retention times. Discussion from the findings of the continuous basis is compared to the untreated sludge as well as the results on the batch basis by previous studies.
- v) Chapter 6 analyses the LSB continuous process from sewage sludge using statistical techniques of RSM in order to maximise the performance of the process with respect to the simultaneous effects of two operating factors (hydraulic retention times and influent substrate concentrations). Nine interrelated parameters are also evaluated as responses. The study has been conducted in order to develop a

continuous response surface of the operating factors with the hope of providing an optimal region which satisfies the operating specifications between all responses. The developed statistical model is verified with the pilot scale of experimental data.

 vi) Chapter 7 is the concluding chapter which summarises the main results from the achievable objectives, comparison between the LSB batch and the LSB continuous process and finally the advantages and importances of the LSB process. Suggestion for future research and perspectives are also briefly suggested.



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