

UNIVERSITI PUTRA MALAYSIA

THERMAL TREATMENT AND UTILISATION OF SEWAGE SLUDGE

ZIAD MAHMOUD ABU-KADDOURAH

FK 2000 31



THERMAL TREATMENT AND UTILISATION OF SEWAGE SLUDGE

By

ZIAD MAHMOUD ABU-KADDOURAH

Thesis Submitted in Fulfilment of the Requirement for the Degree of Doctor of Philosophy in the Faculty of Engineering Universiti Putra Malaysia

June 2000



DEDICATION

This work is dedicated to my father and mother



iii

Abstract of thesis presented to the Senate of Universti Putra Malaysia in

fulfilment of the requirements for the degree of Doctor of Philosophy

THERMAL TREATMENT AND UTILISATION OF SEWAGE SLUDGE

By

ZIAD MAHMOUD ABU-KADDOURAH

June 2000

Chairman:

Associate Professor Azni Idris, Ph.D.

Faculty:

Engineering

Thermal process has become one of the major technologies for the treatment

of sewage sludge to secure final products. The incinerated ash and molten slag as

products of thermal treatment contain various types of heavy metals at high

concentrations. Incineration and melting processes can reduce the sludge volume

and stabilize the chemical compounds in the final product, which can be utilized

beneficially as construction materials.

In this study, dewatered sewage sludge was examined to investigate its

properties when subjected to different heat treatment processes, up to the temperature

of 1550 8C, in terms of chemical, physical, and micro-structure properties, degree of

stabilization and the possibility of utilizing the final products in different

applications.

The study shows that the volume of dewatered sewage sludge reduces up to five times by the drying process, twenty times by the incineration process and fifty five times by the melting process. It was shown that heavy metals can be stabilized during the incineration process by conditioning the dried sludge with CaCO₃.

Heating temperature, holding time and cooling rate are the controlling parameters for the melting process, to produce different needed materials, in terms of chemical, physical, micro-structure and stability of the final products. Incinerated ash and molten slag show stable end products in terms of the leaching properties, and it is within the limit of Japanese regulation for soil environmental limit.

Incinerated ash and molten slag are shown to be very good products that can be utilized as alternatives to cement and sand in concrete. By replacing 5 percent of cement with incinerated ash, the compressive strength can be improved by 50 percent compared to the standard product for the period of 3 days by getting a compressive strength of 30.80 N.mm⁻². Similarly, by replacing a 50 percent of sand with molten slag, the compressive strength can be higher than the standard product for the period of 7 days with a compressive strength of 26.36



v

Abstrak yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai

memenuhi keperluan untuk ijazah Doktor Falsafah

RAWATAN HABA DAN PENGGUNAAN ENAPAN BUANGAN

Oleh

ZIAD MAHMOUD ABU-KADDOURAH

June 2000

Pengerusi: Profesor Madya Azni Idris, Ph.D.

Fakulti:

Kejuruteraan

Proses haba telah menjadi salah satu teknologi utama untuk rawatan enapan

buangan untuk mendepatkan produk akhir. Abu yang telah dibakar dari slag cairan

sebagai hasil rawatan haba yang mengandungi pelbagai jenis logam berat pada

kepekata yang tinggi. Proses-proses pembakaran dan pelupusan boleh

mengurangkan isi pada enapan dan menstabilkan sebatian-sebatian kimia pada

produk terakair yang boleh digunakan faedahya sebagai bahan-bahan penbinaan.

Dalam kejian ini, enapan buagan yang dicairkan telah diperhatikan untuk

mengkaji sifat-sifatnya yang mana apabile dikenakan proses-proses rawatan haba

sehingga 15508C, sebagai sifat-sifat kimia, fizikal, dan struktur mikro, tatap

pensterilan dan kemungkinan menggunakan produk-produk akhir dalam pelbagai

penggunaan.

Kajian ini telah menunjukkan bahawa isi pada bahan buangan yang tercair

berkurangan sehingga lima kali ganda melalui proses pergeringan, dua puluh kali

ganda menerusi proyes pelupusan dan lima puluh lima kali ganda melalui proses

peleburan logam-logam berat menujukkan ianya boleh distabilkan semase proses pelupusan secara "conditioning" enapan yang sudah kering bersama CaCO₃.

Suha memanas, masa menahan dari kadar perdinginan boleh digunakan sebagai pergawal-pergawal semasa proses melabur, untuk menghasilkan bahan-bahan berbeze yang diperlukan dari segi sifat-sifat kamia, fizikal, struktur mikro dan kestabilan produk-produk akhir. Abu yang telah dibakar dari slag tercair menunjukkan produk-produk akhir yang stabil dari segi kepekatan logam berat dalam "leachate", dengan lebih stail untuk slag tercair.

Abu yang terbakar/terlupus dari "slag" tercair menunjukkan kemingkinan kuat digunakan sebagai gentian untuk simen dan pasir dlam konkrit. Dengan menggantikan 5 peratus simen dengan abu tersebut, kekuatan tekenan telah meningkat 50 peratus lebih daripada produk standard, dimana dengan menggantikan 50 peratus pasir dengan slag tercair, kekuatan tekenan adulah lebih tinggi daripada produk standard.



ACKNOWLEDGEMENTS

All Praise and Gratitude is due to Allah, the Lord and Sustainer of the Worlds, for without Him, everything will cease to be.

I would like to acknowledge with deep appreciation, all those who have helped me produce this thesis.

First of all, I would like to extend my deepest gratitude to my supervisors, Assoc. Prof. Dr. Azni Hj. Idris, Assoc. Prof. Ir. Megat Johari Mohd. Noor and Dr. Fakhru'l-Razi for their contributive suggestions and invaluable guidance, without whom this research would not have been completed.

The services and cooperation from the Institute of Post Graduate Studies and the Faculty of Engineering of The University of Putra Malaysia and Indah Water Operations Sdn. Bhd. throughout my research have been tremendous. Therefore, they receive special recognition for their immense efforts.

I wish to express my thanks to my fellow friends in Malaysia for their motivation and sincere support: Aiman Oklat, Nehad Qdaisat, Luai Al-Shalabi, and Amjad Al-Naser.

Last but not least, high accolades go to my beloved parents, sisters and brothers for their prayers, moral support, patience, and faith in me throughout my studies.



TABLE OF CONTENTS

ABST ABST ACKN APPR DECL LIST LIST	NOWL OVAL ARAT OF TA OF FIG		Page ii iii v vii viii x xiv xvii xxii
CHAI	PTER		
1	1 1	ODUCTION Background Objectives of the Study Scope of the Study	1 1 1 1 1 3 1 3
2	LITE: 2 1 2 2	RATURE REVIEW Introduction Non-Thermal Treatment, Utilisation and Disposal of	2 1 2 1
		Sewage Sludge 2 2 1 Treatment Process 2 2 2 Sludge Utilisation and Disposal	2 2 2 2 2 5
	2 3	The Treatment and Disposal of Sewage Sludge in Malaysia Current and Future Status	2 8
	24	Thermal Treatment of Sewage Sludge 2 4 1 Objectives of Thermal Processing 2 4 2 Drying 2 4 3 Incineration 2 4 4 Melting and Cooling Process	2 11 2 12 2 14 2 15 2 16
	2 5	Behaviour of Heavy Metals During Thermal Processes 2 5 1 Evaporation of Metals 2 5 2 Gas Cleaning Systems	2 27 2 28 2 33
	2 6 2 7	• .	2 35 2 36 2 37 2 38
	28	Energy Consumption and Cost Estimation of Thermal Processes	2 44
	2 9 2 10	Crystal Structure Summary	2 47 2 48
3		ERIMENTAL PROCEDURE	3 1
	3 1 3 2	Material Experimental Procedure 3.2.1 Sample Collection	3 1 3 2 3 6



	3.2.	2 Water Content and Drying	3.7
	3.2	.3 Incineration	3.8
	3.2.	4 Melting	3.9
	3.3 Exp	perimental Analyses and Equipment	3.14
	3.3.		3.14
	3.3.	.2 Thermal Properties	3.15
	3.3.	3 Micro-Structure	3.15
		4 Leaching Tests	3.16
		.5 Physical Properties	3.18
		lisation of Incineration Ash and Molten Slag in Mortar	
		nufacturing	3.19
	3.4.		3.20
	3.4.	1 &	3.21
	3.5 Cor	relation Coefficient Analysis	3.21
4	THE PRO	OPERTIES OF SEWAGE SLUDGE	4.1
		emical Composition	4.1
		eight and Volume Reductions	4.1
		ermal Properties of Sewage Sludge	4.4
		haviour of Elements during Incineration Process	4.6
	4.5 For	rmation of Crystals during Heating up to 1550 8C	4.8
5		FECTS OF CHEMICAL COMPOSITION ON HEAVY	
	METAL	BEHAVIOR DURING INCINERATION	5.1
6		EMPERATURE MELTING PROCESS FOR SEWAGE	
	SLUDGE		6.1
		troduction	6.1
		eparating Molten Slag from the Crucible	6.4
		kamination on the Different Types of Produced Slag	6.5
		3.1 Chemical Composition	6.6
		3.2 Microstructure Examination 3.3 Physical Properties of Molton Slee Products	6.8
		3.3 Physical Properties of Molten Slag Products3.4 Correlation Coefficient Analyses	6.18 6.20
	0	5.4 Correlation Coefficient Analyses	0.20
7	LEACH	ABILITY OF HEAVY METALS FROM DRIED	
		E, INCINERATED ASH AND DIFFERENT MOLTEN	
	SLAG PR	RODUCTS	7.1
8		TION OF INCINERATED ASH AND MOLTEN	
		MORTAR MANUFACUTRING	8.1
		llisation of Incinerated Ash in Mortar Manufacturing	8.1
		ilisation of Molten Slag in Mortar Manufacturing	8.14
	8.3 Im	pact of Sewage Sludge Management	8.19
9		SIONS AND FUTURE WORKS	9.1
		nclusions	9.1
	9.2 Futi	ire Works	0.4



REFERENCES	R. 1
APPENDICES	A.1
VITA	V. 1



LIST OF TABLES

Γable		Page
2.1 A	Sludge Disposal Routes in Europe	2.6
2.1B	Sludge Disposal in Japan	2.6
2.2	German and U.S. Standards for Heavy Metals in Sludges Used in Agriculture	2.7
2.3	Current and Future Total Sludge Production in Malaysia	2.9
2.4	Summary of Sludge Treatment and Disposal Methods Used in Malaysia	2.10
2.5	Sludge Incineration In Different Countries	2.16
2.6	Components of Molten Slag	2.20
2.7	Slag Properties	2.21
2.8	Physical Properties of Molten Slag	2.22
2.9	Melting Methods for Sewage Sludge	2.23
2.10	Emission levels (µm m ⁻³ norm dry gas) and Total Removal Efficiencies (%) for Different Gas Cleaning Systems	2.34
2.11	Leaching Test Methods	2.37
2.12	Comparison of Quality Measures between Sewage Bricks and those of Tokyo Metropolitan Standard	2.39
2.13	Quality of Sewage Bricks	2.40
2.14	Chemical Composition of Raw Materials for Portland Cement	2.40
2.15	Results of Road Material Tests on Air-cooled Slag	2.43
2.16	Results of Concrete Aggregate Material Tests on Air-cooled Slag	2.43
2.17	Physical and Chemical Characteristics of ECOROCK, Marble, and Granite	2.44
3.1	Composition of Dewatered Sewage Sludge	3.2
3.2	Relationship between Number of Samples and the Acceptance Range of "r"	3.23



4 1	Composition of Dried Sludge and Incinerated Ash	4 2
4 2	Water Content and Weight Reduction during Thermal Treatment	4 2
4 3	Volume Reduction during Thermal Treatment	4 3
4 4	The Mass Balance of the Incineration Process	4 6
5 1	Conditioning of Dried Sludge with Different Proportion of CaCO ₃	5 2
5 2	The Chemical Composition of Adjusted Dried Sludge Samples	5 2
5 3	The Concentration of Heavy Metals in Dried Sludge Samples at Different Basicities	5 3
5 4	The Concentration of the Residual Heavy Metals in the Incinerated Ash	5 3
5 5	The Percentage of Heavy Metals in Residual Ash after Incineration at 9008C	5 4
5 6	The Percentage of Heavy Metals in Different Off Gases after Incineration	5 4
6 1	Experimental Procedure for Producing a Single Molten Slag	6 5
6 2	Composition of the Molten Slag	6 6
6 3	The Mass Balance of the Melting Process	6 7
6 4	Properties of Molten Slag at Different Heating Temperatures	6 19
6 5	Properties of Molten Slag at Different Cooling Rates	6 19
6 6	Properties of Molten Slag at Different Holding Times	6 20
67	Numbers of Samples for Testing the Different Parameters	6 21
68	Correlation Coefficients for Controlling Parameters and Physical Properties of the Molten Slag	6 21
69	Acceptance Levels for Correlation Coefficient between two Variables Based on the Number of Samples	6 21
7 1	Leaching Test Specification Used in this Study	7 2
7 2	Leachability of Molten Slags at Different pH Values	7 4



7.3	Leachability of Dried Sludge, Incinerated Ash and Molten Slag at pH 3 and pH 5	7.5
7.4	Correlation Coefficients for Controlling Parameters and Leachate Concentration	7.7
7.5	Leachability of Molten Slags	7.9
8.1	Mixing Proportions of Different Types of Mortar	8.2
8.2	Density for Two Different Types of Mortar	8.7
8.3	Maximum Load Applied And Compressive Strength For Each Cubic Sample	8.8
8.4	Water-holding Capacity for Portland Cement and Incinerated Ash	8.11
8.5	Comparison between Portland Cement and Incinerated Ash	8.13
8.6	Mixing Proportions of Different Types of Mortar	8.14
8.7	The Density for Two Different Types of Mortar	8.15
8.8	Maximum Load Applied and the Compressive Strength for Each Cubic Sample	8.16
8.9	Estimated Operation Cost of Sludge Treatment to produce Incinerated Ash and Molten Slag	8.20
8.10	Production Cost per Tone of Cement	8.21
A.A	The Features of the Melting Furnace Model 808P	A .1
A.B	The main Features of the Thermal Analysis	A .2



LIST OF FIGURES

Figure		Page
2.1	Flow Chart for New Sludge Treatment And Disposal Strategy	2.13
2.2	Weight and Volume Reduction of Sludge by Thermal Treatment Processes	2.13
2.3	Relationship between Melting Properties and Basicity	2.18
2.4	The Pouring Point Temperature Distribution of Ash by Using a Three-Component Status Graph	2.19
2.5	System Alternatives for Sludge Treatment	2.24
2.6	The Partitioning of Iron, Copper, Zinc, Lead, Cadmium, and Mercury from Municipal Waste Incineration, in the Off Gas, Electrostatic Precipitator Ash, and in the Furnace Bottom Slag	2.30
2.7	The Proportion of Cd, Pb, Zn and Cu in the Residual in Air Atmosphere	2.32
2.8	Relationship between Compressive Strength and the Replacement Percentage of Ash	2.38
2.9	The Main Applications of the Air-cooled Slag and Water Cooled Slag	2.42
2.10	Comparison of Annual Treatment Costs	2.46
3.1	Dewatered Sewage Sludge	3.1
3.2A	Flow Chart Summarising Experimental Procedure of This Study	3.3
3.2B	Flow Chart Summarising Experimental Procedure of This Study	3.4
3.3	Diagram Showing The Selection at Random of One Substratum in Each Stratum of One Sector	3.8
3.4A	First Batch of Melting Procedures Based on Heating Temperature	3.10
3.4B	Second Batch Of Melting Procedures, Based On Cooling Rate	3.11



3.4C	Third Batch of Melting Procedures, Based on Holding Time	3.12
3.5	Melting Furnace	3.13
3.6	Concrete Flexural Strength Testing Equipment, ELE Model	3.22
4.1	Weight and Volume Reduction by Thermal Processing: Drying, Incineration and Melting	4.4
4.2	Thermal Analyses of Incinerated Ash	4.5
4.3A	The Partitioning of Metals By Sewage Sludge Incineration to the Off Gas and Residual Ash	4.10
4.3B	The Partitioning of Metals By Sewage sludge Incineration to the Off Gas and Residual Ash	4.11
4.4A	X-Ray Diffraction of Sewage Sludge under Different Treating Temperatures	4.12
4.4B	X-Ray Diffraction of Sewage Sludge under Different Treating Temperatures	4.13
4.4C	X-Ray Diffraction of Sewage Sludge under Different Treating Temperatures	4.14
4.4D	X-Ray Diffraction of Sewage Sludge under Different Treating Temperatures	4.15
4.5	X-Ray Diffraction of Sewage Sludge under Microwave Drying	4.16
4.6	Differently Treated Thermal Products	4.17
5.1	The Relationship between Cu and Basicity in the Residual Ash	5.5
5.2	The Relationship between Zn and Basicity in the Residual ash.	5.6
5.3	The Relationship between Pb and Basicity in the Residual Ash	5.7
5.4	The Relationship between Hg and Basicity in the Residual Ash	5.11
5.5	The Relationship between Cr and Basicity in the Residual Ash	5.12
6.1	Incinerated Sewage Sludge	6.2
6.2	Size Distribution Graph for Incineration Ash used in Melting	6.2
6.3A	Actual Cooling Curves for the Cooling Rate of 2.58C/min	6.3
6.3B	Actual Cooling Curves for the Cooling Rate of 5 8C/min	6.3



6.3C	Actual Cooling Curves for the Cooling Rate of 10 8C/min	6.4
6.4	Molten Slag Stocked in a Porcelain Crucible	6.5
6.5A	The Partitioning of Metals By Sewage Sludge Melting Process, to Off Gas and Residual Molten Slag	6.9
6.5B	The Partitioning of Metals by Sewage sludge Melting Process, to Off Gas and Residual Molten Slag	6.10
6.6	X-ray Diffraction Analysis of Molten Slags	6.13
6.7	A Partially Molten Slag Produced at a Heating Temperature of 1250 8C	6.14
6.8	A Brownish-Black Rock-Like Molten Slag Produced at a Heating Temperature of 1350 8C	6.14
6.9	A Polished Molten Slag Produced at a Heating Temperature of 1350°C	6.15
6.10	A Molten Slag Produced at a Heating Temperature of 1350°C	<i>C</i> 15
6.11	A Molten Slag Produced at a Cooling Rate of 2.5°C per Minute	6.15 6.16
6.12	A Molten Slag Produced by Fast Air-Cooling	6.16
6.13	A Bright Black Rock-Like Molten Slag Produced by Fast Cooling	6.17
6.14	A Polished Molten Slag Produced by Fast Cooling	6.17
6.15	A Molten Slag Produced without Holding Time	
7.1	Relationship between pH Values and Leachate Concentration	6.18 7.3
7.2	Effects of Cooling Rate on Leaching Properties	7.6
7.3	Effects of Holding Time on Leaching Properties	7.8
8.1A	Standard Mortar Tested in this Study before Crushing	0.2
8.1B	Mortar with a Replacement of 5% of Cement by Incinerated Ash before Crushing	8.3
8.1C	Mortar with a Replacement of 10% of Cement by Incinerated Ash before Crushing	8.4
8.1D	Mortar with a Replacement of 20% of Cement by Incinerated Ash before Crushing	8.4



8.2A	The Pyramid Shape that Formed by Crushing the Cubes Samples for the Standard Mortar Samples	8.5
8.2B	The Pyramid Shape that Formed by Crushing the Cubes Samples for Mortar with a Replacement of 5% of Cement by Incinerated Ash	8.5
8.2C	The Pyramid Shape that Formed by Crushing the Cubes Samples for Mortar with a Replacement of 10% of Cement by Incinerated Ash	8.6
8.2D	The Pyramid Shape that Formed by Crushing the Cubes Samples for Mortar with a Replacement of 20% of Cement by Incinerated Ash	8.6
8.3	Relationship between Compressive Strength and the Replacement Percentage of Cement by Incinerated Ash	8.9
8.4	Relationship between Mortar Density and Compressive Strength of the Mortar	8.10
8.5A	Standard Mortar Tested in this Study before Crushing	0.15
8.5B	Molten Slag Mortar Tested in this Study before Crushing.	8.17
8.6A	The Pyramid Shape that Formed by Crushing the Cube Samples for the Standard Mortar Samples	8.17 8.18
8.6B	The Pyramid Shape that Formed by Crushing the Cube Samples for the Molten Slag Mortar Samples	8.18



LIST OF ABBREVIATIONS

AAC Annual Average Treatment Cost

AD Anaerobic Digestion

ADIC Anaerobic Digestion Incineration System
ADMT Anaerobic Digestion Melting System

Alite Tricalcium silicate
Aluminate Tricalcium aluminate
AS Air-cooled Slag

ASTM American Standard for Testing Material

Aver. Average

Belite Dicalcium silicate
b.p. Boiling point
BS British Standard

BSI Backscattered Electron Imaging

CC Construction Cost

CS Scrubber With Condensation
DEMT Direct Dewatering Melting System

DS t/a Dried Sludge per annum

DTG Differential Thermogravimetry

DW Dewatering

DWIC Direct Dewatering Incineration System
DWICMT Direct Dewatering Ash Melting System

ESP Electrostatic Precipitator
ESS Electrostatic Scrubber
Ferrite Tetracalcium alumioferrite

FF Fabric Filter
Fin. Wt. Final Weight
GC Gas Treatment
GE Gas Engine

GT Gravity Thickening
HE Heat Exchanger
HT Heat Treatment

HTADMT Thermal Pretreatment Anaerobic Digestion Melting System

HTIC Heat Treatment Dewatering Incineration System
HTMT Heat Treatment Dewatering Melting System

ICP Inductively Coupled Plasma

ID Indirect Drying
INC Incineration
Ini. Wt Initial Weight

JPA Japanese Environmental Agency

KN Kilo Newton MT Melting

MARDI Malaysia Agricultural Research and Development Institute

m.p. Melting point
n Number of samples
n Number of durable years

NA Not Available ND Not Detected



N/mm² Newton per square millimetre

OC_K Annual Operating and Maintenance Cost

ppb part per billion
ppm part per million
PS Primary Raw Sludge
PWF Current Price Coefficient
r Correlation coefficient
rpm round per minute

SEM Scanning Electronic Microscope

TG Thermogravimetry
TH Mechanical Thickening

US.EPA United State Environmental Pollution Agency

WAS Waste Activated Sludge

WC Water Content
WHB Waste heat boiler
WS Water Cooled Slag
XRD X-ray Diffraction



CHAPTER 1

INTRODUCTION

1.1 Background

Sludge is the residual slurry of settleable solids from wastewater treatment plants. Its handling and disposal are of major environmental and economic concern. In recent decades, environmental issues have increasingly focused on sewage sludge treatment. As wastewater treatment standards have become more stringent, and with the widespread use of integrated sewage systems, the volume of sludge to be treated has increased and more stringent regulations have made its allowable disposal increasingly difficult.

Sewage sludges have been previously disposed by means of utilisation as fertilisers or "land filling" for conditioning of barren earth. However, more effective measures for the disposal of sewage sludge need to be implemented as the use of chemical fertilisers is more preferred in farming than organic fertilisers. This is further compounded by the difficulty in securing reclaimed land in large city areas and protecting it from the secondary environmental pollution, and leachability of wastes to groundwater table if it is disposed in sanitary landfills.

Instead of simply treating and disposing sewage sludge, other options should be considered to utilise sewage sludge as reusable materials. Burning and melting sewage sludge result in solidified and stabilised final products, which in turn help in utilising the final products in different applications such as



construction and building materials (Hiraoka, 1994; Nagaharu et al., 1997; TSK, 1995.A; and Tsunemi and Sasaki, 1984).

Previous studies have presented full scale plants with operation procedures including a general specification and advantages of the treatment processes they used, which mainly consist of treatment methods, treating temperature, degree of stabilisation, chemical and physical properties of the final products (Hisashi et al., 1997; Kazunori et al., 1997; and TSK, 1995.A). Some other works have compared different treatment processes and the properties of the final products (Oku et al., 1990 and Tsunemi and Sasaki, 1984).

Even though full scale plants are being built by some companies, there is still a lack of understanding related to the control parameters namely, heating temperature, cooling rate and holding time, which are the main parameters affecting the quality and the stability of the end products (Bolton, 1996). There are some published works on the thermal treatment of sewage sludge but details on temperature control and cooling are still not clear.

By understanding these controlling parameters and how they affect the properties of the final products, a better, higher quality and safe end products can be produced from sewage sludge.

Incinerated ash and molten slag contain various types of heavy metals in high concentrations. Some heavy metals do not evaporate on incineration and melting despite their high volatility (Masaki et al., 1997 and Vogg et al., 1986).

