



UNIVERSITI PUTRA Malaysia

**DEVELOPMENT OF FED-BATCH CULTIVATION PROCESS FOR
ESHERICHIA COLI HARBORING SUPEROXIDE DISMUTASE**

WAN SITI ATIKAH WAN OMAR

IB 2009 17



**DEVELOPMENT OF FED-BATCH CULTIVATION PROCESS FOR
ESHERICHIA COLI HARBORING SUPEROXIDE DISMUTASE**

WAN SITI ATIKAH WAN OMAR

**MASTER OF SCIENCE
UNIVERSITI PUTRA MALAYSIA**

2009



**DEVELOPMENT OF FED-BATCH CULTIVATION PROCESS FOR
ESHERICHIA COLI HARBORING SUPEROXIDE DISMUTASE**

By

WAN SITI ATIKAH WAN OMAR

**Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia,
in Fulfilment of the Requirements for the Master of Science**

October 2009



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in the fulfilment
of the requirement for the Degree of Master of Science

**DEVELOPMENT OF FED-BATCH CULTIVATION PROCESS FOR
ESCHERICHIA COLI HARBORING SUPEROXIDE DISMUTASE**

By

WAN SITI ATIKAH WAN OMAR

October 2010

Chairman : Rosfarizan Mohamad, PhD

Institute : Bioscience

The fed-batch cultivation process for the production of the recombinant protein, superoxide dismutase (SOD) by *E. coli* BL21 (DE3) pLysS was carried out. The cultivation process for recombinant SOD (ESOD) production was optimized through several approaches and strategies. The first approach was to optimize medium and culture conditions of the ESOD culture in shake flask via conventional and the Response Surface Methodology (RSM) methods. Laboratory scale batch cultivation of ESOD was then performed using a 2 L stirred tank bioreactor (STB) in order to further optimize the medium and culture conditions. The effects of glucose concentrations (15 and 20 g/L), agitation speeds (300 – 1000 rpm) and controlled dissolved oxygen tension (DOT) via agitation speeds (20%, 50% and 80%) on the growth performance of the recombinant *E. coli* strain were investigated. In the final stage, fed-batch techniques



were applied to the process for the development of high cell density cultivation. The performance and kinetics of the ESOD fed-batch and batch cultivations were then evaluated and compared.

Plasmid harboring the SOD gene was found to be 100% stable over 200 generations in shake flask culture, which was agitated at 200 rpm and incubated at 37°C for 72 h. A 27kDa protein band representing the intracellular rSOD was detected by SDS-PAGE analysis. Optimized medium and cultural conditions through RSM approach was found at 4.89 g/L of glucose, 21.86 g/L of yeast extract and tryptone (2:1 ratio) and initial pH of 7.84. By using the optimized conditions from the RSM approach, maximum cell concentration of 7.39 g/L was achieved.

Batch cultivations were further performed using 2 L STB in order to investigate the effects of glucose and cultural conditions on the growth performance of ESOD. A concentration of 15 g/L of glucose as a carbon source showed higher maximum cell concentration (14.54 g/L) compared to 20 g/L of glucose. Growth of ESOD was inhibited at high initial glucose concentration supplied to the medium, whereas, controlled DOT via agitation speed at 20% showed the highest cell concentration (7.44 g/L) obtained as compared to other controls. However, there were no significant differences of maximum cell concentration achieved at different DOT controlled cultivations. Meanwhile, a controlled agitation speed at 500 rpm throughout cultivation exhibited a maximum cell concentration of 15.70 g/L, which was two times higher compared to other agitation speeds tested.

Due to the substrate inhibition effect that occurred in the batch cultivation, growth of ESOD and SOD production were further enhanced through constant and pH-stat fed-batch cultivation techniques. In batch and constant fed-batch, significant amount of acetic acid and glucose were found accumulated at the end of cultivation which caused to inhibit ESOD growth and SOD production. Final cell concentration in the culture was significantly improved by the application of pH-stat fed-batch cultivation technique. The maximum cell concentration obtained by such cultivation technique was 5.4 and 2.4 times higher than constant fed-batch and batch cultivation techniques, respectively. Nevertheless, total protein productivity at 0.48 g/L/h was found higher in the batch cultivation compared to fed-batch cultivation techniques owing to the extended culture period.

Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk Ijazah Master Sains

**PEMBANGUNAN PROSES PENGKULTURAN SUAPAN SESEKELOMPOK
BAGI *ESCHERICHIA COLI* PENGELUAR SUPEROKSIDA DISMUTASE**

Oleh

WAN SITI ATIKAH WAN OMAR

Oktober 2009

Pengerusi : Rosfarizan Mohamad, PhD

Institut : Biosains

Pengkulturan suapan sesekelompok protein rekombinan, superoksida dismutase (SOD) oleh *E. coli* BL21 (DE3) pLysS telah dijalankan. Proses pengoptimaan pengkulturan untuk penghasilan rekombinan SOD (ESOD) telah dijalankan dalam beberapa pendekatan dan strategi. Pada peringkat pertama, pengoptimaan media and kondisi ke atas kultur tersebut dijalankan di dalam kelalang kon dengan menggunakan kaedah konvensional dan Kaedah Permukaan Gerakbalas (RSM). Pengkulturan sekelompok skala makmal kemudian dijalankan di dalam 2 L bioreaktor pengaduk (STB) bagi pengoptimaan medium dan kondisi kultur. Kesan pertumbuhan ESOD terhadap kepekatan glukosa (15 g/L dan 20 g/L), kelajuan adukkan (300 – 1000 rpm) dan tekanan oksigen terlarut (DOT) yang dikawal melalui kelajuan adukkan (20%, 50% dan 80%) juga telah dijalankan. Pada peringkat akhir, teknik pengkulturan suapan sesekelompok telah diaplikasi dalam proses bagi pembangunan sel kultur



berketumpatan tinggi. Perkembangan dan kinetik bagi kultur suapan sesekelompok dan sekelompok ESOD telah dinilai dan dibandingkan.

Plasmid pengeluar SOD gen telah menunjukkan 100% stabil sehingga 200 generasi di dalam kultur kelalang kon dengan kelajuan adukkan pada 200 rpm dan dieram pada 37°C selama 72 jam. Jalur protein pada lebih kurang 27kDa mewakili intracellular rSOD didapati melalui analisis SDS-PAGE. Media and kondisi yang dioptimakan menggunakan RSM telah dicapai dengan menggunakan 4.89 g/L glukosa, 21.86 g/L yis ekstrak dan triptone (nisbah 2:1) dan pH awal, 7.84. Dengan menggunakan optimum media daripada pendekatan RSM ini, kepekatan maksima sel 7.39 g/L telah diperoleh.

Kultur sekelompok seterusnya dijalankan dengan menggunakan 2 L STB bagi menyelidik kesan glukosa dan kondisi kultur terhadap pertumbuhan ESOD. Glukosa 15 g/L merupakan sumber karbon telah menghasilkan kepekatan sel maksima yang lebih tinggi (14.54 g/L) berbanding glukosa 20 g/L. Pertumbuhan ESOD telah direncanakan oleh kepekatan glukosa yang tinggi pada awal medium, sementara itu, DOT 20% yang dikawal oleh kelajuan adukkan menunjukkan kepekatan sel yang paling tinggi (7.44 g/L) terhasil berbanding dengan kawalan yang lain. Bagaimanapun, tiada perbezaan ketara bagi kepekatan sel maksima yang terhasil pada kultivasi yang dikawal pada DOT yang berbeza. Di samping itu, kawalan kelajuan adukkan pada 500 rpm telah menghasilkan kepekatan sel maksima 15.7 g/L , yang mana dua kali lebih tinggi berbanding dengan kawalan adukkan lain yang diuji.

Oleh kerana kesan perencatan substrat berlaku dalam kultur sekelompok; pertumbuhan ESOD dan penghasilan SOD seterusnya ditingkatkan dengan menggunakan teknik pengkulturatan suapan sesekelompok konstan dan pH-stat. Di dalam pengkulturatan sekelompok dan suapan sesekelompok konstan, asid asetik dan glukosa telah dijumpai terkumpul sehingga akhir kultivasi yang mana membuatkan pertumbuhan ESOD dan pengeluaran SOD terencat. Kepekatan sel telah bertambah dengan ketara melalui aplikasi teknik suapan sesekelompok pH-stat. Sel maksima yang diperoleh daripada teknik ini adalah masing-masing 5.4 dan 2.4 lebih tinggi daripada teknik kultur suapan sesekelompok konstan dan kultur sekelompok. Walau bagaimanapun, produktiviti protein pada 0.48 g/L/h adalah lebih tinggi dalam kultur sekelompok kerana masa kultur yang lebih panjang dalam teknik suapan sesekelompok.

ACKNOWLEDGEMENTS

Alhamdulillah, I am truly thankful to Allah Subhanahu Wataala for giving me strength and the endless love. I also indebted to my supervisor, Prof. Madya Dr. Rosfarizan Mohamad for accepting me as her post graduate student. Without her giving me the opportunity, my study in the fermentation technology field might not be possible. I also would like to express my appreciation, from the bottom of my heart, to my co-supervisors, Prof. Dr. Arbakariya Ariff and Prof. Dr. Raha Abdul Rahim for their invaluable guidance, never ending patience, kind assistance and time. Their useful suggestions and comments of my research work have been of great help.

My gratitude also goes to Mr. Rosli, Mrs. Aluyah, Mrs. Renuga, Fadzli, Shahrul and Deela, Kak Julia, Cik Lina, Kak Yanti, Kak Azlina, Kak Siew Ling, Abang Bazli, Kak Fid, Kak Elida, Boon Hooi, Kak Suhaila, Kak Yus, Kak Alis, Kak Fuzah, Kak Sarina, Dr. Kamisah, Prof. Dr. Asma' Ismail (TNC USM), Hisham, and all my friends, seniors, staff (UPM and UiTM), and students for their help, support and encouragement.

Last but not least, I would like to take this opportunity to thank Che Pah Mohd Nor and Wan Omar Wan Ismail for being a great Mak and Ayah in the family. My appreciation also goes to my siblings and in-laws for their understanding, care and love (Ijah, Abe Le, Nora, Abe Din, Shariff, Kak Syikin and their respective families).



I certify that an Examination Committee met on **28th October 2009** to conduct the final examination of **Wan Siti Atikah Wan Omar** on her degree thesis entitled “Development of Fed-batch Cultivation Process for *Escherichia coli* Harboring Superoxide Dismutase” in accordance with Universiti Pertanian Malaysia (Higher Degree) Act 1980 and Universiti Pertanian Malaysia (Higher Degree) Regulations 1981. The Committee recommends that the candidate be awarded the relevant degree. Members of the Examination Committee are as follows:

Tey Beng Ti, PhD

Associate Professor
Faculty of Engineering
Universiti Putra Malaysia
(Chairman)

Nor’Aini Abdul Rahman, PhD

Faculty of Biotechnology and Biomolecular Sciences
Universiti Putra Malaysia
(Internal Examiner)

Suhaimi Mustafa, PhD

Associate Professor
Faculty of Biotechnology and Biomolecular Sciences
Universiti Putra Malaysia
(Internal Examiner)

Rosli Md Ilias, PhD

Associate Professor
Faculty of Chemical dan Natural Resources Engineering
Universiti Teknologi Malaysia
(External Examiner)

BUJANG BIN KIM HUAT, PhD

Professor and Deputy Dean
School of Graduate Studies
Universiti Putra Malaysia

Date: 12th February 2010



This thesis submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfillment of the requirement for the degree of Master Science. The members of the Supervisory Committee were as follows:

Rosfarizan Mohamad, PhD

Associate Professor
Faculty of Biotechnology and Biomolecular Science
Universiti Putra Malaysia
(Chairperson)

Raha Abdul Rahim, PhD

Professor
Faculty of Biotechnology and Biomolecular Science
Universiti Putra Malaysia
(Member)

Arbakariya Ariff, PhD

Professor
Faculty of Biotechnology and Biomolecular Science
Universiti Putra Malaysia
(Member)

HASANAH MOHD GHAZALI, PhD

Professor and Dean
School of Graduate Studies
Universiti Putra Malaysia

Date: 17th March 2010



DECLARATION

I hereby declare that the thesis is based on my original work except for quotations and citations which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at UPM or other institutions.

WAN SITI ATIKAH WAN OMAR

Date: 28 October 2009



TABLE OF CONTENTS

	Page
ABSTRACT	ii
ABSTRAK	v
ACKNOWLEDGEMENTS	viii
APPROVAL	ix
DECLARATION	xi
LIST OF FIGURES	xv
LIST OF TABLES	xvi
LIST OF ABBREVIATIONS	xvii
CHAPTER	
1 INTRODUCTION	1
2 LITERATURE REVIEW	6
2.1 Superoxide Dismutase	6
2.2 Reactive Oxygen Species	9
2.3 <i>Escherichia coli</i>	10
2.3.1 <i>Escherichia coli</i> BL21 Host Strain	10
2.3.2 Recombinant Protein	11
2.3.3 Plasmid Stability	14
2.4 Development of <i>Escherichia coli</i> Cultivation Process	16
2.4.1 Carbon Source	16
2.4.2 Nitrogen Source	20
2.4.3 Carbon-Nitrogen Ratio	21
2.4.4 pH	22
2.4.5 Agitation Speed	23
2.4.6 Dissolved Oxygen	24
2.5 High Cell Density Cultivation	26
2.5.1 Constant Fed-batch	28
2.5.2 pH-stat Fed-batch	30
2.5.3 Exponential Fed-batch	30
2.6 Kinetics of Cultivation Process	33
2.6.1 Batch	33
2.6.2 Fed-batch	39
2.7 Response Surface Methodology	42
2.8 Concluding Remarks	45



3	GENERAL MATERIALS AND METHODS	46
	3.1 Microorganism and Maintenance	46
	3.2 Inoculum Preparation	47
	3.3 Media Composition	48
	3.4 General Experimental Work	48
	3.5 2 L Stirred Tank Bioreactor	51
	3.6 Analytical Procedures	53
	3.6.1 Biomass Concentration	53
	3.6.2 Viable Cell Count	54
	3.6.3 Plasmid Stability Assay	55
	3.6.4 Plasmid Extraction	57
	3.6.5 SDS-PAGE Analysis of Total Protein	58
	3.6.6 Total Protein Quantification	59
	3.6.7 Determination of Organic Acids, Sugar and Alcohol	59
	3.6.8 Determination of Volumetric Oxygen Transfer Rate (K_{La})	60
4	OPTIMIZATION OF MEDIUM AND CULTURAL CONDITIONS FOR ESOD CULTIVATION USING RESPONSE SURFACE METHODOLOGY	63
	4.1 Introduction	63
	4.2 Materials and Methods	64
	4.2.1 Microorganism and Inoculum Preparation	64
	4.2.2 Batch Cultivation	64
	4.2.3 Preliminary Study on ESOD Cultivation	65
	4.2.4 Response Surface Methodology	66
	4.2.5 Analytical Procedures	71
	4.3 Results and Discussion	72
	4.3.1 Stability of ESOD and Determination of pRSOD	72
	4.3.2 Medium and Cultural Conditions Optimization by Using Conventional Method	75
	4.3.3 Response Surface Methodology	77
	4.4 Conclusion	86
5	BATCH CULTIVATION OF ESOD USING 2 L STIRRED TANK BIOREACTOR	87
	5.1 Introduction	87
	5.2 Materials and Methods	88
	5.2.1 2L Stirred Tank Bioreactor	88
	5.2.2 Effect of Glucose Concentration	89
	5.2.3 Effect of Agitation Speed	89
	5.2.4 Effect of Controlling Dissolved Oxygen Tension	90
	5.2.5 Analytical Procedures	90
	5.3 Results and Discussion	91
	5.3.1 Effect of Different Concentration of Glucose	91
	5.3.2 Effect of Different Controlled Agitation Speed	98



5.3.3 Effect of Different Controlled Dissolved Oxygen Tension	103
5.4 Conclusion	105
6 FED-BATCH CULTIVATION OF ESOD IN 2 L STIRRED TANK BIOREACTOR	106
6.1 Introduction	106
6.2 Materials and Methods	107
6.2.1 Microorganism and Inoculum Preparation	107
6.2.2 Medium	108
6.2.3 Batch Cultivation	108
6.2.4 Constant Fed-batch Cultivation	108
6.2.5 pH-Stat Fed-batch Cultivation	109
6.2.6 Analytical Procedures	110
6.3 Results and Discussion	110
6.3.1 Constant Fed-batch Cultivation	110
6.3.2 pH-stat Fed-batch Cultivation	115
6.4 Conclusion	119
7 GENERAL DISCUSSION	120
8 CONCLUSIONS AND SUGGESTIONS FOR FURTHER WORK	128
REFERENCES	131
APPENDICES	141
BIODATA OF STUDENT	149
LIST OF PUBLICATIONS	150



LIST OF FIGURES

Figure	Page
3.1 Map of the Constructed pRSOD	47
3.2 Flow Diagram of the Experimental Work	50
3.3 Schematic Diagram of a 2 L Stirred Tank Bioreactor	52
3.4 2 L Stirred Tank Bioreactor	53
3.5 Viable Cell of ESOD on the Selective Agar Plate for Determination of Plasmid Stability	56
3.6 Profile of DOT during Dynamic Gassing Out Technique	62
4.1 Photo of Electrophoresis Gel for Plasmid Determination	73
4.2 Photo of Protein Visualized by SDS-PAGE 12% for Determination of SOD	74
4.3 Growth Profile of ESOD in Batch Cultivation Using Different Media Composition	76
4.4 Response Surface Plots for the Effects of Initial pH (A), Yeast Extract and Tryptone, g/L (B) and Glucose, g/L (C)	85
5.1 Time Course of ESOD Batch Cultivation Using 15 g/L and 20 g/L of Glucose	92
5.2 ESOD Batch Cultivation Using Glucose as a Carbon Source	93
5.3 SDS-PAGE of Total Protein Production by ESOD Using 15 g/L Glucose as Carbon Source	95
5.4 SDS-PAGE of Total Protein Production by ESOD Using 20 g/L Glucose as Carbon Source	96
5.5 Time Course of Batch Cultivation of ESOD at Different Agitation Speeds Using 2 L STB	102
5.6 Time Course of Batch Cultivation of ESOD at Different Controlling DOT Using 2 L STB	104
6.1 Schematic Diagram of Fed-batch Set up	109



6.2	Time Course of Constant Fed-batch Cultivation of ESOD Using 2 L STB	112
6.3	SDS-PAGE of Total Protein Production of ESOD in Constant Fed-batch	114
6.4	Time Course of pH-stat Fed-batch Cultivation of ESOD Using 2 L STB	117
6.5	SDS-PAGE of Total Protein Production of ESOD in pH-stat Fed-batch	118
7.1	Maximum Cell Concentrations and Total Protein Achieved in the Present Research	127



LIST OF TABLES

Table		Page
2.1	Characteristic of SODs and Related Diseases	8
2.2	Empirical Reports of Recombinant Protein Produced by <i>E. coli</i> Strains	13
2.3	Empirical Reports of Fed-batch Cultivation of Recombinant <i>E. coli</i>	32
2.4	Empirical Reports on Optimization Studies on Microorganisms and Assay by using Response Surface Methodology	43
3.1	Dimension and Variables of 2 L Stirred Tank Bioreactor	52
4.1	Full Factorial Design Experimental Factors	67
4.2	Central Composite Design Experimental Factors and Levels	68
4.3	Central Composite Design Experiments	69
4.4	Plasmid Stability of ESOD in Shake Flask	72
4.5	Results of Full Factorial Design	78
4.6	Result of Central Composite Design	80
4.7	Analysis of Variables of ESOD Cultivation	81
5.1	Performance of ESOD Cultivations with Different Concentration of Glucose	97
5.2	Performance of ESOD Cultivations at Different Controlled Agitation Speed	99
5.3	Performance of ESOD Cultivation at Different Control Strategies of Dissolved Oxygen Tension	104
6.1	Performance of ESOD in Batch and Fed-batch Cultivations Using 2 L STB	113



LIST OF ABBREVIATIONS

C/N	Carbon to nitrogen ratio of medium in mm basis
D_i	Impeller diameter
DOT	Dissolved Oxygen Tension
μ	Specific growth rate (h ⁻¹)
μ_{max}	Maximum specific growth rate
m	Growth associated rate constant for production (g product/g cell)
S_i	Initial substrate concentration (g/L)
T	Fermentation time (h)
UiTM	Universiti Teknologi MARA
UPM	Universiti Putra Malaysia
X	cell concentration (g/L)
X_i	Initial cell concentration (g/L)
X_{max}	Maximum cell concentration (g/L)
Y_{x/s}	Yield of cell on basis of consumed substrate (g cell/ g substrate)

CHAPTER ONE

INTRODUCTION

Antioxidants are reducing agents that can slow down or prevent the oxidation of other molecules. Although oxidation reactions are crucial for life, they can also be damaging since the world wide pollutions level becoming a serious problem. Most people nowadays consume vitamin C as their supplementary diet for prevention and treatment deficiency such as scurvy. It also acts as an antioxidant that helps to prevent oxidative damage to cellular components such as DNA, proteins and lipids. Lately, the injection of vitamin C into the face skin is introduced by women to make their skin look youthful and firm.

The superoxide dismutase (SOD) is an enzyme that catalyzes the dismutation of superoxide into oxygen and hydrogen peroxide. As such, it is an important antioxidant defense in nearly all cells exposed to oxygen. Naturally, SOD would be the antioxidants in aqueous compartments for example in the cytosol and the extracellular fluids in human cell that defends against reactive oxygen species (Valentine *et al.*, 1998). This enzyme is used in pharmaceutical products and also in cosmetic products as antioxidant that can help to protect against cell destruction.



SOD was first discovered almost five decades ago by McCord and Fridovich, 1969 (Fridovich, 1974). SOD is divided by five metalloforms; two containing copper and zinc, one manganese, one iron and one nickel. Yi Sun (1990) stated that different SOD type would be found in different type of species. In prokaryotic cells, there are three forms of SOD, which are FeSOD, MnSOD and NiSOD (Yi Sun, 1990 and Youn *et al.*, 1996). The latter SOD is the latest found in several types of *Streptomyces sp.* .While in eukaryotic cells, three forms of SOD are known to exist; Cu ZnSOD, ECSOD, and FeSOD. On the other hand, Kinnula and Crapo (2003) stated three types of SOD found in mammalian cell, Cu ZnSOD, MnSOD and ECSOD. These SODs would act as anticarcinogens, the inhibitors at the initiation stage of mutation, protectors against oxidative damage and also indicator of abnormal level of SOD secreted by the cell. As the SOD would feasibly become one of the important proteins in human care products, it would be needed in large amount and carefully cultivated in control and optimize production cost.

The advent of molecular biology makes manipulation of microorganism and the production of recombinant proteins possible. Tan (2009) has successfully cloned and expressed a gene coding for SOD from *Lactococcus lactis* M4 in *Escherichia coli*. The purification and characterization of SOD are explained in detail by Tan (2009). The SOD was confirmed visualized by Western Blot analysis at 27 kDa. *E. coli* has been well characterized found to be a good host for expression of heterologous protein and numerous proteins have been studied using *E. coli* on the expression vehicle. This recombinant was the first that carrying SOD gene from *Lactococcus sp.*, compared

others that taken from human gene (recombinant human SOD, rhSOD) (Monica *et al.*, 2002; Steinhorn *et al.*, 2001). The expression of the protein in laboratory scale cultivation was therefore come into highlight as the potential of SOD in the therapeutic and pharmaceutical as well as cosmetic products.

High cell density cultivation may be achieved using fed-batch culture if the growth of the cultured microorganism is subjected to substrate inhibition. The main advantage of the high density cell cultivation technique is the possibility of reducing the size of the production bioreactor for production of proteins. By employing laboratory scale bioreactor, the cost of production can be reduced greatly to enable economic production of the recombinant SOD. In addition, the fed-batch techniques also enhanced downstream processing and reduced wastewater (Yee and Blanch, 1992). Most proteins are accumulated intracellularly in recombinant *E. coli*, hence the productivity is proportional to the final cell density and the specific productivity. Cell concentrations of greater than 50 grams dry cell weight per liter (g/L) can be routinely obtained by fed-batch culture of both non-recombinant and recombinant *E. coli* (Riesenberg, 1999, Kim *et al.*, 2004). However, this technique has several drawbacks, including: substrate inhibition, limited oxygen transfer capacity, the formation of growth-inhibitory by-products and limited heat dissipation (Kilikian *et al.*, 2000).

Regardless of the disadvantages, genetic alteration, medium optimization and cultivation techniques would be crucial in maximizing the yield of the proteins on interest. Thus, scope of this study focuses on the development process aimed at

establishing high cultivation of cell density of recombinant *E. coli* harboring SOD (ESOD) using fed-batch culture technique. Therefore, the objectives of this research are;

1. To optimize the medium and cultural conditions of ESOD cultivation using Response Surface Methodology.
2. To investigate the effect of glucose and cultural conditions (DOT and agitation speed) in batch cultivation of ESOD using 2 L Stirred Tank Bioreactor.
3. To develop fed-batch cultivation process of ESOD with an optimal controlled strategy to achieve high cell density cultivation.

In this thesis, literature review is covered in chapter two with detailed discussion on various aspects of research on the development of ESOD involving small to large scale production, including details of the current state of knowledge of superoxide dismutase application. In chapter three, general materials and methods used in this study have been briefly described where all analytical procedures were described. The results and discussion of the research have been prepared and divided into several chapters (chapter four to six). Chapter four covers the study of culture media and condition of ESOD in shake flasks by using conventional method and response surface methodology (RSM).



Cultural condition optimization of batch cultivation in 2 L stirred tank bioreactor is discussed in chapter five, which also includes the comparison performance of ESOD cultivation by different concentration of glucose, different agitation speed and control of dissolved oxygen tension. Meanwhile, chapter six focuses on the development of fed-batch cultivation that aims to achieve HCDC by different feeding mode (pH-stat and constant) approached to ESOD. In chapter seven, general discussion is explaining more detail of the results in each chapter. Finally, chapter eight concludes the whole study and included suggestions for further work.

