



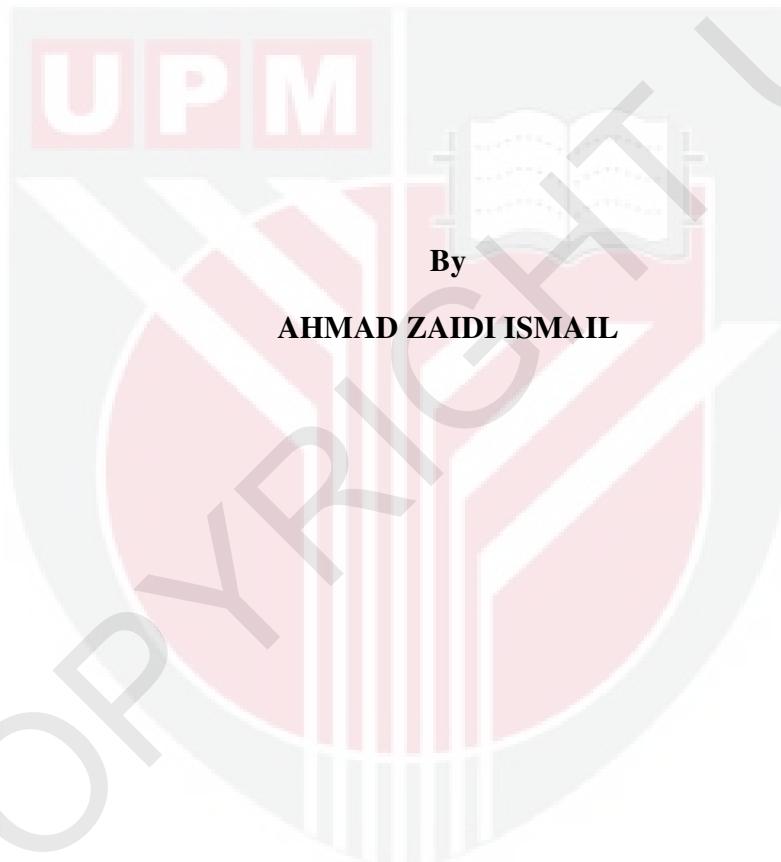
**UNIVERSITI PUTRA MALAYSIA**

**REFLUX SYNTHESIS AND PHYSICOCHEMICAL CHARACTERISATION  
OF MoVTeNbO<sub>x</sub> CATALYST FOR PROPANE OXIDATION  
INTO ACRYLIC ACID**

**AHMAD ZAIDI ISMAIL**

**FS 2011 63**

**REFLUX SYNTHESIS AND PHYSICOCHEMICAL CHARACTERISATION  
OF MoVTeNbO<sub>x</sub> CATALYST FOR PROPANE OXIDATION  
INTO ACRYLIC ACID**



**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,  
in Fulfilment of the Requirements for the Degree of Master of Science**

**November 2011**

Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfillment of  
the requirement for the degree of Master of Science

**REFLUX SYNTHESIS AND PHYSICOCHEMICAL CHARACTERISATION OF  
MoVTeNbO<sub>x</sub> CATALYST FOR PROPANE OXIDATION INTO ACRYLIC ACID**

By

**AHMAD ZAIDI ISMAIL**

**November 2011**

**Chairman: Assoc. Prof. Irmawati Ramli, PhD**

**Faculty: Science**

The abundance of propane and its low price is one of the main factors that made selective oxidation of this light alkane to acrylic acid through heterogeneous catalytic pathway receives intensive research. MoVTeNbO<sub>x</sub> a quarternary metal oxide catalyst is reported to have shown the best performance for the direct oxidation of propane to acrylic acid to this date. In this work, MoVTeNbO<sub>x</sub> catalysts were prepared by reflux method. Synthesis parameters such as reflux time and drying method were found to have profound effect on the catalyst structure and chemical properties. Spray drying was found to give precursor which upon calcinations produced better formation of M1 and M2 phase MoVTeNbO<sub>x</sub> catalyst compared to samples dried by rotary evaporation method. This is proved by the X-ray diffractogram of the samples as it shown peak at  $2\theta=6.6, 7.9, 9.0, 22.1$  and  $45^\circ$  which correspond to orthorhombic (M1) phase and  $2\theta=28.3, 36.2$  and  $50^\circ$  of hexagonal (M2) phase. Longer reflux time gave better structural

formation and higher specific surface area ( $S_{BET}$ ) thus led to a better catalyst performance of samples dried using spray dry method. Investigation on calcinations environment revealed that calcination in air followed by calcination in nitrogen flow gives better catalyst (catalyst B2). Catalyst B2 gave higher specific surface area ( $S_{BET}$ ) and oxygen removed in  $H_2$ -TPR which is  $5.3\text{ m}^2\text{g}^{-1}$  and  $2.8 \times 10^{21}\text{ atomg}^{-1}$  respectively. Thus indicates that sample B2 is an active catalyst. However calcination in air should not exceed 1 hour as longer calcination in air will impede the properties of the catalyst. Finally, washing the synthesized catalyst with hydrogen peroxide managed to eliminate the non-active M2 phase and improved the formation of the M1 phase. This is proved by a more significant X-ray diffraction patterns at  $2\theta = 6.6, 7.9, 9.0, 22.1, 27.0$  and  $45^\circ$  with absences of diffraction peaks at  $2\theta = 28.3, 36.2$  and  $50^\circ$  that related to the existence of M2 phase for after washing with  $H_2O_2$  sample (B2W). Higher  $S_{BET}$  also observed for sample B2W which is  $12.5\text{ m}^2\text{g}^{-1}$  compared to  $5.3\text{ m}^2\text{g}^{-1}$  for sample before washing (B2). The catalytic tests were done at three different reaction temperatures which are 653, 673 and 693 K. Propane conversion was found to increase when the temperature was increased up to 693 K. Catalyst obtained from a longer reflux time (72 hours) and dried using a spray dry method give a better activity which is 6.53% at 693 K compared to the catalyst obtained from a shorter reflux time (24 hours) with 4.55% or the sample dried using rotary evaporator (3.76%) at the same temperature. The catalytic test of the catalyst after washing with  $H_2O_2$  (B2W) showed very promising propane conversion (22.01 %) and higher reaction selectivity towards acrylic acid (24.21%).

Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai  
memenuhi keperluan untuk ijazah Master Sains

**SINTESIS REFLUKS DAN PENCIRIAN FIZIKOKIMIA MANGKIN  
MoVTeNbO<sub>x</sub> UNTUK PENGOKSIDAAN PROPANA KEPADA ASID AKRILIK**

Oleh

**AHMAD ZAIDI ISMAIL**

**November 2011**

**Pengerusi: Prof. Madya Irmawati Ramli, PhD**

**Fakulti: Sains**

Banyaknya sumber dan kos yang lebih murah gas asli propana adalah salah satu faktor utama yang menjadikan pengoksidaan terpilih alkana kepada asid akrilik dengan mangkin heterogen menjadi tumpuan penyelidikan secara intensif. Mangkin MoVTeNbO<sub>x</sub> oksida logam kuarternari dilaporkan telah menunjukkan prestasi yang terbaik untuk pengoksidaan langsung propana ke asid akrilik. Sintesis MoVTeNbO<sub>x</sub> dilakukan melalui kaedah refluks. Sintesis parameter seperti masa reflux dan kaedah pengeringan didapati mempunyai kesan yang mendalam kepada struktur dan sifat-sifat kimia mangkin. Pengeringan secara semburan didapati memberikan prekursor yang menghasilkan pembentukan yang lebih baik fasa M1 dan M2 MoVTeNbO<sub>x</sub> berbanding sampel yang dikeringkan dengan kaedah penyejatan. Ini dibuktikan oleh diffractogram sinar-X sampel yang menunjukkan puncak pada  $2\theta = 6.6, 7.9, 9.0, 22.1$  dan  $45^\circ$  untuk fasa ortorombik (M1) dan  $2\theta = 28.3, 36.2$  dan  $50^\circ$  untuk fasa heksagonal (M2). Masa

refluks yang lebih lama membantu dalam pembentukan struktur yang lebih baik dan luas permukaan spesifik yang lebih tinggi ( $S_{BET}$ ). Ini membawa kepada prestasi mangkin yang lebih baik untuk sampel yang dikeringkan menggunakan kaedah semburan. Persekutaran pengkalsinan mangkin secara pemanasan pada suhu yang tinggi juga mempengaruhi sifat mangkin. Pemanasan dalam persekitaran udara bebas diikuti pemanasan dalam persekitaran N<sub>2</sub> menghasilkan mangkin yang lebih baik (mangkin B2). Mangkin B2 memberikan luas permukaan spesifik yang lebih tinggi ( $S_{BET}$ ) dan oksigen yang dikeluarkan H<sub>2</sub>-TPR yang  $5.3 \text{ m}^2\text{g}^{-1}$  dan  $2.8 \times 10^{21} \text{ atom g}^{-1}$ . Ini menunjukkan bahawa mangkin B2 merupakan mangkin yang aktif. Walau bagaimanapun proses pengkalsinan dalam udara tidak boleh melebihi 1 jam. Pembasuhan dengan hidrogen peroksida berjaya menghapuskan fasa tidak-aktif M2 dan meningkatkan pembentukan fasa M1. Ini dibuktikan oleh corak pembelauan sinar-X yang lebih jelas di  $2\theta = 6.6, 7.9, 9.0, 22.1, 27.0$  dan  $45^\circ$  dan ketiadaan puncak pembelauan pada  $2\theta = 28.3, 36.2$  dan  $50^\circ$  yang berkaitan dengan kewujudan fasa M2 untuk mangkin selepas dibasuh dengan H<sub>2</sub>O<sub>2</sub> (B2W).  $S_{BET}$  yang lebih tinggi untuk mangkin B2W juga boleh dilihat iaitu  $12.5 \text{ m}^2\text{g}^{-1}$  berbanding dengan  $5.3 \text{ m}^2\text{g}^{-1}$  untuk mangkin sebelum dibasuh (B2). Ujian pemangkinan untuk tindak balas propana telah dilakukan pada tiga suhu tindak balas yang berbeza yang 653, 673 dan 693 K. Aktiviti mangkin didapati meningkat apabila suhu telah meningkat sehingga 693 K. Mangkin diperolehi dari masa refluks yang lebih lama (72 jam) dan dikeringkan menggunakan kaedah semburan memberikan aktiviti yang lebih baik iaitu 6.53% pada suhu 693 K berbanding dengan mangkin yang diperolehi dari masa refluks yang lebih singkat (24 jam) dengan aktiviti 4.55% atau sampel yang dikeringkan menggunakan kaedah

penyejatan (3.76%) pada suhu yang sama. Ujian pemangkinan selepas dibasuh dengan H<sub>2</sub>O<sub>2</sub> (B2W) menunjukkan aktiviti penukaran propane yang lebih cekap (22.01%) dan kepilihan tindak balas yang lebih tinggi ke arah pembentukan asid akrilik (24.21%).

## **ACKNOWLEDGEMENT**

In the name of Allah, the most merciful I am grateful for giving me the strength to complete this task.

I would like to take this opportunity to express my appreciation to my supervisor Associate Prof. Dr. Irmawati Ramli for her guidance, advices and help in completing the course of the project. In this opportunity, I would also like to thank Prof. Dr Wataru Ueda and his students of the Catalysis Research Centre for their helps during my attachment at Hokkaido University. The greatest thanks I convey to my parents and family as well for their continuous supports and encouragements during my study in Universiti Putra Malaysia (UPM).

Last but not least, I would like to thank all of the staffs in the Department of Chemistry UPM, for their helps and co-operation during this research. A special thanks also goes to my coursemates and all of the masters and PhD students of PutraCAT lab for their helps in my research works.

I certify that an Examination Committee has met on .....to conduct the final examination of Ahmad Zaidi Ismail on his Master of Science thesis entitled “Reflux Synthesis And Physicochemical Characterisation Of MoVTeNbO<sub>x</sub> Catalyst Used Propane Oxidation To Acrylic Acid” in accordance with Universiti Pertanian Malaysia (Higher Degree) Act 1980 and Universiti Pertanian Malaysia (Higher Degree) Regulation 1981. The Committee recommends that the student be awarded the.....



---

Noritah Omar, PhD  
Assoc. Professor and Deputy Dean  
School of Graduate Studies  
Universiti Putra Malaysia

Date:

This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfillment of the requirement for the degree of Master of Science. The members of the Supervisory Committee were as follows:

**Irmawati Ramli, PhD**

Associate Professor

Faculty of Science

Universiti Putra Malaysia

(Chairman)

**Mohamed Ibrahim Mohamed Tahir, D.Phil**

Senior Lecturer

Faculty of Science

Universiti Putra Malaysia

(Member)

**Taufiq Yap Yun Hin, PhD**

Professor

Faculty of Science

Universiti Putra Malaysia

(Member)

---

**BUJANG BIN KIM HUAT, PhD**

Professor and Dean

School of Graduate Studies

Universiti Putra Malaysia

Date:

## **DECLARATION**

I declare that the thesis is my original work except for quotation and citation which have been duly acknowledged. I also declare that if it has not been previously and is not concurrently, submitted for any other degree at Universiti Putra Malaysia or at any other institution.

**AHMAD ZAIDI ISMAIL**

Date: 29<sup>th</sup> November 2011

## TABLE OF CONTENTS

	<b>Page</b>
<b>ABSTRACT</b>	ii
<b>ABSTRAK</b>	iv
<b>ACKNOWLEDGEMENTS</b>	vii
<b>APPROVAL</b>	viii
<b>DECLARATION</b>	x
<b>LIST OF TABLES</b>	xiii
<b>LIST OF FIGURES</b>	xiv
<b>LIST OF ABBREVIATIONS</b>	xvii
 <b>CHAPTER</b>	
<b>1 INTRODUCTION</b>	
1.1 Acrylic Acid	1
1.2 Acrylic Acid Production	3
1.3 Propane as an Alternative Feedstock for Production of Acrylic Acid	5
1.4 Fundamental principles in Heterogeneous Catalysis	6
1.5 Problem statements	8
1.6 Objectives	9
<b>2 LITERATURE REVIEW</b>	
2.1 Catalytic Conversion of Propane Using Heterogeneous Catalysis Processes	10
2.2 MoVTeNbO <sub>x</sub> Catalyst	14
2.2.1 Elemental Composition	15
2.2.2 Role of Each Element in MoVTeNbO <sub>x</sub> Catalyst	16
2.2.3 Structure of the Catalyst	19
2.3 Active Sites of MoVTeNbO <sub>x</sub> Catalyst and Mechanism in Propane Oxidation to Acrylic Acid	24
2.4 Synthesis of MoVTeNbO <sub>x</sub> Catalyst	28
2.4.1 Hydrothermal method	29
2.4.2 Slurry method	30
2.4.3 Other Synthesis Method	31
2.5 Parameters	32
2.5.1 Effects of Drying Methods	32
2.5.2 Effects of Calcination Environment	33
2.5.3 Effects of Other Modification	35

<b>3 MATERIALS AND METHODS</b>	
3.1 Materials	40
3.2 Catalyst Preparation	41
3.2.1 Effect of Reflux Time and Drying Method	41
3.2.2 Effect of Calcinations Environment	42
3.2.3 Effect of Washing by Using Hydrogen Peroxide	43
3.4 Catalyst Characterization	43
3.4.1 X-ray Diffraction Analysis (XRD)	43
3.4.2 Brunnauer-Emmet-Teller surface area Analyzer (BET)	45
3.4.3 Temperature Programmed Reduction in Hydrogen (H <sub>2</sub> -TPR)	48
3.4.4 Scanning Electron Microscopy (SEM)	49
3.4.5 Inductive Coupled Plasma Atomic Emission Spectroscopy (ICP-AES)	51
3.5 Catalytic Test	52
<b>4 RESULTS AND DISCUSSION</b>	
4.1 Catalyst characterization	55
4.1.1 Effect of Reflux Time and Drying Method	55
a. X-Ray Diffraction (XRD)	55
b. Elemental composition and BET surface area	59
c. Scanning Electron Microscopy (SEM)	61
d. Temperature Programmed Reduction in Hydrogen	64
e. Catalytic Test	68
4.1.2 Effects of Calcinations Environment	71
a. X-Ray Diffraction (XRD)	71
b. Elemental composition and BET surface area	74
c. Scanning Electron Microscopy (SEM)	75
d. Temperature Programmed Reduction in Hydrogen	78
e. Catalytic Test	80
4.1.3 Catalyst Improvement by Washing in Hydrogen Peroxide	82
a. X-Ray Diffraction (XRD)	83
b. Elemental composition and BET surface area	84
c. Temperature Programmed Reduction in Hydrogen	86
e. Catalytic Test	88
4.2 Summary of catalysts characterization	93
4.3 Summary of the Catalytic Test	94
<b>5 CONCLUSION AND RECOMMENDATION FOR FUTURE RESEARCH</b>	98
<b>REFERENCE</b>	100
<b>APPENDICES</b>	
<b>BIODATA OF STUDENT</b>	106
<b>LIST OF PUBLICATIONS</b>	107